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ERRATA - September 1962

The following addition is made to ASD Technical Report 61-260, Part I, Volumes 1 and 2 entitled "Thermodynamics of Certain Refractory Compounds":

# Cover Pages

The name of the principal author was not included on the covers:
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# THERMODYNAMICS OF CERTAIN REFRACTORY COMPOUNDS

VOL. 1. LITERATURE SEARCH, COMPUTATIONS, AND PRELIMINARY STUDIES

TECHNICAL DOCUMENTARY REPORT No. ASD-TR-61-260 PT. I, VOLUME 1

MAY 1962

DIRECTORATE OF MATERIALS AND PROCESSES
AERÔNAUTICAL SYSTEMS DIVISION
AIR FORCE SYSTEMS COMMAND
WRIGHT-PATTERSON AIR FORCE BASE, OHIO

Project Nos. 7350 & 7381, Task Nos. 73500 & 73812

(Prepared under Contract AF 33(616)-7327 by the Research and Advanced Development Division, Avco Corporation, Wilmington, Massachusetts; S. L. Bender, R. E. Dreikorn, T. H. Einwohner, R. C. Feber, R. E. Gannon, P. L. Hanst, M. E. Ihnat, J. P. Phaneuf, H. L. Schick, and C. H. Ward, authors.)

# FOREWORD

This report was prepared by the Avco Research and Advanced Development Division under USAF Contract No. AF33(616)-7327. This contract was initiated under Project No. 7350, "Ceramic and Cermet Materials", Task No. 73500, "Ceramic and Cermet Materials Development"; and Project No. 7381, "Materials Application", Task No. 73812, "Data Collection and Correlation". The work was administered under the direction of the Directorate of Materials and Processes Deputy for Technology, Aeronautical Systems Division, with Mr. P. W. Dimiduk acting as project engineer.

This report covers work conducted from 1 May 1960 to 30 April 1961.

Assistance from a number of sources has given vital support to the work on this project. The authors wish to acknowledge contributions from Prof. W. Klemperer in giving advice on spectroscopic experiments, Dr. D. R. Stull of the Dow Chemical Co. for many valuable discussions, the loan of microfilms, etc., Mr. T.R. Munson for providing the program for the machine computations on diatomic molecules, Dr. G. T. Furukawa for counsel on methods of smoothing C data, the staff of the Avco RAD Mathematics Section in programming and computing machine assistance, Dr. Joan B. Berkowitz-Mattuck and Mr. S. N. Goldstein at the A. D. Little Company in providing translations of Russian articles, Dr. S. Ruby for interest in the work and supervisory assistance, Mr. T. Licht in making chemical analyses, Mr. P. F. Jahn in sample preparation, and Mr.R. E. Walters and Mrs. Ann Wise in the literature search. Other contributors at Avco RAD have been Messrs. J. K. Hill and P. Demenkow (assistance in X-ray diffraction studies), J. Achramowicz (sample preparation), V.H. Early (spectroscopic studies), E. J. Kay and D. V. LaRosa (coding and other assistance in the work with IBM cards and computations), D. A. Dreselly (manuscript preparation), L. Fitzpatrick (chemical analyses), and W. S. Bennett (glassblowing). Reprints, reports, and other sources of data were contributed by Mr. P. W. Dimiduk (ASD), Dr. K. K. Kelley (U. S. Bureau of Mines), Dr. G. M. Rosenblatt (Univ. of California), Dr. G. R. Somayajulu (Univ. of California), Dr. D. L. Hildenbrand (Aeronutronics), Dr. R. H. Crist (Union Carbide Corp.), Dr. J. L. Margrave (Univ. of Wisconsin), and Dr. C. W. Beckett and others at the National Bureau of Standards (Heat Division).

# ABSTRACT

Theoretical and experimental studies were undertaken of the thermodynamics of certain refractory compounds from 298.15° to 6000°K. The list of compounds included the oxides, borides, carbides, and nitrides of the metals in groups IVB, VB, VIB, and VIIB of the periodic chart in addition to those of silicon, scandium, beryllium, magnesium, calcium, strontium, and osmium.

Tables of ideal gas thermodynamic functions of all the above elements were either prepared or brought up to date. Reviews and critical analyses of the available data were completed on the oxide systems of Be, Ca, Cr, Mg, Mo, Sr, Ti, and W, the borides of Ti, and the monocarbide of Ti. Sixty-one tables of thermodynamic functions, in various degrees of completion, were prepared on the important chemical species of the above systems.

A comprehensive review of the literature was made for the existing theoretical background needed in the interpretation of high-temperature  $C_p^o$  data and for the improvement of methods of estimating missing data.

In the experimental studies, careful checks were made of the purity of all samples. A Bunsen ice calorimeter apparatus was developed for specific heat measurements up to 1500°C. An apparatus employing the pulse method of specific heat measurements was used to make determinations in the temperature range from 1500° to 2500°C on borides of Mo, Ti, W, and Zr, on carbides of Nb, Ta, Ti, and Zr, and on a nitride of Ti. Spectroscopic studies were carried out on the Si-C, Mo-C, W-O, and the B-O system vapor species to determine their molecular structures and spectroscopic constants.

# PUBLICATION REVIEW

This report has been reviewed and is approved.

FOR THE COMMANDER:

J. I. Wittebort

Chief, Thermophysics Branch

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# I. INTRODUCTION

Contract AF33(616)-7327 has for its purpose the determination of the thermodynamic functions of a limited number of highly refractory compounds up to 6000°K. The scope of the contract encompasses the oxides, carbides, nitrides, and borides of elements in groups IIA, IVB, VB, VIB, VIIB, plus scandium, osmium, and silicon. This is summarized in figure 1 wherein the elements in the solid boxes are to be combined with those in the broken box to form the subject compounds. The metals Ir, Pt, and Rh were added to the list at the request of the project engineer.

The state of knowledge on these highly refractory compounds is such that much preliminary work was necessary to search for and to adapt required basic material property data before reliable computations could be made. Moreover, much of the existing data were inadequate, inaccurate, and in many cases even contradictory. Thus, only a limited number of the compounds could be completely characterized thermodynamically without a program of experimental measurements to provide additional basic data and to verify the existing data that are uncertain. Accordingly, the scientific effort on this project was distributed among three major phases as follows:

Phase I -- Review of the literature and compilation of all available data.

Phase II -- Calculation and tabulation of thermodynamic properties from available data.

Phase III -- Experimental studies to provide missing data, to prove the adequacy of computational techniques, and to verify any assumptions made throughout the program.

The list of basic data sought in Phase I includes not only those directly useful in the computations of Phase II, but also some that may find use in later applications of the thermodynamic functions. The list is as follows:

- 1. Phase diagrams
- 2. Heat capacity versus temperature
- 3. Enthalpy versus temperature
- 4. Entropy versus temperature
- 5. Heats of phase transformations
- 6. Heats of formation or reaction
- 7. Thermal expansion coefficients and compressibilities
- 8. Melting and triple points
- 9. Free energies of formation
- 10. Vapor pressures
- 11. Composition of gaseous species in vapor
- 12. Spectroscopic constants

Manuscript released by the authors (September 1961) for publication as an ASD Technical Report.

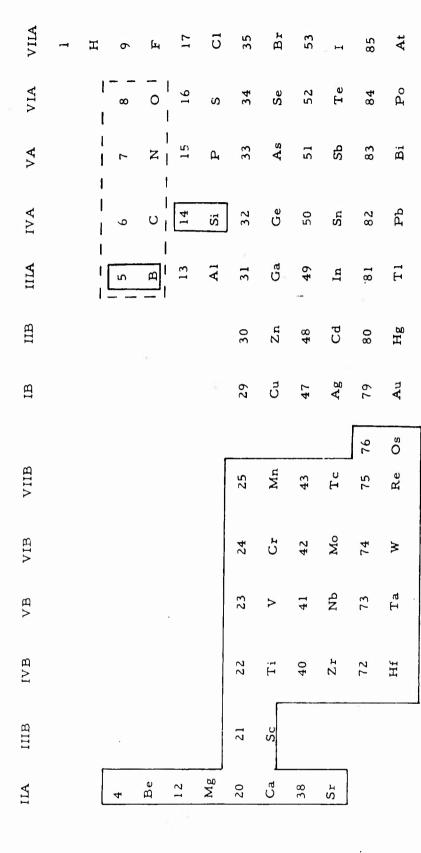


Figure 1 AREAS OF PERIODIC CHART INCLUDING ELEMENTS WHOSE COMPOUNDS ARE THE SUBJECT OF THE PROJECT

- 13. Ionization or appearance potentials
- 14. Emf's of electrolytic cells
- 15. Heats of solution or dilution
- 16. Other thermodynamic functions.

The experimental studies of Phase III can be grouped into the following three categories:

- a. Preparation of compounds and specimens. This includes analyses to verify purity and crystal structure, or the existence of special conditions such as extent of solid solution, etc.
- b. Heat capacity and total heat content determinations with a pulse-method apparatus and a Bunsen ice calorimeter.
- c. Spectroscopic studies of vapor species.

# II. REVIEW OF THE LITERATURE AND COMPILATION OF AVAILABLE DATA

# A. SCOPE OF THE LITERATURE SEARCH

The literature search has been very comprehensive, the intention being to cover all the literature of at least the last ten years. The following is a list of the literature sources searched:

- 1. Nat. Bur. Stds. Circular 500, Selected Values of Chemical Thermodynamic Properties (1952-1956).
- 2. Kubaschewski, O. and E. Evans, Metallurgical Thermochemistry, Pergamon Press, N. Y. (1958).
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- 6. Ehl, R. G., R. J. Sime, and J. L. Margrave, Binary Nitrogen Compounds of the Elements: A Literature Survey, WADC Tech. Note 59-115 (1959).
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- 20. Kelley, K. K., Bur. Mines Bull. 477, Entropies of Inorganic Substances (1950).
- 21. Goldsmith, A., T. Waterman, and H.J. Hirschhorn, Thermophysical Properties of Solid Materials, WADC TR-58-476;

AD-207905 (January 1959),

Vol. 1. Elements, AD-247193 (August 1960),

Vol. 2. Alloys, WADC-58-476 (November 1960).

- 22. Goldsmith, A. et al, Additional volumes to supplement 21 above obtained from ASD and Armour Research Foundation.
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- 24. Ann. Revs. Phys. Chem. (1950 1959).
- 25. Smith, J.M. et al, Ann. Revs. Thermodynamics

Ind. Eng. Chem. 50, 561 (1958)

Ind. Eng. Chem. 51, 472 (1959)

Ind. Eng. Chem. 52, 451 (1960)

Ind. Eng. Chem. 49, 583 (1957)

Ind. Eng. Chem. 48, 676 (1956)

Ind. Eng. Chem. 47, 664 (1955)

Ind. Eng. Chem.  $\frac{46}{45}$ , 947 (1954) Ind. Eng. Chem.  $\frac{45}{45}$ , 963 (1953).

- 26. Sinke, G. C. et al, Thermodynamic Properties of Combustion Products, WADC and ARPA, Rept. AR-214-587, Dow Chem. (1 April 1959).
- 27. Beckett, C. W. et al, Preliminary Report on the Thermodynamic Properties of Lithium, Beryllium, Magnesium, Aluminum, and Their Compounds with Oxygen, Hydrogen, Fluorine, and Chlorine, Nat. Bur. Stds. (U.S.) Rept. 6297 (1 June 1959); Rept. 6484 (1 July 1959).
- 28. Beckett, C.W., et al, Preliminary Report on the Thermodynamic Properties of Selected Light-Element Compounds, Nat.Bur.Stds.(U.S.) Rept. 6645 (Supplement to Repts. 6297 and 6484), (1 January 1960, amended 1 April 1960). Also Rept. 6928 (Supplement to NBS Repts. 6297, 6484, and 6645), (1 July 1960).
- 29. Chem. Abstracts (1950-1961).
- 30. Nuclear Sci. Abstracts (1950-1961).
- 31. Eng. Index (1953-1958).
- 32. Phys. Abstracts (1950-1961).
- 33. Ceram. Abstracts (Recent Years).
- 34. Dissertation Abstracts (Recent Years).
- 35. IUPAC Bibliography (April 1960-1961).
- 36. Battelle Tech. Rev.
- 37. Monthly Index of Russian Accessions (Library of Congress), (1960).

The scope of the entire primary literature uncovered is best indicated by the list of references in the reference code file in section VII-B.

# B. ACCUMULATED FILES

Four files have been accumulated as products of the literature search. The primary ASM card file contains all the information obtained and handwritten by the searchers and abstractors. All references were coded and punched into IBM cards for the second file. An author index file could have been made from duplicate IBM cards of the "L" type (described in section C). However, it was found more convenient to use printouts from the IBM cards (one for each

abstractor) in place of the author index, whose purpose has been to expedite the elimination of duplicate references at the source and avoid needless repetition of effort. The IBM card file was intended to store all the information in a form that could be handled by sorting, collating, and computing machines. The fourth file is a subject index made up from the IBM card file.

# C. DATA CODING AND IBM CARD FILE SYSTEM

# 1. Introduction

# a. General Remarks

In the work on Phase I of this project, it has been necessary to store in readily accessible form large amounts of bibliographic information and numerical data on thermodynamic properties of certain chemical elements and compounds. In Phase II, it has been necessary to calculate thermodynamic properties by routine and often repeated procedures. The problems of information storage, retrieval, and modification, and calculation of related thermodynamic properties were expedited and simplified by the use of electronic calculators and sorting equipment available at Avco RAD. For this, a system for handling both bibliographic information and numerical data had to be developed.

The system was designed to treat one phase of the problem, that of storing the data in relatively accessible form when coded on standard IBM cards in a fixed format. By means of the IBM Sorter, information of any category could be easily culled out of the master file.

The following paragraphs describe the part of this system which was used extensively in the literature search and bibliographic work.

# b. Mnemonic Symbols

Limited storage space, the unwieldliness of large files, and minimization of machine running time require symbols of minimum number of characters to describe categories of information, units, values, etc. On the other hand, this minimum length symbol might not easily be remembered and coding time would be lost in continual reference to a glossary and codes. A compromise has been reached in allowing the symbol to correspond as much as possible to the commonly accepted abbreviation. When shorter codes were required, the attempt was to make them correspond to the sound of the quantity being coded.

### c. Structure of IBM Cards

For purposes of reference, the IBM card is divided into rows and columns. Columns are numbered consecutively 1 to 80 from left to right. Rows are numbered from top to bottom 12, 11, zero and 1 to 9. To record information in the card, a given character (i.e., number, letter, or special symbol such as \*) is punched as a characteristic hole or series of holes, all in the same column. Any character can be punched into any column, but two or more characters cannot occupy the same column. The character can be simultaneously printed at the head of the column it occupies, allowing ready reading of information on the card. A number is represented by a single hole (or punch) in the given column. Thus, for example, the number 9 in column 73 would be represented by a punch in column 73 row 9. A letter is represented by two characteristic holes in the same column and a special character by three.

For more compact storage of information, one allows a punch in the 12, 11, or zero row of a column where numeric information is stored. Sometimes row 12 is called + and row + 11 -. This is called an overpunch + 10/p).

# d. Fixed Field Format

Since a character occupies a column, a multicharacter symbol occupies a series of contiguous columns called a field. For ease in sorting, it is convenient to have all symbols of the same general type occupy the same columns on different cards. Thus, for example, suppose one denotes molar heat capacity at constant pressure by the symbol CP (all letters must be capitals and no subscripts or superscripts are allowed). The convention is made that, for a given series of cards, each card with a symbol for a thermodynamic property will have the property in columns 2-5. Then to distinguish cards with Cp data from those of other thermodynamic properties, sorts for C in column 2, P in column 3, and blanks in 4 and 5 are made. The cards selected in this way will have the desired information.

# 2. Types of Cards

In general, widely different types of information to be handled and sorted will result in different types of formats. For compatibility with other machines, which will eventually handle and use the data, the format of the rest of the card is denoted in column 1. The various types of cards are as follows:

Column 1	Meaning
D	Definition Card
L	Library Card
С	Comment Card
Other	Type A Card.

In all these cards, column 1 describes the type of card, 2 to 72 describe the information, and 73 to 80 are reserved for card identification.

# 3. Card Identification Format

To have absolute, sequential numbering of cards and reference to the person who took the abstract and the approximate date, the following format was used in columns 73 to 80 of cards of all types.

	Column	Character	Meaning
***	73	α	One character symbol for month A = May 1960, B = June 1960, etc.
	74	o V	Abstractor. O/p indicates finder card
	75 to 79	ν	Serial number
	80	a'	Not used.

The explanation of character symbols is as follows:

- μ Numeric character
- ν Overpunched (O/p) numeric character
- a Alphabetic character
- a' Alphabetic or numeric character
- σ Special character
- b Blank.

# 4. Library Cards

It was supposed that several pieces of data would often be taken from the same reference. Each piece of data needs to be punched on a card which will also have coded the reference by journal, volume, page, and year. It would also be convenient to give further information about a given reference. For example, one might want to know the names of the authors or a reference to an abstract, if any. This information was recorded on the library cards, whose format is summarized below.

# a. The symbols used in library card coding were as follows:

Column	Character	Meaning
1	L	Identifies library card.
2-11	10 a	Last name of first author. (The "10" means that the 10 columns (2-11) contain letters (alphabetic symbols).
12	, or a	A comma is the usual character, it is used to separate last name from the first initial. For last names of eleven or more letters however, the comma is replaced by the eleventh letter.
13	a ,	First initial of author's name. If the last name is eleven letters long however, this column is blank. If last name is twelve or more letters long, the twelfth letter of the author's name occupies this column.
14-22	9 α	Second author's name.
23	, or a	Follow the procedure indicated for column 12, unless last name contains ten or more letters, in which case comma is replaced by the tenth letter.

Column	Character	Meaning
24	a	First initial of second author's name. However if the last name is ten letters long, this column is blank. If last name is eleven or more letters long, the elev- enth letter occupies this column.
25-29	5α	Five-letter symbol for the original reference. Column 25 must be a. Occasionally, numerical information is put in columns 27, 28, and 29. For example, a report with a designation AD-101-773 would have the AD-101 located in columns 25-29, while the 773 would be in columns 30-32.
30-32 (usual case)	3ν (see excep-	Volume number of original reference. Several variations are possible for 30-32,
	tions below)	33, and 34-39.
30 (alternative 30-1)	R	Report number will be given in the following columns (31-39), using a fixed-field format (31, 32), (33, 34), (35, 36), (37, 38, 39). Dashes will be assumed but not written between columns 32 and 33, etc.
30 (alternative 30-2)	F	Report number will follow in (31-39), using a free field. Report numbers are given with no regard for field. Any combination of numbers and dashes can be used, but the dashes must be written explicity.
30 (alternative 30-3)	Р	Paper number will follow, using same type of fixed field as for alternative 30-1 above.
32 (alternative 32-1)	*	Asterisk means no volume number is given.
32 (alternative 32-2)	+	Plus means volume number is the same as the year.

Column	Character	Meaning
33 (usual)		Comma is the usual symbol used to indicate that the page number of the original reference follows in columns 34-38.
33 (alternative 33-1)	or *	Means an abstract number follows in columns 34-38, rather than a page number.
33 (alternative 33-2)	or/	Means next two columns (34 and 35) contain issue number, while column 36 must contain another virgule, and page numbers are in columns 37-39.
33 (alternative 33-3)	or S	Means a supplement number will follow in column 34. Page numbers will be placed in columns (35-38).
33 (alternative 33-4)	or P	Means a part number of a report follows in column 34.
34-38 (usual case)	5 v	Page number or abstract number of original reference. The smallest number is placed in column 38. This system is used if comma, or asterisk, is located in column 33.
39 (usual case)	a '	A letter or a number is used with the preceding page number to locate the column or row on the page where the reference is found. If this information is not available, this column is blank.
34-39 (alternative)		
Alternatives are available as 32-2, 33-1, 33-2, and 33-3.		described by 30-1, 30-2, 30-3, 32-1,
40	( or *	Beginning parenthesis means that original reference was consulted; asterisk means that data were taken from a source other than the original reference.

Column	Character	Meaning
41-42	0 0 V	Last two figures of the year. A minus  (-) overpunch in column 41 means nine- teenth century. In column 42 a plus (+) overpunch means in Russian; a minus  (-) overpunch means in German.
43-44	2 a	Symbol for abstracting journal. If the symbol has four characters, the last two characters are coded in columns 57-58.
45-46	2 v	Volume number of abstract,
47	, or *	Comma denotes page number to follow; asterisk denotes abstract number to follow.
48-53	5 να΄	Page, column, or abstract number.
54	( or *	Same as column 40. Usually, the beginning parenthesis will be used here.
55-56	2 v	Last two figures of the year of abstract publication.
57-58	2 a	Last two symbols for the abstracting journal.
59	a'	Character to denote availability of original reference (see paragraph b of this section).
60-69	10 a	Third author's last name.
70	,	Follow procedure for column 12.
71	а	First initial of third author's name (see procedure for column 13).
72	E or M	If more than 3 authors, use "E" (et al). If any of the author's names could not be completely coded; i. e., if any first initials are missing, use "M".

Column	Character	Meaning
73	a	A letter to designate month in which original ASM card was taken. Thus, May (1960) = "B"
74-79	6v	Serial number for original ASM card.
80	ν	This column is not used with "L" cards. However, "T" cards may have numbers starting with 1 in column 80. These in- dicate the order in which "T" cards should follow "L" cards in a bibliography.

b. A glossary of availability characters for column 59 of library cards follows:

Character	Meaning
L	Avco RAD Research Library.
E	Avco-Everett Technical Library.
M	MIT Library.
Н	Harvard Libraries.
G	AFCRL* Library.
·c	Avco Crosley.
N	Other nearby libraries (Boston area).
φ	Original on order.
ν	Abstractor with number.
P	Personnel at Avco RAD.
Z	Abstract not available at Avco RAD.
x	Original practically unavailable.

<sup>\*</sup>Now, the Air Force Cambridge Research Laboratories, Bedford, Massachusetts; formerly AFCRC (the Air Force Cambridge Research Center).

# 5. Title Cards

Since title cards have a relatively free field, they were quite simple to prepare. The coding scheme has been as follows:

Column	Character	Meaning
1	Т	Title card.
2	ь	Must be blank.
3-72	70 a′	Case(1) (Author elaboration card). If an "E" or "M" were located in column 72 of "L" card, then a title card is prepared wherein all authors' names are given in order.
4-72	69a′	Case (2). Both columns 2 and 3 must be blank. The exact title is placed in columns 4-72 in first and any succeeding title cards if necessary.
73-79	a, 6 v	Same code is used as for "L" cards.
80	ν	Denotes sequence of title cards. If an author elaboration card (Casel) is used, a figure 1 is placed in column 80, and all succeeding title cards are numbered in sequence. If no author elaboration card is used (Case 2), the first title card is numbered 1, and the rest numbered in sequence.

# 6. Comment Cards

For verbal comment storage, column 1 of the card is a C, columns 2 to 8 are a symbol for the comment, column 9 is blank, and columns 10 to 72 are reserved for the comment. This type of card has been used sparingly.

# 7. Subject File

To avoid disruption of the file of ASM cards, a file arranged according to subjects was developed through the use of a special set of IBM cards. Only selected fields of these cards were coded as follows:

Column	Symbol	Meaning
1	P or M	"P" = pure compound, "M" = mixture.
2-5	4 a	Property which was investigated. (A list is shown in property codes below.)
22-34	13 a'	Name of compound or material studied.
73-80	8 a'	Usual serial number.

Property codes for the subject file are as follows:

DEBTA	PRO	COMPRESSIBILITY COEFF BETA 1/V DV/DPT	
DBIB	PRO	BIBLIOGRAPHY	
DCEMP	PRO	CONDENSED PHASE, ELEC OR MAGNETIC PROP, EG WORK FUNC	
DCOPT	PRO	CONDENSED PHASE, OPTICAL PROP	
DCP -	PRO	HEAT CAPACITY	
DCRYS	PRO	CRYSTAL STRUCTURE	
DCTEX	PRO	COEFF OF THERMAL EXPANSION	
DDF	PRO	FREE ENERGY OF FORMATION, REACTION, ETC.	
DDH	PRO	HEAT OF FORMATION, REACTION, ETC.	
DE	PRO	INTERNAL ENERGY	
DELCH	PRO	ELECTROCHEMICAL	
DEMF	PRO	ELECTROMOTIVE FORCE	

PRO	ELECTRICAL RESISTIVITY	
PRO	FREE ENERGY FUNCTION	
PRO	HEAT CONTENT	
PRO	KINETICS	
PRO	MISCELLANEOUS	
PRO	MASS SPECTROMETRIC DATA	
PRO	PHASE DATA, MELTING, TRANSITION, BOILING TEMPS	
PRO	MECHANICAL PROPERTIES	
PRO	CHEMICAL REACTIONS	
PRO	REVIEW	
PRO	DENSITY	
PRO	ENTROPY	
PRO	SPECTROSCOPIC DATA	
PRO	THERMAL CONDUCTIVITY	
PRO	THEORY	
PRO	THERMODYNAMIC DATA	
PRO	VAPORIZATION DATA	
PRO	EQ CONST	
	PRO	

# 8. Definition Cards

a. The usual format for definition cards has been as follows:

Column	Symbol	Meaning
1	D	Definition.
2-6	2 a, 3 a '	Symbol for the reference.
2-11	REF	Stands for reference.
12	Α	An abstracting journal is being coded.
	В	A book is being coded.
	S	A symposium is being coded.
	х	A journal or report number is being coded, and a portion of this number is to be included in the five-character symbol for the reference.
20-72	53 α'	Definition of journal using abbrevations of Chemical Abstracts and a free field except for books or symposia (see below).

b. For books (designated "B" in column 12), the following pertains:

Column	Symbol	Meaning
21-31	9 a , a	First author, first initial.
32-41	8α, α	Second author, first initial
42-63	22 α	Title of book.
64-70	(5a)	Publisher (abbreviated).
71-72	2 ν	Year of publication.

c. For symposia (designated "S" in column 12), the following were used:

Column	Symbol	Meaning
21-31	11 α	Name of town.
32-41	10 a	Name of country.
42-70	29 a	Name of symposium.
71-72	2 v	Year of meeting.

## d. Code-Field Entries

Columns 72-80 of the L-type and certain other cards are called the "code" field. For other fields, symbolic entries have to be defined by definition cards. The interpretation of the code field is too simple to require this, and thus, no "D" cards have been made for code-field entries.

## e. Additional Functions of "D" Cards

It is useful to have the "D" cards not only to give the verbal definition of a symbol, but to show relationships between symbols. Thus, the "D" cards become a "thesaurus" as well as a "dictionary." Provision has been made for this in the "D" cards by including an associated symbol field and a control character.

One of the main purposes of the definition cards will be to find duplicate references. Thus, if two ASM cards have been prepared inadvertently from the same original reference, the "code" card will show that this similarity exists. Codes for other methods of using these cards are shown immediately below.

Column	Symbol	Meaning
1	D	Definition.
2-8	α, 6ν	Symbol for the ASM card to be defined.
9-11	CØD	Code.
12 (usual)	S	Identical (synonymous).
12 (Alternative	L	Similar. If a publication had appeared as a journal publication, the contents might be quite similar but not identical.
12 (Alternative 12-2)	T	A translation of basic reference is available.
13-19	a, 6 v	Symbol for the ASM card in terms of which the entry in columns 2-8 is defined.

## f. The following symbol types have become established:

Symbol Type	Meaning	
PRØ	Property	
TNU	Units	
SAG	State of aggregation	
WAY	Method of determination	
REF	Reference	
TBL	Table	
MIX	Mixture	
сøм	Comment	
CND	Condition.	

Certain of these symbol types require specification of the A field.

Symbol Type	A Field
UNT	Property measured in these units
WAY	Quantity calculated by this method
CND	Property given by standard state value.

At present, there is only one use for the control character in column 12. S in column 12 means that the symbols in the D and A fields are synonymous. Other control characters can denote other relationships between the D and A fields.

# III. CALCULATION AND TABULATION OF THERMODYNAMIC FUNCTIONS FROM AVAILABLE DATA

#### A. FORMAT AND SCOPE OF TABULATIONS

An important aspect of any project of this type, where thermodynamic functions are to be tabulated, is the format of the tables and the summaries of basic data used in their computation. The standard state reference temperature and the units of numerical data also require careful choice. Standardization in these matters has evolved from a number of such compilations of recent years from the National Bureau of Standards, the Bureau of Mines, etc. A particularly good model for the type of compilation undertaken in this project is that of the JANAF-Thermochemical Panel which is issued under the direction of Dr. D. R. Stull. Except for the introduction of a few innovations, the example of the Thermochemical Panel has been followed in the work on this project so that the results of the two compilations will be compatible. The innovations referred to are the addition of uncertainty estimates and extra entries to define property discontinuities at transition points.

#### B. STANDARDIZATION OF PHYSICAL AND CHEMICAL CONSTANTS

Another important aspect of data computation and tabulation work is the choice of a consistent set of physical constants such as the atomic weights, gas constants, temperature scales, etc., because more than one atomic weight scale is in general use, and the accepted best value of most constants changes from time to time.

The source of constants (other than atomic weights) selected for this study is the data tabulation by Cohen, Crowe, and Dumond. However, their data have been obtained by reference to the physical atomic scale; whereas for the present work, the chemical atomic scale has been used. The factor for conversion of atomic weights from the physical to the chemical scales was taken as 1.000275 from Birge. Constants converted in this way are given in Table I.

<sup>&</sup>lt;sup>1</sup>Cohen, E.R., K.M. Crowe, and J.W.M. Dumond, Fundamental Constants of Physics, Interscience, N.Y. (1957), 287 p.

<sup>&</sup>lt;sup>2</sup>Birge, R.T., Repts. Progr. Phys. 8, 90 (1942).

TABLE I

# VALUES OF USEFUL CONSTANTS ON THE PHYSICAL AND CHEMICAL SCALES

Quantity	Physical Scale Value	Chemical Scale Value
Avogadro's number, N	$(6.02486 \pm 0.00016) \times 10^{23}$	(6.02320 ± 0.00016) x 10 <sup>23</sup>
Gas constant,	1.98780 cal/°K mole	1.98726 cal/ °K mole

Wichers 3 has reported the latest status of the atomic weights on the chemical scale, and the table from his paper was used in this work. The authors are unaware of any further changes resulting from the proposed unification of physical and chemical scales by the International Commission on Atomic Weights discussed in Wichers paper. 3

Some additional constants used in the computations of the project are as follows:

1	Thermochemical calorie (designated	= 4.1840 absolute joules
	''cal'' in the tables)	***************************************

''cal'' in the tables)		
e		= 2.7182818284
log <sub>e</sub> 10		= 2.3025850929
log <sub>10</sub> e		= 0.4342944819
e x R <sub>o</sub>		= 4.575835 cal/°K mole (chem)
$1 \text{ cm}^{-1}$		= 2.8592696 cal/mole (chem)
l erg/molecule	,	= $1.439584 \times 10^{16} \text{ cal/mole (chem)}$
l ev		= 23,062.999 cal/mole (chem)
Ice Point		= 273. 150° K
hc/k		= 1.43880 ± 0.00007 cm° K.

<sup>3</sup>Wichers, E., J. Am. Chem. Soc. 80, 4121 (1958).

# C. THEORETICAL RELATIONS FOR HEAT CAPACITY VERSUS TEMPERATURE

One of the most important steps in the computation of thermodynamic functions of solids is smoothing and curvefitting of  $C_p^\circ$ -versus-temperature data. One looks to the existing theories for mathematical functions to use in this kind of analysis. The theory provides mathematical functions for  $C_v$ .  $C_v$  and  $C^\circ$  are almost equal at low temperatures, and these theories are applicable to the data under these conditions. In fact, it may be only at low or moderate temperatures that there is any hope at present for finding suitable mathematical functions for these purposes. This is in no way an attempt at a comprehensive review of the theory but merely at a summary of the best available theories that have direct bearing on the problems of this project. Some comprehensive reviews are available on this subject. 4-8

### 1. The Law of Dulong and Petit

An empirical rule that has been often used and quoted is the law of Dulong and Petit,  $^9$  which states that "All solid elements have the same heat capacity per gram atom." At moderate temperatures, the atomic heat capacities are almost constant at  $6.2 \pm 0.4$  cal deg<sup>-1</sup> in spite of the increase in atomic weight from 7 to 238.  $^9$  In time, it became evident that there were many notable exceptions to this rule, and recent theories have provided a basis for the rule and explanations for the exceptions.

## 2. Kopp's Law

Kopp's law<sup>9</sup> states that "The molar heat capacity of a solid compound is approximately equal to the sum of the atomic heat capacities of its constituents." This rule has been very useful; for example, it has been used to estimate molecular weights in doubtful cases. Winkelmann's<sup>4</sup>, 10 expression for the specific heats of glasses is of the same form.

<sup>&</sup>lt;sup>4</sup>Montroll, E.W., Vibrations of Crystal Lattices and Thermodynamic Properties of Solids, In: Handbook of Physics, McGraw-Hill, N.Y. (1958), part 5, chap. 10, p. 159.

<sup>&</sup>lt;sup>5</sup>Blackman, M., The Specific Heat of Solids. Handbuch der Physik, Springer Verlag, Berlin (1955), p. 325-382.

<sup>&</sup>lt;sup>6</sup>deLaunay, J., The Theory of Specific Heats of Lattice Vibrations, vol. 2, Solid State Physics, In: Advances in Research and Applications, Academic Press, N.Y. (1956), p. 219-303.

<sup>&</sup>lt;sup>7</sup>Partington, J.R., An Advanced Treatise on Physical Chemistry, Vol III, Longmans Green, London (1952), p. 264-320.

<sup>&</sup>lt;sup>8</sup>Born, M. and K. Huang, Dynamical Theory of Crystal Lattices, Oxford Univ. Press, Oxford (1954).

Glasstone, S., Textbook of Physical Chemistry, Van Nostrand, N.Y. (1946), p. 413.

<sup>10</sup> Winkelmann, A., Ann. Physik, 49, 401 (1893).

#### 3. Vibrational Contributions at Low Temperatures

#### a. Einstein's Theory

The Einstein<sup>5</sup>, 11 theory was not completely successful in fitting experimental heat capacities, but the function derived from it is often used in other ways as shall be seen later.

The Einstein model for a crystal system of N identical particles is that each atom vibrates harmonically in the isotropic potential field of all the other atoms. The energy of the particles can be written in terms of three linear harmonic oscillators, one for each dimension in space. The mean energy of a quantum mechanical linear harmonic oscillator with a frequency  $\nu$  is

$$\overline{\epsilon} = \frac{h\nu}{\exp(h\nu/kT) - 1} \qquad (1)$$

The total energy of the system at equilibrium is therefore 3N7; and its constant volume heat capacity, obtained by differentiation with respect to temperature, is

$$C_{\mathbf{v}} = 3 \,\mathrm{N} \,\mathrm{k} \,\mathrm{E}(\mathbf{x}) \,, \tag{2}$$

where

$$x = h\nu/kT , \qquad (3)$$

and E(x)is the Einstein function, 12

$$E(x) = \frac{(x/2)^2}{\sinh^2(x/2)} . (4)$$

The limit approached by equation (2) as the temperature increases is 3R per gram atom as it should be, but the limiting form at low temperatures is

$$C_{\mathbf{v}} \cong 3R\mathbf{x}^2 e^{-\mathbf{x}} \quad , \tag{5}$$

and this does not fit the low-temperature data of solids very well.

<sup>11</sup> Einstein, A., Ann. Physik, 22, 180 (1907).

<sup>12</sup> Sherman, J. and R.B. Ewell, A six-place table of the Einstein functions, J. Phys. Chem. 46, 641 (1942).

## b. Debye's Elastic-Continuum Theory

Debye<sup>4</sup>, 13 was the first to derive a theoretical expression that fitted experimental heat capacities well over the entire range of temperatures for which data existed at that time. It is widely used by itself and in combination with Einstein functions.

Any system of N harmonically coupled point masses has 3N independent, normal modes of vibration with frequencies  $\nu_1$ ,  $\nu_2$ , ---,  $\nu_{3N}$ . The total energy of such a system is

$$E = kT \sum_{j=1}^{3N} x_j \left( \frac{1}{2} - \frac{1}{1 - \exp x_j} \right) , \qquad (6)$$

where

$$\mathbf{x}_{j} = h\nu_{j}/kT \quad . \tag{7}$$

 $C_{\mathbf{v}}$  is therefore given by

$$C_{\mathbf{v}} = k \sum_{j=1}^{3N} \frac{(\mathbf{x}_{j}/2)^{2}}{\sinh^{2}(\mathbf{x}_{j}/2)}$$
 (8)

For very large values of N, the sum can be approximated by an integral and  $C_{\boldsymbol{v}}$  is given by

$$C_{\mathbf{v}} = k \int_{0}^{\nu_{\mathbf{L}}} g(\nu) \frac{(h\nu/2kT)^{2}}{\sinh^{2}(h\nu/2kT)} d\nu$$
, (9)

wherein  $g(\nu)$  is the frequency distribution function or frequency spectrum, and  $\nu_L$  is the limiting (largest) or cutoff frequency resulting from the fact that there is a finite number of normal mode frequencies.

<sup>13</sup> Debye, P., Ann. Physik, 39, 789 (1912).

Equation (9) is obviously just an integration of the Einstein function over the distribution function  $g(\nu)$ .

Debye  $^{13}$  derived expressions for  $g(\nu)$  and  $\nu_L$  from the theory of vibrations of an elastic continuum.

$$g(\nu) = 4\pi V \nu^2 (2 c_t^{-3} + c_{\frac{1}{2}}^{-3}),$$
 (10)

$$\nu_{\rm L} = \left[ \frac{9N}{4\pi V(2 c_{\rm t}^{-3} + c_{\rm t}^{-3})} \right]^{1/3}. \tag{11}$$

Therefore, the correct distribution function that allows for the cutoff is

$$g(\nu) = \begin{cases} \frac{9N}{\nu_L} \left(\frac{\nu}{\nu_L}\right)^2 & \text{if } \nu < \nu_L \\ 0 & \text{if } \nu > \nu_L \end{cases}$$
 (12)

The final expression for  $C_{\boldsymbol{v}}$  is then

$$C_{v} = 3 Nk \left[ 4D^{\bullet}(x) - \frac{3 x}{exp(x) - 1} \right] = 3 N k D(x),$$
 (13)

where the entire function in the brackets is called the Debye specific heat function, D(x),

$$x = \theta_{\rm D}/T , \qquad (14)$$

$$\theta_{\rm D} = h \nu_{\rm L} / k , \qquad (15)$$

and

$$D^{\bullet}(x) = \frac{3}{x^{3}} \int_{0}^{x} \frac{\eta^{3} d\eta}{e^{\eta} - 1} \qquad (16)$$

In equation (16),  $\eta$  is a dummy variable, and  $\mathbf{x}$  is defined by equations (14) and (15).  $\theta_D$  and  $D^\bullet(\mathbf{x})$  are called the Debye temperature and the Debye energy function, respectively. Beattie 14 has tabulated values of the  $D(\mathbf{x})$  and  $D^\bullet(\mathbf{x})$  functions.

The limiting form of equation (13) at low temperatures; i.e., x >> 1, is

$$C_{v} = 3Nk \left[ (4/5)\pi^{4}x^{-3} + \cdots \right]$$
 (17)

The T<sup>3</sup> function has been extensively used to fit low-temperature heat-capacity data.

The high-temperature limiting form is

$$C_{v} = 3 \text{ Nk} \left[ 1 - \left( \frac{1}{20} \right) x^2 + \left( \frac{1}{560} \right) x^4 + \cdots \right]$$
 (18)

The limit approached by  $C_{\mathbf{v}}$  as the temperature increases is therefore 3R.

Closer examinations of the fit of the Debye theory expression to experimental data have shown that it is not perfect. <sup>5</sup> According to the theory,  $C_{\mathbf{v}}$  is a universal function of the temperature with only one adjustable parameter,  $\theta_D$ . Yet the value of  $\theta_D$  is found to be a function of the temperature for all substances. <sup>5</sup> Improvement of the theory has been sought in sophisticated studies of the discrete lattice. <sup>8</sup>

#### c. Conclusions from Discrete Lattice Theory

It is only natural that attempts would be made to improve the fitting of experimental data by employing combinations of Einstein and Debye functions. The Nernst-Lindemann 15 formula.

<sup>&</sup>lt;sup>14</sup>Beattie, J.A., J. Math. Phys. <u>16</u>, 1 (1926).

<sup>15</sup> Nernst, W. and F.A. Lindemann, Z. Elektrochem; 17, 817 (1911).

$$C_{\mathbf{v}} = \left(\frac{3N\mathbf{k}}{2}\right) \left[ \mathbf{E}(\mathbf{x}) + \mathbf{E}(\mathbf{x}/2) \right] , \qquad (19)$$

is an example which fitted some data well because the vibrational spectra happened to contain two peaks, one at roughly one half of the frequency of the other. 5, 16 Wise et al 17 have recently employed the formula,

$$C_p^0/R = D(\theta_D/T) + 2E_1(\theta_1/T) + E_2(\theta_2/T),$$
 (20)

to represent their boron data where the significance of the subscripts 1 and 2 on  $E_1$  and  $E_2$  was not explained. This must be regarded as an arbitrary curve-fitting procedure since it is not applied to  $C_{\text{v}}$ , it leads to a high temperature limit of 4R for  $C_{\text{p}}^{\text{o}}$ , and it neglects contributions from anharmonicity corrections as well as the  $9\beta^2\,\text{VT/k}$  term to be discussed later.

Sophisticated theories of the discrete lattice<sup>8</sup>, <sup>18</sup> have provided a rational basis for this type of approach. For a lattice containing s atoms per unit cell, it has been deduced that there are 3s solutions to the secular equations for the angular frequency. Three solutions (acoustic branches) tend to  $\omega = 0$  as the wavelength approaches infinity; 3s-3 solutions (optic branches) tend to  $\omega = \text{constant}$  as the wavelength approaches infinity.

An important approximation has been obtained by application of the following assumptions:

- 1) The optical branches are considered to contain a narrow range of frequencies, and the specific heat contribution of each is approximated by an Einstein function ("i" summation index).
- 2) The acoustic branches are each represented by a Debye spectrum with a suitable Debye temperature. ("j" summation index).

<sup>16</sup>Blackman, M., Proc. Roy. Soc. (London), A148, 384 (1935).

<sup>17</sup> Vise, S. J.L. Margrave, and R.L. Altman, The heat content of boron at high temperatures, J. Phys. Chem. 64, 915 (1960).

<sup>18</sup> Born, M., Atomtheorie des festen Zustandes (1923).

Therefore, the heat capacity for a gram formula weight of the s atoms is

$$C_{\mathbf{v}}^{\mathbf{s}} = R \sum_{j=1}^{3} D(\overline{\theta_{j}}/T) + R \sum_{i=4}^{3\mathbf{s}} E(\overline{\theta_{i}}/T) . \qquad (21)$$

 $D(\overline{\theta}_j/T)$  is the Debye specific heat function (in Eq. (13)), and  $E(\overline{\theta}_j/T)$  is the Einstein function (Eq. 4).

The  $\overline{\theta_j}$  must be chosen so that  $C_v$  fits the data well at low temperatures (where the acoustic branches are important), and the corresponding average velocities satisfy the relation,

$$\frac{1}{c_j^3} = \int \frac{1}{c_j^3} \frac{d\Omega}{4\pi} , \qquad (22)$$

for each acoustic branch where  $\Omega$  is the solid angle. This is necessary since the velocities can be orientation-dependent and the frequency spectrum, in the limit of low frequencies, is 3 VF  $\nu^2$ , where

$$F = (4\pi/3) \int \sum_{j=1}^{3} \left(\frac{1}{c_{j}^{3}}\right) \frac{d\Omega}{4\pi} . \tag{23}$$

The quantity F corresponds to  $(2c_t^{-3} + c_0^{-3})$  in the Debye theory. Values of  $\overline{\theta}_j$  for the acoustic branches can be estimated from the elastic constants of the solid since

$$\bar{\theta}_{j} = \left(\frac{h}{k}\right) \bar{\nu}_{j} = \left(\frac{h}{k}\right) \bar{c}_{j} \left(\frac{3}{4\pi V_{a}}\right)^{1/3} , \qquad (24)$$

where  $\overline{c_j}$  is the average sonic velocity for each branch, and  $V_a$  is the volume of the unit cell. The average velocity can be calculated directly using the determinant for the velocity of propagation of elastic waves from the standard theory of elasticity of solids. This determinant

provides an equation relating  $c_j$  to the lattice parameters and the direction of propagation which makes it possible to evaluate the integral in equation (22) and obtain the average velocity  $\overline{c_j} = \sqrt[3]{\overline{c_j}}$ . The optical frequencies  $\nu_4$  to  $\nu_{3s}$  can be taken as the frequencies where the solid shows minimum transmission in the infrared.

The limit approached by equation (21) as the temperature increases is 3Rs for a gram formula weight of the satoms. The average limiting heat capacity per gram atom is therefore the classical value 3R.

Equation (21) applies best where the acoustic and optical branches are well separated. When they are not well separated, it may give a worse fit than a single Debye spectrum. <sup>5</sup>

In trying to obtain a fit to low-temperature data by simultaneous solution with 3s points, one should remember that the points must be "smoothed" since the raw data contain statistical variations within their accuracy limits. This method should be used in combination with a least-squares regression analysis to obtain the most probable values of the  $\overline{\theta_i}$ 's and  $\overline{\theta_i}$ 's.

Detailed calculations of frequency spectra have been made for several systems such as a body-centered cubic lattice (fitted to the tungsten elastic constants  $^{19}$ ), ionic crystals of the alkali halide type  $^{20}$  (characterized by long-range coulombic forces between ions), diamond,  $^{21}$  facecentered (close-packed) cubic crystals,  $^{22}$  and alkali metals.  $^{23}$  In general, these frequency spectra have a form not in good agreement with the assumptions in equation (21). Debye spectra do not generally represent the acoustic branches well. In the case of ionic crystals, there is a pronounced, high-frequency tail to the optic branches that makes the use of Einstein functions dubious. However, one must bear in mind that the heat capacity is rather insensitive to the form of the frequency spectrum, especially at very high temperatures, and crude approximations in  $g(\nu)$  can give surprisingly useful representations of the harmonic vibration contributions to  $C_{\pi}$ .

<sup>&</sup>lt;sup>19</sup>Fine, P.C., Phys Rev. <u>56</u>, 355 (1939); Montroll, E.W. and D. Peaslee, J. Chem. Phys. <u>12</u>, 98 (1944).

<sup>&</sup>lt;sup>20</sup>Kellermann, E.W., Phil. Trans. Roy. Soc. (London) 238A, 513 (1940); Jona, M., Phys Rev. 60, 823 (1941).

<sup>&</sup>lt;sup>21</sup>Smith, H., Phil. Trans. Roy. Soc. (London) <u>241A</u>, 105 (1948).

<sup>&</sup>lt;sup>22</sup>Leighton, R.B., Rev. Mod. Phys. <u>20</u>, 165 (1948).

<sup>&</sup>lt;sup>23</sup>Fuchs, K., Proc. Roy. Soc. (London) <u>157A</u>, 444 (1936).

A number of methods have been worked out for obtaining Debye temperatures from other physical properties,  $^5$  such as the temperature dependence of the intensity of X-ray diffraction spots, infrared absorption or reflection peaks, compressibilities, melting points, electrical resistance, and expansion coefficients. Such methods provide only crude estimates of  $C_{\mathbf{v}}$  at low or moderate temperatures because of the inadequacy of a single Debye temperature in fitting actual data. Moreover, the Debye temperatures so obtained do not exactly equal those obtained directly from  $C_{\mathbf{v}}$  data at any temperature. The "thermal spot" theory appears to offer some promise since it can be used to obtain detailed frequency spectra indirectly from lattice constants derived from studies of X-ray scattering.  $^5$ 

### 4. Electron Gas Contributions at Very Low Temperatures

The free electron gas in electrical conductors is responsible for most of their heat capacity at very low temperatures. <sup>4</sup> The free electrons obey Fermi-Dirac statistics, and this results in a low-temperature heat capacity contribution proportional to the absolute temperature. When combined with equation (17), this results in the expression often used with metals at very low temperatures

$$C_p^o = 464.4 (T/\theta_D)^3 + \alpha T$$
 (25)

The electron gas contribution is negligible at the intermediate temperature level.

## 5. High-Temperature Specific Heat of Solids

Some progress has been made in the development of the theory of specific heats of solids at high temperatures 5, 24, 25 but more progress needs to be made in calculations for individual systems before our understanding of this property is complete.

Experimental measurements provide  $C_p^\circ$  data, but the theory is usually concerned with  $C_v$ . These two quantities are related by means of the well-known equation derived from rigorous thermodynamic relations i.e.

$$C_{p}^{o} = C_{v} + 9\beta^{2} VT/\kappa . \qquad (26)$$

<sup>24</sup> Born, M. and E. Brody, Z. Physik 6, 132 (1921).

<sup>&</sup>lt;sup>25</sup>Schroedinger, E., Z. Physik <u>11</u>, 170 (1922).

TAB LE II
REPRESENTATIVE HIGH-TEMPERATURE HEAT CAPACITY DATA

Number	Element or		T	C° p cal/gfw°C	Reference	C°p/: cal/gfw
of Atoms	Compound	°F	°K	- car/grw o	Number	cai/giw
2	TiC	2800		13.180	26	6.59
2	TiN	2800		13.496	26	6.75
2	TiN	4000		14. 2	27	7.1
3	ThO2		2000	22.40	26	7.47
2	MgO	3200		13.669	26	6.83
2	BN	1700		8.207	26	4.10
2	BeC	2800		7.022	28	3.51
2	BeO	1400		12. 256	26	6.13
1	Graphite	2000		5.405	26	5 - 40
1	ATJ Graphite	4000		5.5	29	5.5
1	Graphite	3125		5.92	This Project	5.92
1	Graphite	3040		5.94	27	5.94
3	UO <sub>2</sub>	2200		21.330	26	7.11
3	TiO <sub>2</sub>	2800		13.496	26	4.50
4	UCL3	1400		31.682	30	7.92
2	ZrN*	4000		12.6	29	6.3
5	Zr <sub>3</sub> N <sub>2</sub>	975		42. 235	26	8.46
5	A1203	2800		32.627	26	6.53
5	$Al_2O_3$		1873-2273	38.2	31	7.65
5	Cr <sub>3</sub> C <sub>2</sub>	1790		37 811	26	7.56
1	W		1273	6.66	7	6.66
1	W	4000		7.7	29	7.7
1	Fe-y		1773	9.44	7	9.44
1	Fe-a		773	9.10	7	9.10
1	Fe-a		973	12.84	7	12.84
1	Fe-a		1073	11.70	7	11.70
1	В		2000	7 288	17	7.288
1	В		2000	7 20	32	7.20
7	Si 3N4*	4000		42.1	29	6.0
2	TaB*	4000		18.8	29	9.4
2	ZrC*	4000		12.4	29	6.2
2	NbC*	4000		13.1	29	6.6
2	TaC*	4000		13.9	29	7 0
2	ZrB*	4000		18.4	29	9 2

<sup>\*</sup>Assumed formula; not given by source.

<sup>26</sup>Kelly, K.K., Data on Theoretical Metallurgy, X. High Temperature Heat Content and Entropy for Inorganic Compounds, U.S.Bur. Mines Bull. 476 (1949).

<sup>27</sup> Rasor, N.S. and J.D. McClelland, Part 1. Thermal Properties of Materials, Properties of Graphite, Molybdenum and Tantalum to Their Destruction Temperatures #ADC-TR-36-400 (1936).

<sup>28</sup> Ginnings, D.C. and G.T. Furukawa, Heat capacity standards for the range 14° to 1200° K. J. Am. Chem. Soc. 75, 525 (1953).

<sup>29</sup> Southern Research Institute, Quarterly Progress Report No. 4 to WADD, Repr. No. 4398-1068-XII, The Thermal Properties of Solid Materials to Very High Temperatures, Contract AF33(616)-6312 (8 April 1960).

<sup>&</sup>lt;sup>10</sup>Commings, D.C. and R.J. Corruccini, An Improved Ice Calorimeter-The Determination of Its Calibration Factor and The Denaity of Ice at 0°C, J. Research Nat. Bur. Stds. 38, 383 (1942).

<sup>11</sup> Kirillin, V.A., A. YeSheyndlin, and V. YaChenkovakiy, Akademiya nauk SSSR, Doklady, 135, 125 (1960).

<sup>32</sup> Sinks, G.C., D.R. Stull, R.M. Hunter, H.A. Robinson, and R.P. Rub, Thermodynamic Properties of Combustion Products, #ADC and ARPA, Rept. AF-214-587, Dow Chem. Co. (1 April 1939).

where  $\beta$  is the linear thermal expansion coefficient, v is the volume, and  $\kappa$  is the bulk compressibility. \*The first term on the right takes care of the vibrational energy contributions and approaches a high-temperature limit of 3R per gram atom for a harmonically vibrating lattice. The second term on the right accounts for the energy absorbed due to expansion against the cohesive forces of the solid.

In many actual cases, as one can see from Table II, the 3R limit per average gram atom is exceeded at high temperatures, and one must look for large contributions from the expansion term and other possible terms due to anharmonicity, conduction electrons, gradual transitions, and higher electronic energy levels. The extensive heat capacity data for tungsten 33 plotted in figure 2 show how these additional contributions and the expansion term vary with temperature for that substance.

## a. Constant Volume (Vibrational) Heat Capacity Contribution

Born and Brody  $^{24}$  and Schroedinger  $^{25}$  investigated the specific heat of an anharmonically vibrating lattice. Born and Brody approached the problem by studying the contributions of terms higher than quadratic in the displacement coordinates of the potential energy to the Helmholtz free energy of a system of quantum mechanical oscillators at large amplitudes. From this, they calculated corresponding contributions to the entropy and internal energy and obtained those for  $C_{\mathbf{v}}$  by differentiation of the latter with respect to temperature. They found the limiting form of  $C_{\mathbf{v}}$  at high temperatures to be

$$C_{\mathbf{v}} = 3R(1 - 6\sigma RT) \tag{27}$$

From equation (27), it can be seen that the anharmonicity correction over the classical limiting value is  $-18\sigma R^2 T$ .  $\sigma$  is a characteristic constant of the crystal whose sign is thought by some to be not determined so that it could presumably be either positive or negative.  $^{5}$ ,  $^{7}$  Born and Brody  $^{24}$  state that  $\sigma$  is negative and that  $C_v$  values above  $_{3R}$  are to be expected.

The case of rocksalt has been analyzed by two methods,  $^{34}$ ,  $^{35}$  and there appears to be a maximum in  $C_v$  versus temperature of uncertain validity. There is no evidence for such a maximum in the tungsten  $^{33}$  data in figure 2. It is also obvious from the figure that harmonic vibration contributions do not account for the value of  $C_v$  at high temperatures. The difference between  $C_v$  and 3R at high temperatures is large and not quite linear with temperature.

<sup>33</sup> Zwikker, C. and G. Schmidt, Physica, 8, 329 (1928).

<sup>34</sup> Eucken, A. and W. Dannöhl, Z. Elektrochem. 40, 814 (1934).

<sup>35</sup> Siegel, S. and L. Hunter, Phys. Rev. 61, 84 (1942).

 $<sup>^{\</sup>bullet}\beta = (1/k) \left(\partial k/\partial T\right)_{p}$  and  $\kappa = -(1/V) \left(\partial V/\partial p\right)_{T}$  where k is length and p is pressure.

It is possible in principle to calculate  $C_{\rm v}$  for ionic crystals, using the free energy, by a method developed by Born. <sup>36</sup>

## b. The Expansion Term

Euken and Dannohl<sup>34</sup> have made an analysis of  $C_p^{\circ} - C_v$  for a number of substances relying upon the assumption that the Gruneisen constant  $\gamma$  is independent of temperature to obtain the compressibility from the thermal expansion coefficient. In the case of rocksalt, the results of their analysis differ enough from those of Siegel and Hunter, <sup>35</sup> who used a complete set of available data, that the method must be considered with some reservations. Siegel and Hunter found that the  $9V\beta^2T/\kappa$  term is large at high temperatures.

Gruneisen's  $^4$ ,  $^{37}$ ,  $^{38}$  theory for the equation of state of a solid neglects anharmonicities. This theory assumes that the normal mode frequencies are volume- or lattice-spacing-dependent. This dependence is represented by a parameter  $\gamma$ , the Gruneisen constant. The equation of state and expansion coefficients are therefore functions of  $\gamma$ . For the well-known Debye continuum model of a crystalline solid,  $\gamma$  is defined as

$$\gamma = -\frac{\partial \log \theta_{\rm D}}{\partial \log V} , \qquad (28)$$

where  $\theta_{\rm D}$  is the Debye temperature, and V is the volume. From the equation of state of a Debye crystal, one finds that

$$(\partial p/\partial T)_{V} = yC_{v}/V . (29)$$

and

$$\beta = \kappa \gamma C_{\pi}/3V , \qquad (30)$$

since

$$\beta = (1/3)\kappa(\partial p/\partial T)_{V}. \tag{31}$$

<sup>36</sup> Born, M., J. Chem. Phys. 7, 591 (1939).

<sup>&</sup>lt;sup>37</sup>Gruneisen, E., <u>Handbuch der Physik</u>, vol. 10, p. 22, Springer-Verlag, Berlin (1953).

<sup>&</sup>lt;sup>38</sup>Slater, J.C., Introduction to Chemical Physics, McGraw-Hill, N.Y. (1939), p. 215-220.

This provides a useful approximation for evaluating the expansion term 9V  $\beta^2 T/\kappa$  in equation(26). y for many metals remains constant over a wide range of temperatures and densities.

Lindemann and Magnus proposed the empirical equation,

$$C_p^{\circ} - C_v = aT^{3/2}$$
, (32)

wherein a is a different constant for each substance. Since this formula, with a equal to  $7 \times 10^{-6}$  cal  ${}^{\circ}K^{-5/2}/g$  atom, fits the tungsten data in figure 2 within a few tenths of a cal/g atom  ${}^{\circ}K$ , it appears to be a useful approximation for use in extrapolating rough data. A more exacting test of this approximation is presented in figure 3 which shows more precisely the extent of accuracy that can be expected.

#### c. Conduction Electron Contributions

For the heat capacity of electrical conductors such as metals, there is a contribution proportional to the temperature for the conduction electrons at low temperatures as discussed in section III-C4. This contribution is negligibly small for most metals at room temperature except for the transition elements such as platinum and palladium. Since this contribution is an increasing function of the temperature, it could well contribute outside the experimental error at very high temperatures for many refractory metals. Many of the compounds within the scope of this project become conductors at high temperature, but the importance of this contribution to their heat capacity is unknown.

The large contribution in the case of ferroelectric metals has been discussed in some detail.  $^{39}$ ,  $^{40}$ ,  $^{41}$ 

#### d. Transitions

The occurrence of thermal transitions complicates the analysis of high-temperature specific heat data even further. These can be of several types which in principle can be clearly classified but in practice are less definite. A brief but penetrating review of this subject has been provided by Smoluchowski. 42

<sup>39</sup>Stoner, E.L., Proc. Roy. Soc. (London) A169, 339 (1939).

<sup>&</sup>lt;sup>40</sup>Mott, N.F., Proc. Roy. Soc. (London) A152, 43 (1935).

Hunt, K.L., Proc. Roy. Soc. (London) A216, 103 (1953).

<sup>42</sup>Smoluchowski, R., Phase Transformations in Solids, In: Handbook of Physics, McGraw-Hill, N.Y. (1958), Chap. 8, p. 8-108.

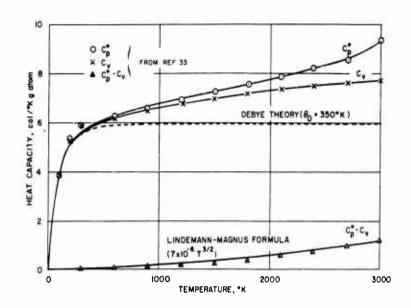


Figure 2 ATOMIC HEAT CAPACITY OF TUNGSTEN VERSUS TEMPERATURE

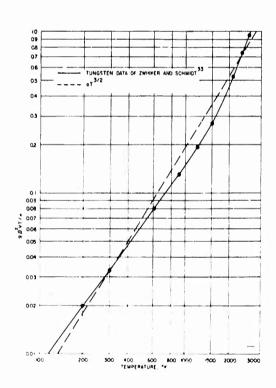


Figure 3 TEST OF LINDEMANN-MAGNUS FORMULA WITH TUNGSTEN DATA

Ehrenfest suggested a classification of transitions into orders according to which a transition is of the n<sup>th</sup> order when temperature derivatives of F, the free energy, lower than the n<sup>th</sup> are continuous at the transition temperature while the n<sup>th</sup> derivative is discontinuous. Strictly speaking, only first-order transitions are phase transformations, but this designation has been commonly used for all transitions.

The usefulness of Ehrenfest's classification has been limited because of various intermediate kinds of anomalies that make it difficult to determine whether or not continuity of thermodynamic functions exists. Figure 4, due to Mayer and Streeter, 43 illustrates various common types of transformations.

First-order transformations are in principle simple to treat. They are the most common type where two phases can coexist in equilibrium and there is a definite heat of transformation. Integrations for thermodynamic functions can be performed smoothly over the two separate phases on either side of the transition point, and a heat and an entropy of transition can be added above the transition temperature, the free energy of transition being zero. Often in practice however, each phase anticipates the onset of the other so that the transition is not perfectly sharp. Large rises in  $C_p^{\sigma}$  just below the melting point, called premelting, have been observed.

Second-order transformations are usually of the "lambua" type. In such cases, some continuous change is evident, and a definite heat of transformation cannot be assigned.

Diffuse transformations are spread out over a large range of temperature. Here again a definite heat of transformation cannot be assigned to them.

Certain crystals such as ammonium and hydrogen halides undergo a transformation as the temperature is increased that was first thought to be due to the onset of free rotation.  $^{44}$  A better interpretation appears to be that of Frenkel,  $^{45}$  who proposes that it corresponds to a progressive decrease in orientation of oscillation axes of the ions up to a critical temperature and then random orientation above the critical temperature.  $^{46}$ ,  $^{47}$ ,  $^{48}$  How generally this type of transformation

<sup>43</sup> Mayer, J.E. and S.F. Streeter, J. Chem. Phys. 2, 1019 (1939).

<sup>44</sup> Pauling, L., Phys. Rev. 36, 430 (1930).

<sup>45</sup> Frenkel, J., Acta Physiochem. (USSR) 3, 23 (1935).

<sup>46</sup> Wagner, E.L. and D.F. Hornig, J. Chem. Phys. 18, 296 (1950).

<sup>47</sup> Levy, H.A. and S.W. Peterson, Phys. Rev. 83, 1270 (1951).

<sup>48</sup> Lawson, A.W., Phys. Rev. 57, 417 (1940).

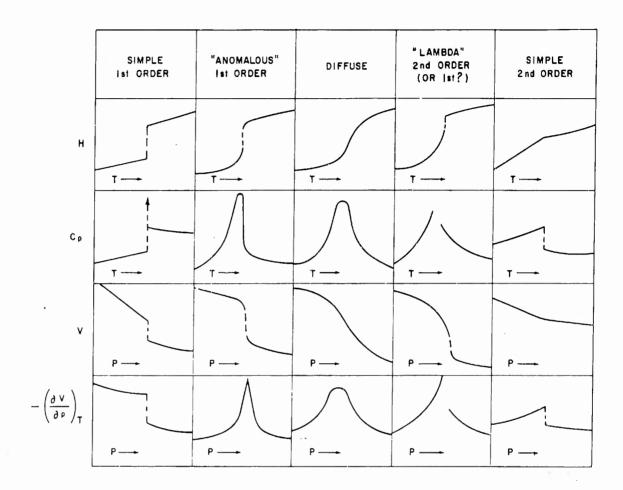


Figure 4 TYPES OF TRANSFORMATIONS IN SOLIDS

occurs is not known, but a similar type has been reported to occur in many organic compounds and even polymers. 49

Another phenomenon which appears in many metals and compounds at very high temperatures is thermionic emission. This also cannot strictly speaking be considered a transformation since it develops gradually as the temperature is increased. Its importance to the thermodynamic properties of the solid depends upon the extent to which it occurs which in turn depends upon the work function. Since it provides an electron gas species in the vapor at equilibrium with the solid, it is related to the ionic equilibria in the vapor.

<sup>49</sup> Glasstone, S., op. cit., p. 428.

#### D. THE MONATOMIC GAS COMPUTER PROGRAM

## 1. Method of Calculation

The methods of calculation for the thermodynamic properties of monatomic gases are well known and have been described in many standard texts, articles, reports, etc. 50,51 The general procedure followed in the present project has been that of Kolsky, Gilmer, and Gilles. 51 Their equations were modified in some cases to give the following formulas adopted for use in the present work:

$$Q = \sum_{i} (2J_{i} + 1) e^{-\frac{\alpha \nu_{i}}{T}} , \qquad (33)$$

$$Q_1 = \sum_{i} (2J_{i} + 1) \nu_{i} e^{-\frac{\alpha \nu_{i}}{T}} , \qquad (34)$$

$$Q_2 = \sum_{i}^{\infty} (2J_{i} + 1) \nu_{i}^{2} e^{-\frac{\alpha \nu_{i}}{T}} , \qquad (35)$$

$$H_{298}^{\circ} - H_{0}^{\circ} = K_{1} \left(\frac{Q_{1}}{Q}\right)_{298} + 298.15 K_{2}$$
 (36)

$$H_T^{\circ} - H_{298}^{\circ} = \kappa_1 \left[ \left( \frac{Q_1}{Q} \right) - \left( \frac{Q_1}{Q} \right)_{298} \right] + \kappa_2 \frac{(T - 298.15)}{1000} ,$$
 (37)

$$C_p^{\circ} = \frac{\kappa_3}{T^2} \left[ \left( \frac{Q_2}{Q} \right) - \left( \frac{Q_1}{Q} \right)^2 \right] + \kappa_2 \quad , \tag{38}$$

$$S_T^{\circ} = \frac{\kappa_1}{T} \left( \frac{Q_1}{Q} \right) + R \ln Q + K_4 \ln M + K_2 \ln T + K_5$$
, (39)

<sup>50</sup> Mayer, J. E. and M. G. Mayer, Statistical Mechanics, Wiley, N.Y. (1940), p. 109.

<sup>&</sup>lt;sup>51</sup>Kolsky, H. G., R. M. Gilmer, and P. W. Gilles, The Thermodynamic Properties of 54 Elements Considered As Ideal Monatomic Gases, Los Alamos Scientific Laboratory, Rept. LA-2110 (15 March 1957).

$$-\left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right) = R \ln Q + K_{4} \ln M + K_{2} \ln T + K_{6} + \frac{K_{1}}{T} \left(\frac{Q_{1}}{Q}\right)_{298} + K_{2} \left(\frac{298.15}{T}\right), \tag{40}$$

$$-\left(\frac{F_{T}^{\circ}-H_{Q}^{\circ}}{T}\right) = R \ln Q + K_{4} \ln M + K_{2} \ln T + K_{6} ,$$

$$-\left(\frac{F_{T}^{\circ} - H_{O}^{\circ}}{T}\right) + \left(\frac{H_{298}^{\circ} - H_{O}^{\circ}}{T}\right) = -\left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right) , \qquad (41)$$

$$\Delta H_{f}^{\circ} = \Delta H_{f298}^{\circ} + (H_{T}^{\circ} - H_{298}^{\circ})_{\text{monatomic gas}} - (H_{T}^{\circ} - H_{298}^{\circ})_{\text{ref. state}}$$
, (42)

$$\Delta F_{f}^{\circ} = \Delta H_{f298}^{\circ} - \frac{T}{1000} \left[ - \left( \frac{F_{T}^{\circ} - H_{298}^{\circ}}{T} \right)_{\text{monatomic gas}} \right]$$

$$+ \left(\frac{F_T^{\circ} - H_{298}^{\circ}}{T}\right)_{\text{ref. state}}$$

$$Log_{10} K_{p} = \frac{-1000 \text{ AF}_{f}^{\circ}}{4.575835 \text{ T}}$$
 (44)

Definitions of some of the symbols used above can be found in Table III. The remainder are defined as follows:

- Q = partition function,
- J, = inner quantum number of the ith state,
- = wave number for a given energy level in cm<sup>-1</sup>;
- T absolute temperature in degrees Kelvin,
- $H_{298}^{\circ} H_{O}^{\circ}$  = enthalpy of an ideal gas at 298.15°K relative to the ideal gas at absolute zero,

 $\frac{\mathtt{TABLE}\ \mathtt{III}}{\mathtt{VALUES}\ \mathtt{OF}\ \mathtt{PHYSICAL}\ \mathtt{CONSTANTS}\ \mathtt{FOR}\ \mathtt{GAS-PHASE}\ \mathtt{CALCULATIONS}}$ 

Constant	Definition	Value of Kolsky <u>et al</u> 51	Units	Value Used in Present Work	"Perturbed" Value Used in Error Calculation
а	hc k	1.43880	cm deg	"1.43880 ±0.00007	1.43873
к,	Ra	2.860047	cal cm mole-1	2.8592696 ±0.000254	2. 859523
κ <sub>2</sub>	(5/2)R	4.96950	cal deg-1mole-1	4.968150 ±0.00020	4.968350
к <sub>3</sub>	Ra <sup>2</sup>	4. 115035	cal cm <sup>2</sup> deg mole <sup>-1</sup>	4.1139163 ±0.000565	4. 114481
к <sub>4</sub>	(3/2)R	2.98170	cal deg-1mole-1	2.98089 ±0.00012	2. 98101
к,	Sackur- Tetrode Constant <sup>20</sup>	-2.316818	cal deg <sup>-1</sup> mole <sup>-1</sup>	-2.315380 ±0.00013	-2.31525
к <sub>6</sub>	K <sub>5</sub> + (5/2) R	-7.286318	cal deg-lmole-l	-7.283530 ±0.00033	-7.28320
R	Gas Constant	1.98780	cal deg-lmole-l	1.98726 ±0.000081	1.98734

H<sup>o</sup><sub>T</sub> - H<sup>o</sup><sub>298</sub> = enthalpy of an ideal gas at temperature T, relative to the ideal gas at 298.15°K.

C<sup>o</sup><sub>P</sub> = heat capacity of ideal gas in cal/°K, g mol,

S<sup>o</sup><sub>T</sub> = entropy of ideal gas in cal/°K, g mol,

 $-\left(\frac{F_T^o - H_{298}^o}{T}\right)$  = free-energy function, in cal/ °K, g mol,

m = molecular weight,

R = gas constant, cal/ K g mol,

 $\Delta H_t^0$  = standard heat of formation at temperature  $\Gamma$ , in Kcal/g mole,

ΔH<sub>6298</sub> = standard heat of formation at 298.15 °K, in Kcal/g mole,

ΔF<sub>f</sub> = standard free energy of formation at temperature T, in Kcal/g mole,

E = equilibrium constant for sublimation or vaporization to a monatomic gas from the condensed phase of the pure

The values of the constants used in these equations were based on the work of Cohen, Crowe, and Dumond.\(^1\) The derived constants for the above equations are listed in TableIII. For the sake of comparison, the constants used by Kolsky et al<sup>51</sup> were also included. It should be noted that their value of the gas constant was based on the physical atomic weight scale, whereas the value based on the chemical atomic weight scale has been adopted in the fifth column of the table. All derived quantities were therefore correspondingly adjusted. The uncertainties in the fifth column were derived from the values of Cohen, Crowe, and Dumond.\(^1\)

The machine program used for preparing ideal monatomic gas tables con-

taining 
$$C_p^\circ$$
 ,  $S_T^\circ$  ,  $-\left(\!\frac{F_T^\circ-H_{298}^\circ}{T}\!\right)\!,~H_T^\circ-H_{298}^\circ$  ,  $\Delta H_f^\circ$  ,  $\Delta F_f^\circ$  , and  $\text{Log}_{10}\,K_p$  was

based on the equations summarized above. The required input data for its use are:

- a.  $J_i$  versus  $v_i$  (cm<sup>-1</sup>),
- b. The eight constants in the last two columns of Table III,
- c. The molecular weight on the chemical scale,
- d. ΔH<sub>1298</sub> in Kcal/mole,
- e. Enthalpy of the reference state as a function of temperature,
- f. Free energy of the reference state as a function of temperature,
- g. The temperature for each entry of the table.

## 2. Uncertainty-Range Calculations

The uncertainty limits were obtained by repeating the calculation described immediately above with the "perturbed" values in the last column of Table III and individually chosen values of the other input data. The difference between the results of the two calculations was taken as the uncertainty range.

Considerable thought had to be given to the choice of the other input data for the uncertainty analysis. This is worthwhile to discuss in more detail.

## a. Ji versus vi

The  $\nu_i$  values were obtained by a "perturbation" of the last significant figure given in Moore's tables;  $^{52}$  i.e., the ones used in the normal calculation above. For example, if  $\nu_i = 16$  cm<sup>-1</sup> as reported by Moore, then the perturbation was -1, giving  $\nu_{i(perturbed)} = 15$  cm<sup>-1</sup>. A negative "perturbation" was used since this should lead to an increased occupation of excited levels at a given temperature, as compared with the "unperturbed" states.

This means that the partition function (and consequently, the free-energy function) was maximized. Since the free-energy function is basically the most important single thermochemical quantity with the exception of the heat of formation, it is seen that this procedure is the optimum one. However, if desired, a positive perturbation could also be used, and the calculations repeated.

<sup>52</sup> Moore, C. E., Atomic Energy Levels, NBS Circular 467, vol. 1 (15 June 1949).

#### b. The Eight Constants of Table III

The constants in Table III were "perturbed" from the "best" values in the fifth column, again in such a manner as to maximize the errors in the free-energy function.

#### c. The Molecular Weight on the Chemical Scale

Normally, no perturbation was included for the molecular weight, but this could be included if the uncertainties in molecular weight became appreciable. For example, if the uncertainty in molecular weight became 1 part in 2500, an error of about 0.001 e.u. could be assigned to  $S_{\mathsf{T}}^{\mathsf{o}}$  or the free-energy function.

## d. ΔH<sub>2298</sub> in Kcal/mole

Errors in  $\Delta H_{f298}^o$  are ordinarily the largest and most significant in thermodynamic calculations. These errors will lead to errors in  $\Delta H_f^o$ ,  $\Delta F_f^o$ , and  $Log_{10}K_p$ . The input to the calculation routine described above consisted of the absolute value of the uncertainty, designated above. This is equivalent to considering the true value of  $\Delta H_{f298}^o$  to lie in the range of  $\Delta H_{f298}^o$   $\pm$   $a_{298}$ .

#### e. Uncertainties in Enthalpy Functions

Uncertainties in the enthalpy functions of the monatomic gas were labeled  ${\bf b}_T$  (Kcal/gram atom of gas). Thus,( ${\bf H}_T^\circ-{\bf H}_{298}^\circ$ ) was considered to be within the range of values of  $({\bf H}_T^\circ-{\bf H}_{298}^\circ) \pm {\bf b}_T$ . Values of  ${\bf b}_T$  were taken from results of the calculation based on the data in steps (a) through (c) above.

Uncertainties in the enthalpy functions of the reference state were labeled  $^cT$  and fed into the program as input data.

#### f. Uncertainties in Free-Energy Functions

Uncertainties in the free-energy functions of the monatomic gas and reference state were designated as  ${\rm d}_T$  and  ${\rm e}_T$ , respectively. They were obtained in the same manner as  ${\rm b}_T$  and  ${\rm c}_T$  described just above.

## g. Uncertainties in $\Delta \text{H}^{\circ}_f$ , $\Delta \text{F}^{\circ}_f$ , and $\text{Log}_{10}\text{K}_p$

The uncertainties in  $\Delta H_f^{\circ}$ ,  $\Delta F_f^{\circ}$ , and  $Log_{10}K_p$  were obtained as the sum of the component uncertainties since each term in the summation is independent of any other. For example, since

$$\Delta H_{f}^{\circ} + \delta \Delta H_{f}^{\circ} = (\Delta H_{f298}^{\circ} + a_{298}) + \left[ (H_{T}^{\circ} - H_{298}^{\circ})_{gas} + b_{T} \right]$$

$$- \left[ (H_{T}^{\circ} - H_{298}^{\circ})_{ref} + c_{T} \right] , \qquad (45)$$

then,

$$\delta (\Delta H_f^{\circ}) = a_{298} + b_T + c_T$$
 (46)

Likewise, the other uncertainties are

$$\delta (\Delta F_f^{\circ}) = a_{298} + \frac{T}{1000} (d_T + e_T)$$
, (47)

and

$$\delta \left( \text{Log}_{10} \, \text{K}_{\text{p}} \right) = \left[ \delta \left( \Delta F_{\text{f}}^{\circ} \right) \right] \left[ \frac{1000}{4.575835 \, \text{T}} \right] \quad . \tag{48}$$

#### E. DIATOMIC MOLECULE CALCULATIONS

The computer program used in the calculations of the thermodynamic functions of diatomic molecules was based on a treatment of the diatomic molecule developed by Mr. T. Munson of Avco RAD over a period of time. A program for a single electronic state using this treatment has been in use on other projects at Avco RAD. The present program was designed to be applied to the general case of the diatomic molecule with multiple electronic states. The following discussion of the calculation is based on the standard equations and symbols of the spectroscopists, except where duplications of symbol usage might result in confusion.

The treatment of a given electronic state is an elaboration of the method of Mayer and Mayer<sup>50</sup> but takes into account spectroscopic constants of higher order than the latter.

The input data for the program are the electronic energy (defined later) and the standard spectroscopic constants  $\omega_e$ ,  $\omega_e x_e$ ,  $\omega_e y_e$ ,  $B_e$ ,  $\alpha_e$ ,  $\gamma_e$ , and  $D_e$ . Although values of  $\gamma_e$  are not commonly tabulated, they may be estimated from Dunham's equations. Spectroscopic constants which are sometimes determined but which are not included in the present calculation are  $\omega_e z_e$ ,  $\beta_e$ , and coefficients of powers of  $\gamma$  ( $\gamma$  + 1) greater than the second.

It is assumed that the internal energy, exclusive of the electronic energy, may be expressed as a function of the quantum numbers v and j for a given electronic state by the expression

$$\epsilon_{i} = \omega_{e} \left( \mathbf{v} + \frac{1}{2} \right) - \omega_{e} \mathbf{x}_{e} \left( \mathbf{v} + \frac{1}{2} \right)^{2} + \omega_{e} y_{e} \left( \mathbf{v} + \frac{1}{2} \right)^{3} + j (j+1) \left[ B_{e} - \alpha_{e} \left( \mathbf{v} + \frac{1}{2} \right) + y_{e} \left( \mathbf{v} + \frac{1}{2} \right)^{2} \right] - D_{e} j^{2} (j+1)^{2} ,$$
(49)

where the energy is expressed in wave numbers.

If the energy of the lowest level (v = 0, j = 0) is taken as zero, equation (49) may be re-arranged and put in the form

$$(\epsilon - \epsilon_0)_i = \omega \, \mathbf{v} - \omega \mathbf{x} \, \mathbf{v} (\mathbf{v} - 1) + \omega y \, \mathbf{v} (\mathbf{v} - 1) (\mathbf{v} - 2)$$

$$+ j (j+1) \left[ 1 - \rho \, j (j+1) - (\delta - \phi) \mathbf{v} - \phi \, \mathbf{v}^2 \right] B_{\mathbf{e}} (1 - \delta/2) ,$$
(50)

<sup>53</sup>Dunham, J.L., Phys. Rev. 41, 721 (1932).

where

$$\omega = \omega_{e} - 2 \omega_{e} x_{e} + (13/4) \omega_{e} y_{e},$$

$$\omega x = \omega_{e} x_{e} - (9/2) \omega_{e} y_{e},$$

$$\omega y = \omega_{e} y_{e},$$

$$x = \omega x/\omega,$$

$$y = \omega y/\omega,$$

 $\rho \cong D_{\mathbf{e}}/B_{\mathbf{e}} , \tag{5}$ 

(51)

$$\delta = \alpha_{e}/B_{e} + (\alpha_{e}/B_{e})^{2} - 2\gamma_{e}/B_{e} ,$$

$$\phi = -\gamma_{e}/B_{e} + \frac{1}{2}(\alpha_{e}/B_{e})^{2} .$$
(52)

In arriving at the above definitions, it is convenient to use the approximation

$$\gamma_{\rm e} \approx (2/3)\alpha_{\rm e}^2/B_{\rm e} , \qquad (53)$$

which follows from Dunham's equations. 53

and the following definitions are added

The internal partition function, exclusive of a term for the electronic energy, may be written as

$$Q(v,j) = \sum_{v,j} (2j+1) \exp \left\{ -u \left[ v - xv(v-1) + yv(v-1)(v-2) \right] \right\}$$

$$-\sigma j(j+1) \left[ 1 - \rho j(j+1) - (\delta - \phi) v - \phi v^{2} \right] = \frac{Q_{c}}{\sigma (1 - e^{-u})}, \quad (54)$$

where  $1/\sigma$  is the partition function for the rigid rotator,  $1/(1-e^{-u})$  is the partition function for the harmonic oscillator, and  $Q_c$  contains the terms for anharmonicity and rotation-vibration interactions. Further definitions for these terms are

$$\sigma = B_{\rho}(1 - \delta/2) \, hc/kT , \qquad (55)$$

and

$$u \approx hc\omega/kT$$
 . (56)

A procedure analogous to that of Mayer and Mayer<sup>50</sup> was used to expand the exponential and approximate the summation in equation (54). The contributions to the thermodynamic functions from internal degrees of freedom (designated by subscript i) then become

$$-\left(\frac{F_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{i}^{\circ} = \ln Q(\mathbf{v}, \mathbf{j}) = -\ln \sigma - \ln \psi + \sigma/3 + \sigma^{2}/90 + 2\rho/\sigma$$

$$+ \delta e^{-\mathbf{u}}/\psi + 2\mathbf{x}\mathbf{u}e^{-2\mathbf{u}}/\psi^{2}$$

$$+ 2\mathbf{x}^{2}e^{-2\mathbf{u}}\mathbf{u}^{2}(1 + 4e^{-\mathbf{u}})/\psi^{4} + \delta^{2}e^{-\mathbf{u}}/2\psi^{2}$$

$$+ 4\delta \mathbf{x}\mathbf{u}e^{-2\mathbf{u}}/\psi^{3} - 6y\mathbf{u}e^{-3\mathbf{u}}/\psi^{3} + 2\phi e^{-2\mathbf{u}}/\psi^{2}$$

$$\left(\frac{H_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{i}^{\circ} = 1 + \mathbf{u}e^{-\mathbf{u}}/\psi - \sigma/3 - \sigma^{2}/45 + 2\rho/\sigma + \delta e^{-\mathbf{u}}\mathbf{u}/\psi^{2}$$

$$+ 4\mathbf{x}\mathbf{u}^{2}e^{-2\mathbf{u}}/\psi^{3} - 2\mathbf{x}\mathbf{u}e^{-2\mathbf{u}}/\psi^{2} + 6y\mathbf{u}e^{-3\mathbf{u}}/\psi^{3}$$

$$- 18y\mathbf{u}^{2}e^{-3\mathbf{u}}/\psi^{4} + 4\mathbf{x}^{2}\mathbf{u}^{3}e^{-2\mathbf{u}}(1 + 7e^{-\mathbf{u}} + 2e^{-2\mathbf{u}})/\psi^{5}$$

$$- 4\mathbf{x}^{2}\mathbf{u}^{2}e^{-2\mathbf{u}}(1 + 4e^{-\mathbf{u}})/\psi^{4} + 4\delta \mathbf{x}\mathbf{u}^{2}e^{-2\mathbf{u}}(2 + e^{-\mathbf{u}})/\psi^{4}$$

$$- 4\delta \mathbf{x}\mathbf{u}e^{-2\mathbf{u}}/\psi^{3} + \delta^{2}\mathbf{u}e^{-\mathbf{u}}(1 + e^{-\mathbf{u}})/2\psi^{3} + 4\phi e^{-2\mathbf{u}}\mathbf{u}/\psi^{3}$$
(58)

and

$$\left(\frac{C_p^o}{R}\right)_i = 1 + u^2 e^{-u} / \psi^2 + 4\rho / \sigma + \sigma^2 / 45 + \delta e^{-u} u^2 (1 + e^{-u}) / \psi^3 
- 8xu^2 e^{-2u} / \psi^3 + 4xu^3 e^{-2u} (2 + e^{-u}) / \psi^4 
+ 36yu^2 e^{-3u} / \psi^4 - 18yu^3 (3 + e^{-u}) e^{-3u} / \psi^5$$

$$+ 4x^{2}u^{2}e^{-2u}(1 + 4e^{-u})/\psi^{4} - 8x\delta u^{2}e^{-2u}(2 + e^{-u})/\psi^{4}$$

$$- 16x^{2}u^{3}e^{-2u}(1 + 7e^{-u} + 2e^{-2u})/\psi^{5}$$

$$+ \delta^{2}u^{2}e^{-u}(1 + 4e^{-u} + e^{-2u})/2\psi^{4}$$

$$+ 8x^{2}u^{4}e^{-2u}(1 + 12e^{-u} + 11e^{-2u} + e^{-3u})/\psi^{6}$$

$$+ 4\phi u^{2}e^{-2u}(2 + e^{-u})/\psi^{4} + 4x\delta u^{3}e^{-2u}(4 + 7e^{-u} + e^{-2u})/\psi^{5} , \qquad (59)$$

where

$$\psi = (1 - e^{-u}) . ag{60}$$

The total internal energy,  $\epsilon_n$  , of the  $n^{th}$  electronic state is

$$\epsilon_{\mathbf{n}} = \mathbf{E}_{\mathbf{e}}' + \omega \mathbf{v} - \omega \mathbf{x} \mathbf{v} (\mathbf{v} - 1) + \dots, \tag{61}$$

where  $E_e'$  is the electronic energy of the state expressed in wave numbers. Since, for a given electronic state, the energy of the lowest level (v = 0, j = 0) is taken as the reference point of the energy scale,  $E_e'$  becomes  $T_e$  (the electronic energy as defined by Herzberg<sup>54</sup>) less the difference between the zero point energies of the  $n^{th}$  state and the ground state; i.e.,

$$E'_{e} = T_{e} - \left[ (1/2)\omega_{e} - (1/4)\omega_{e}x_{e} + (1/8)\omega_{e}y_{e} + \dots \right] + \left[ (1/2)\omega'_{e} - (1/4)\omega_{e}x'_{e} + (1/8)\omega_{e}y'_{e} + \dots \right],$$
(62)

where the unprimed terms are for the ground state, and the primed terms are for the upper state.

The total internal partition function for all electronic states is given by

$$Q = \sum_{n} g_{n}(2j+1) e^{-hc} \epsilon_{n}/kT - \sum_{n} g_{n} e^{-E} e^{/kT} \left\{ \sum_{\mathbf{v},j} (2j+1) \exp[-u\mathbf{v} + u\mathbf{x}\mathbf{v}(\mathbf{v} - 1) + ...] \right\}$$

$$= \sum_{n} g_{n} e^{-E} e^{/kT} Q_{n} - \sum_{n} \frac{g_{n} e^{-E} e^{/kT}}{\sigma \psi}, \qquad (63)$$

<sup>54</sup> Herzberg, G., Molecular Spectra and Molecular Structure, I. Spectra of Diatomic Molecules, Van Nostrand, N.Y. (1950).

where  $g_n$  is the multiplicity of the  $n^{th}$  electronic state,  $E_e$  is  $hcE_e'$ ,  $Q_n$  and  $(Q_c)_n$  are Q(v,j) and  $Q_c$ , respectively, from equation (54).

The temperature derivatives of Q are therefore

$$\frac{dQ}{dT} = \sum_{n} g_{n} Q_{n} e^{-E_{e}/kT} (E_{e}/kT^{2}) + \sum_{n} g_{n} e^{-E_{e}/kT} (dQ_{n}/dT) , \qquad (64)$$

$$\frac{d^2Q}{dT^2} = \sum_{n} g_n e^{-E_e/kT} (d^2Q_n/dT^2) + 2 \sum_{n} g_n e^{-E_e/kT} (dQ_n/dT) (E_e/kT^2)$$

$$+ \sum_{n} g_{n} e^{-E_{e}/kT} Q_{n} (E_{e}/kT^{2})^{2} - 2 \sum_{n} g_{n} e^{-E_{e}/kT} Q_{n} (E_{e}/kT^{3}) .$$
 (65)

Values for  $Q_n$  and its derivatives are obtained from equations (66), (67), and (68).

$$Q_{n} = \frac{e^{\ln(Q_{c})_{n}}}{\sigma \psi} , \qquad (66)$$

$$dQ_{\mathbf{n}}/dT = \frac{Q_{\mathbf{n}}}{T} \left( \frac{H_{\mathbf{T}}^{\circ} - H_{\mathbf{O}}^{\circ}}{RT} \right)_{\mathbf{i}, \mathbf{n}} , \qquad (67)$$

and

$$d^{2}Q_{n}/dT^{2} = \frac{Q_{n}}{T^{2}} \left(\frac{C_{p}^{\circ}}{R}\right)_{i,n} + \frac{Q_{n}}{T^{2}} \left(\frac{H_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{i,n}^{2} - \frac{2}{T} (dQ_{n}/dT), \qquad (68)$$

where

$$\ln(Q_c)_n = \sigma/3 + \sigma^2/90 + 2\rho/\sigma + \delta e^{-u}/\psi + \dots$$
 (69)

From the above expressions, the contribution of the internal energies of all electronic states to the thermodynamic functions (designated by the subscript  $\Sigma i$ ) may be derived.

$$-\left(\frac{F_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{\Sigma_{i}} = \ln Q , \qquad (70)$$

$$\left(\frac{H_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{\Sigma_{i}} = (T/Q)(dQ/dT),$$
(71)

$$\left(\frac{C_{p}^{\circ}}{R}\right)_{\Sigma i} = (2T/Q)(dQ/dT) - (T/Q)^{2}(dQ/dT)^{2} + (T^{2}/Q)(d^{2}Q/dT^{2})$$

$$= 2 \left( \frac{H_T^{\circ} - H_O^{\circ}}{RT} \right)_{\Sigma_i} - \left( \frac{H_T^{\circ} - H_O^{\circ}}{RT} \right)_{\Sigma_i}^2 + (T^2/Q)(d^2Q/dT^2), \qquad (72)$$

and

$$\left(\frac{S_{T}^{\circ}}{R}\right)_{\Sigma_{i}} = \left(\frac{H_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{\Sigma_{i}} - \left(\frac{F_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{\Sigma_{i}}$$
(73)

After addition of the contribution of translational degrees of freedom, changing of the reference temperature from 0° to 298.15°K, and substitution of the values of the fundamental constants adopted here, the total thermodynamic functions (in units of cal, °K, and moles) become

$$C_p^o = 1.98726 \left(\frac{C_p^o}{R}\right)_{\Sigma_i} + 4.96815$$
, (74)

$$S_T^{\circ} = 1.98726 \left( \frac{S_T^{\circ}}{R} \right)_{\Sigma_i} + 6.863753 \log M + 11.439588 \log T$$

$$-4.575835\log\theta - 2.31538$$
, (75)

$$-\left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right) = -1.98726 \left(\frac{F_{T}^{\circ} - H_{0}^{\circ}}{RT}\right)_{\Sigma_{i}} + \frac{\left(H_{298}^{\circ} - H_{0}^{\circ}\right)_{\Sigma_{i}}}{T}$$

+ 6.863753log M + 11.439588log T

$$-4.575835\log\theta + \frac{1481.2539}{T} - 7.28353, \qquad (76)$$

$$(H_{T}^{\circ} - H_{298}^{\circ}) = 1.98726T \left(\frac{H_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{\Sigma i} - \left(H_{298}^{\circ} - H_{O}^{\circ}\right)_{\Sigma i} + 4.96815 \left(T - 298.15\right),$$

$$(77)$$

and

$$(H_{298}^{\circ} - H_{O}^{\circ}) = 592.5016 \left(\frac{H_{T}^{\circ} - H_{O}^{\circ}}{RT}\right)_{\Sigma i, 298} + 1481.25392,$$
 (78)

where  $\underline{M}$  is the molecular weight of the diatomic gas, and  $\theta$  is the symmetry number of the molecule (1 for a heteronuclear and 2 for a homonuclear diatomic molecule).

The program for machine computation of the thermodynamic functions of diatomic gases was based on the above formulas. Calculations for the natural isotopic mixture of molecular oxygen are in excellent agreement with those of Woolley when the spectroscopic constants he selected are used for the  $^3\Sigma_g^-$ ,  $^1\Delta_g$ ,  $^1\Sigma_g^+$ ,  $^3\Sigma_u^+$ , and  $^3\Sigma_u^-$  states. The results after minor adjustments are compared in Table IV.

Woolley's values were corrected for a change in the gas constant  $\underline{R}$  and the Sackur-Tetrode constant and converted to a reference temperature of 298.15°K. Woolley used a different summation procedure and included some higher-order spectroscopic constants for the ground state which the present calculation does not include. He also broke off rotational sums at the dissociation limit, whereas they are extended here to infinite energy. The additional contribution to the enthalpy would be about 15 cal/gfw at  $5000^{\rm O}{\rm K}$  and negligible at  $4000^{\rm O}{\rm K}$  had he extended his rotational summation to infinite energy.

<sup>&</sup>lt;sup>55</sup>Woolley, H.W., J. Research Nat. Bur. Stds. <u>40</u>, 163 (1948); Nat. Bur. Stds. (U.S.) Circ. 564 (1955).

 $\underline{\text{TABLE IV}}$  COMPARISON OF THERMODYNAMIC FUNCTIONS OF MOLECULAR OXYGEN

Temp	S <sub>T</sub> cal/ <sup>O</sup> K gfw		-	- H <sub>298</sub> )/T <sup>/</sup> °K gfw	(H <sup>o</sup> T - H <sup>o</sup> 298) Kcal/gfw		
*K	Woolley <sup>55</sup>	Present Work	Woolley <sup>55</sup>	Present Work	Woolley <sup>55</sup>	Present Work	
300	49. 055	49. 058	49.012	49.015	0.013	0.013	
1000	58. 199	58. 200	52. 773	52.774	5. 427	5. 427	
2000	64. 218	64. 218	57.144	57.145	14.148	14.147	
3000	67. 980	67. 980	60.165	60. 166	23. 447	23. 441	
4000	70 785	70.782	62.484	62.485	33.202	33.188	
5000	73.028	73.028	64. 376	64. 379	43. 259	43. 249	

#### F. POLYATOMIC MOLECULE CALCULATIONS

The program for the calculation of thermodynamic functions for ideal gases of polyatomic molecules was based upon the standard relations of molecular dynamics employed by spectroscopists.

One of these basic relations is that the total energy of an ideal polyatomic molecule is the sum of its translational and internal energies.

$$\epsilon = \epsilon_t + \epsilon_{\text{int}} . \tag{79}$$

The internal energy is composed of electronic, vibrational, rotational, and interaction or coupling contributions. The interaction terms are rarely, if ever, accurately known and are usually ignored. The internal energy was therefore considered to be the sum of the electronic, vibrational, and rotational contributions.

$$\epsilon_{\rm int} = \epsilon_{\rm f} + \epsilon_{\rm v} + \epsilon_{\rm el}$$
 (80)

The partition function (Q) can then be written as the product of the individual partition functions

$$Q = Q_r Q_r Q_q Q_{el} , \qquad (81)$$

and the thermodynamic functions can be separated into sums of translational, rotational, vibrational, and electronic contributions.

$$C_{p}^{\circ} = C_{p(t)}^{\sigma} + C_{p(r)}^{\circ} + C_{p(v)}^{\circ} + C_{p(el)}^{\circ}$$
, (82)

$$H_{T}^{\circ} - H_{O}^{\bullet} = \left(H_{T}^{\circ} - H_{O}^{\bullet}\right)_{t} + \left(H_{T}^{\bullet} - H_{O}^{\bullet}\right)_{t} + \left(H_{T}^{\bullet} - H_{O}^{\circ}\right)_{v} + \left(H_{T}^{\bullet} - H_{O}^{\circ}\right)_{e1}, \tag{82A}$$

$$-\left(\frac{F_{T}^{o}-H_{O}^{o}}{T}\right) = -\left(\frac{F_{T}^{o}-H_{O}^{o}}{T}\right)_{t} - \left(\frac{F_{T}^{o}-H_{O}^{o}}{T}\right)_{t} - \left(\frac{F_{T}^{o}-H_{O}^{o}}{T}\right)_{v} - \left(\frac{F_{T}^{o}-H_{O}^{o}}{T}\right)_{v} - \left(\frac{F_{T}^{o}-H_{O}^{o}}{T}\right)_{el}, \quad (82B)$$

and

$$S_{T}^{0} = S_{1}^{0} + S_{2}^{0} + S_{2}^{0} + S_{3}^{0}$$
 (82C)

Evaluation of the Q's in the usual manner, <sup>50</sup> combination of the translational and rotational contributions, and substitution of required physical constants <sup>1</sup> then leads to the following equations which were employed in the computer program:

#### 1. Linear Polyatomic Molecules

a. Heat Capacity in cal/°K mole

$$C_{\mathbf{p}}^{\bullet} = C_{\mathbf{p}(\mathbf{t},\mathbf{r})}^{\circ} + C_{\mathbf{p}(\mathbf{v})}^{\circ} + C_{\mathbf{p}(\mathbf{el})}^{\circ} , \qquad (83)$$

$$C_{p(t,t)}^{\circ} = 6.95541 + 0.091420 \left(\frac{E}{T}\right)^2$$
, (84)

$$B = 2.79889 \times 10^{-39}/I$$
 , (85)

$$C_{p(v)}^{\circ} = \sum_{i} \frac{1.98726 \left(\frac{1.43880 \omega_{i}}{T}\right)^{2} \left(e^{-\frac{1.43880 \omega_{i}}{T}}\right)}{\left(-\frac{1.43880 \omega_{i}}{T}\right)^{2}},$$
(86)

$$C_{p(el)}^{o} = \frac{4.113917}{T^2} \left[ \frac{Q_2}{Q} - \left( \frac{Q_1}{Q} \right)^2 \right],$$
 (87)

$$Q = \sum_{i} g_{i} e^{-\frac{1.43880 \epsilon_{i}}{T}}, \qquad (88)$$

$$Q_{1} - \sum_{i} \epsilon_{i} s_{i} e^{-\frac{1.43880 \epsilon_{i}}{T}}, \qquad (89)$$

$$Q_{2} = \sum_{i=1}^{\infty} \epsilon_{i}^{2} g_{i} = \frac{1.43880 \epsilon_{i}}{T}$$
(90)

 $\omega_i$  is a fundamental frequency in units of cm<sup>-1</sup>, I is the principal moment of inertia,  $\epsilon_i$  is an electronic energy level in units of cm<sup>-1</sup>, and  $g_i$  is the degeneracy of the corresponding electronic energy level.

b. Enthalpy in cal/mole

$$H_{T}^{\circ} - H_{298}^{\circ} = \left(H_{T}^{\circ} - H_{O}^{\circ}\right)_{t,r} + \left(H_{T}^{\circ} - H_{O}^{\circ}\right)_{v} + \left(H_{T}^{\circ} - H_{O}^{\circ}\right)_{el} - \left(H_{298}^{\circ} - H_{O}^{\circ}\right)_{t,r,v,el} , \qquad (91)$$

$$\left(H_{T}^{\circ} - H_{O}^{\circ}\right)_{t, f} = T \left[6.95541 - 0.953090 \left(\frac{B}{T}\right) - 0.091420 \left(\frac{B}{T}\right)^{2}\right]$$
, (92)

$$\left(H_{T}^{\circ} - H_{O}^{\circ}\right)_{V} = \sum_{i} \frac{1.98726T \left(\frac{1.43880\omega_{i}}{T}\right) \left(e^{-\frac{1.43880\omega_{i}}{T}}\right)}{-\frac{1.43880\omega_{i}}{T}}, \qquad (93)$$

$$\left(H_{T}^{\sigma} - H_{O}^{\sigma}\right)_{el} = 2.859270 \left[\frac{Q_{1}}{Q}\right] ,$$
 (94)

$$\left(H_{298}^{\circ} - H_{0}^{\circ}\right)_{t,r,v,el} = 298.15 \left[6.95541 - 0.953090 \left(\frac{B}{298.15}\right) - 0.091420 \left(\frac{B}{298.15}\right)^{2}\right]$$

$$+ \left[ \sum_{i} 1.98726(298.15) \frac{\left(\frac{1.43880\omega_{i}}{298.15}\right) \left(-\frac{1.43880\omega_{i}}{298.15}\right)}{\left(-\frac{1.43880\omega_{i}}{298.15}\right)} \right]$$

$$+ \left[ \frac{\sum_{i} \epsilon_{i} \mathbf{g}_{i} e^{-\frac{1.43880 \epsilon_{i}}{298.15}}}{\sum_{i} \mathbf{g}_{i} e^{-\frac{1.43880 \epsilon_{i}}{298.15}}} \right]$$

$$(95)$$

c. Free-Energy Function in cal/ K mole

$$-\left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right) = -\left(\frac{F_{T}^{\circ} - H_{0}^{\circ}}{T}\right)_{t, \, t} - \left(\frac{F_{T}^{\circ} - H_{0}^{\circ}}{T}\right)_{v}$$

$$-\left(\frac{F_{T}^{\circ} - H_{0}^{\circ}}{T}\right)_{el} + \left(\frac{H_{298}^{\circ} - H_{0}^{\circ}}{T}\right)_{t, \, t, \, v, \, el}$$

$$-\left(\frac{F_{T}^{\circ} - H_{0}^{\circ}}{T}\right)_{t, \, t} = 6.863753 \log M + 11.439588 \log T$$
(96)

$$-4.575835 \log \left(\frac{B\theta}{T}\right) + 0.953090 \left(\frac{B}{T}\right) + 0.045710 \left(\frac{B}{T}\right)^2 - 8.00651 , \qquad (97)$$

$$-\left(\frac{F_{T}^{\circ} - H_{0}^{\circ}}{T}\right)_{v} = -\sum_{i} 4.575835 \log \left(\frac{-\frac{1.43880\omega_{i}}{T}}{1 - e}\right) , \qquad (98)$$

$$-\left(\frac{F_{T}^{\circ} - H_{O}^{\circ}}{T}\right)_{el} - 4.575835 \log \sum_{i} g_{i} e^{-\frac{1.43880\epsilon_{i}}{T}}$$
 (99)

B,  $\omega_i$  and  $\epsilon_i$  were defined earlier. M is the molecular weight, and  $\theta$  is the symmetry number.

d. Entropy in cal/\* K mole

$$S_{T}^{\circ} = \left(\frac{H_{T}^{\circ} - H_{298}^{\circ}}{T}\right) - \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right) . \tag{100}$$

## 2. Nonlinear Polyatomic Molecules

a. Heat Capacity in cal/\* K mole

Equations (83), (86), and (87) through (90) were used with

$$C_{p(t,r)}^{\circ} = 7.949040$$
 (101)

b. Enthalpy in cal/mole

$$\begin{split} H_{T}^{\circ} - H_{298}^{\circ} &= \left( H_{T}^{\circ} - H_{O}^{\circ} \right)_{t, \, r} + \left( H_{T}^{\circ} - H_{G}^{\circ} \right)_{v} \\ &+ \left( H_{T}^{\circ} - H_{O}^{\circ} \right)_{ei} - \left( H_{298}^{\circ} - H_{O}^{\circ} \right)_{t, \, r, \, v, \, el} \end{split} , \tag{102}$$

$$\left(H_{T}^{o} - H_{O}^{o}\right)_{t,r} = 7.949040 \text{ T},$$
 (103)

$$\left(H_{298}^{\circ} - H_{0}^{\circ}\right)_{t, \, r, \, v, \, el} = \left[7.949640(298.15)\right]$$

$$+ \left[ \sum_{i} \frac{1.98726(298.15) \left( \frac{1.43880 \omega_{i}}{298.15} \right) \left( e^{-\frac{1.43880 \omega_{i}}{298.15}} \right)}{-\frac{1.43880 \omega_{i}}{298.15}} \right]$$

$$+ \left[ \sum_{i} \frac{\sum_{i} \epsilon_{i} g_{i} e^{-\frac{1.43880 \epsilon_{i}}{298.15}}}{\sum_{i} g_{i} e^{-\frac{1.43880 \epsilon_{i}}{298.15}}} \right]$$
 (104)

 $(H_T^\circ - H_0^\circ)_v$  and  $(H_T^\circ - H_0^\circ)_{el}$  are given by equations (93) and (94). All other parameters are as previously defined.

c. Free-Energy Function in cal/°K mole

$$-\left(\frac{F_{T}^{\circ} - H_{298}^{\sigma}}{T}\right) = -\left(\frac{F_{T}^{\circ} - H_{Q}^{\circ}}{T}\right)_{t, r} - \left(\frac{F_{T}^{\circ} - H_{Q}^{\circ}}{T}\right)_{v}$$

$$-\left(\frac{F_{T}^{\circ} - H_{Q}^{\circ}}{T}\right)_{el} + \left(\frac{H_{298}^{\circ} - H_{Q}^{\circ}}{T}\right)_{t, r, v, el}$$
(105)

$$-\left(\frac{F_{T}^{\circ} - H_{O}^{\circ}}{T}\right)_{t, r} = 6.863753 \log M + 18.303341 \log T$$

$$-4.575835 \log \theta + 2.287918 \log I_{A}I_{B}I_{C} \times 10^{120}$$

$$-17.16242. \tag{106}$$

$$-\left(\frac{F_{T}^{\circ}-H_{O}^{\circ}}{T}\right)_{v}^{\circ} \text{ and } -\left(\frac{F_{T}^{\circ}-H_{O}^{\circ}}{T}\right)_{el}^{\circ} \quad \text{are given by equations (98) and (99).}$$

 $I_A I_B I_C$  is the product of the three principal moments of inertia. All other parameters are as previously defined.

d. Entropy in cal/ K mol (given by Eq. 100).

#### G. CONDENSED-PHASE CALCULATIONS

Solid and liquid-phase thermodynamic functions are calculated in essentially the same way. Calculations for both phases can therefore be discussed together.

#### 1. Solid Phases

#### a. Basic Equations

In a reference state table, only  $C_p^{\circ}$ ,  $S_T^{\circ}$ ,  $-\left(\frac{F_T^{\circ} - H_{298}^{\circ}}{T}\right)$ , and  $(H_T^{\circ} - H_{298}^{\circ})$ 

are included. For the solid phase, the last three functions can be calculated if  $C^{\circ}$  and solid-state transition data are available. The formulas for a psolid with n first order transitions below the temperature T and above the reference temperature are

$$S_{T}^{\circ} = \int_{0}^{T_{1}} \left(\frac{C_{p}^{\circ}}{T}\right) dT + \sum_{i=1}^{n} \lambda_{i} / T_{i} + \sum_{i=2}^{n} \int_{T_{i-1}}^{T_{i}} \left(\frac{C_{p}^{\circ}}{T}\right) dT + \int_{T_{n}}^{T} \left(\frac{C_{p}^{\circ}}{T}\right) dT$$
(107)

$$-\left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right) = S_{T}^{\circ} - \left(\frac{H_{T}^{\circ} - H_{298}^{\circ}}{T}\right) , \qquad (108)$$

$$H_{T}^{\circ} - H_{298}^{\circ} = \int_{298.15}^{T_{1}} C_{p}^{\circ} dT + \sum_{i=1}^{n} \lambda_{i} + \sum_{i=2}^{n} \int_{T_{i-1}}^{T_{i}} C_{p}^{\circ} dT$$

$$+ \int_{T_{a}}^{T} C_{p}^{o} dT, \qquad (109)$$

$$H_T^{\circ} - H_{298}^{\circ} = (H_T^{\circ} - H_0^{\circ}) - (H_{298}^{\circ} - H_0^{\circ}),$$
 (110)

where  $\lambda_i$  is the heat of the i<sup>th</sup> transition at  $T_i$ . The solid-liquid transition can be included as the n<sup>th</sup> one in which case, the  $C_p^o$  of the liquid is used in the last term of eqs. (107) and (109).

# b. Method of Choosing Basic Data

Since experimental  $C_p^\circ$  data are often reported directly in the literature and since empirical equations are often presented for the temperature dependence of this quantity, there appear to be several advantages for conducting calculations with this quantity, rather than doing so with other quantities such as  $(H_T^\circ - H_{298}^\circ)$ . Therefore, in the work of this project, first priority was given to locating  $C_p^\circ$  data for each solid as it came under consideration. The second step was to plot graphs and compare the data from various sources. After a choice of the "best" data was made, several alternatives presented themselves for proceeding with the calculations, depending upon the state of the available  $C_p^\circ$  data.

- 1) The "best" data for  $C_p^o$  and the other functions may already have been tabulated at the desired temperatures throughout the entire temperature range of the tables.
- 2) Data may have been tabulated only for portions of the desired temperature range.
- 3) The  $C_p^o$  data may have been in the form of data points given at various temperature intervals.
- 4) The C<sup>o</sup><sub>p</sub> data may have been presented in the form of an analytical expression. A variety of possible analytical expressions have been used. These include Debye or Einstein functions, polynominals, etc.

# c. Machine Computation

The computer program used on this project for condensed phases was designed to accept numerical values of  $C_p^{\circ}$  at the  $100^{\circ}$ K intervals required in the final tables and carry out a numerical integration of these input data to give the other thermodynamic quantities. This eliminated the need for first reducing the original data to an analytical expression.

#### d. Uncertainty Analysis

The standard procedure adopted in the computation of error estimates has been to assign uncertainties to the primary  $C_p^{\circ}$  and heat-of-transition data and to calculate the uncertainties in the derived functions  $S_T^{\circ}$ ,

$$-\left(\frac{F_T^{\circ}-H_{298}^{\circ}}{T}\right)$$
, and  $(H_T^{\circ}-H_{298}^{\bullet})$  from them. An assigned uncertainty could

be made at each of the tabular temperatures. Since highly precise calculations were not expected in these cases, an average value for the uncertainty in a given temperature interval was used.

#### 1) Heat capacity

Heat capacities are usually obtained experimentally, and the original experimenter is the one best able to set the uncertainty limits. However, this is often neglected and must be done instead by the reviewer. If data from several sources are available, the spread in the data can give some indication of their reliability. Questions of purity of samples, the method of, and the care taken in the measurements, etc., should all be considered.

# 2) Entropy

The range of heat capacity values is defined as

$$C_{\mathbf{p}}^{\circ} = C_{\mathbf{p}o}^{\circ} + \delta_{C_{\mathbf{p}}^{\circ}} , \qquad (111)$$

where

$$\delta C_{\mathbf{p}}^{\circ} = (C_{\mathbf{p}U}^{\circ} - C_{\mathbf{p}L}^{\circ})/2 \quad , \tag{112}$$

Copo = best value for heat capacity available,

 $C_{pU}^{\circ}$  = upper limit of uncertainty range,

and

C<sub>pL</sub> = lower limit of uncertainty range.

The true value  $C_{pt}^{\circ}$  is expected to lie somewhere between the limits given by equation (111).

From the thermodynamic definition of entropy, one can write

$$S_T^{\circ} = S_{298,o}^{\circ} \pm s_{298} + \int_{298}^{T} \frac{C_{po}^{\circ}}{T} dT \pm \int_{298}^{T} (\delta C_p^{\circ}/T) dT$$
, (113)

where

 $S_{298,0}^{\circ}$  = the best available value of  $S_{298}^{\circ}$ , and

 $\bullet_{298}$  = the uncertainty in  $\circ_{298}$ .

The uncertainty in  $S_{T}^{\circ}$  is therefore,

$$s_T = s_{298} + \int_{298}^T (\delta C_p^o/T) dT.$$
 (114)

Or assuming that  $\delta C_p^o \neq f(T)$ ,

$$s_T = s_{298} + \delta C_p^o \ln (T/298.15)$$
 (115)

is obtained.

# 3) Enthalpy

Since

$$H_T^{\circ} - H_{298}^{\circ} = \int_{298}^{T} C_p^{\circ} dT,$$
 (116)

one obtains, for an actual point with its associated uncertainties,

$$H_{T}^{\circ} - H_{298}^{\circ} + \delta(H_{T}^{\circ} - H_{298}^{\circ}) = \int_{-298.15}^{T} C_{po}^{\circ} dT + \int_{-298.15}^{T} \delta C_{p}^{\circ} dT$$
 (117)

from equation (111). The uncertainty in  $H_{T}^{o} - H_{298}^{o}$  is therefore,

$$h_{T} = \int_{298.15}^{T} \delta C_{p}^{o} dT = \delta (H_{T}^{o} - H_{298}^{o})$$
 (118)

# 4) Free energy Function

The uncertainty in the free-energy function defined as

$$f_{T} = \delta \left( \frac{F_{T}^{\circ} - H_{298}^{\circ}}{T} \right) \tag{119}$$

can be obtained from those of the entropy and enthalpy functions just discussed because of equation (100). Due to this equation, one can simply write the uncertainty in the free-energy function as

$$f_{\rm T} = s_{\rm T} - h_{\rm T}/T$$
 (120)

This is contrary to the usual practice in summing errors because in this particular case, the uncertainties  $\mathfrak{s}_T$  and  $\mathfrak{h}_T$  are due to a common uncertainty in C° and are matched. The independent error in  $\$^\circ_{298}$  is simply added on.

From equations (114) and (118), it can be seen that  $s_T > h_T/T$ .

# 2. Liquid Phases

The calculation of thermodynamic functions for liquid phases was done in essentially the same manner as described above for solid phases. Primary heat capacity data were scantier and less precise for liquid phases and more ingenuity in making estimates was required.

# H. EVALUATION OF STANDARD HEAT OF FORMATION OF ELEMENTS AT 298.15° κ[Δ H<sub>f298</sub>]

Heats of vaporization or sublimation may be derived from vapor pressure measurements in two different ways.

The first technique, based on the Clausius-Clapeyron equation, is called the "Second Law Method." When applied to the vaporization of an element it will give a single value of  $\Delta H_{298}^{\circ}$  equal to  $\Delta H_{v298}^{\circ}$  or  $\Delta H_{s298}^{\circ}$  from each set of vapor pressure measurements.

If it is assumed that the vapor of the element is ideal, the Clausius-Clapeyron equation may be written as a form of Van't Hoff's equation,

$$\frac{d(-R \ln K_p)}{dT} = -\frac{\Delta H_f^{\circ}}{T^2} \qquad (121)$$

where  $K_p$  is the equilibrium constant for the vaporization process. For the special case of liquid or solid vaporization without polymerization,  $K_p$  equals the vapor pressure.

The heat of formation,  $\Delta H_f^o$ , may be obtained as a function of the temperature from the equation

$$\Delta H_{f}^{\circ} = \Delta H_{f298}^{\circ} + \int_{298}^{T} \Delta C_{p}^{\circ} dT$$
, (122)

where  $\Delta C_p^o$  is the difference between the heat capacity of the gas and that of the condensed phase. The exact analytical expression used for  $\Delta C_p^o$  will depend on the precision of available heat capacity data and on the form of the functions used to express the temperature dependence of the heat capacities of both phases concerned. If the form of the expression for  $\Delta C_p^o$  is that favored by Kelley<sup>56</sup> for the heat capacity of solids; namely,

$$\Delta C_{D}^{\bullet} = \Delta A + \Delta B T - \Delta C T^{-2}$$
 (123)

where the coefficients are related to those of the enthalpy expression by  $\Delta A = \Delta a$   $\Delta B = 2\Delta b$  and  $\Delta C = \Delta c$ , equation (122) then becomes

$$\Delta H_{f}^{\circ} = (\Delta H_{f298}^{\circ} + \Delta \Lambda (T - 298.15) + \frac{\Delta B}{2} [T^{2} - (298.15)^{2}] + \Delta C (1/T - 1/298.15). \tag{124}$$

<sup>&</sup>lt;sup>56</sup>Kelley, K. K., Bureau of Mines Bull. 584 (1960).

If equation (124) is substituted into equation (121), the result may be integrated and re-arranged to give

$$- R \ln K + \Delta A \ln T + \frac{\Delta BT}{2} - \frac{\Delta CT^{-2}}{2} + \Delta DT^{-1} = \frac{\Delta H^{\circ}_{f298}}{T} + I , \qquad (125)$$

where

$$\Delta D = 298.15 \Delta A + \frac{(298.15)^2 \Delta B}{2} + \frac{\Delta C}{298.15}$$
, (126)

and I is an integration constant. If terms on the left-hand side of equation (125) are designated by  $\Sigma$ , the equation becomes

$$\sum = \frac{\Delta H_{f298}^{\circ}}{T} + I . \tag{127}$$

Therefore, one may calculate  $\Delta H^{\circ}_{f298}$ , by the Second Law Method, by computing  $\Sigma$  for each experimental vapor pressure measurement, and plotting it against the reciprocal of the temperature. The resulting plot should be a straight line, and the slope of that line is the value of  $\Delta H^{\circ}_{f298}$ . The constant of integration, I , is related to the entropy of formation at 298.15° K by the equation

$$\Delta S_{f298}^{\circ} = \Delta A + \Delta A \ln(298.15) + \Delta B (298.15) + \frac{\Delta C (298.15)^{-2}}{2} - I$$
 (128)

When free-energy functions are available for the condensed and gas phases, these functions may be used in combination with experimental vapor pressure data to calculate a value of  $\Delta H_{298}^{o}$  for each vapor pressure measurement. This technique is known as the "Third Law Method." Thus, the difference between the free-energy functions of the gas and condensed phases,  $\Delta$  (f.e.f.) is

$$\Delta(f.e.f.) = \left[\frac{F_{T}^{o} - H_{298}^{o}}{T}\right]_{g} - \left[\frac{F_{T}^{o} - H_{298}^{o}}{T}\right]_{c} - \frac{\Delta F_{f}^{o}}{T} - \frac{\Delta H_{f298}^{o}}{T}.$$
 (129)

However,

$$\frac{\Delta F_{i}^{2}}{T} = -R \ln K_{p}. \tag{130}$$

Therefore,

$$\Delta H_{f298}^{o} = T \left[ -R \ln K_p - \Delta(f.e.f.) \right]$$
 (131)

Ideally, the two methods should give the same results. In practice, they seldom do because of errors in the experimental results or approximations made in analytical expressions for the temperature dependence of heat capacities in the Second Law treatment. The Third Law treatment is to be preferred for the present work, and was the one adopted. Because the latter method permits a calculation of AH? corresponding to each vapor pressure measurement, a sensitive check for a possible drift with temperature is available. Calculations are possible for situations in which the temperature dependence of heat capacities may not have been reduced to an analytical expression. Most important however, the thermodynamic compilations are thereby made internally consistent. In this way, experimental vapor pressures are more closely reproduced from the compilations than they would be if the Second Law treatment were used. In that sense, the values of  $\Delta H_{f298}^{\circ}$  listed will be legitimately used only with the free-energy functions for gas and condensed phases with which they are tabulated.

The two techniques just described have general applicability to the vaporization of systems other than those of the elements. When applied to the vaporization of compounds, however, they simply yield heats of the vaporization or decomposition process which yields the vapor species.

# IV. REVIEWS OF DATA AND COMPUTATION SUMMARIES FOR INDIVIDUAL ELEMENTS AND COMPOUNDS

With the exception of Th and Ce for which there were insufficient data, ideal monatomic gas tables were prepared for all the elements within the scope of the contract plus several other metals which were included at the request of Materials Central, WADD. Emphasis was placed initially on the preparation of tables for the elements because they were needed for the preparation of tables on compounds. In some cases, it was only necessary to add uncertainty estimates to existing tables for the elements. A number of existing tables were re-computed because better energy level data had become available. Oxide compounds were also given high priority in the work because more data were available on them than on the other classes of compounds such as the carbides, borides, and nitrides.

#### A. ELEMENTS

#### 1. Beryllium

#### a. Crystal Structure and Melting Point

At room temperature, elemental beryllium has a hexagonal, close-packed structure. <sup>57</sup> The possible allotropy of beryllium has been a subject of dispute for over thirty years. In general, two allotropic transformations have been discussed; one occurring in the temperature range from 400° to 800°C, and the other around 20° to 30°C below the melting point. Most of the evidence in support of allotropy in the lower-temperature range can probably be discounted as originating from impure beryllium. The most likely impurity, BeO, will not be revealed by the usual spectroscopic analysis.

Lewis  $^{58}$  inferred the existence of allotropic transformations at -45 and  $450^{\circ}$ C by thermal emf and electrical resistivity measurements. Jaeger and Rosenbohm found evidence for a second beryllium phase from specific heat measurements. From X-ray measurements, Jaeger and Zanstra proposed that,  $\beta$ -Be is hexagonal close-packed with a relatively large unit cell and is metastable at room temperature. They also reported that the high-temperature phase was most successfully produced by heating to  $630^{\circ}$ C. Kosolapov and Trapoznikov  $^{61}$  obtained

<sup>57</sup> Pearson, W.B., Handbook of Lattice Spacings and Structures of Metals, Pergamon Press, N.Y. (1958).

<sup>&</sup>lt;sup>58</sup>Lewis, E.J., Phys. Rev. 34, 1575 (1929).

<sup>&</sup>lt;sup>59</sup> Jaeger, F.M. and E. Rosenbohm, Proc. Acad. Sci. (Amsterdam) 35, 1055 (1932); Proc. Acad. Sci. (Amsterdam) 37, 67 (1934); Rec. trav. chim. 53, 451 (1934).

<sup>60</sup> Jaeger, F.M. and J.E. Zanstra, Proc. Acad. Sci. (Amsterdam) 36, 636 (1933).

<sup>61</sup> Kosolapov, G.F. and A.K. Trapoznikov, J. Exper. Theor. Phys. (U.S.S.R.) 6, 1136 (1936).

evidence for allotropy from extra reflections in X-ray measurements on beryllium samples. Noyce and Daane<sup>62</sup> reported an allotropic transformation at 730°C from thermal and dilatometric effects. However, Gordon and Kaufmann<sup>63</sup> were unable to confirm the latter results. Gordon<sup>64</sup> measured the thermal coefficients of expansion of beryllium up to 1000°C by X-ray methods, and found no evidence for allotropy. However, Chatterjee and Sidhu<sup>65</sup> reported allotropy by X-ray measurements on 99.9 percent pure beryllium. Sidhu and Henry<sup>66</sup> examined spectroscopically pure beryllium and very dilute gold-beryllium alloys, and from the position and intensity variations of extra lines, concluded that a  $\beta$  -Be phase was present which had a complex hexagonal structure. Seybolt et al 67 criticized these conclusions and stated that the extra reflections were probably due to BeO or AuBes. Kaufmann et al<sup>68</sup> found no evidence for allotropy by thermal analysis studies and microstructure examination of beryllium that had been cooled down from temperatures up to the melting point. The last investigators further stated that the fact that single crystals of beryllium could be successfully grown from the melt was evidence for the nonexistence of the disputed phase.

In addition to the questionable allotropic transformation below 1000°C, a double thermal arrest has been reported in the temperature range from 1250° to 1260°C (20 or 30 degrees below the melting point). 69-72 This observation has been variously interpreted as due to an allotropic transformation or the presence of a eutectic with a contaminant. Losano <sup>73</sup> reported finding only a single thermal arrest in 99.96 percent pure beryllium. However, Martin and Moore <sup>74</sup> later found no evidence, with thermal analysis techniques, for the existence of a solid-state change between 25° and 1000°C, but they detected a double thermal arrest in the vicinity of the melting point. On cooling, the second arrest started on the average 20°C below the melting point arrest; on heating, the average was 17°C below the melting point. The latter measurements

<sup>62</sup>Noyce, W.K. and A.H. Daane, AEC Rept. No. CT-2404 (15 March 1945).

<sup>63</sup> Gordon, P. and A.R. Kaufmann, AEC Rept. No. CT-3379 (11 December 1945).

<sup>64</sup>Gordon, P., J. Appl. Phys. 20, 908 (1949).

<sup>65</sup> Chatterjee, G.P. and S.S. Sidhu, Phys. Rev. <u>76</u>, 175 (1949).

<sup>66</sup>Sidhu, S.S. and C.O. Henry, J. Appl. Phys. 21, 1036 (1950).

<sup>67</sup> Seybolt, A., J.S. Lukesh, and D.W. White, J. Appl. Phys. 22, 986 (1951).

<sup>68</sup>Kaufmann, A.R., P. Gordon, and D.W. Lillie, Trans. ASM 42, 785 (1950).

<sup>69</sup>Sloman, H., J. Inst. Metals, 50, 365 (1932).

<sup>70</sup> Teitel, R.J. and M. Cohen, J. Metals 185, 285 (1949).

<sup>&</sup>lt;sup>71</sup>Tuer, G.L., Fundamental Mechanical and Physical Characteristics of Beryllium As Related to Single Crystals, Sc.D. Thesis, M.I.T. (1954).

<sup>72</sup> Buzzard, R.W., J. Research Nat. Bur. Stds. 50, 63 (1953).

<sup>73</sup>Losano, L., Alluminio 8, 67 (1939).

<sup>74</sup> Martin, A. and A. Moore, J. Less Common Metals, 1, 85 (1959).

were made on beryllium samples of varying purity and included zone-refined beryllium containing 0.056 weight percent of metallic impurities, 0.4 cc/g of  $H_2$ , and 0.008 weight percent of  $O_2$ . They also reported lattice spacings for 99.4 percent pure beryllium containing 0.3 weight percent of BeO from -193° to 1265°C. They found deviations from linearity for the temperature dependence of the lattice spacings at about 200° and 800°C. These deviations were attributed to the effects of solutes. A discontinuity in lattice spacings at about 1250°C was stated to coincide with the transformation of hexagonal close-packed  $\beta$ -beryllium to body-centered cubic  $\alpha$ -beryllium.

It was concluded, in summary, that beryllium is hexagonal, close-packed from room temperature to about 20 degrees below its melting point. A transformation to a body-centered cubic phase is quite possible at the latter temperature, but was ignored in the present compilation.

The melting point of beryllium was taken as  $1556^{\circ} \pm 3^{\circ}K$  on the basis of the available information. 56, 75-78

#### b. Thermodynamic Properties

# 1) Heat of fusion

The heat of fusion of beryllium was taken as 2.800 ± 0.500 Kcal/gfw from the review of Kubaschewski et al. 79 This value was derived from Oesterheld's 80 thermal analysis studies (2.40 Kcal/gfw), Losano's 73 measurements on the pressure dependence of the melting point (1.98, 2.23, 2.56 Kcal/gfw), Sloman's 81 measurements on the melting-point depression of beryllium by silver (3.4 Kcal/gfw), and regularities among the entropies of transformation of the alkali and alkaline earth metals (3.0 Kcal/gfw). It should be noted that the value for the heat of fusion of magnesium accepted here destroys some of the regularity of Kubaschewski's comparison. However, the limits of error assigned to the value are probably adequate to cover any shift in the estimated value. The heat of fusion of beryllium adopted here was the one in general acceptance. 56, 75-78

<sup>75</sup> Dergazarian, T.E. et.al. JANAF Interim Thermochemical Tables, vols 1 and 2, Dow Chem. Co. (31 December 1960).

<sup>76</sup> Hultgren, R. et.al. Selected Values for the Thermodynamic Properties of Metals and Alloys, Min. Res. Lab., Inst. of Eng. Res., Univ. of California, Berkeley (1956); rev. eds. (1958 and (1960).

<sup>&</sup>lt;sup>77</sup>Stull, D.R. and G.C. Sinke, Thermodynamic Properties of the Elements, No. 18, In: Advances in Chemistry Series, Am. Chem. Soc., Washington (1956).

<sup>&</sup>lt;sup>78</sup>National Bureau of Standards Rept 6484 (1959).

<sup>79</sup> Kubaschewski, O., P. Brizgys, O. Huchler, R. Jauch, and K. Reinartz, Z. Elektrochem. 54, 275 (1950).

<sup>80</sup> Oesterheid, G., Z. Anorg. u. allgem. Chem. 97, 1 (1916).

<sup>81</sup> Sioman, H.A., J. Inst. Metals 54, 161 (1934).

# 2) Entropy and heat content at 298.15°K

Values of the entropy and heat content of elemental beryllium at 298.15°K were based on the measurements of Hill and Smith<sup>82</sup> (4° to 300°K). These data have been joined with the high-temperature data of Ginnings, Douglas, and Ball<sup>83</sup> (367° to 1169°K) by the Bureau of Standards. <sup>78</sup> S<sub>298</sub> was calculated to be 2.282  $\pm$  0.02 e.u., and (H<sub>298</sub> - H<sub>0</sub>) was computed to be 467 cal/gfw by the Bureau of Standards. The latter values were accepted for the present work. These same low-temperature data have been used elsewhere <sup>75</sup>, <sup>76</sup> to calculate the value of S<sub>298</sub> = 2.280 e.u.

Other low-temperature heat capacity measurements on beryllium included those of Simon and Ruhemann<sup>84</sup> (71° to 79°K), Lewis<sup>58</sup> (97° to 463°K), and Cristescu and Simon<sup>85</sup> (10° to 300°K).

# 3) High-temperature heat content

The measurements of Ginnings, Douglas, and Ball<sup>83</sup> (367° to 1169°K) were used to calculate the high-temperature heat capacity and heat content of beryllium. These authors gave results for two samples, each of which contained 99.5 percent beryllium, but differed in the composition of their impurities. An average of the results for the two samples, which differed a maximum of 0.5 percent, was adopted. The heat contents to 1000°K were considered to be good to ± 1 percent. The uncertainty of an extrapolation from the highest temperature of measurement (1169°K) to the melting point is larger. Derived values of the heat capacity, which increase essentially at a uniform rate with temperature from 700° to 1000°K, show an inflection around 1000°K to a more rapid increase with temperature. The extrapolation made herein assumed that the heat capacity above 1100°K increases at the same rate as it does between 1000° and 1100°K; namely,  $2.5 \times 10^{-3}$  cal/°K<sup>2</sup> gfw. Between 1000°K and the melting point, the heat capacities were considered to be good to ± 3 percent. It should be noted that the temperature of the observed inflection lies in the region of one of the disputed allotropic transformations discussed above.

<sup>82</sup>Hill, R.W. and P.L. Smith, Phil. Mag. 44, 636 (1953).

<sup>83</sup> Ginnings, D.C., T.B. Douglas, and A.F. Ball, J. Am. Chem. Soc. 73, 1236 (1951).

<sup>84</sup>Simon, F. and H. Ruhemann, Z. physik. Chem. 129, 321 (1927).

<sup>65</sup> Cristescu, S. and F. Simon, Z. physik. Chem. 25B, 273 (1934).

Other available data for the high-temperature heat capacity or heat content of solid beryllium included those of Fieldhouse et al<sup>86</sup> (434° to 1328°K), Jaeger and Rosenbohm<sup>59</sup> (273° to 1338°K), Lewis<sup>58</sup> (282° to 463°K), Magnus and Holzmann<sup>87</sup> (295° to 1173°K), and Nilson and Pettersson<sup>88</sup>(273° to 573°K).

In the absence of experimental data for the heat capacity of liquid beryllium, the value of 7.50 cal/ $^{\circ}$ K gfw recommended by Kelley was used.

# 4) Heat of formation of monatomic gas

The Third Law Method was used with the free-energy functions for beryllium tabulated herein and the vapor pressure data from the following sources to give the indicated values for the heat of formation of beryllium at 298. 15°K:

Source	Temperature	ΔH <sup>2</sup> at 298.15°K
	(°K)	(Kcal/gfw)
Gulbransen and Andrew <sup>89</sup>	1103 - 1229	78.170 ± 0.600
Holden et al <sup>90</sup>	1172 - 1552	77.840 ± 0.700
Schuman and Garrett <sup>91</sup>	1174 - 1336	80.590 ± 1.300
Baur and Brunner 92	1850 - 2331	79.540 ± 2.500

Original data points were used for the calculations.

The value for  $\Delta H^{\circ}_{f298}$  adopted herein was an average of the results of the first two authors listed; namely,  $78.00 \pm 0.500$  Kcal/gfw. The uncertainty given was based on the scatter of experimental vapor pressures, and did not include uncertainties due to estimated heat capacities for liquid beryllium.

<sup>86</sup>Fieldhouse, I.B., J.C. Hedge, J.I. Lang, and T.E. Waterman, Wright Air Development Center, Tech. Rept. WADC-TR-57-487, AD-1550954 (1958).

<sup>87</sup> Magnus, A. and H. Holzmann, Ann. Physik (5) 3, 585 (1929).

<sup>88</sup> Nilson, L.F. and O. Pettersson, Oversigt Kongl. Svenska Vetenskaps-Akad. 37, 33 (1880).

<sup>89</sup> Gulbransen, E.A. and K.F. Andrew, J. Electrochem. Soc. 97, 383 (1950).

<sup>90</sup> Holden, R.B., R. Speiser, and H.L. Johnston, J. Am. Chem. Soc. <u>70</u>, 3897 (1948).

<sup>91</sup> Schuman, R. and A.B. Garrett, J. Am. Chem. Soc. 66, 442 (1944).

<sup>92</sup> Baur, E. and R. Brunner, Helv. Chim. Acta 17, 958 (1934).

An extrapolation of  $\Delta F_f^o$  to zero gave a normal boiling point for berylliumof 2754°K. An uncertainty of 50 degrees was estimated for the boiling point from uncertainties in  $\Delta H_{f298}^o$  and liquid heat capacities. At the boiling point,  $\Delta H_f^o$  was calculated to be 70.498 Kcal/gfw.

# 5) Thermodynamic functions

The beryllium reference state thermodynamic functions are given in Table  $V_{\cdot}$ 

The thermodynamic functions for beryllium as an ideal monatomic gas in Table VI were calculated using all the levels listed by Moore.  $^{52}$   $\rm H_{298}^{\circ}-H_{O}^{\circ}$  was found to be 1, 481 cal/mole. Uncertainty estimates are given on the backs of the tables.

#### 2. Boron

Existing tabulations on boron were found to be inadequate for three reasons. First, they were not based upon the most up-to-date data; second, they did not extend up to 6000°K; and third, estimates of uncertainty in the data were not included. Therefore, the re-computation of the boron data was undertaken.

#### a. Crystal Structure

Elemental boron exists in several modifications. However, the stable modifications and their temperature ranges of stability are still in doubt.

It is generally accepted that  $\beta$ -rhombohedral boron is the stable form above 1500°C, 93-95 and also that it may be stable down to as low as  $1100^{\circ}$ C. 93 a-rhombohedral boron is also fairly well documented, 96, 97 being stable at lower temperatures than the  $\beta$ -rhombohedral form. 94 Other common forms include the tetragonal, 98, 99 and amorphous borons 94 Several other polymorphs have been reported, but it appears likely that many of them are formed as a result of kinetic considerations and the presence of a foreign substrate and have no real thermodynamic range of stability. 93

In view of the uncertainties regarding the stable phases of boron, it is impossible to specify solid transition-point temperatures. Such transitions usually have low but generally unknown heats of transition (commonly a few hundred calories). Hence, the thermodynamic tabulations will contain these added uncertainties.

#### b. Melting Point

For the melting point of boron, there were also many reported values. These are summarized in Table VII.

<sup>93</sup> Hoard, J.L. and A. E. Newkirk, An analysis of polymorphism in boron based upon X-ray diffraction results, J. Am. Chem. Soc. 82, 70 (1960).

<sup>94</sup> Williams, D.N., The Properties of Boron, Defense Metals Information Center, Battelle Memorial Institute, Memorandum 41 (4 January 1960).

<sup>95</sup> Sands, D.E. and J.L. Hoard, Rhombohedral elemental boron, J. Am. Chem. Soc. 79, 5582 (1957).

<sup>96</sup> Decker, B.F. and J.S. Kasper, The crystal structure of a simple rhombohedral form of boron, Acta Cryst. 12, 503 (1959).

<sup>97</sup> McCarty, L.V. and D.R. Carpenter, J. Electrochem. Soc. 107, 38 (1960).

<sup>98</sup> Hoard, J.L., S. Geller, and R.E. Hughes, J. Am. Chem. Soc., 73, 1892 (1951).

<sup>99</sup> Hoard, J.L., R.E. Hughes, and D.E. Sands, The structure of tetragonal boron, J. Am. Chem. Soc. 80, 4507 (1958).

Reference State for Calculating ΔH<sup>o</sup><sub>f</sub>, ΔF<sup>o</sup><sub>f</sub>, and Log K<sub>p</sub>: Solid from 298.15° to 1556°K, Liquid from 1556° to 2754°K, Gas from 2754° to 6000°K

8	[w	Ξ	9.	0	13	
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m.p. = 1556 \* ± 3 \*K

b.p. = 2754° ± 50°K

W = 9.013		1/04 4	m.p. = 15	30 E 3 K		W . 1 . 4	J. p.	
T,*E	c <b>,</b>	I/°jK s/v S <sup>2</sup> T	-(F <sub>T</sub> ° - H <sub>298</sub> )/T	HT - H250	ΔH.;	Keni/gfw =	Δ.	Log Kp
0	0.000	0.000	Infinite	-0.467	•			11
298.15	3.932	2. 282	2. 282	0.000				
300	3.951	2.307	2. 283	0.007				
400	4.773	3.565	2. 447	0.447				
500	5. 260	4.687	2.787	0.950				
600	5.588	5.676	3. 186	1.494				
700	5.846	6.557	3.606	2.066				
800	6.072	7.353	4.025	2.662				
900	6. 287	8.081	4. 437	3. 280				
1000	6.508	8.754	4. 835	3.919				
1100	6.758	9.386	5. 221	4.582				
1200	7.008	9.985	5.593	5. 270				
1300	7.258	10.556	5.953	5.984				
1400	7.508	11.103	6.302	6.722				
1500	7.758	11.620	6.630	7.485				
1556	7.898	11.916_	6.823	7.924				
1556	7.500	13.715	6.823	10.724				
1600	7.500	13.924	7.015	11.054				
1700	7.500	14.379	7.435	11.804				
1800	7.500	14.808	7.834	12.554				
1900	7.500	15.213	8.211	14.054				
2000	7.500	15.598	8.571	14.034				
2100	7.500	15.964	8.914	14.804				
2200	7.500	16.313	9. 243	15.554				
2300	7.500	16.646	9.557	16.304				
2400	7.500	16.965	9.859	17.054				
2500	7.500	17.272	10.150	17.804				
	1.			In the second				
2600	7.500	17.565	10.429	18.554				
2700	7.500	17.848	10.698	19.304				
2754 2754	7.500	17.996 43.595	10.839	19.709 90.207				
2800	4.993 4.997	43.675	11.376	90.437				
2900	5.007	43.851	12.493	90.937				
3000	5.021	44.021	13.542	91.438				
3100	5.037	44.186	14.528	91.941				
3200	5.057	44.346	15. 457	92.446				
3300	5.061	44.502	16.334	92. 953				
3400	5.109	44.654	17.165	93.462				
3500	5-142	44.803	17.953	93.975				
3600	5.179	44.948	18.700	94.491				
3700	5.221	45.090	19.412	95.010				
3800	5.268	45.230	20.089	95.535				
3900	5.320	45.368	20.736	96.064				
1000	5.378	45.503	21.353	96.599				
		44 637	33.044	07 140				
6100 6200	5.440 5.508	45.637	21.944 22.510	97.140 97.687				
1300	5.581	45.899	23.052	98.242				
400	5.658	46.028	23.573	98.804				
500	5.741	46.156	24.073	99.373				
600	5.828	46.283	24.554	99.952				
700	5.919	46.410	25.019	100.539				
800	6.014	46.535	25.465	101-136				
900	6.113	46.660	25.896	101.742				
000	6.215	46.785	26.313	102.358				
100	6.320	46.909	26.716	102.985				
200	6.428	47.033	27.106	103.622				
300	6.538	47.136	27.482	104.271				
400	6.649	47, 279	27.848	104.930				
500	6.763	47.402	28 - 202	105.601				
600	6.877	47.525	28.546	106. 283				
700	6.993	47.646	28.680	106.976				
500 -	7.108	47.771 47.893	29. 205 29. 520	107.681				
900	7.224 7.340	47.893	29.520	108.398 109.126				
000	7.340	##. U.I.D	47.848	107.120				

BERYLLIUM REFERENCE STATE

# SUMMARY OF UNCERTAINTY ESTIMATES

	· ca	1/°K gfv			Kcal/	el =	
T, °E	C.	s <sub>T</sub>	$-(F_{T}^{\circ} - H_{296}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF	Log Kp
298.15	± .050	±.020	±.020	± .000			
1000	± .060	±.070	±.030	± .040			
1556	± .240	± - 160	±.050	± .150			
1556	± .380	± . 470	±.050	± .650			
2000	±1.040	± - 640	±.160	± .960			
2754	± 2.170	±.990	±.200	± 2.170		•	

Reference State for Calculating ΔHP, ΔFP, and Log Kp.: Solid from 298.15° to 1556°K, Liquid from 1556° to 2754°K, Gas from 2754° to 6000°K.

af w	3	Q.	0.1	1

		i/°K et			Kcal/gfw-		
T, °K	c,	ST	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>2</sup> <sub>f</sub>	ΔF f	Log Kp
0	0.000	0.000	Infinite	-1.481	76.986	76.986	Infinit
298.15	4.968	32.545	32.545	0.000	78.000	68.977	-50.55
300	4.968	32.576	32.545	0.009	78.002	68.921	-50.20
400	4.968	34.005	32.740	0.506	78.059	65.983	- 35. 99
500	4. 986	35.114	33.108	1.003	78.053	62.839	- 27 . 46
600	4.968	36.020	33.520	1.500	78.006	59.800	-21.78
700	4.968	36.785	33.933	1.996	77.930	56.770	-17.72
800	4.968	37.449	34. 332	2.493	77.831	53.754	-14.68
900	4.968	38.034	34.712	2.990	77.710	50.752	-12.32
000	4.968	38.557	35.070	3.487	77.568	47.765	-10.43
1100	4.968	39.031	35.409	3.984	77.402	44.792	-8.89
200	4.968	39.463	35.729	4. 481	77.211	41.837	-7.61
300	4. 968	39.861	36.032	4.977	76.993	38.896	-6.53
400	4.968	40.229	36.319	5.474	76.752	35.976	-5.61
500	4.968	-40.572	36.591	5.971	76.486	33.058	-4.81
***	4.010	40.754	3/ 739	4 340	74 125	21.462	
556	4. 968	40.754	36.738 36.738	6. 249	76. 325 73. 525	31.452 31.452	4.41 -4.41
600	4. 968	40.892	36.850	6.468	73.414	30.265	-4.13
700	4.968	41.194	37.097	6.965	73.161	27.575	-3.54
800	4.968	41.478	37.332	7.461	72.907	24.901	-3.02
900	4.968	41.746	37.558	7.958	72.654	22. 241	-2.55
000	4.969	42.001	37.774	8.455	72.401	19.595	-2.14
100	4.969	42. 244	37.981	8.952	72.148	16.960	-1.76
200	4.969	42.475	38.180	9.449	71.895	14.339	-1.42
300	4.972	42.696	38.371	9.946	71.642	11.727	-1.42
400	4.974	42.997	38. 556	10.443	71.389	9.128	-0.83
500	4. 977	43.110	38.734	10.941	71.137	6.542	-0.57
			10		** ***		
600 700	4.982	43.306 43.494	38.906 39.073	11.439 11.937	70.885 70.633	3.958 1.389	-0.33 -0.11
75 <b>4</b>	4.993	43.595	39.163	11, 937	70.498	0.000	0.00
754	4. 993	43.595	39. 163	12.207	/ .	0.000	0.00
800	4. 997	43.675	39. 234	12.437			
900	5.007	43.851	39. 390	12.937			
000	5.021	44.021	39. 542	13.438			
100	5 037	44 104	30 490	13 041			
100 200	5.037 5.057	44.186 44.346	39.689 39.832	13.941 14.446			
300	5.081	44.502	39.971	14.953			
400	5. 109	44.654	40.106	15.462			
500	5.142	44.803	40.238	15.975			
		44.040	40.347	17 401			
600	5.179	44.948	40. 367	16.491			
700	5. 221	45.090	40.493 40.616	17.010			
800	5. 268	45.230 45.368	40.736	17.535 18.064			
900 000	5. 378	45.503	40.853	18.579			
100	5.440	45.637	40.968	19.140			
200	5.508	45.769	41.081	19.687			
100	5.581	45.899	41.192	20. 242			
400 500	5.658 5.741	46.028 46.156	41.300 41.407	20.804 21.373			
600	5.828	46.283	41.511	21.952			
700	5,919	46.410	41.614	22.539			
800	6.014	46.535	41.715	23.136			
700 100	6.113	46.660 46.785	41.815 41.913	23.742 24.358			
-							
100	6.320	46.909	42.010	24.985			
200	6.428	47.033	42.105	25.622			
100	6.518	47.156	42, 199	26.271 26.930			
100 100	6.649 6.763	47.279 47.402	42. 292 42. 384	27.601			
	· 101	11, 104	12. 707	2001			
500	6 877	47.525	42.475	28. 283			
	6.993	47.648	42.565	28.976			
100	7.108	47.771	42.653	29.681			
900 100	7.224 7.340	47.893 48.016	42.741 42.828	30.398 31.126			
100	, , , , ,	10.010	45.050	71-120			

BERYLLIUM IDEAL MONATOMIC GAS

#### SUMMARY OF UNCERTAINTY ESTIMATES

		u/°K gfv			Keal/	ď=	`
T, <b>°K</b>	ς <b>;</b>	S <sup>o</sup> T	$-(F_{\rm T}^{\rm o}-H_{298}^{\rm o})/{\rm T}$	H <sub>T</sub> - H <sub>298</sub>	AH (	ΔΥ	Log Kp
298.15	±.000	±.002	±.002	±.000	± .500	± .510	±.370
1000	±.000	±.002	±.002	±.000	± .540	± .530	±.120
1556					± .650	± .580	±.080
1556					± 1.150	± .580	±.080
2000	±.000	±.002	±.003	±.000	±1.460	± .820	±.090
2754					± 2.670	±1.050	±.090
3000	±.001	±.002	±.003	±.001			
4000	±.002	±.003	±.003	±.002			
5000	±.002	±.003	±.003	±.004			
6000	±.002	±.003	±.004	±-005			

TABLE VII

REPORTED MELTING POINTS OF BORON

° C	° K	Original Reference	Quoting Reference No.
2400	2673	Weintraub 112	106
2300	2573	Probably ICT* or Weintraub 112	102, 109
2200	2473	Tride and Birnbrauer 111	110
>2147	>24 20	Searcy and Myers 104	
2100-2200	(2373-2473)	Cooper 106	
2130 ± 10	2403 ± 10	Piper 108	
2130	2403	Cline 105	
2040	2313	Cueilleron 100	103,113
2000 - 2075	2273-2448	Cueilleron 107	77, 106

<sup>\*</sup>International Critical Tables 101 give the figure as 2300°C, implying that the melting point is somewhere between 1800° and 2800°C.

<sup>100</sup>Cueilleron, J., Ann. chim. 19, 459 (1944).

<sup>101</sup> International Critical Tables, Vol. I, (1926), p. 103.

<sup>102</sup> Hodgman, C.D., R.C. Weast, and S.M. Selby, Handbook of Chemistry and Physics, 40th ed., Chem. Rubber Pub. Co., Cleveland (1958-59), p. 344.

<sup>103</sup> Lange, A.L. and G.M. Forker, Handbook of Chemistry, 9th ed., Handbook Pub., Sandusky, Ohlo (1956).

<sup>104</sup> Searcy, A.W. and C.E. Myers, J. Phys. Chem. 61, 957 (1957).

<sup>105</sup> Cline, C.F., An investigation of the compound eilicon boride (SiB6), J. Electrochem. Soc. 106 (4), 332 (1959).

<sup>106</sup> Cooper, H.S., In: Rare Metals Handbook, C.A. Hampel, ed., Reinhold, N.Y. (1954), p. 78.

<sup>107</sup>Cuellieron, J., The melting point of boron, Compt. Rend. 221, 698 (1945).

<sup>108</sup> piper, E.L., Research Study to Determine the Phase Equilibrium Relations of Selected Metal Carbides at High Temperatures, Natl. Carbon Research Labs., Prog. Rept. 1, Contract AF33(616)-6286, Task No. 73500 (30 June 1959).

<sup>109</sup> Forsythe, W.E., Smithsonian Tables, Vol. 120, 9th ed. Rev., Smithsonian Inst. Pub., Washington (1956), 827 p.

<sup>110</sup> Laubengayer, A.W., A.E. Newkirk, and R.L. Brandaur, J. Chem. Education 19, 382 (1942).

<sup>111</sup> Tride and Birnbrauer, Z. anorg. u. allgem. Chem. 87, 129 (1941).

<sup>112</sup>Weintraub, E.J., Ind. Eng. Chem. 5, 106 (1913).

<sup>113</sup> Natl. Bur. Standards (US) circ 500, Series I and II (1952).

In evaluating these various melting-point data, the most important consideration is probably sample purity. Usually, small amounts of impurities are expected to lower the melting point, and cause an increase in the melting-point range. The highest values in Table VII (from 2200° to 2400°C) are based on very old work, and were not given serious consideration. The values of Cueilleron 100, 107 appear to be too low in the light of the more recent work. The values from references 104-106 and 108 in Table VII should be considered in more detail.

TABLE VIII
SUMMARY OF RECENT BORON MELTING-POINT DATA

Reference	Type of Boron	Purity (percent)	Melting Point (°K)
Searcy and Myers 104	{ Fairmount amorphous, sublimed.	98. 9 99. 95 }	> 2420
Cline 105	Pacific Coast Borax, "fused!	95-97	2403
Cooper 106	Briquette,		2373-2473
Piper 108	Pacific Coast Borax, powder.	98. 9	2403 ± 10

The work of Searcy and Myers <sup>104</sup> seems to be the most reliable since some of their samples had purities up to 99.95 percent. Since they could still not obtain fusion at 2420°K, it is necessary to estimate the melting point. In view of the lower, recent values given in references 105 and 108, it would seem that the melting point could not be much higher than 2420°K. Accordingly, the melting point was taken to be 2450° ± 50°K, which would encompass these recent values.

# c. Thermodynamic Data

For crystalline boron as the reference state, the data of Wise, Margrave, and Altman<sup>17</sup> to 2400°K have been used in the present report. Their values were based on the low-temperature data of Johnston et al, <sup>114</sup> and their own measurements to 1200°K. They have extrapolated these data to 2400°K. Their data have been extrapolated here to the estimated melting point of 2450°K. For the heat of fusion, the

<sup>114</sup> Johnston, H.L., H.N. Hersh, and E.C. Kerr, J. Am. Chem. Soc. 73, 1112 (1951).

Sinke et al  $^{32}$  procedure has been followed to obtain an entropy of melting of 2.3 e.u., or a heat of fusion of 5635 cal/g atom. Similarly, the liquid heat capacity has been estimated as 7.5 cal/°K g atom.

#### d. Sublimation Data

The available data for the sublimation of boron showed considerable uncertainty also (see Table IX).

TABLE IX
BORON SUBLIMATION DATA (Kcal/g atom)

Reference	Method	ΔH° s298	ΔH°O
Searcy and Myers 104	Effusion	139 ± 4	137.7 (see reference 117)
Robson <sup>115</sup>	Effusion	135.0	133.8 ± 0.7
Thorn, 116 and Evans et al 117			133
Chupka et al 118 and Leitnaker 119	Mass spectrometer	129	128.3 (see reference 117)
Schissel and Williams 120	Mass spectrometer	129 ± 5	
Akishin et al <sup>121</sup>	Mass spectrometer		131.6 ± 5

<sup>115</sup> Robson, H.R., Ph. D. Thesis, Univ. of Kansas, Lawrence (1958).

<sup>116</sup> Thorn, R.J., Private Communication to Evans et al 117.

<sup>117</sup> Evans, W.H., D.D. Wagman, and E.J. Prosen, The Vapor Pressure of Some Boron Compounds, Natl. Bur. Standards (U.S.), Rept. 5663 (23 December 1957), Thermodynamic Properties of Some Boron Compounds, Natl. Bur. Standards (U.S.), Rept. 4943 (31 August 1956).

<sup>118</sup> Chupka, W.A. to P.O. Schissel and W.S. Williams, Quoted in Reference 119.

<sup>119</sup> Leitnaker, J.M., Thermodynamic Properties of Refractory Borides, Los Alamos Sci. Lab. LA-2402 (TID-4500), (13 April 1960).

<sup>120</sup> Schissel, P.O. and W.S. Williams, Mass spectrometric study of the vaporization of certain refractory compounds, Bull. Am. Phys. Soc. 4, 139 (1959).

<sup>121</sup> Akishin, P.A., D.O. Nikitin, and L.N. Gorokhov, Determination of the heat of sublimation of boron by mass spectrometry, Dokl. Akad. Nauk, SSSR (Proc. Acad. Sci. USSR) 129, 1075 (1959).

#### e. Calculations

#### 1) Condensed phases

Wise, Margrave, and Altman  $^{17}$  have tabulated values of  $C_p^o, H_T^o - H_O^o, -\left(\frac{F_T^o - H_O^o}{T}\right)$ , and  $S_T^o$  from  $100^o$  to  $2400^o$ K. These values were con-

verted to the standard reference temperature of 298°K according to equations (107) through (110).  $H_{298}^{\circ} - H_{0}^{\circ} = 290.4$  cal/gfw was taken from that reference. 17

The formula given by Wise, Margrave, and Altman, <sup>17</sup> (see eq. (20) and its discussion)

$$C_p^o/R = D(\theta_D/T) + 2 E_1(\theta_1/T) + E_2(\theta_2/T)$$
, (132)

was used to obtain the C\_p^o value at 2450°K by extrapolation. It was used as in equation (133) with available tabulations of D( $\theta_D$ /)T and E( $\theta$ /T) with the reported values of  $\theta_D$ ,  $\theta_1$  and  $\theta_2$ .

$$C_p^{\circ}/R = D(\theta_D/T) + 2 E(\theta_1/T) + E(\theta_2/T).$$
 (133)

The Einstein functions  $E(\theta_1/T)$  and  $E(\theta_2/T)$  were evaluated from the tables of Sherman and Ewell, <sup>12</sup> and the Debye function  $D(\theta_D/T)$  was evaluated from the tables of Taylor and Glasstone which give  $3RD(\theta_D/T)$ . <sup>122</sup> The  $C_p^o$  and other values in Table X, calculated from this formula at 2450 K, were in good agreement with those obtained by extrapolation of Wise, Margrave, and Altman's <sup>17</sup> table by a difference method.

At the chosen melting point,  $2450^{\circ}$ K, the value of  $C_p^{\circ}$  = 7.50 was taken for the reasons discussed in section c. above. Similarly, the heat of fusion was taken to be 5635 cal/g atom, and the entropy of melting was taken to be 2.3 e.u. Hence, the quantities  $H_T^{\circ} - H_{298}^{\circ}$  and  $S_T^{\circ}$  had the respective increments of 5635 and 2.3 for the liquid phase at  $2450^{\circ}$ K.

For temperatures above 2450  $^{\circ}$  K, the heat capacity was assumed to be constant at 7.50 cal/ $^{\circ}$  K g atom. Therefore,  $H_{T}^{\circ} - H_{298}^{\circ}$  became

$$H_T^{\circ} - H_{298}^{\circ} = \left[ H_{2450}^{\circ}(1iq) - H_{298}^{\circ} \right] + 7.5 (T - 2450).$$
 (134)

<sup>122</sup> Taylor, H.S. and S. Glasstone, A Treatise on Physical Chemistry, Vol. I: Atomistics and Thermodynamics, Van Nostrand, N.Y. (1942), p. 669.

Reference State for Calculating  $\Delta H_F^0$ ,  $\Delta F_F^0$ , and  $\log K_p$ : Solid from 298.15° to 2450°K, Liquid from 2450° to 6000°K (Metastable above b.p.).

10.82 n	n.p. = 2450 ° ± 50 °K
---------	-----------------------

w = 10.82	<u></u>	L/AM A		50 • 50 K		0.p 3	70°± 2
T, *K	c <sub>p</sub>	s'T	-(FT -H298)/T	H <sub>T</sub> - H <sub>296</sub>	AH? Kenl/gfw -	ΔF	Log
0	0.000	0.000	Infinite	-0.290			
298.15	2.823	1.392	1. 392	0.000			
300	2.845	1.409	1.389	0.006			
400	3.841	2.374	1.516	0.343			
500	4. 498	3.307	1.783	0.762			
600	4. 966	4 170	1 100	1 227			
700	5. 333	4.170 4.964	2.108 2.461	1.237 1.752			
800	5.639	5.697	2.820	2.301			
900	5.902	6.377	3.178	2.879			
1000	6.130	7.011	3.530	3.481			
1100	6.329	7.605	3.874	4.104			
1200	6.502	8.163	4. 208	4.746			
1300	6.652	8.689	4.532	5.403			
1400	6.783	9.187	4.847	6.075			
1500	6.897	9.659	5. 153	6.759			
1600	6.996	10.107	5.448	7.454			
1700	7.083	10.534	5.735	8.158			
1800	7.160	10.941	6.013	8.870			
900	7.228	11.330	6. 282	9.590			
2000	7. 288	11.703	6.545	10.316			
2100	7.341	12.059	6.798	11.047			
2200	7.388	12.402	7.045	11.784			
300	7.430	12.731	7. 285	12.525			
400	7.468	13.048	7.519	13.269			
450	7.485	13.222	7.654	13.642			
450	7.500	15.522	7.654	19. 277			
500	7.500	15.673	7.812	19.652			
600	7.500	15.967	8.120	20.402			
780							
	7.500	16.250	8.416	21.152			
800	7.500	16.523	8.701	21.902			
900	7.500 7.500	16.786 17.041	8.975 9.240	22.652 23.402			
100 200	7.500 7.500	17.287 17.525	9. 496 9. 743	24.152 24.902			
300	7.500	17.756	9.982	25.652			
400	7.500	17.756	10.214	26.402			
500	7.500	18.197	10.439	27.152			
600	7.500	18.408	10.658	27.902			
700	7.500	18.614	10.870	28.652			
800	7.500	18.814	11.077	29.402			
900	7.500	19.009	11.277	30.152			
000	7.500	19.199	11.473	30.902			
100	7.500	19.364	11.664	31.652			
200	7.500	19.565	11.850	32.402			
300	7.500	19.741	12.031	33. 152			
400	7.500	19.913	12.208	33.902			
500	7.500	20.082	12.382	34.652			
600	7. 500	20. 247	12,441	35.402			
700	7.500	20.408	12.716	36.152			
00	7.500	20.566	12-070	36.902			
900	7.500	20.721	13.037	37.652			
000	7.500	20.072	13.192	38.402			
100	7.500	21.021	13.344	39.152			
200	7.500	21,167	13.493	39.902			
300	7.500	21.309	13.639	40.652			
400	7.500	21.450	13.783	41.402			
300	7.500	21.587	13,923	42.152			
600	7.500	21.723	14.062	42.902			
700	7.500	21.855	14.197	43.652			
00	7.500	21.986	14. 330	44. 40 1			
00	7.500	22.114	14.461	49. 152			
000	7.500	22. 240	14.590	45.902			
		,					

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BORON REFERENCE STATE

# SUMMARY OF UNCERTAINTY ESTIMATES

,	ca	V°E et-				/v	$\overline{}$
T, <b>E</b>	\$	S <sub>T</sub>	-(FT -H298)/T	H <sub>T</sub> - H <sub>298</sub>	AK ?	ΔF <sub>f</sub>	Lag Ep
298.15	± .200	± .020	±.020	± .000			
1000	± .200	± .260	±.120	± -140			
2000	± .200	± -400	±.230	± .340			
2450	± .200	± .420	± · 250	± .430			
2450	±1.000	± .720	± · 250	±1.160			
3000	±1.000	± .920	±.350	±1.710			
4000	±1.000	±1.200	±.520	± 2.710			
5000	±1.000	±1.430	±.690	±3.710			
6000	±1.000	±1.610	±.830	±4.710			

Reference State for Calculating  $\Delta H_f^{p}$ ,  $\Delta F_f^{o}$ , and  $Log\,K_p$ : Solid from 298.15° to 2450 °K,

w = 10.82			m.p. = 2450 * ± 50 *K			b.p. = 3	p. = 3970°± 250°	
		al/°K giu			Kcal/	gfw	\	
T, °K	C <sub>p</sub>	ST	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	VΗ,	ΔF	Log Kp	
0	0.000	0,000	Infinite	-1.511	131,779	131,779	Infinite	
298.15	4.971	36.649	36.649	0.000	133.000	122.489	-89.782	
300	4.971	36.680	36.650	0.009	133.003	122.422	-89.180	
400	4.970	38.110	36.845	0-506	133.163	118.869	-64.943	
500	4. 969	39.218	37.212	1.003	133. 241	115. 286	- 50. 389	
600 700	4.969	40.124	37.624 38.037	1.500 1.997	133.263	111.691 108.097	-40.681	
800	4. 968	41.554	38.436	2.494	133. 245 133. 193	104.508	-33.747 -28.548	
900	4. 968	42.139	38.815	2.991	133.143	100.927	-24.507	
1000	4.968	42.662	39.175	3.487	133-006	97.355	- 21. 275	
1100	4.968	43.136	39.514	3.984	132.880	93.796	-18.634	
1200	4.968	43.568	39.833	4.481	132.735	90.250	-16.435	
1300	4.968	43.966	40.136	4.978	132.575	86.715	-14.577	
1400	4.968	44.334	40,423	5.475	132.400	83.194	-12.986	
1500	4.968	44.677	40.695	5-972	132.213	79.687	-11.609	
1600	4.968	44.998	40.955	6.468	132.014	76.189	-10.406	
1700	4.968	45.299	41.202	6.965	131.807	72.707	-9.346	
1800	4.968	45.583	41.437	7.462	131.592	69.237	-8.406	
1900	4.968	45.851	41.662	7.959	131.369	65.778	-7.565	
2000	4. 968	46.106	41.878	8.446	131.140	62.334	-6.811	
2100	4.968	46.349	42.086	8.952	130.905	58.896	-6.129	
2 2 0 0	4.968	46.580	42.285	9.449	130.665	55,472	-5.510	
2300	4.968	46.801	= 42.476	9-946	130.421	52.061	-4.946	
2400	4.968	47.012	42.660	10.443	130.174	48.662	-4. 431	
2450	4.968	47.114	42.750	10.691	130.049	47.015	-4.193	
2 <b>4</b> 50 2500	4.968	47.114 47.215	42.750 42.839	10.691 10.940	124.414 124.288	47.015 45.433	-4.193 -3.971	
2600	4.968	47.410	43.011	11 417	124 015	42 284	2 654	
2700	4. 968	47.597	43.177	11.437 11.933	124.035 123.781	42. 284 39. 146	-3.554 -3.168	
2800	4.968	47.778	43.338	12.430	123.528	36.017	-2.811	
2900	4.969	47.952	43. 494	12.927	123. 275	32.895	-2.478	
1000	4.969	48.121	43.646	13.424	123.022	29.782	- Z. 169	
100	4.969	48.284	43.793	13.921	122.769	26.680	-1.880	
200	4.970	48.441	43.935	14.418	122.516	23.586	-1.610	
300	4.970	48.594	44.074	14.915	122.263	20.497	-1.357	
400	4.971	48.743	44.210	15.412	122.010	17.414	-1.119	
500	4.972	48.887	44. 341	15.909	121.757	14. 343	-0.895	
600	4.973	49.027	44.469	16.406	121.504	11.281	-0-684	
700	4. 975	49.163	44.594	16.904	121.252	8.222	-0.485	
800	4. 977	49. 296	44.716	17.401	120.999	5.172	-0.297	
900	4.979	49.425	44.835	17.899	120.747	2.124	0.049	
100	4. 985	40 674	45.066	10 004	130 344	3 048	0.310	
200	4.988	49.674 49.794	45.176	18.896 19.394	120.244 119.992	-3.948 -6.969	0.210	
300	4.993	49.912	45. 285	19.893	119.741	-9.992	0.507	
400	4.997	50.027	45. 392	20.393	119.491	-13.009	0.646	
500	5.002	50.139	45.496	20.893	119.241	-16.013	0.777	
600	5.008	50.249	45.598	21. 393	118.991	-19.016	0.903	
700	5.015	50.357	45.698	21.894	118.742	-22.015	1.023	
800	5.022	50.463	45.797	22.396	118.494	-25.011	1.138	
900	5.030	50.566	45.892	22.899	118.247	- 27. 989	1.248	
000	5.038	50.668	45.987	23.402	118.000	- 30. 975	1.353	
100	5.048	50.768	46.080	23.906	117.754	-33.953	1.454	
200	5.058	50.866	46.171	24.412	117.510	- 36. 925	1.551	
300	5.069	10.962	46. 260	24.918	117.266	-39.891	1.644	
600 500	5.081	51.057 51.151	46. 348 46. 435	25.426 25.934	117.024	-42,851 -45,816	1.734	
500 700	5.107	51.242 51.333	46.519	26. <b>444</b> 26. 956	116.542	-48.759 -51.714	1.902	
100	5. 136	51.422	46.686	27.468	116.066	-54.664	2.059	
					110.000	- 2 4 . 00 4	D. 0 J 7	
700	5.152	51.510	46.767	27.983	115.831	-57.605	2.133	

BORON IDEAL MONATOMIC GAS
SUMMARY OF UNCERTAINTY ESTIMATES

,	c	ol/°K gfv ──			Kcal/	d+	
T, °E	c,	$s_{\mathbf{T}}^{\bullet}$	$-(F_{T}^{\circ} - H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	ØH ος β	ΔF	Log Kp
298.15	±.001	±.001	1.001	±.000	±4.000	±4.000	± 2. 930
1000	±.001	±.001	±.001	±.001	±4.140	±4.120	± .90
2000	±.001	±.061	±.001	±.002	±4.340	±4.460	± .480
2450	±.001	±.001	±.001	±.002	±4.430	±4.610	± .410
2450	±.001	±.001	±.001	±.002	±5.160	±4.610	± .410
3000	±.001	±.001	±.001	±.003	±5.710	±5.050	± .360
4000	±.001	±.001	±.001	±.004	±6.710	±6.080	± .330
5000	±.001	±.001	±.001	±.005	±7.710	±7.450	± .32
6000	±.001	±.001	±-001	±.006	±8.720	±8.980	± .320

The entropy was calculated according to equation (107) which reduced to equation (135),

$$S_T^{\circ} = S_{2450}^{\circ} (liq) + 17.2693 \log_{10} \frac{T}{2450}$$
 (1.35)

The free-energy function was calculated according to equation (108). The reference state functions are summarized in Table X.

# 2) Gas phase

Wilkins and Altman  $^{123}$  tabulated  $C_p^\circ, H_T^\circ - H_o^\circ$ , and  $S_T^\circ$  in the range from  $0^\circ$  to  $6000^\circ K$  at  $100^\circ K$  intervals. All these values were used as tabulated. The enthalpy (heat content) and free-energy functions were calculated from equations (108) and (110). The remaining functions were calculated from equations (42), (43), and (44). The ideal gas functions are summarized in Table XI.

# 3) Error analyses

a) Uncertainty estimates in condensed phase functions are given on the back of Table  $X_{\bullet}$ 

# l Heat capacity

In the case of boron,  $C_p^\circ$  data from more than one source have been available for comparison. They are summarized in Table XII.

TABLE XII
BORON HEAT CAPACITY DATA FROM VARIOUS SOURCES

Source	C° (cal/°K g atom)				
	298. 15 <sup>0</sup> K	2000°K			
Wise et al	2.823	7.288			
Sinke and Stull <sup>32</sup>	2.63	7.20			
Evans et al 117	2.650				

<sup>123</sup> Wilkins, R.L. and R.L. Altman, J. Chem. Phys. 31, 337 (1959).

It can be immediately seen from Table XII that there is a spread of about 0.20 cal/oK g atom in the values of heat capacity at room temperature. Although the measurements of Wise et al<sup>17</sup> were made on crystalline samples, whereas the others apparently used "amorphous" boron, the results of the former measurements could not be simply accepted since it would appear that their samples were not from a pure, single phase. For example, they made the statement that "some of the high temperature  $\beta$ - rhombohedral form" was present in all samples. A conservative evaluation therefore would require assuming that their samples contained a mixture of phases and adopting an uncertainty of 0.2 cal/g atom OK for the room-temperature heat capacity of boron. In the absence of any better information, the same uncertainty was assigned to the heat capacity at 2000°K even though the agreement between values from the two sources was better at that temperature.

For the liquid, a value of  $C_p^{\circ} = 7.50 \text{ cal/}^{\circ} \text{K g atom}$  and an uncertainty in this value (as well as  $\Delta C_p^{\bullet}$ ) equal to 1.0 cal/ $^{\circ} \text{K g}$  atom was simply assumed.

### 2 Entropy

Uncertainty ranges were calculated from equation (115) with  $\delta C_p^o$  equal to 0.2 cal/ $^{O}$ K gfw in the temperature range from 298.15 $^{O}$  to 2450 $^{O}$ K.

An uncertainty of 0.3 e. u.was assumed for the entropy of fusion of boron.

In the melt (2450° < T <  $6000^{\circ}$ K), the uncertainty in heat capacity was assumed to be 1.0 cal/°K gfw.

#### 3 Enthalpy

Uncertainty range calculations were made with equation (118).

# 4 Free Energy function

Free energy function uncertainty range calculations were made with equation (120).

## 5 Uncertainty in gas phase functions

The effect of energy assignments on ideal gas function accuracy has been briefly considered by Kolsky, Gilmer, and Gilles. 51

On the basis of their analysis, it appears that the energy levels of B(g) are well-established and that their small uncertainty causes an error of only  $\pm$  0.0002 cal/°K g atom in C<sub>p</sub>° for the ideal gas. It is also reassuring to compare the available C<sub>p</sub>° data from two separate tabulations.

Temperature (°K)	Values* of Wilkins et al 123	Values* of Kolsky <u>eť al</u> 51	Difference*
298.15	4. 971	4. 9709**	0.0001
6000	5.168	5.1683**	0.0003

Thus, one can conclude conservatively that these  $C_p^o$  data are accurate at least to  $\pm$  0.001 cal/ $^o$ K g atom.

A similar analysis of those authors  $^{123,51}$  entropy data shows that  $S_T^{\circ}$  is also accurate to + 0.001 cal/ $^{\circ}$ K g atom.

Temperature (°K)	Values* of Wilkins et al	Values* of Kolsky <u>et</u> al <sup>51</sup>	Difference*
298.15	36. 649	36. 648**	0.001
6000	51.597	51.5959**	0.0011

Free-energy and entropy functions calculated from these data have insignificant uncertainties for most practical purposes.

The uncertainties in  $\Delta H_1^p$ ,  $\Delta F_2^p$ , and  $\log_{10} K_p$  are much greater. These uncertainties are obtained from equations (42), (43), and (44).

<sup>\*</sup>Cal/OK g atom.

<sup>\*\*</sup> Converted to chemical atomic-weight scale.

The uncertainty estimates on the back of Table XI are slightly conservative in that the uncertainty in the heat of sublimation at 298°K has been used for all other temperatures. Since heats of sublimation of boron have been obtained from high-temperature (near 2000°K) experiments, it is reasonable to expect the values in the neighborhood of 2000°K to be more precise than the value at 298°K. Actually, the difference in uncertainties at these two temperatures is less than 0.5 kcal/g atom. This is small compared to the total error in the heat of sublimation.

### 3. Calcium

a. Crystal Structure, Transition Point, and Melting Point

Elemental calcium was shown by Smith, Carlson, and Vest<sup>124</sup> to have a face-centered, cubic structure from room temperature to 737°K and to transform at the latter temperature to a body-centered form stable up to the melting point.

These results are in contrast with those of earlier work from which the existence of additional allotropic modifications of calcium was inferred. Both a "low symmetry" or "complex" phase 125 and a hexagonal, close-packed phase had been previously reported. 125-128

The transition temperatures and phase stabilities had been found to depend on the thermal history of the calcium samples. Smith, Carlson, and Vest 124 concluded that the additional phases were due to impurities. Schottmiller, King, and Kanda 129 later also reported the two additional phases and suggested that small amounts of impurities (presumably metallic) could nucleate a transformation that occurred only very slowly in highly pure calcium. However, Smith and Bernstein 130 subsequently concluded that nitrogen or carbon induced the formation of the "low symmetry" phase and that hydrogen was responsible for the formation of the hexagonal close-packed phase. The matter has probably not been unambiguously resolved to everyone's satisfaction because the impurities responsible are difficult to control and are relatively difficult to determine quantitatively.

The results of Smith, Carlson, and Vest<sup>124</sup> have been accepted, and  $737^{\circ} \pm 10^{\circ}$ K has been adopted as the transition temperature for the present project. Stull and Sinke<sup>77</sup> and Kelley<sup>56</sup> adopted a transition temperature of 713°K from the earlier review of Kubaschewski et al. <sup>79</sup>

<sup>124</sup>Smith, J., O. Carlson, and R. Vest, J. Electrochem. Soc. 103, 409 (1956).

<sup>125</sup> Graf, L., Physik Z. 35, 551 (1934).

<sup>126</sup> Evert, F., H. Hartmann, and H. Peisker, Z. anorg. u. allgem. Chem. 213, 126 (1933).

<sup>127</sup> Schulze, A., Physik Z. 36, 595 (1935).

<sup>128</sup> Melbert, H., T.J. Tiedema, and W.G. Burgers, Acta Cryst. 9, 525 (1956).

<sup>129</sup> Schottmiller, J., A. King, and F. Kanda, J. Phys. Chem. 62, 1446 (1958).

<sup>130</sup> Smith, J. and B. Bernetein, J. Electrochem. Soc. 106, 448 (1959).

The melting point of calcium used here,  $1123^{\circ} \pm 10^{\circ}$ K, was listed by Kubaschewski et al, <sup>79</sup> and was also used in other recent compilations. <sup>56</sup>, <sup>76</sup>, <sup>77</sup> The more reliable values reported range from 1116° to  $1124^{\circ}$ K. <sup>125</sup>, <sup>129</sup>, <sup>131</sup>-<sup>133</sup>

### b. Thermodynamic Properties

#### Heat of transition

The heat of transition of face-centered cubic calcium to bodycentered cubic calcium was taken as 240  $_{\pm}$  60 cal/gfw. This value was recommended by Kubaschewski et al  $^{79}$  from the heat content measurements of Moser and Schulze  $^{127}$  (212 cal/gfw), Jauch  $^{134}$  (240  $_{\pm}$  60 cal/gfw), and the thermal analysis results of Rinck  $^{135}$  (275 cal/gfw). Eastman, Williams, and Young  $^{136}$  reported the heat of transition to be  $100 \pm 25$  cal/gfw from their heat content measurements. It was assumed that a change of the transition temperature from the previously accepted  $^{713^{\circ}}$  to  $^{737\,^{\circ}}$ K alters the heat of transition within the uncertainty given above.

## 2) Heat of fusion

Kubaschewski et al<sup>79</sup> list the heat of fusion of calcium as 2070  $\pm$  100 cal/gfw. This value is based on Jauch's <sup>134</sup> heat content measurements and was adopted here. Kelley <sup>137</sup> arrived at a value of 2230  $\pm$  300 cal/gfw from a review of phase diagrams of calcium alloys. Other determinations of the heat of fusion of calcium have been made by Zalesinski and Zulinski <sup>138</sup> (3150 cal/gfw, 3000 cal/gfw) and by Rinck <sup>135</sup> (1640 cal/gfw).

<sup>131</sup> Antropoff, A. von and E. Falk, Z. anorg. u. allgem. Chem. 187, 405 (1930).

<sup>132</sup> Hoffmann, F. and A. Schulze, Physik Z. 36, 453 (1935).

<sup>133</sup> Weibke, F. and W. Bartels, Z. anorg. u. allgem. Chem. 218, 241 (1934).

<sup>134</sup> Jauch, R. Diplomarbeit, Techn. Hochschule, Stuttgart (1946).

<sup>135</sup>Rinck, E., Ann. Chim. (10) 18, 510 (1932).

<sup>136</sup> Eastman, E.D., A.M. Williams, and T.F. Young, J. Am. Chem. Soc. 46, 1178 (1924).

<sup>137</sup>Kelley, K.K., Bureau of Mines Bull. 393 (1936).

<sup>138</sup> Zalesinski, E. and R. Zulinski, Bull. Int. Polon. Sci. Lettres (A), p. 479 (1928).

# 3) Entropy and heat content at 298.15°K

Kelley  $^{139}$  gave the entropy of elemental calcium at 298.  $^{160}$ K as  $^{9.95}\pm^{0.10}$  cal/ $^{0}$ Kgfw, based almost entirely on the low-temperature heat capacity data of Clusius and Vaughen  $^{140}$  ( $^{100}$  to  $^{2010}$ K). Hultgren  $^{76}$  arrived at the same value from these data plus the heat capacity measurements of Griffel, Vest, and Smith  $^{141}$  ( $^{1.80}$  to  $^{4.20}$ K), and Roberts  $^{142}$  ( $^{1.50}$  to  $^{200}$ K). H $^{298}$  - H $^{0}$ 0 was calculated by the present authors to be  $^{1375}$  cal/gfw for the solid.

Other low temperature heat capacity measurements on calcium include those of Gunther  $^{143}$  (22° to 62°K), and of Eastman and Rodebush  $^{144}$  (68° to 294°K).

### 4) High-temperature heat content

The heat capacity and heat content of elemental calcium are not very well-known. The only available low-temperature heat capacity data, those of Clusius and Vaughen, <sup>140</sup> terminate at 201°K and have been extrapolated to a value of 6.28 cal/°K gfw at 298.15°K. Above room temperature, data were derived from the heat content measurements of Eastman, Williams, and Young <sup>136</sup> (373° to 878°K), and of Jauch <sup>134</sup> (298° to 1223°K). For the face-centered cubic phase, heat capacities derived from the first source are 0.25 to 0.35 cal/°K gfw higher than those from the second source over the entire range of stability from room temperature to 737°K. Extrapolation of an algebraic expression for the data of Eastman, Williams, and Young <sup>136</sup> to 298.15°K gave a heat capacity of 6.20 cal/°K gfw.

For purposes of the present compilation, the following algebraic expression for the heat capacity of  $\alpha$ -Ca in cal/ ${}^{\circ}$ K gfw was used over the temperature range from 298.15 to 737 ${}^{\circ}$ K.

$$C_p^{\circ} = 5.205 + 3.605 \times 10^{-3} T.$$
 (136)

<sup>139</sup> Kelley, K.K., Bureau of Mines Bull. 477 (1950).

<sup>140</sup> Clusius, K. and J. V. Vaughen, J. Am. Chem. Soc. 52, 4684 (1930).

<sup>141</sup> Griffel, M., R.W. Vest, and J.F. Smith, J. Chem. Phys. 27, 1267 (1957).

<sup>142</sup> Roberts, L.M., Proc. Roy. Soc. (London) 70B, 738 (1957).

<sup>143</sup> Gunther, P., Ann. Physik 51, 828 (1916).

<sup>144</sup> Eastman, E.D. and W.H. Rodebush, J. Am. Chem. Soc. 40, 489 (1918).

This expression gives a heat capacity of 6.28 cal/ $^{\circ}$ K gfw at 298.15 $^{\circ}$ K and an average value of the results of Eastman, Williams and Young,  $^{136}$  and Jauch $^{134}$  extrapolated to  $^{737}$  $^{\circ}$ K. This expression is slightly different from others which have been used elsewhere,  $^{56}$ ,  $^{76}$ ,  $^{77}$ 

An algebraic representation of the heat content measurements of Jauch in cal/ $^{O}$ K gfw over the temperature range from 737 $^{O}$  to 1123 $^{O}$ K was the basis for the calculation of thermodynamic functions of body-centered cubic  $\beta$ -Ca.

$$C_{\mathbf{p}}^{\bullet} = 1.50 + 7.74 \times 10^{-3} \,\mathrm{T} + 2.5 \times 10^{5} \,\mathrm{T}^{-2}.$$
 (137)

These data have also been accepted elsewhere  $^{56}$ ,  $^{76}$ ,  $^{77}$  with slight modification. The heat capacities of  $\beta$ -Ca derived from the data of Eastman, Williams, and Young  $^{136}$  (to  $878^{\rm o}{\rm K}$ ) are considerably lower than the accepted values. Zalesinski and Zulinski  $^{138}$  are in better agreement with Jauch  $^{134}$  than with Eastman, Williams, and Young.  $^{136}$ 

Other sources for high-temperature heat capacity or heat content data for solid calcium are Bernini 145 (273° to 430°K), Bunsen 146 (273° to 373°K), and Schulze 127 (723° to 803°K).

Jauch's  $^{134}$  value for the heat capacity of liquid calcium, 7.40 cal/ $^{\circ}$ K gfw, was adopted on the basis of measurements of heat content from the melting point to 950 $^{\circ}$ K. This value has been used to the boiling point with increasing assigned uncertainty. Zalesinski and Zulinski  $^{138}$  reported the heat capacity of liquid calcium to be 10.7 cal/ $^{\circ}$ K gfw. Jauch's  $^{134}$  value was preferred because it was more consistent with the heat capacity of liquid magnesium, 7.8 cal/ $^{\circ}$ K gfw(See section IV-A8).

### 5) Heat of formation of the monatomic gas

Free-energy functions tabulated herein were used with vapor pressure data from the following sources to calculate the indicated heats of formation at 298.15°K using the Third Law Method:

<sup>145</sup> Bernini, A., Physik Z. 7, 168 (1906).

<sup>146</sup>Bunsen, R., Poggendorf's Ann. 141; 1 (1879).

Source	Temperature Range	ΔH <sup>9</sup> 298
	(°K)	(Kcal/gfw)
Priselkov and Nesmeyanov 147	748 - 943	42. 200 <u>+</u> 0. 200
Hartmann and Schneider 148	1254 - 1546	42.140 <u>+</u> 0.400
Douglas 149	807 - 918	42.310 <u>+</u> 0.350
Tomlin 150	801 - 877	42.230 <u>+</u> 0.200
Pilling 151	775 - 973	42. 220 <u>+</u> 0. 650
Smith and Smythe <sup>152</sup>	730 - 965	43.010 <u>+</u> 0.350
Ruff and Hartmann 153	1233 - 1380	41.060 <u>+</u> 3.000
Rudberg 154	774 - 897	46.060 <u>+</u> 0.350
Pidgeon and Atkinson <sup>155</sup>	1401 - 1477	54. 520 <u>+</u> 0. 700

The data of Smith and Smythe <sup>152</sup> were derived from an algebraic representation of their results. The heat of formation tabulated from the results of Pidgeon and Atkinson <sup>155</sup> has been taken from Hultgren. <sup>76</sup> Original data points were used from the remaining sources. The results of Rudberg <sup>154</sup> and Pidgeon and Atkinson <sup>155</sup> were excluded in arriving at an average value of 42. 220 Kcal/gfw to which an uncertainty of 0. 250 Kcal/gfw was assigned.

<sup>147</sup> Prizelkov, Y. and A. Nesmeyanov, Doklady Akad. Nauk SSSR 95, 1207 (1954).

<sup>148</sup> Hartmann, H. and R. Schneider, Z. anorg. Chem. 180, 275 (1929).

<sup>149</sup> Douglas, P.E., Proc. Phys. Soc. (London) 67B, 783 (1954).

<sup>150</sup> Tomlin, D.H., Proc. Phys. Soc. (London) 67B, 787 (1954).

<sup>151</sup> Pilling, N.B., Phys. Rev. 18, 362 (1921).

<sup>152&</sup>lt;sub>Smith</sub>, J.F. and R.L. Smythe, Acta Met. <u>7</u>, 261 (1959).

<sup>153</sup>Ruff, O. and H. Hartmann, Z. anorg. Chem. 133, 29 (1924).

<sup>154</sup>Rudberg, E., Phys. Rev. 46, 763 (1934).

<sup>155</sup> Pidgeon, L.M. and J.T.N. Atkinson, Can. Mining Met. Bull. 249, 14 (1949).

The normal boiling point of calcium was calculated to be  $1765^{\circ}\pm45^{\circ}$ K, and  $\Delta H_{f}^{o}$  at the boiling point was taken to be 35.871  $\pm$  0.870 Kcal/gfw.

# 6) Thermodynamic functions

The reference state thermodynamic functions of calcium are given in Table XIII. The ideal monatomic gas thermodynamic functions of calcium given in Table XIV were calculated using all the energy levels listed by Moore.  $^{52}$  Uncertainty estimates are summarized on the back of the tables.  $H_{298}^{\bullet}$  -  $H_0^{\bullet}$  was found to be 1, 481 cal/mole for the ideal gas.

REFERENCE STATE

Ca

Reference State for Calculating AHP, AFP, and Log Kp : Solid from 298.15° to 1123° K, Liquid from 1123° to 1765° K, Gas from 1765° to 6000° K.

gfw = 40.08 $T_t = 737^{\circ} \pm 10^{\circ} K$ m.p. = 1123\* ±10\*K b.p. = 1765° ±45° K cal/°K gfw - Keal giv sr c°  $-(F_{T}^{o} - H_{298}^{o})/T$ AF ,  $\text{H}_{T}^{\sigma} - \text{H}_{290}^{\uparrow}$ AH ? Log Kp 0,000 Infinite -1.375 0.000 9. 950 9. 989 9. 950 9. 950 0.000 298.15 6.280 6.287 300 10, 201 0.658 500 7.007 13, 369 10.687 1.341 14.678 600 7.368 11, 245 2.060 15,841 2.815 7.729 700 16, 242 16, 568 3, 103 3, 343 737 7.862 12.032 7.664 737 8.083 17, 213 12 414 1.839 18,205 13.003 4.682 900 8.775 19, 166 13,571 5,595 1100 10.221 20.105 14.123 5.580 6.817 1123 10 390 20.318 14.248 14, 248 8.887 1123 7.400 9.457 1200 7,400 22.652 14,771 23, 244 7.400 1300 1400 7.400 23, 792 15,980 10.937 24, 303 16.518 1500 7.400 12.417 24,781 17,020 7.400 1600 17.490 13.157 13.638 7,400 25. 229 25, 504 1765 7,400 49,509 49,683 4.980 17,777 18. 325 1800 4.982 45.927 4.993 50.182 1900 2000 5,008 46.453 21.112 50.684 22, 325 51.184 2100 5.030 46. 698 46.933 23,438 51,689 5.061 2200 47. 158 47. 377 24.464 25.415 2300 5.101 52, 197 52,709 5, 153 2400 5.219 47,588 26, 297 53,228 53, 753 2600 5.300 47,794 27.120 54.288 47.996 27.889 2700 5.397 54.833 55.391 5.511 48, 194 28,611 2900 5.644 48.390 29, 290 5.796 29.930 55.963 56.551 57.157 48,777 30.535 3100 3200 6.160 48.969 31, 107 6.371 49, 162 57.783 3300 3400 3500 6.601 49.355 32, 169 58.432 49.550 59.104 32,663 6.849 7.115 33, 135 59.802 49.747 3600 49.946 50.147 33,587 34,020 60.528 61.282 3700 7.397 7.692 3800 8.001 50. 351 34.436 62 067 62.883 50,557 34,836 4000 8, 120 63.731 50. 767 35, 223 4100 8.648 35. 59<sup>5</sup> 35. 955 64,613 65,528 8.983 4200 51, 194 4 300 9, 323 4400 36. 305 66.477 4500 10.010 51.634 36,643 67,461 68,479 51 R5R 36. 971 4600 10 15 1 52.084 69.532 10.694 4700 4800 11.030 52, 313 52, 543 37, 601 70.618 11, 362 4900 5000 11,687 52, 776 38, 198 72.890 74,075 38, 487 5100 12.004 53,011 53, 247 75.290 12, 313 5200 76.537 77,813 12.612 53, 484 53, 723 5 300 39.043 5400 5500 13,181 53.962 39. 577 79,117 13,450 13,708 80.448 54, 202 39.836 40.090 81,806 54.442 5700 54, 683 54, 923 5800 13, 954 40, 340 83, 190 40,585 84.597 14,190 5900 6000 40. B26 86.027

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CALCIUM REFERENCE STATE

### SUMMARY OF UNCERTAINTY ESTIMATES

	cel/°K gfe				Kcal/s	d	`
T, <b>°</b> K	c*	s <sub>T</sub>	$-(F_{T}^{\bullet} - H_{296}^{\circ})/T$	H <sub>T</sub> - H <sub>296</sub>	AH C	ΔF	Log K
298.15	± .100	±.100	±.100	±.000			
737	± .200	±.140	±.120	±.020			
737	<b>x</b> .300	±.230	±.120	±.080			
1123	±1.000	±,370	±.180	±,220			
1123	± .500	±.460	<b>±.180</b>	±.320			
1765	±1.500	±.690	±,320	±.640			
1765	± .000	±.002					
2000	<b>±</b> .000	±.002					
3000	± .001	±.002					
4000	± .002	±,002					
5000	± .003	±.003					
6000	± .003	±.003					

Ca

IDEAL MONATOMIC GAS

Reference State for Calculating AH?, AF?, and Log Kp · Solid from 298.15 ° to 1123 °K, Liquid from 1123 ° to 1765 °K, Gas from 1765 ° to 6000 °K.

m.p. = 1123" ± 10"K gfw = 40.08 Tt = 737\* = 10 \*K b, p, = 1765° ± 45°K cal/\*K gfv Kcal/efv ΔF; T, "K c, 4  $-(F_{\rm T}^{\circ} - H_{290}^{\circ})/T$ HT - H298 AH ? Leg Kp 0.000 0.000 Infinite -1.481 42, 114 34, 157 34, 107 42, 114 42, 220 42, 217 Infinite 298.15 300 4.968 36.993 37.024 36. 993 36. 993 0.000 -25,037 -24.846 400 4.968 38.453 39.562 37.188 37.556 0.506 31.426 28.786 500 1.003 41.882 -12,582 600 4.968 40.468 37, 968 1.500 - 9.538 - 7.376 41.660 26, 186 700 41.233 41.401 23.627 4.968 4.968 41.297 41.057 - 6, 728 - 6, 728 737 41.489 38. 531 2.180 22 690 2.180 22,690 800 4.968 41.897 38.780 2.493 40.874 40.528 21.127 . 5.771 900 4.968 42, 482 39.160 2.990 18.679 - 4.536 1000 4.968 43,005 39.519 3.487 40, 112 16, 273 - 3,556 1100 4.968 43,479 39.857 3.984 39.624 13.913 - 2.764 1123 4.968 43,582 39.933 4.098 39, 501 13, 376 - 2,603 1123 4.968 43,582 39, 933 4.098 37, 431 13. 376 - 2.603 1200 4.968 43,911 40, 178 4.481 37, 244 11.733 - 2.137 1300 37.000 9.616 - 1.617 1400 4.969 44.677 40.767 5.474 36, 757 7 51A - 1, 174 45.020 5.971 41.039 36,514 5.438 - 0.792 4.972 1600 45, 341 36. 271 6.468 3, 375 - 0.461 6. 966 7. 289 - 0.171 0.000 1700 4.976 45.642 41.545 36, 029 1, 327 4.980 45.827 41.696 35, 871 1765 0,000 1765 45.827 41,696 7.289 41.781 4.982 45.927 7.463 1900 4.993 46 197 42 006 7 962 2000 5.008 46.453 42. 222 8.462 2100 5.030 46.698 42.429 8.964 5.061 46, 933 47, 158 42.629 42.821 9,469 2200 2300 2400 47.377 43,006 10.489 2500 5, 219 47,588 43, 185 11,008 5.300 47, 794 43, 358 11.533 2600 2700 5. 397 2800 5,511 48.194 43.690 12.613 2900 48,390 43.848 13.171 3000 5.796 48.584 44,003 13.743 3100 5.968 4R 777 44, 154 14. 331 3200 6.160 48.969 44.301 14.937 3 300 6.371 6.601 49.162 44.446 44.587 15.563 3400 49, 355 16.212 3500 6.849 44.726 16.884 3600 7.115 49.747 44,863 17,582 7, 397 7, 692 3700 19.946 44.998 18.308 3800 50.147 45, 131 19.062 3900 8.001 50, 351 45.262 19.847 4000 8.320 45. 392 20.663 4100 50.767 45,520 4200 8.983 50,979 45,648 22, 393 4 300 9.323 51.194 45,774 4400 9.666 51,413 45, 900 24.257 4500 25.241 51,634 4600 10.353 26.259 27, 312 28, 398 4700 10.694 52.084 46, 273 4800 11.030 52, 313 46, 396 4900 11.362 52.543 46.519 29.517 5000 11.687 52.776 46.642 30,670 5100 12,004 53.011 31.855 5200 12, 313 53.247 46.887 33.070 12.612 47.009 34. 317 5 300 53,484 5400 12.902 53,723 47 132 35.593 5500 13, 181 53.962 47, 254 36.897 13.450 54,202 47.376 38,228 5600 5700 5800 13,708 13,954 54,442 54,683 47, 497 47, 619 39,586 40,970 5900 14.190 54.923 47,741 42.377 6000 14.414 55.164 47,663 43,807

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CALCIUM IDEAL MONATOMIC GAS

### SUMMARY OF UNCERTAINTY ESTIMATES

		al/ok gfu			Kcal/	-Kcal/gf=			
T,°K	c*	s <sub>T</sub>	$-(F_{T}^{\circ}-H_{298}^{\circ})/T$	H <sub>T</sub> ~ H <sub>298</sub>	VH 6	ΔF <sub>1</sub>	Log Kp		
298.15	±,000	±,002	±.002	±.000	±,250	±.300	±.220		
737	±.000	±.002	±.002	±.000	±.250	±.340	±.110		
737	±.000	±,002	±.002	±,000	±.250	±.340	±.110		
1123	±.000	±.002	±,002	±.000	.+ . 450	±.450	±.088		
1123	±.000	±.002	±.002	±.000	±.550	±.450	±.088		
1765	±.000	±.002	±.002	±.000	±.870	±.830	±.100		
1765	±.000	±.002	±.002	±.000					
2000	±.000	±.002	±.002	±.000					
3000	±.001	±,002	±.002	±.001					
4000	±.002	±.002	±.002	±.002					
5000	±.003	±.003	1.003	±.003					
6000	±.003	±.003	±.003	±.005					

#### 4. Carbon

### a. Graphite

The thermodynamic data for graphite have required extended critical review. The most recent compilations have been those of Evans <sup>156</sup> (up to 4000°K) and of Stull and co-workers <sup>75</sup> (an extension of the work of Evans up to 6000°K). The only experimental heat capacity values above 3000°K appear to be those of Rasor and McClelland. <sup>27</sup>, <sup>157</sup> This work leads to values of C ° versus T that show a very sharp rise above 3600°K and would therefore bring about marked alterations in existing thermodynamic tables for graphite if taken into account.

The rise in  $C_p^{\circ}$  versus T in question is extremely rapid and its theoretical explanation appears to be uncertain. It occurs at such a high temperature that one is led to suspect insipient sublimation.

With only the available information on hand, the preparation of a reference table would be impossible at temperatures above 3600 °K because  $C_D^{\circ}$  (T) appears to have no finite limit.

For the above reasons, condensed phase calculations on graphite were postponed until further measurements could be made and the problem given more thought. Recent studies on this project are presented in section V-B with a detailed discussion of other available data.

#### b. Monatomic Gas (C)

Thermodynamic functions for the ideal monatomic gas in Table XV were calculated using the spectroscopic energy levels listed by Moore. 52 Energy levels and J values not definitely established in these tables were estimated. The calculation was carried out using the monatomic gas machine program discussed earlier in this report. Uncertainty estimates are summarized on the back of the table.

# c. Diatomic Gas (C2)

The thermodynamic properties of  $C_2$  gas have been the subject of some disagreement for several years. 77, 158, 159 The dispute has centered about the location and number of electronic states and in particular the

<sup>156</sup>National Bureau of Standards Report 6928 (1960).

<sup>157</sup> Rasor, N.S. and J.D. McClelland, J. Phys. Chem. Solids 15, 17 (1960).

<sup>158</sup> Pitzer, K.S. and E. Clementi, J. Am. Chem. Soc. 81, 4477 (1959).

<sup>159</sup> Altman, R.L., J. Chem. Phys. 32, 615 (1960).

characterization of the ground state. The work of Ballik and Ramsay  $^{160}$ ,  $^{161}$  is now accepted, thus firmly establishing the  $^{1}\Sigma$  state as the ground state for the  $C_2$  molecule. Altman  $^{159}$  has recently calculated the thermodynamic functions of  $C_2$  gas up to  $5000^{\circ}$ K based on the observed spectroscopic constants of Ballik and Ramsay.  $^{160}$ ,  $^{161}$  More recently, Clementi  $^{162}$  has predicted the existence, location, and spectroscopic constants for several additional electronic states and has re-calculated the thermodynamic functions for  $C_2$  gas from 2000° to  $6000^{\circ}$ K taking into account all experimentally observed and estimated electronic states. The thermodynamic functions of  $C_2$  gas will be calculated using the diatomic computer program described earlier in this report with the spectroscopic data of Clementi  $^{162}$  and will be reported at a later date.

# d. Triatomic Gas (C3)

Available spectroscopic constants for  $C_3$  gas are at present estimated rather than experimentally determined values. The work of Engelke  $^{163}$  offers further evidence that the  $^{1}\Sigma$  state is the ground state of  $C_3$  as indicated by Thorn and Winslow.  $^{164}$  The fundamental frequencies were estimated by Pitzer and Clementi  $^{158}$  by analogy with the allene molecule. It should be noted that the frequencies estimated by Pitzer and Clementi  $^{158}$  are somewhat higher than those estimated earlier by Glockler.  $^{165}$  The thermodynamic properties of  $C_3$  in Table XVI were calculated using the linear polyatomic molecule computer program described earlier in this report with the following input data:

Moment of inertia =  $65.448 \times 10^{-40} \text{g cm}^2$ 

Symmetry number = 2

$$\omega_1 = 1300 \text{ cm}^{-1}$$

$$\omega_2 = 550 \text{ cm}^{-1} (2)$$

$$\omega_3 = 220 \text{ cm}^{-1}$$

Ground electronic state =  $\Sigma$ 

<sup>160</sup>Ballik, E.A. and D.A. Ramsay, J. Chem. Phys. 29, 1418 (1958).

<sup>&</sup>lt;sup>161</sup>Ballik, E.A. and D.A. Ramsay, J. Chem. Phys. <u>31</u>, 1128 (1959).

<sup>162</sup> Clementi, E., Astrophys. J. 133, 303 (1961).

<sup>163</sup> Engelke, J., U.S. AEC Report UCRL 8727 (1959).

<sup>164</sup> Thorn, R.J. and G.H. Winslow, J. Chem. Phys. 26, 186 (1957).

<sup>165</sup> Glockler, G., J. Chem. Phys. 22, 159 (1954).

afw = 12.01

		al/°K gfu			Kcal/	gf *	`
T, °E	C.	S <sub>4</sub>	-(FT -H5298)/T	H <sub>T</sub> - H <sub>298</sub>	ΔH°	$\Delta F_f$	Log J
•					·	•	
0 298.15	0.000 4.981	0,000 37,761	Infinite 37, 761	0.000			Infini
300	4.981	37.792	37. 761	0.009			
400	4.975	39, 224	37,957	0.507			
500	4.973	40, 334	38, 325	1,004			
600	4.971	41, 240	38, 738	1.502			
700	4.970	42,007	39, 152	1.999			
800	4.970	42, 670	39.551	2.496			
900	4.970	43.256	39, 931	2.993			
000	4.969	43.779	46.290	3,490			
100	4.969	44. 253	40,629	3.986			
200	4.970	44, 685	40.949	4.483			
300	4.971	45,083	41, 252	4.980			
100	4.972	45, 452	41.539	5.478			
500	4.975	45, 795	41,811	5.975			
600	4.978	46, 116	42,071	6.473			
700	4. 984	46.418	42, 317	6. 971			
800	4.990	46.703	42,553	7.469			
900	4.998	46.973	42.779	7.969			
000	5.008	47.229	42.995	8.469			
100	5.019	47.474	43, 202	8.970			
200	5, 032	47, 708	43, 402	9.473			
300	5,046	47. 932	43.594	9.977			
100	5,061	48, 147	43, 779	10,482			
300	5.077	48. 354	43, 958	10.989			
00	5.094 5.112	48, 553 48, 746	44, 131 44, 298	11.497			
00	5, 110	48, 932	44, 461	12,008 12,520			
00	5. 149	49, 112	44.618	13.034		•	
00	5, 168	49. 287	44.771	13.550			
00	5, 187	49, 457	44, 919	14.067			
00	5, 206	49,622	45,064	14.587			
100	5, 224 5, 243	49. 939	45, 204 45, 341	15, 108			
100	5, 261	50.091	45, 475	15.632 16.157			
00	5, 279	50, 239	45.605	16,684			
00	5, 296	50, 384	45, 732	17, 213			
00	5.313	50.526	45,856	17.743			
00	5.329 5.345	50.664 50.799	45, 978 46, 097	18,275 18,809			
00	5.360	50, 931	46, 213	19.344			
00	5. 375	51,061	46. 327	19.381			
00	5, 386	51, 187	46.439	20,419			
00	5,402	51, 311	46.548	20,959			
00	5,414	51, 433	46, 655	21.500			
00	5.426	51, 552	46.760	22,042			
00	5, 437	51,669	46,863	22,585			
00	5.448	51.783	46. 965	23, 129			
00	5, 459	51, 896	47.064	23,674			
00	5,468	52,006	47.162	24.221			
00	5.477	52, 115	47.258	24,768			
00	5.486	52, 221	47, 352	25, 316			
00	5.494	52, 526	47, 445	25.865			
00	5, 502	52, 428	47, 537	26.415			
00	5.509	52, 529	47,627	26.966			
00	5, 516	52, 629	47,715	27, 517			
00	5, 543	52, 726	47.802	38.069			
00	5, 529	51, 822	47.888	28,621			
00	5, 535	52, <del>9</del> 17	47, 974	29, 175			
00	5, 541	53,010	48,055	29.728			

CARBON IDEAL MONATOMIC GAS

### SUMMARY OF UNCERTAINTY ESTIMATES

		al/°K gfv			Kcal/	ri w	$\overline{}$
T,° <b>K</b>	c,	S <sup>a</sup> T	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF	Log Kp
298.15	±,000	±.002	±.002	±.000			
1000	±.000	±.002	±.002	±.000			
2000	±.000	±.002	±.002	±.000			
3000	±.000	±.002	±.002	±.001			
4000	±.000	±.002	±.002	±.001			
5000	±.000	±.002	±.003	±.001			
6000	±.000	±.002	±.003	±.001			

The input data and calculated quantities in Table XVI are identical to those recently reported by Stull and co-workers.  $^{75}\,$ 

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,		al/°K gfw			Kcsl/	/ v	
T, *K	C,	S <sub>T</sub>	$-(F_{T}^{0}-H_{298}^{0})/T$	H <sub>T</sub> - H <sub>296</sub>	AH?	ΔF	Log K
		0.000					
0 298.15	0.000 9.388	50.689	Infinite 50, 689	0.000			Infinit
300	9.407	50.748	50.690	0.017			
400	10.311	53, 583	51.070	1.005			
500	11.030	55. 964	51.817	2,073			
600	11,623	58.029	52, 684	3.207			
700	12.115	59.859	53.581	4.395			
800	12.574	61.504	54.470	5.627			
900	12.862	62.999	55, 336	6.897			
000	13, 141	64.369	56, 172	6.198			
100	12 272	48 411		0.634			
200	13.373 13.566	65. 633 66, 805	56, 975 57, 746	9,524 10.871			
300	13.727	67.898	58, 485	12, 236			
600	13,662	68,920	59.195	13.615			
500	13.977	69.880	59.875	15.008			
600	14.074	70,786	60.529	16.410			
700	14.158	71.641	61.158	17.822			
800	14.230	72, 453	61.763	19, 241			
900	14. 292	73.224	62.346	20.668			
000	14.347	73.958	62, 908	22,100			
100	14, 394	74, 659	61 481	21 517			
200	14.436	75.330	63. 451 63. 976	23.537 24.978			
900	14.473	75. 973	64.484	26.424			
100	14.506	76, 589	64.976	27.873			
300	14.536	77. 182	65.452	29. 325			
500	14.562	77.753	65.914	30.780			•
700	14.586	78.303	66. 363	32.237			
300	14.607	78, 834	66.799	33,697			
000	14.626	79.346	67, 223	35.159			
000	14.644	79.843	67, 635	36.622			
00	14.660	80 171	40 017	10 007			
100	14.674	80, 323 80, 789	68.037 68.428	38,087 39,554			
100	14,687	81.240	68.810	41.022			
100	14.700	81.679	69. 182	42.491			
100	14,711	82, 105	69.545	43.962			
		1331111	******	,			
000	14.721	82,520	69.899	45.434			
00	14.731	82. 923	70,246	46.906			
100	14.739	63.316	70.585	48.380			
00	14,748	83.699	70.916	49.854			
00	14.755	84,073	71, 241	51.329			
00	14.762	84, 437	71 554	52,805			
00	14.769	84.793	71.558 71.869	54, 282			
00	14.775	85, 141	72, 173	55. 759			
00	14,761	85.480	72.472	57, 237			
00	14.786	85, 813	72, 765	58.715			
00	14.791	86, 136	73,052	60, 194			
00	14.796	86, 456	73.334	61,673			
00	14,600	86.767	73.610	63, 153			
00	14.804	87.073	73,882	64,633			
00	14.808	87, 372	74, 149	66.114			
00	14.812	87.665	74.411	67, 595			
00	14.815	87, 953	74.669	69.076	i.		
0	14.819	86, 235	74.922	70,558			
00	14.822	68, 512	75.171	72.040			
00	14,825	88,784	75,416	73.522			
00	14.827	89.051	75.657	75.005			
00	14.830	09, 313	75.895	76.488			
00	14.833	89.571	76.128	77.971			
00	14,835	89, 825	76.358	79.454			
00	14.837	90.075	76.505	80.938			

# 5. Chromium

# a. Solid-State Transitions of Chromium

The stable form of solid chromium at 25°C is the body-centered cubic crystal.  $^{166-168}$  A transition, believed to be antiferromagnetic, occurs at  $38.5^{\circ} \pm 0.3^{\circ}$ C. A second solid-state transition, of unknown type, occurs at  $1375^{\circ} \pm 25^{\circ}$ C. The transition from body-centered cubic to face-centered cubic occurs at  $1815^{\circ} \pm 30^{\circ}$ C. The melting point of chromium is  $1875^{\circ} \pm 30^{\circ}$ C, and the estimated standard boiling point is  $2649^{\circ} \pm 200^{\circ}$ C. These transitions and their accompanying heat effects are listed in Table XVII.

### l) The 38.5°C transition

Abnormalities in several properties near 40°C were observed by a number of workers,  $^{169}$  but only recently was an anomaly in the heat capacity experimentally observed.  $^{170}$  The shape and position of the heat-capacity anomaly were consistent with those of an antiferromagnetic transition. The transition was observed to occur at 38.5°  $\pm$  0.3°C with  $\Delta H_{\rm t}$  equal to 1.4 cal/g atom and  $\Delta S_{\rm t}$  equal to 0.0044 e.u./g atom.

TABLE XVII
TRANSITION DATA FOR CHROMIUM

Transition	Temperature (°K)	ΔH <sub>t</sub> (cal/g atom)
Solid I	311.65 ± 0.3	1.4
Solid II Solid III	1648 ± 25	800 ± 200
Solid III	2088 ± 30	350 ± 100
Solid IV Liquid	2148 ± 30	4920 ± 1000
Liquid Gas	2967 ± 200	80, 220 ± 3150
Solid I — Gas	298.15	94,820 ± 500

<sup>166</sup>Fine, M.E., E.S. Greiner, and W.C. Ellis, J. Metals 191, 56 (1951).

<sup>16</sup> Sully, A.H., E.A. Brandes, and K.W. Mitchell, J. Inst. Met. 81, 585 (1953).

<sup>168</sup> Pearson, W.B. and W. Hume-Rothery, J. Inst. Met. <u>81</u>, 311 (1953).

<sup>169</sup> Sully, A.H., Chromium, Butterworths, London (1954).

<sup>170</sup>Beaumont, R.H., H.Chikera, and J.A. Morrison, Phil. Mag. 5, 188 (1960).

### 2) The 1375°C transition

The existence of a transition [Cr(II)  $\longrightarrow$  Cr(III)] at about 1400°C was indicated by the observation of an anomaly in magnetic susceptibility. <sup>171</sup> More conclusive evidence was provided by heat capacity measurements recently reported by Krauss. <sup>172</sup> The latter measurements showed a maximum in the heat capacity versus temperature curve at about 1375°C. Approximate graphical integration of the area under the observed heat capacity curve has yielded a heat of transition( $\Delta H_t$ ) value of 800 ± 200 cal/g atom. A comparison of Lucks <sup>173</sup> enthalpies measured by the drop method in this temperature range and enthalpies estimated (assuming the nonexistence of any transition) by Kelley <sup>56</sup> has led to an estimated  $\Delta H_t$  of about 800 cal/g atom. It should be noted that evidence for the existence of this transition was not observed by McCaldin and Duwez <sup>174</sup> in a thermal analysis study.

# 3) The body-centered cubic to face-centered cubic transition

The existence of the  $Cr(III) \longrightarrow Cr(IV)$  transformation was established by cooling-curve analysis. <sup>175</sup> The crystal structure of the new phase was studied by Abrahamson and Grant. <sup>176</sup> The temperature of the transition was reported to be  $1840^{\circ} \pm 15^{\circ}C$ , <sup>175</sup> but was herein revised downward since the melting point reported in the same paper was probably high. The difference between the melting-point and transition temperatures was not altered in doing this. Heat capacities have not been measured in the vicinity of this transition, and no experimental value for  $\Delta H_t$  was available. The estimate of Stull and Sinke; <sup>77</sup> i.e.,  $\Delta H_t = 350$  cal/g atom, was accepted. The uncertainty in this value was estimated to be  $\pm$  100 cal/g atom. Again, the existence of a transition at this temperature was not observed by McCaldin and Duwez. <sup>174</sup>

### 4) The melting point of chromium

Values of the melting point of chromium reported in the literature ranged from 1515° to 1903°C. 169 Even recent measurements using very pure chromium showed a considerable spread. The "best" values were the following:

<sup>171</sup> McGuire, T.R. and C.J. Kriessman, Phys. Rev. 85, 452 (1952).

<sup>172</sup> Krauss, F., Z. Metalik 49, 386 (1958).

<sup>173</sup> Lucks, C.F. and H.W. Deem, WADC Tech. Rept 55-496 (November 1955).

<sup>174</sup> McCaldin, J.O. and F. Duwez, J. Metals 6; AIME Trans. 200, 619 (1954).

<sup>175</sup> Bloom, D.S., J.W. Putman, and N.J. Grant, J. Metals 4, 626 (1952).

<sup>176</sup> Abrahamson, E.P. and N.J. Grant, J., Metals 8; AIME Trans. 206, 975 (1956).

1890 ± 10°C, <sup>177</sup>
1860 ± 10°C, <sup>178</sup>
1845 ± 10°C, <sup>179</sup>
1903 ± 10°C, <sup>175</sup>
1875 ± 5°C, <sup>180</sup>

An average of these values was chosen as the most probable melting point, i.e.,  $1875^{\circ} \pm 30^{\circ}C$ . The uncertainty was picked to include all the above values.

The heat of fusion at the melting point has also not been unambiguously established. Measured and estimated values reported include the following:

3650 cal/g atom, 181
4200 cal/g atom, 26
3300 cal/g atom, 77
4600 cal/g atom, 182
5000 cal/g atom. 56, 76

In the absence of conclusive experimental data, an estimated heat of fusion of 4920 cal/g atom was calculated from an assumed entropy of fusion of 2.3 e.u./g atom.

In view of the wide range of reported values, an uncertainty of ± 1000 cal/g atom was assigned to the heat of fusion at the melting point.

Graube, H. and R. Knabe, Z. Elektrochem. 42, 793 (1936).

<sup>178</sup> Carlile, S.J., J.W. Christian, and W. Hume-Rothery, J. Inst. Met. 16, 169 (1949).

<sup>179</sup> Greenaway, H.T., S.T.M. Johnstone, and M.K. McQuillan, J. Inst. Met. 19, 109 (1951).

<sup>180</sup> Wyman, L.L. and J.T. Sterling, Ductile Chromium and Ita Alloya, American Society for Metala, Cleveland (1957), p. 180.

<sup>&</sup>lt;sup>181</sup>Umino, S., Sci. Repts. Tohoku Imp. Univ. First Series <u>15</u>, 597 (1926).

<sup>182</sup> Kubaschewski, O. and E. Evans, Metallurgical Thermochemistry, Pergamon Press, N.Y. (1958).

# 5) The standard heat of sublimation at 298.15°K (ΔH<sub>\$298</sub>)

Vapor pressure measurements for solid chromium have been reported by several workers during the past decade. 183-189 The first four papers contained experimental vapor pressure values, whereas only vapor pressure equations were available from the other papers.  $\Delta H_{\rm S298}^{\circ}$  values, calculated using reported vapor pressure values and free-energy functions from the present compilation, were as follows:

94,710 cal/g atom, 183

95, 250 cal/g atom, 184

94,870 cal/g atom, 185

94, 750 cal/g atom, 187

94,530 cal/g atom. 188

An average value of  $\Delta H_{s298}^{o}$  = 94,820 ± 500 cal/g atom was chosen. The vapor pressure measurements of Nesmeyanov and Man, <sup>186</sup> and of Burlakov, <sup>189</sup> lead to appreciably lower  $\Delta H_{s298}^{d}$  values, and were not included.

# 6) The boiling point of chromium

A value of 2200°C was reported by Greenwood 190 for the boiling point of Cr, but it was considered to be low by later workers. 77, 191 Baur and Brunner 92 have calculated a value of 2660°C from vapor pressure measurements. Later workers 76, 77 have estimated the boiling point from calculated values of  $\Delta H_{v0}^{o}$  or  $\Delta H_{v298}^{o}$  and free-energy functions for the gas and the condensed phase (i.e., the standard boiling temperature was taken as the temperature at which  $\Delta F$  becomes zero for the change from condensed phase to gaseous phase).

<sup>&</sup>lt;sup>183</sup>Speiser, R., H.L. Johnston and P. Blackburn, J. Am. Chem. Soc. <u>72</u>, 4142 (1950).

<sup>184</sup>Gulbransen, E.A. and K.F. Andrew, J. Electrochem. Soc. 99, 402 (1952).

<sup>185</sup> McCabe, C.L., R.G. Hudson, and H.W. Paxton, Trans. Am. Inst. Mining. Met. Petrol. Engrs. 212, 102 (1958).

<sup>186</sup> Nesmeyanov, A. and D. Man. Proc. Acad. Sci. (U.S.S.R.), Phys. Chem. Sec. (English Transl.) 131, 373 (1960).

 $<sup>^{187}</sup>$ Kubaschewaki, O. and G. Heymer, Acta. Met.  $\underline{8}$ , 416 (1960).

<sup>188</sup> Vintaiker, E.Z. Proc. Acad. Sci. (U.S.S.R.), Phys. Chem. Sec. (English Transl.) 129, 951 (1959).

<sup>189</sup> Burlakov, V.D., Fiz. Metal. i. Metalloved. 5, 91 (1957).

<sup>&</sup>lt;sup>190</sup>Greenwood, H.C., Proc. Roy. Soc. A82, 396 (1905).

<sup>&</sup>lt;sup>191</sup>Kelley, K.K., U.S. Bur. Mines Bull. 383 (1935).

Stull and Sinke  $^{77}$  thus calculated a value of 2642°C, and Hultgren  $^{76}$  calculated a value of 2665°C. For the present compilation, a boiling point of 2694°  $\pm$  200°C was adopted. The  $\Delta H$  of vaporization could then be estimated from the value of  $\Delta H_{298}^{\circ}$  and the enthalpy functions for the two phases at the standard boiling point. A value of  $\Delta H$  of vaporization at the standard boiling point of 80, 220  $\pm$  3150 cal/g atom was thus calculated in the present work.

b. Thermodynamic Functions for the Condensed Phases of Chromium

Recent compilations of the thermodynamic functions of solid and liquid chromium included those of Stull and Sinke, <sup>77</sup> Hultgren, <sup>76</sup> and Kelley. <sup>56</sup> Stull and Sinke used a rather low value for the  $\Delta H$  of fusion and did not include the solid-solid transformations at 38.5° and 1375°C. The other two compilations did not include the solid-solid transformations at 38.5°, 1375°, and 1815°C. The values of enthalpy and entropy at 298.15°K listed by Hultgren were accepted in the present work.

$$H_{298}^{\circ} - H_{0}^{\circ} = 970 \text{ cal/g atom,}$$

$$S_{208}^{\circ} = 5.68 \text{ e.u./g atom.}$$

The enthalpy functions for solid chromium (i.e.,  $H_T^\circ - H_{298}^\circ$ ) in Table XVIII were those of Kelley,  $^{56}$  corrected to include the various transitions given in Table XVII. The tabular entropy values for solid chromium were calculated by the method of Kelley.  $^{56}$  Uncertainty estimates are are summarized on the back of Table XVIII.

Values for the 
$$-\left(\frac{F_T^{\circ} - H_{298}^{\circ}}{T}\right)$$
 function of solid chromium were calculated

from equation (108).

Heat capacity values for solid chromium were not well established (see section IV-A5d below), and very limited data were available near the various transitions. 170, 172 Tabular values of  $C_{p}^{\circ}$  for solid chromium were therefore calculated from Kelley's equation. 56 These calculated values represented experimental values fairly accurately except in transition regions where experimental data were nonexistent or insufficient for complete evaluation.

The value of the heat capacity of liquid chromium was taken to be constant at 9.40 cal/ $^{\circ}$ K g atom $^{56}$ ,  $^{76}$  even though the only experimental determination of  $C_p^{\circ}$  on liquid chromium yielded a value of 9.7 cal/ $^{\circ}$ K g atom,  $^{181}$  because the chromium used in this single experimental determination must be considered to have been impure since the observed melting

point was about  $350^{\circ}$ C lower than the "true" value. Entropy values for liquid chromium were calculated, using the value of 9.40 cal/  $^{\circ}$ K g atom for  $C_{p}^{\circ}$ , according to the equation

$$S_T^o = C_p^o \ln T + C_1$$
 (138)

H<sub>T</sub>- H<sub>208</sub> values for liquid chromium were calculated from the equation

$$H_T^{\circ} - H_{298}^{\circ} = C_p^{\circ} T + C_2$$
 (139)

The values of the constants,  $C_1$  and  $C_2$ , in the above equations were evaluated from the tabular values of  $S_T^\circ$  and  $H_T^\circ - H_{298}^\circ$  for liquid chromium at the melting point. The free-energy function for liquid chromium was evaluated in the same manner as that used for solid chromium.

### c. Thermodynamic Functions for Gaseous Chromium

Thermodynamic properties for the ideal monatomic gas given in Table XIX were calculated using the spectroscopic energy levels listed by Moore.  $^{52}$  Energy levels and values not definitely established in these tables were estimated. The equations employed in these calculations have been summarized in two recent publications  $^{51}$ ,  $^{75}$  (see Sect. III-D). Uncertainty estimates are summarized on the back of Table XIX.  $\rm H^{208}_{208} - \rm H^{0}_{O}_{O}_{C}$  found to be 1481 cal/mole.

 $\Delta H_f^o$  ,  $\Delta F_f^o$  , and  $L\circ g_{10}\,K_p$  for gaseous chromium were calculated by means of the equations in section III-D1g.

# d Uncertainties in Condensed Phase Functions

The available basic data for chromium included both heat capacity 170, 172, 192, 193 and enthalpy 173, 181, 194, 195 values. The error analysis used was based on the uncertainty of the C  $_{\rm p}^{\circ}$  data, as explained in section III-Gld.

### 1) Heat capacity

Sully 169 has critically reviewed reported  $\frac{C_p}{p}$  values near room temperature and concluded that their accuracy was about  $\pm 3$  percent. A graphical comparison in this work also led to about the same uncertainty. The uncertainty in  $\frac{C_p}{p}$  at 298.15°K was thus

<sup>[107]</sup> Anderson, C.T., J. Am. Chem. Soc. 59, 488 (1937).

<sup>&</sup>lt;sup>193</sup> Armstrong, L.D. and H. Gravson-Smith, Can. J. Phys. 28A, 51 (1950).

<sup>1991</sup> ust, L., A. Meuthen and R. Durrer, Forsch, Arb. Ver. Deut. Ing., Nr. 204 (1918).

<sup>1938</sup> Luczer, F.M. and F. Rosenbohn, Proc. A. ad. Sci. (Amsterdam) 37, 489 (1934).

Reference State for Calculating ΔH°, ΔF°, and Log Kp : Solid from 298.15° to 2148°K, Liquid from 2148° to 2967°K, Gas from 2967° to 6000°K.

 $gfw = 52,01 - T_t(I) = 311,65 \, ^*\pm 0,3 \, ^*K - T_t(II) = 1648 \, ^*\pm 25 \, ^*K - T_t(III) = 2088 \, ^*\pm 30 \, ^*K - m,p, = 2148 \, ^*\pm 30 \, ^*K - b,p, = 2967 \, ^*\pm 200 \, ^*K - m,p, = 2148 \, ^*\pm 30 \, ^*K - b,p, = 2967 \, ^*\pm 200 \, ^*K - m,p, = 2148 \, ^*\pm 30 \, ^*K - m,p, = 2148 \, ^*K - m,p, = 214$ 

T, °K	C <sub>p</sub>	I/°K gfv ──	$-(F_{T}^{o}-H_{290}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	AH of	$\Delta F_{I}^{\circ}$	Lag
0	0.000	0.000	Infinite	-0.970			
298.15	5.577	5.680	5.680	0.000			
300	5.579	5.714	5.681	0.010			
311.65	5.597	5.934	5.687	0.077			
311.65	5.597	5.938	5. 687	0.078			
400	5.800	7.400	5.913	0.595			
500	6.090	8.794	6.354	1.220			
600	6.415	9.978	6.861	1.870			
700	6.755	10.995	7,380	2.530			
800	7.103	11.902	7.890	3.210			
900	7.455	12.726	8.382	3.910			
.000	7.810	13.495	8.855	4. 640			
100	8.167	14. 229	9.310	5.410			
200	8.525	14.942	9.750	6. 230			
300	8.884	15.638	10.177	7.100			
400	9.243	16.312	10.591	8.010			
500	9.603	16.961	10.994	8.950			
600	9.964	17.587	11.387	9.920			
648	10.137	17.882	11.571	10.400			
648	10. 137	18.368	11.571	11. 200			
700	10.324	18.684	11.784	11.730			
800	10.685	19.284	12.184	12.780			
900	11.046	19.879	12.573	13.880			
000	11.408	20.463	12.953	15.020			
	11 537	30.077	12 201	14 040			
088	- 11.726	20.975 21.142	13. 281	16. 065 16. 415			
100	11.769	21. 212	13.327	16.560			
148	_ 11.942	21. 486	13.517	17.117			
148	9.400	23.786	13.517	22. 057			
200	9.400	24.011	13.763	22. 545			
300	9.400	24. 429	14. 218	23. 485			
400	9.400	24.829	14.652	24. 425			
500	9.400	25. 213	15.067	25. 365			
600	9.400	25.581	15.464	26.305			
700	9.400	25.936	15.845	27. 245			
800	9.400	26. 278	16.212	28.185			
900	9.400	26.608	16.565	29.125			
967	9.400	26.822	16.794	29.755			
967	7.317	53.861	16.794	109.974			
000	7. 359	53.943	17. 204	110.216			
100	7.481	54.186	18.393	110.958			
200	7.599	54. 425	19.515	111.712			
300	7.713	54.661	20.577	112.478			
400	7.825	54.893	21.583	113.255			
500	7.935	55. 121	22.537	114.043			
300	1.733	33.161	22, 331	114.045			
600	8.045	55.346	23.445	114.842			
700	8.157	55.568	24.311	115.652			
800	8.270	55. 787	25.136	116.473			
900	8.386	56.004	25.926	117.306			
000	8.506	56. 217	26.679	118.151			
100	8.631	56. 429	27. 402	119.008			
200	8.761	56.638	28.096	119.877			
300	8.896	56.846	28.762	120.760			
400	9.036	57.052	29.403	121.657			
300	9, 183	57. 257	30.020	122.567			
600	9.335	57.460	30.614	123.493			
700	9.492	57.663	31.187	124, 435			
800	9.654	57.864	31.741	125.392			
900	9.821	58.065	32. 276	126.366			
000	9.992	58. 265	32.794	127.356			
100	10.175		11 304	120 244			
100	10.167	58. 465	33. 296	128.364 129.390			•
200	10.344	58.664	33.781 34.253				
300	10.524	58.863		130, 433			
400 500	10.705 10.887	59.061 59.259	34.710 35.155	131. 495 132. 574			
	10.00	3,. 637	,,,,,	1.2.3.4			
600	.1.069	59.457	35.587	133.672			
700	11.250	59.655	36.008	134.788			
800	11.429	59.852	36.417	135.922			
900	11.605	60.049	36.816	137.074			
000	11.779	60. 245	37. 204	138.243			
000							

CHROMIUM REFERENCE STATE

### SUMMARY OF UNCERTAINTY ESTIMATES

		al/°K gfv			Kcal/	ef =	_
T, °E	C <sub>p</sub>	S.T	$-(F_{T}^{o}-H_{298}^{n})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>n</sup>	ΔF <sub>1</sub>	Log Kp
298.15	± .200	± .070	± .070	± .000			
311.65	± .200	± .080	± .070	± .003			
311.65	± .200	± .080	± .070	± .003			
1000	± .700	± .600	± .290	± .310			
1648	±1.200	±1.070	± .510	± .930			
1648	±1.200	±1,140	± .510	±1.130			
2000	±1.200	£1.420	± .640	±1.550			
2088	±1.200	±1.470	± .680	±1.660			
2088	±1.200	±1.520	± .680	±1.760			
2184	±1.200	±1.550	± .700	±1.830			
2184	±1.000	± 2. 020	± .700	± 2.830			
2967	±1.000	± 2. 340	±1.450	± 2.650			
2967	± .000	± .003					
3000	± .001						
4000	± .001	± .003					
5000	± .002	± .003					
6000	± .002	± .003					

IDEAL MONATOMIC GAS

Cr

Reference State for Calculating  $\Delta H_{\gamma}^{o}$ ,  $\Delta F_{\gamma}^{o}$ , and  $L_{og} K_{p}$ : Solid from 298.15° to 2148°K, Liquid from 2148° to 2967°K, Gas from 2967° to 6000°K.

 $g(\mathbf{w} = 52, 0! - T_t(I) = 311, 65^* \pm 0, 3^*K - T_t(II) = 1648^* \pm 25^*K - T_t(III) = 2088^* \pm 30^*K - m, p. = 2148^* \pm 30^*K - b, p. = 2967^* \pm 200^*K - m, p. = 2148^* \pm 30^*K - b, p. = 2967^* \pm 200^*K - m, p. = 2148^* \pm 30^*K - b, p. = 2967^* \pm 200^*K - m, p. = 2148^* \pm 30^*K - m, p. = 2148^* \pm 30^*K - b, p. = 2967^* \pm 200^*K - m, p. = 2148^* \pm 30^*K - m, p. = 214$ 

T, °K	C <sub>p</sub>	/°K et∙ St	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH °	ΔF	Log K
0			Infinite	-1.481	94. 309	94.309	Infini
	0.000	0.000	41.637	0.000	94.820	84.099	-61.6
298.15	4.968	41.637					
300	4.968	41.668	41.637	0.009	94.819	84. 033	-61.2
311.65	4. 968	41.857	41.642		94.810	83.615	-58.6
311.65	4.968	41.857	41.642	0.067	94.809	83.615	-58.6
400	4.968	43.097	41.832	0.506	94.731	80.452	-43.9
500	4.968	44. 205	42. 200	1.003	94.603	76.897	-33.6
	4 045	45 111	42 (12	1 500	04.450	73 740	26 7
600	4.968	45.111	42.612	1.500	94.450	73.369	-26.7
700	4.968	45.877	43.025	1.996	94. 286	69.868	-21.8
800	4,969	46,541	43.424	2. 493	94. 103	66.393	-18.1
ġ00	4.972	47.126	43.803	2.990	93.900	62.942	-15.2
000ر	4.980	47.650	44. 162	3.488	93.668	59.513	-13.0
	4.00/	10 126	44. 501	2 000	01 105	66 100	
001	4.996	48.126		3.987	93.397	56.109	-11.1
200	5. 023	48.561	44.822	4.487	93. 077	52.734	-9.6
300	5.065	48.965	45.125	4.992	92.712	49.387	-8.3
400	5. 125	49.342	45. 413	5.501	92.311	46.070	-7.1
500	5.203	49.698	45.687	6.017	91.887	42.780	-6.2
600	5.300	50.037	45.948	6.542	91.442	39.523	-5.3
648	5, 353	50, 195	46.070	6.798	91.218	37.965	-5.0
648	5.353	50.195	46.070	6.798	90.418	37.965	-5.0
700	5.414	50.362	46. 199	7.078	90.168	36.314	-4.6
800	5.545	50.675	46.439	7.626	89.666	33.161	-4.0
900	5.688	50,979	46.670	8.187	89.127	30.035	-3.4
000	5.841	51.274	46.892	8.763	88.563	26. 222	- 2. 8
088	5.982	51.529	47.082	9.284	88.039	24. 244	-2.5
088	5.982	51.529	47.082	9. 284	87.689	24. 244	-2.5
100	6.001	51.563	47.108	9.356	87.616	23.879	-2.4
148	6.080	51.700	47. 209	9.646	87.349	22.449	-2.2
148	6. 080	51.700	47. 209	9.646	82.409	22.449	-2.2
200	6. 165	51.846	47.317	9.964	82. 239	21.001	-2.0
300	6.330	52.124	47.520	10.589	81.924	18. 225	-1.7
400	6. 493	52. 397	47.717	11. 230	81.625	15.463	-1.4
500	6,652	52.665	47.910	11.887	81.342	12.713	-1.1
,,,,	0.076	JE: 003	111710	11.301	31.314		1
600	6.806	52.929	48.098	12.560	81.075	9.971	-0.8
700	6.954	53. 188	48. 282	13. 248	80. 823	7. 241	-0.5
300		53. 444	48.462	13.951	80.586	4.519	-0.3
900	7.095		48.638	14.667	80.362	1.810	-0.3
	7. 230	53.695		15.154		0.000	0.0
967	- 7.317	53.861	48.754		80.219	V. 000	0.0
967	7.317	53.861	48.754	15. 154			
000	7.359	53.943	48.810	15.396			
100	7.481	54.186	48.980	16.138			
200	7.599	54. 425	49.146	16.892			
300	7.713	54.661	49.310	17.658			
100	7.825	54.893	49.471	18.435			
500	7.935	55.121	49.629	19.223			
			40 -0-	10.01-			
500	8.045	55. 346	49.785	20.022			
700	8.157	55.568	49.938	20.832			
300	8.270	55. 787	50.089	21.653			
00	8.386	56.004	50. 238	22.486			
000	8.506	56. 217	50.385	23.331			
00	8.631	56. 429	50.529	24.188			
200	8.761	56.638	50.672	25.057			
300	8.896	56.846	50.814	25.940			
00	9.036	57.052	50.953	26.837			
00	9.183	57. 257	51.091	27.747			
00	9, 135	57.460	51.227	28.673			
00	9.492	57.663	51.362	29.615			
100	9.654	57.864	51.495	30.572			
00	158.9	58.065	51.627	31.546			
000	9,992	58. 265	51.758	32.536			
00	10.167	58.465	51.888	33,544			
00	10.344	58.664	52.016	34.570			
00	10.524	58.863	52.143	35.613			
00	10.705	59.061	52.270	36.675			
00	10.887	59. 259	52. 395	37.754			
00	11.069	59.457	52.519	38.852			
00	11. 250	59.655	52.641	39.968			
	11.429	59.852	52. 765	41.102			
0.0			A	<del>-</del>			
00		60.049	52.887	42, 254			
00	11.605	60.049	52.887 53.008	42, 254 43, 423			

CHROMIUM IDEAL MONATOMIC GAS

### SUMMARY OF UNCERTAINTY ESTIMATES

	cal/°K afv				Kcal/gfv		_	
7,°K	c*	ST	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH o	ΔF	Log Kp	
298.15	±.000	±.002	±.002	±.000	± .500	÷ .520	±.380	
311.65	±.000	±.002	±.002	±.000	± .500	± .520	±.360	
311.65	±.000	±.002	±.002	±.000	± .500	± .520	±.360	
1000	±.000	±.002	±.002	±.000	± .810	± .790	±.170	
1648	±.000	±.002	±.002	±.000	±1.430	±1.340	±.180	
1648	±.000	±.002	±.002	±.000	±1.630	£1.340	±.180	
2000	±.001	±.002	±.003	±.000	± 2. 050	±1.790	±.200	
2088	±.001	±.002	±.003	±.000	± 2. 160	±1.930	±.200	
2088	±.001	±.002	±.003	±.000	± 2, 260	±1.930	±.200	
2148	±.001	±.002	±.003	±.001	± 2.330	± 2, 010	±.200	
2148	±.001	±.002	±.003	±.001	±3.330	±2.010	±.200	
2967	±.001	±.003	±.003	±.001	±3.150	±4.810	±.350	
2967	±.001	±.003	±.003	±.001				
3000	±.001	±.003	±.003	±.001				
4000	±.001	±.003	±.003	±.002				
5000	±.002	±.003	±.003	±.003				
6000	±.002	±.003	±.003	±.005				

taken to be  $\pm$  0.2 cal/°K g atom. The uncertainty was taken to be the same at the first transition point of 311.65°K. An uncertainty of  $\pm$  0.7 cal/°K g atom was estimated from a comparison of reported values near 1000°K. 172, 173, 181, 193, 195 The uncertainty at the 1648°K transition point was difficult to assign since direct C°values have been reported in only one paper, 172 and other workers 173, 181, 194 have measured enthalpies which included or partially included the heat of transition. The uncertainty was therefore increased to  $\pm$  1.2 cal/°K g atom at 1648°K.

The only measurements above  $1800\,^{\circ}\text{K}$  were those of Umino  $^{181}$  made on impure chromium. In the absence of experimental  $C_p^{\bullet}$  values, the uncertainties at  $2000\,^{\circ}$ ,  $2088\,^{\circ}$ , and  $2148\,^{\circ}\text{K}$  were assumed to be the same as the uncertainty at  $1648\,^{\circ}\text{K}$ ; i.e.,  $\pm 1.2\,$  cal/ $^{\circ}\text{K}$  g atom. As stated earlier, the  $C_p^{\circ}$  of liquid chromium was measured by only one worker  $^{181}$  using impure chromium; an uncertainty of  $\pm 1.0\,$  cal/ $^{\circ}\text{K}$  g atom was therefore arbitrarily assigned over the whole liquid range.

### 2) Entropy

Uncertainties in entropy values were calculated from assigned uncertainties in  $C_p^\circ$  values and heats of transition as explained in Section IV-Gld. The uncertainty in  $S_{298}^\circ$  was taken to be  $\pm 0.07$  e.u./g atom after Kelley.  $^{139}$ 

# 3) Enthalpy

Uncertainties in enthalpy values were calculated from  $C_p^\circ$  uncertainties and assigned values of  $\Delta H$ -of-transition uncertainties as explained in section III -Gld. The equations used for single-phase regions and transitions were as follows:

$$h_{T_2} = h_{T_1} + \delta C_p^o (T_2 - T_1) , \qquad (140)$$

$$h_{B} = h_{A} + \delta \Delta H_{t} . \tag{141}$$

### 4) Free energy

The uncertainty in the free-energy function was calculated from calculated uncertainties in  $S_T^o$  and  $H_{T}^{\bullet}$ -  $H_{298}^o$  using equations (119) and (120).

### e. Uncertainties in Gas-Phase Functions

Uncertainty estimates for the calculated thermodynamic functions of the ideal monatomic gas were made with the machine program described in section III and are summarized on the back of Table XIY. f. Other References Pertaining to the Thermodynamics of Chromium

Sully 169 has reviewed other heat capacity measurements not previously mentioned in the present discussion. His review included the work of Dewar, 196 Richards and Jackson, 197 Nordmeyer and Bernoulli, 198 Lammel, 199 Schimpff, 200 Schubel, 201 and Mache. 202

Heat capacity measurements at very low temperatures (below 20°K) have been reported and discussed by Rayne and Kemp, <sup>203</sup> Wolcott, <sup>204</sup> Friedberg, Estermann, and Goldman, <sup>205</sup> and Estermann, Friedberg, and Goldman. <sup>206</sup>

Transitions in solid chromium have been reviewed by Sully,  $^{169}$  and discussed more recently by Pursey $^{207}$  and by Beaumont and co-workers. $^{170}$  The possible existence of a hexagonal modification of chromium has been discussed by Sully,  $^{169}$  and in more recent papers; e.g., Brummer and Suwalski.  $^{208}$ 

A useful annotated bibliography of thermal properties of chromium was that of Goodwin.  $^{209}$  A recent review of the properties of high-purity chromium was that of Edwards, Nish, and Wain.  $^{210}$ 

<sup>196</sup> Dewar, J., Proc. Roy. Soc. A89, 158 (1913).

<sup>197</sup> Richards, T.W. and F.G. Jackson, Z. Phys. Chem. 70, 414 (1910).

<sup>198</sup> Nordmeyer, P. and A.L. Bernoulli, Ber. <u>6,</u> 175 (1907).

<sup>199</sup> Lammel, R., Ann. Phys. Lpz. 16, 551 (1905).

<sup>&</sup>lt;sup>200</sup>Schimpff, H., Z. Phys. Chem. <u>71</u>, 257 (1910).

<sup>&</sup>lt;sup>201</sup>Schubel, P., Z. Anorg. Chem. <u>87</u>, 81 (1914).

<sup>202</sup> Mache, H., Akad. Wiss. Wien 106, 590 (1897).

<sup>203</sup> Rayne, J.A. and W.R. G. Kemp, Phil. Mag. 1, 918 (1956).

<sup>204</sup> Wolcott, N.M., Bull. Inst. Intern. Froid Annexe (1955), p. 286.

<sup>205</sup> Friedberg, S.A., I. Estermann, and J.E. Goldman, Phys. Rev. <u>85</u>,375 (1952).

<sup>206</sup> Estermann, I., S.A. Friedberg, and J.E. Goldman, Phys. Rev. 87, 582 (1952).

<sup>&</sup>lt;sup>20</sup> Pursey, H., J. Inst. Met. <u>86</u>, 362 (1958).

<sup>208</sup> Brummer O. and Suwalski, G. Naturwissenschaften 46, 223 (1959).

<sup>209</sup> Goodwin, T.C. and M.W. Ayton, WADC TR-56-423, AD-111-846 (August 1956).

<sup>&</sup>lt;sup>210</sup>Edwards, A.R., J.I. Nish, and H.L. Wain, Met. Revs. 4, 403 (1959).

# 6. Hafnium

### a. Selection of Condensed Phase Data

# 1) Crystal structure and solid-state transition

Hafnium exists in two known crystalline modifications. <sup>211</sup> The ordinary room-temperature form has a hexagonal, close-packed structure, while the high temperature form has a body-centered cubic structure.

The transition temperature for equilibrium between the two crystalline modifications was taken to be 2033°  $\pm$  35° K, as found by Deardorff and Kato, <sup>212</sup> and accepted by Thomas and Hayes. <sup>211</sup> Other reported values mentioned by Hansen<sup>213</sup> are as follows:

Temp. (° K)	Source		
1603-1903	Zwikker <sup>214</sup>		
1583	Duwez215		
2223 ± 100	Fast <sup>216</sup>		
1973	Hansen and Anderko <sup>213</sup>		

It is noteworthy that the value chosen by Hansen and Anderko<sup>213</sup> does not differ markedly from the one chosen here which is based on newer data.

# 2) Melting point

A temperature of 2495° ± 30° K was accepted as the melting point for hafnium metal. This value is based on the work of Deardorff and Hayes, <sup>217</sup> and has been accepted by Thomas and Hayes. <sup>211</sup> Earlier data have been reviewed by Stull and Sinke <sup>77</sup> who chose a value of 2250° K. The more recent value recommended herein appears to be preferable.

<sup>211</sup> Thomas, D.E. and E.T. Hayes, The Metallurgy of Hafnium, U.S. AEC (1960).

<sup>212</sup> Deardorff, D.K. and H. Kato, The Transformation Temperature of Hafnium, USBM-U-426 (8 April 1958).

<sup>213</sup> Hansen, M. and K. Anderko, Constitution of Binary Alloys, McGraw-Hill, N.Y. (1958).

<sup>214/</sup>wikker, C., Physics 6, 361 (1936).

<sup>215</sup> Duwez, P., J. Appl. Phys. 22, 1174 (1951).

<sup>216</sup> Fast, J.D., J. Appl. Phys. 23, 350 (1952).

<sup>217</sup> Deardorff, D.K. and E.T. Hayes, Melting point determinations of hafnium metal, Trans. AIME 206, 509 (1956).

### Heat of transition

No experimental data were available for the heat of transition of Hf. Stull and Sinke  $^{77}$  combined the heats of transition and melting into a single quantity. For the present case, it was calculated from an entropy of transition estimated from those of titanium and zirconium (i.e., 0.822 and 0.806 e.u., respectively). The intermediate value of 0.811 e.u. was chosen for Hf, resulting in a heat of transition of  $1650 \pm 200$  cal/mole at  $2033^{\circ}$  K.

### 4) Heat of fusion

The heat of fusion of Hf also had to be estimated. For titanium, the entropy of fusion was taken to be 2.10 e.u. This same value was used for Hf along with a melting point of 2495° K to give a  $\Delta$  Hfusion value of 5239  $\pm$  1000 cal/mole. This value of the heat of fusion agrees well (probably fortuitously) with that of Stull and Sinke,  $^{77}$  who included the heat change associated with the transition to obtain a contribution of  $\Delta$  Hfusion = 5200 cal/g atom.

# 5) Low-temperature heat capacity and S<sub>298</sub>

Heat capacity data for the temperature range from 10° to 200° K have been reported by Burk et al. <sup>218</sup> For the range from 25° to 100° C, Adenstedt<sup>219</sup> has reported an average value of  $\overline{C_p^o}$  = 6.27 cal/° K g atom. From the rate of change of  $C_p^o$  with temperature given by Stull and Sinke, <sup>77</sup> values of  $C_p^o$ , 298° K = 6.225 cal/° K g atom,  $C_p^o$ , 375° K = 6.315 cal/° K g atom, and  $C_p^o$ , 400° K = 6.345

cal/° K g atom were calculated with Adenstedt's  $^{219}$  data. These values have been used with the data of Burk et al<sup>218</sup> to determine that  $\rm H^{\circ}_{298}$  -  $\rm H^{\circ}_{0}$  = 1.428 Kcal/g atom and  $\rm S^{\circ}_{298}$  = 10.666 e.u. This value of  $\rm H^{\circ}_{298}$  -  $\rm H^{\circ}_{0}$ , obtained by graphical integration, agreed well with a trapezoidal rule integration value of 1.429 Kcal/g atom. The entropy value was obtained by graphical integration of  $\rm C^{\circ}_{p}/T$  versus T data. The values of  $\rm H^{\circ}_{298}$  -  $\rm H^{\circ}_{0}$ , and  $\rm S^{\circ}_{298}$  found by Stull and Sinke  $^{77}$  were 1.448 Kcal/g atom and 10.91 e.u. respectively.

#### 6) High-temperature heat capacity

Experimental heat capacity data for elemental hafnium at elevated temperatures were not available. Accordingly, values were

<sup>218</sup> Burk, D.L., I. Estermann, and S. Friedberg, Z. physik, chem. Neue Folge 16, 183 (1958).

<sup>&</sup>lt;sup>219</sup>Adenatedt, H.K., Trans ASM <u>44</u>, 949 (1952).

estimated with the help of data on titanium and zirconium. C<sup>o</sup><sub>p</sub> data given by Kelley<sup>56</sup> for zirconium and titanium were plotted against temperatures with the hafnium data from Stull and Sinke. The final choice was a set of data intermediate between the Ti, Zr, and Hf data. This corresponded to a line parallel to and about 0.18 cal/° K g atom above the Stull and Sinke data, but joining smoothly with the low temperature data discussed in Section IV-A6 above.

### 7) Heat of vaporization

Direct experimental values for the heat of vaporization were not known. However, Lewis and Randall<sup>220</sup> have tabulated a value of  $168 \pm 10$  Kcal/g atom. This value is the one used by Stull and Sinke<sup>77</sup> and was accepted here.

# 8) The liquid heat capacity

For temperatures above the accepted melting point, the liquid heat capacity was estimated to be 8.0 cal/°K g atom. This is the value used by Stull and Sinke. 77

### 9) Calculation of the reference-state table

The data used in the reference-state calculations for Table XXI are given in Table XX which provides a convenient summary of the "best" property values. Uncertainty estimates are summarized on the back of Table XXI.

### b. Selection of Data for the Ideal Monatomic Gas

The energy levels given by Moore, <sup>221</sup> based on the work of Meggers, <sup>222</sup> were used to calculate the values of the ideal monatomic gas thermodynamic functions in Table XXII.

The values in Table XXII should be regarded as tentative, even though they supersede those of Stull and Sinke,  $^{77}$  because Meggers  $^{223}$  has found 29 new even and 32 odd levels since his earlier work,  $^{221}$ ,  $^{222}$  The table will be brought up to date as soon as Megger's new energy levels become available. The value of  $^{4298}$  -  $^{480}$  was found to be 1, 481 cal/mole. Error estimates are summarized on the back of the table.

<sup>220</sup> Lewis, G.N., M. Randall, K. Pitzer and L. Brewer, Thermodynamics, 2nd ed. Mc Graw-Hill, N.Y. (1961).

<sup>221</sup> Moore, C., Nat. Bur. Stds. Circ. 467, vol. 3 (1 May 1958).

<sup>222</sup> Meggers, V.F., J. Research Nat. Bur. Stds. 61, 269 (1958).

<sup>223</sup> Meggers, W.F., Private Communication (7 April 1961).

 $\frac{\mathtt{TABLE}\ \mathtt{XX}}{\mathtt{SUMMARY}\ \mathtt{OF}\ \mathtt{HAFNIUM}\ \mathtt{DATA}}$ 

Quantity	· Units	Value
T <sub>t</sub> (transition temp.)	* K	2033 ± 35
$\Delta H_{t}$ (heat of transition)	Kcal/gfw	1.650 ± 0.200
Melting point	° K	2495 ± 30
$\Delta H_{f m}$ (heat of fusion)	Kcal/gfw	5.239 ± 1.000
S°298 (solid)	e.u.	10.666 ± 0.10
$\Delta H_{\mathbf{v}}$	Kcal/gfw	159.248
T <sub>b</sub> (boiling point)	° K	5536.37
ΛH° 298	Kcal/gfw	168.000 ± 10.000
H° - H° (solid)	Kcal/gfw	1.428 ± 0.010

### REFERENCE STATE

Reference State for Calculating ΔHJ, ΔFJ, and Log K<sub>p</sub>: Solid from 298.15° to 2495°K, Liquid from 2495° to 5536°K, Gae from 5536° to 6000°K.

T 0=		cal/°K gfv ———	(F°° . –	u°°	——— Keal/gfs ΔΗβ	ΔF	las F
T, °E	C <sub>p</sub>	S <sup>e</sup> t	$-(F_{T}^{o} - H_{298}^{e})/T$	$H_T^0 - H_{290}^0$	ΔH I	. AF I	Log Kp
0	0.000	0.000	Infinite	-1.428			
298.15	6. 225	10.666	10.666	0.000			
300 400	6. 226	10.705	10.666	0.012			
500	6.345 6.466	12.504 13.936	10.907 11.377	0.639 1.280			
300	3. 400	13.730	11.377	1. 200			
600	6.583	15.127	11.906	1.932			
700	6. 701	16.151	12.442	2, 596			
800	6.815	17.054	12.963	3.272			
900	6.925	17.863	13.464	3.959			
1000	7.045	18.599	13.941	4.658			
1100	7.164	19. 276	14.396	5.368			
200	7. 284	19.904	14.829	6.090			
1300	7. 399	20.492	15. 242	6.825			
1400	7.518	21.045	15.637	7.570			
1500	7.640	21.568	16.015	8.328			
600	7.765	22.065	16.378	9.099			
700	7.885	22.539	16.727	9.881			
800	8.005	22.993	17.062	10.676			
900	8.126	23.429	17.386	11.482			
000	8. 248	23.849	17.699	12.301			
:033	8. 288	23.984	17.800	12.574			
:033	8. 295	24.796	17.800	14. 224			
100	8.378	25.066	18.027	14.782			
200	8.501	25. 459	18.356	15.626			
300	8.623	25.840	18.673	16.482			
400	8.745	26. 212	18.980	17.358			
495	- 8.861 -	26, 653	19. 261	18.442			
1495 1500	8.000 8.000	28.753 28.769	19.261 19.280	23.681			
600	9 000	20 093	10 451	24. 521			
700	8.000 8.000	29.083 29.385	19.651 20.006	25. 321			
800	8.000	29.676	20. 346	26. 121			
900	8.000	29.956	20.673	26.921			
000	8.000	30. 227	20.987	27.721			
100	8.000	30.490	21.289	28. 521			
200	8.000	30.744	21.581	29. 321			
300	8.000	30.990	21.862	30.121			
400	8.000	31.229	22. 134	30.921			
500	8.000	31.461	22.397	31.721			
600	8.000	31.686	22.652	32.521			
700	8.000	31.905	22.899	33.321			
800	8.000	32.119	23.139	34.121			
900	8.000	32.326	23.372	34.921			
000	8.000	32.529	23.599	35.721			
100	8.000	32.727	23.819	36.521			
200	8.000	32.919	24.033	37. 321			
300	8.000	33.108	24, 242	38.121			
100	8.000	33. 291	24. 446	38.921			
500	8.000	33. 471	24.644	39.721			
00	8.000	33.647	24.838	40.521			
700	8.000	33.819	25. 027	41. 321			
100	8.000	33.988	25. 212	42.121 42.921			
000	8.000 8.000	34. 152 34. 314	25. 391 25. 570	43.721			
100 200	8.000 8.000	34.473 34.628	25.743 25.912	44, 521	**		
00	8.000	34.780	26.078	46, 121			
100	8.000	14.910	26. 241	46,921			
00	8.000	15.074	26.400	47.721			
16, 17	8.000	35.127	26.457	47.999			
16. 37	9.366	63.891	26. 457	207.247			
00	9.419	63.498	26.883	207.845			
00	9.500	64.166	27.536	208.791			
100	9.578	64.332	28.169	209.745			
00	9.653	64.496	28,783	210.706			
000	9.725	64.659	29.380	211.675			

HAFNIUM REFERENCE STATE

### SUMMARY OF UNCERTAINTY ESTIMATES

		al/ak gfu	Kcal/gfu				
T, <b>°E</b>	, د	s <mark>*</mark>	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF	Log Kp
0				± .010			
298.15	± .100	± .100	± .100	± .000			
1000	±1.000	± .267	± .152	± .115			
2000	±1.500	± .973	± .402	±1.140			
2033	±1.500	±1.000	± .412	±1.195			
2033	±1.500	±1.098	± .412	±1.395			
2495	±1.500	±1.307	± .550	±1.888			
2495	±1.500	±1.708	± .550	± 2.888			
3000	±2.000	±1.924	± .701	±3.670			
4000	± 2. 000	± 2.167	± .999	±4.670			
5000	£2.000	± 2. 613	±1.279	±6.670			
5536.37	±2.000	±2.817	±1.418	±7.743			

#### IDEAL MONATOMIC GAS

Reference State for Calculating Mf, AFf, and LogE, : Solid from 298.15° to 2495°K, Liquid from 2495° to 5536°K, Gas from 5536° to 6000°K.

<del></del>			33° ± 200°K	m.p. = 2495		b.p. = 55	
T,*K		ai/°K gf+	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>		ΔF,	Log K
0		•		-	167, 947	167.947	-
298.15	0.000 4.972	0.000 44.645	Infinite 44.645	-1.481 0.000	168.000	157.869	Infinite
300	4. 973	44. 675	44.645	0.009	167.997	157.806	-114.9
400	5. 010	46.110	44.840	0.508	167.869	154. 427	-84. 3
500	5. 114	47.237	45.211	1.013	167. 733	151.083	-66.0
600	5. 285	48. 184	45.629	1.533	167.601	147.766	-53.8 -45.1
700	5.500	49.015	46.055	2. 072	167.476	144.471	-38.5
800	5. 734 5. 970	49.764 50.453	46. 472 46. 877	2.634 3.219	167.362 167.260	141.193 137.929	-33.4
900	6. 196	51.094	47. 267	3.827	167. 169	134.674	- 29, 4
100	6.407	51.695	47.642	4. 458	167.090	131.429	-26.1 -23.3
200 300	6.596	52.260	48.004	5.108	167.018	128. 190 124. 957	-23.3
	6.763	52. 795 53. 302	48.352	5.776	166.951	121.729	-19.0
1400 1500	6.906 7.026	53.782	48.688 49.011	6.460 7.157	166.890 166.829	118.505	-17. 2
600	7. 123	54. 239	49.324	7.864	166.765	115.286	-15.7
700	7. 201	54.673	49.626	8.581	166.700	112.072	-14.4
800	7. 260	55.087	49.918	9.304	166.628	108.859	-13.2
900	7.305 7.338	55.481 55.856	50. 200 50. 474	10.032 10.764	166.550 166.463	105.653 102.450	-12.1 -11.1
.000	77.550	33.030	307 171	101.101	1001103		
033	7. 346	55.976	50.562	11.007	166. 433		-10.8
033	7. 346	55.976	50.562	11.007	164.783	101. 394	-10.89
100	7.361	56. 215	50.739	11.499	164.717	99.305	-10.3
200	7.378	56.558	50.996	12.236	164.610	96. 193	-9.5
300	7. 391	56.886	51.245	12.975	164. 493	93.085	-8.8
400	7.401	57. 201	51.486	13.714	164. 356	89.985	-8.14
495	7-411	57.488	51.709	14.418	163.976	87.041	-7.6
495 500	7.411 7.411	57.488 57.503	51.709 51.721	14.418 14.455	158.737 158.734	87.041 86.898	-7.6. -7.5
600	7.423	57.794	51.949	15. 197	158.676	84. 025	-7.06
700	7. 436	58, 074	52.171	15.940	158.619	81.156	-6.56
800	7. 453 7. 474	58. 345	52.386	16.684 17.430	158.563	78. 287 75. 422	-6.11 -5.68
900 000	7. 499	58.607 58.861	52.596 52.801	18.179	158.509 158.458	72.558	-5. 28
		******		,			
100	7.530	59.107	53.000	18.930	158.409	69.695	-4.91
200	7. 565	59. 347	53.195	19.685	158.364	66.835	-4.56
300	7.606	59.580	53.385	20.444	158.323	63.974	-4. 23
400 500	7.653 7.704	59.808 60.030 -	53.571 53.752	21.207 21.974	158.286 158.253	61.116 58.258	-3.92 -3.63
500	1.10	00.030	33.132	21.7.1	150.255	30. 230	3, 0,
600	7.761	60. 248	53.929	22.748	158. 227	55. 402	-3.36
700	7.822	60.462	54. 103	23.527	158. 206	52.545	-3.10
800	7.889	60.671	54. 273	24.312	158.191	49.690	-2.B5
900 000	7. 959 8. 033	60.877 61.079	54. 440 54. 603	25.105 25.904	158. 184 158. 183	46.835 43.983	-2.62 -2.40
000	0,000	01.017	34.003	23. 704	150. 105	13.703	-2.40
100	8.111	61.279	54.764	26.711	158.190	41.127	-2.19
200	8.191	61.475	54.921	27.526	158.205	38.270	-1.99
300	8. 275	61.669	55.076	28.350	158. 229	35. 415	-1.80
400	8.360	61.860	55. 228	29. 181	158.260	32.560	-1.61
500	.8. 448	62.049	55.377	30, 022	158, 301	29.700	-1.44
500	8.537	62. 235	55.524	30.871	158.350	26.843	-1.27
700	8.627	62.420	55.669	31.729	158.408	23.982	-1.11
900	8.717	62.603	55.812	32.596	158.475	21.122	-0.96
900	8.808	62. 783	55.952	33.473	158.552	18, 260	-0.B1
000	8.898	62.962	56.091	34.350	158.637	15.397	-0.67
100	8.988	63.139	56, 227	35. 252	158.731	12.532	-0.53
200	9.078	63.315	56.362	36.156	158.835	9.662	-0.40
300	9.166	63.488	56.494	37.068	158.947	6.793	-0.28
00	9.252	63.661	56.626	37.989	159.068	3.923	-0.15
500	9.337	63.831	56.755	38.918	159.208	1.047	-0.04
36. 37	9.367	63.893	56.802	39.258	159.259	0.000	0.00
36. 37	9.367	63.893	56.802	19. 258			
500	9.419	64.000	56.883	39.856			
700	9.500	64.167	57.009	40.802			
100	9.578	64.333	57.134	41.756			
00	9.653	64. 498	57. 258	42.717			
000	9.725	54.661	57.380	43.686			

#### HAFNIUM IDFAL MONATOMIC GAS

		al/°K gfo —			Kcal/	stv	$\overline{}$			
T,° <b>K</b>	c <sub>p</sub>	s <mark>*</mark>	$-(F_{T}^{\circ}-H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH °	ΔF į	Log Kp			
298.15	±.000	±.002	±.002	±.000						
1000	±.001	±.002	±.003	±.000		,				
2000	±.001	±.003	±.003	±.001						
2033	±.001	±.003	±.003	±.001						
2033	±.001	±.003	±.003	±.001						
2495	±.001	±.003	±.003	±.001						
2495	±.001	±.003	±.003	±.001						
3000	±.001	±.003	±.003	±.001						
4000	±.003	±.003	±.003	±.003						
5000	±.006	±.004	±.003	±.007						
5536.37	±.009	±.005	±.003	±.01i						
5536.37	±.009	±.005	±.003	±.011						
6000	±.011	±.006	±.003	±.015						

gfw = 192,2

		cal/oK N			Kcal/gfw -	n	
T, °E	C.	5	$-(F_{T}^{o}-H_{798}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔН	ΔF <sub>f</sub>	Log K
0	0.000	0.000	Infinite				Infinit
298.15	4.969	46, 242	46, 242	0.000			
300	4.969	46, 273	46. 242	0.009			
00	4.976	47, 703	46, 437	0.506			
500	5.007	48, 816	46, 806	1.005			
600	5.075	49.734	47.219	1.509			
700	5. 180	50,524	47.636	2.021			
800	5.314	51, 224	48.042	2,546			
900	5.465	51.859	48, 431	3.085			
000	5.622	52,443	48,804	3.639			
100	5,780	52, 986	49.159	4.209			
200	5, 933	53, 495	49.500	4.795			
300	6.079	53.976	49.826	5.396			
400	6.215	54.432	50.139	6.010			
500	6.340	54.865	50.439	6,638			
600	6.455	55, 278	50,729	7, 278			
700	6.560	55, 672	51,008	7.929			
800	6.654	56.050	51,278	8.590			
900	6.739	56.412	51.539	9.259			
000	6.815	56.760	51.791	9.937			
100	6,883	57.094	52,036	10.622			
200	6. 944	57, 415	52, 273	11.314			
300	6.999	57,725	52, 503	12.011			
400	7.048	58,024	52, 727	12.713			
500	7.093	58, 313	52, 945	13.420			
600	7, 133	58, 592	53. 157	14.132			
700	7, 170	58, 862	53, 363	14, 847			
800	7, 204	59, 123	53, 564	15.566			
900	7.235	59.377	53,760	16.288			
000	7, 263	59.622	53.952	17.012			
100	7.289	59.861	54, 138	17.740			
200	7.313	60.093	54. 321	16.470			
300	7.336	60.318	54.499	19.203			
,00	7.357	60.537	54.674	19.937			
500	7, 377	60.751	54,844	20.674			
600	7.396	60, 959	55.011	21,413			
700	7.413	61, 162	55, 175	22, 153			
800	7.430	61, 360	55, 335	22, 895			
900	7,446	61.553	55.492	23,639			
000	7.461	61,742	55.646	24.385			
100	7,475	61, 926	55,797	25.131			
200	7.489	62, 107	55, 945	25.880			
300	7,503	62. 283	56.090	26, 629			
400	7.516	62.456	56, 233	27, 380			
500	7.529	62.625	56.373	28, 132			
600	7 541	62 700	56 511	78 894			
700	7,541 7,554	62,790 62,953	56.511 56.646	28.886 29.641			
800	7.567	63, 112	56.779	30. 397			
900	7.579	63.268	56.910	31, 154			
000	7.592	63, 421	57.039	31,913			
.00	7, 605	63, 572	57.165	32,672			
100	7,618	63.719	57, 290	33, 434			
100	7, 632	63.865	57, 413	34.196			
00	7.646	64.007	57.533	34.960			
00	7,661	64, 148	57, 652	35, 725			
00	7.676	- 64, 286	57, 770	36.492			
00	7.692	64. 422	57, 885	37. 261			
100	7.708	64.556	57, 999	38,031			
00	7,726	64,688	56, 111	38,802			
00	7,744	64,818	58, 222	39.576			

IRIDIUM IDEAL MONATOMIC GAS

		al/°K gtv			Kcel/	·	
T,*K	່ ເ	s <sub>T</sub>	-(FT -H298)/T	H <sub>T</sub> - H <sub>298</sub>	AH °	AF I	Log Kp
298.15	±.000	±.002	±.002	±.000			
1000	±.000	±.002	±.003	±.000			
2000	±.001	±.003	±,003	<b>±.001</b>			
3000	±.001	±.003	±.003	±.001			
4000	±.001	±.003	±,003	±.002			
5000	±.002	±.003	±.003	±.003			
6000	±.004	±.004	<b>±</b> ,003	±.006			
L							

# 7. Iridium

The ideal gas thermodynamic functions in Table XXIII were calculated with the energy levels given by Moore 221 and the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

#### 8. Magnesium

#### a. Crystal Structure and Melting Point

Elemental magnesium has a hexagonal, close-packed structure from room temperature to its melting point. <sup>57</sup> The latter temperature was taken to be  $923^{\circ}\pm3^{\circ}\text{K}$ , in agreement with other recent compilations. <sup>76</sup>, 156, 77, 56, 78

#### b. Thermodynamic Properties

#### 1) Heat of fusion

Kelley  $^{137}$  reviewed the early data on the heat of fusion of magnesium which was derived from phase studies of binary alloys. He gave a mean value of 2.16 Kcal/gfw. Stull and McDonald  $^{224}$  made heat content measurements on solid and liquid magnesium, and reported the heat of fusion to be 2.14  $\pm$  0.05 Kcal/gfw. The Bureau of Standards  $^{78}$  reviewed available solid and liquid heat content measurements for the period up to 1959 and arrived at a value of 2.127 Kcal/gfw. The value of 2.127  $\pm$  0.03 Kcal/gfw was adopted for the heat of fusion of magnesium in the present work.

Other determinations of the heat of fusion of magnesium included the following:

Source	Heat of Fusion (Kcal/gfw)
Wittig (reported by Kubaschewski <sup>79</sup> )	1.83 ± 0.09
Reinartz (reported by Kubaschewski <sup>79</sup> )	2.03 ± 0.08
Treadwell <sup>225</sup>	1.37
Treadwell <sup>226</sup>	1.04
Zalesinski and Zulinski	1.12
Awbery and Griffiths <sup>227</sup>	1.13
Roos <sup>228</sup>	1.70

<sup>224</sup> Stull, D.R. and R. McDonald, J. Am. Chem. Soc. 27, 5293 (1955).

<sup>225</sup> Trendwell, W.D., Schw. Arac. angew. Wiss. Technik 6, 69 (1940).

<sup>&</sup>lt;sup>226</sup>Treadwell, W.D., A. Amann, and T. Zurrer, Helv. Chim. Acta 19, 1255 (1936).

<sup>227</sup> Awbery, J.H. and E. Griffiths, Proc. Phys. Soc. (London) 38, 378 (1926).

<sup>228</sup> Roos, G.D., Z. anorg. Chem. 94, 329 (1916).

Kubaschewski<sup>79</sup> arrived at a value for the heat of fusion of 2.00  $\pm$  0.12 Kcal/gfw from these other results plus the analysis of Kelley.<sup>56</sup>

# 2) Entropy and heat content at 298.15 °K

The reported entropy and heat content of magnesium at 298.15 °K have been based on the measurements of Craig et al  $^{229}$  (12° to 320°K); Smith  $^{230}$  (1° to 20°K); Logan, Clement, and Jeffers  $^{231}$  (3° to 13°K); and Estermann, Friedberg, and Goldman  $^{206}$  (1.8° to 4.2°K). On the basis of these data, the Bureau of Standards  $^{78}$  selected S $_{298}^{\circ}$  to be 7.800  $\pm$  0.05 e.u., while Dergazarian et al  $^{75}$  (JANAF Interim Thermochemical Panel Tables) selected the value 7.824 e.u. The difference is due to variations in adopted numerical techniques for smoothing and joining the low-temperature data to high-temperature data. Craig et al  $^{229}$  calculated S $_{298}^{\circ}$  to be 7.81 e.u. by graphical integration (using an unexplained correction factor of 1.0041). A value of 7.800  $\pm$  0.03 was adopted for the present work and was used to calculate  $H_{298}^{\circ}-H_{0}^{\circ}$  equal to 1195 cal/gfw.

Other low-temperature data for the heat capacity of magnesium have been given by Mannchen and Bornkessel  $^{232}$  (12° to 300°K), Clusius and Vaughen  $^{140}$  (11° to 228°K), Eastman and Rodebush  $^{144}$  (75° to 289°K), and Nernst and Schwers  $^{233}$  (27° to 94°K).

#### 3) High-temperature heat content

Heat contents for magnesium from 298.15 °K to the melting point have been based on the measurements of Saba, Sterrett, Craig, and Wallace 234 (298 ° to 543 °K), and Stull and McDonald 224 (700 ° to 1100 °K). These data have been smoothed and joined by the Bureau of Standards. 78 The Bureau's compilation for magnesium up to the melting point was accepted with a re-calculation to fit the format used herein. In the NBS compilation, the low-temperature data (in cal/gfw) were joined smoothly at 475 °K with the high-temperature heat content equation

$$H_{T}^{\circ} - H_{298}^{\circ} = 4.689T + 1.718 \times 10^{-3} T^{2} - 2.0776 \times 10^{4} T^{-1} - 1481.$$
 (142)

<sup>229</sup> Craig, K.S., C.A. Krier, L.W. Coffer, E.A. Bates, and W.E. Wallace, J. Am. Chem. Soc. 76, 238 (1954).

<sup>230</sup> Smith, P.L., Phil. Mag. 46, 744 (1955).

<sup>&</sup>lt;sup>231</sup>Logan, J.K., J.R. Clement, and H.R. Jeffers, Phys. Rev. 105, 1435 (1957).

<sup>232</sup> Mannchen, W. and K. Bornkessel, Z. Naturforsch, 14a, 925 (1959).

<sup>233</sup>Nernst, W. and F. Schwers, Sitzb. Konig preuss. Akad. Wiss. 1, 355 (1914).

<sup>&</sup>lt;sup>234</sup>Saba, W.G., K.F. Sterrett, R.S. Craig, and W.E. Wallace, J. Am. Chem. Soc. <u>79</u>, 3637 (1957).

The accuracy of the tabulated heat contents was taken to be  $\pm 1$  percent. Other recent compilations using different smoothing procedures have used the same original data sources to derive slightly different thermodynamic functions.

Stull and McDonald<sup>224</sup> measured the heat content of liquid magnesium up to 1100 °K and represented their data for the liquid phase (in cal/° K g) by the equation.

$$H_T^{\circ} - H_{298}^{\circ} = 0.2176T + 5.35 \times 10^{-5} T^2 + 484.63 T^{-1} + 16.851.$$
 (143)

However, within the error of the measurements (± 2 percent) their data could be equally well-represented by a constant heat capacity of 7.8 cal/° K gfw, so that the heat content in cal/° K gfw from 923° to 1377°K could be represented by

$$H_T^{\circ} - H_{298}^{\circ} = 7.8 \text{ T} - 781 .$$
 (144)

Above 1100 °K, the uncertainty in the heat content was assumed to increase at the rate of 0.015 Kcal/gfw per 100 °C of temperature increase.

High-temperature heat content or heat capacity measurements have also been made on magnesium by Poppema and Jaeger 235 (373° to 823°K), Honda and Tokunaga 236 (298°K), Seekamp 237 (271° to 773°K), Awbery and Griffiths 227 (525° to 1023°K), Eastman, Williams, and Young 136 (373° to 888°K), Schubel 238 (373° to 773°K), Magnus 239 (373° to 812°K), Kubaschewski 240 (923° to 1123°K), Lorenz 241 (293° to 403°K), Losano 242 (293° to 573°K), Stücker 243 (293° to 923°K), and Zalesinski and Zulinski 138 (295° to 1048°K).

# 4) Heat of formation of the monatomic gas

The tabulated free-energy functions were used with vapor pressure data from the following sources to calculate the indicated heats of formation at 298.15 °K by use of the Third Law Method:

<sup>235</sup> Poppema, T.J. and F.M. Jaeger, Proc. Acad. Sci. (Amsterdam) 38, 510 (1935).

<sup>236</sup> Honda, K. and M. Tokunaga, Sci. Repts. Tohoku Imp. Univ. 23, 816 (1935).

<sup>&</sup>lt;sup>237</sup>Seekamp, H., Z. anorg. u. allgem. Chem. 195, 345 (1931).

<sup>238</sup> Schubel, P., Z. anorg. Chem. 87, 81 (1914).

<sup>239</sup> Magnus, A., Habilitationsschrift, Eberhard-Karls Universitat, Tübingen (1910).

<sup>240</sup> Kubaschewski, O., Z. Metallkunde 41, 445 (1950).

<sup>&</sup>lt;sup>241</sup>Lorenz, L., Poggendorf's Ann. 13, 422 (1881).

<sup>242</sup> Losano, L., Ind. Chim. 5, 145 (1930).

<sup>243</sup> Stücker, N., Sitzb. konig. Akad. Winn. 114, 657 (1905).

Source of	Temperature	Calculated AH <sub>f298</sub>
Vapor Pressure Data	Range (°K)	(Kcal/gfw)
Smith and Smythe 152	626-818	35.130 ± 0.020
Vetter and Kubaschewski 244	973-1073	35.180 ± 0.110
Schneider and Stoll <sup>245</sup>	917-1002	35.260 ± 0.100
Schneider and Esch 246	1376 (b.p.)	35,320
Coleman and Egerton 247	700-738	35,300 ± 0.040
Baur and Brunner 92	926-1283	35.355 ± 0.400
Leitgebel <sup>248</sup>	1370 (b.p.)	35.190
Hartmann and Schneider 148	1009-1293	35.660 ± 0.250
Ruff and Hartmann 153	911-1344	34.910 ± 1.500
Greenwood <sup>249</sup>	1393 (b.p.)	35.480
Ditte <sup>250</sup>	1383 (b.p.)	35.700
Scheil and Wolf <sup>251</sup>	1016-1102	35.510 ± 0.040
Wejnarth <sup>252</sup>	unavailable	

With the exception of the results of Smith and Smythe <sup>152</sup> and of Scheil and Wolf, <sup>251</sup> all of these calculations were based on the original data points. For the former only was an equation available; and for the latter, the data were taken from graphs.

<sup>244</sup>Vetter, F.A. and O. Kubaschewski, Z. Elektrochem. 57, 243 (1953).

<sup>245</sup> Schneider, A. and E.K. Stoll, Z. Elektrochem. 47, 519 (1941).

<sup>246</sup> Schneider, A. and V. Esch, Z. Elektrochem. 45, 888 (1939).

<sup>247</sup>Coleman, F.F. and A.C. Egerton, Phil. Trans. Roy. Soc. London 234A, 177 (1935).

<sup>&</sup>lt;sup>248</sup>Leitgebel, W., Z. anorg. Chem. 202, 305 (1931).

<sup>249</sup>Greenwood, H., Proc. Roy. Soc. (London) 83A, 413 (1910).

<sup>250&</sup>lt;sub>Ditte</sub>, B., Compt. Rend <u>73</u>, 111 (1871).

<sup>251</sup>Scheil, E. and F. Wolf, Z. Metallkunde 50, 229 (1959).

<sup>252</sup> Fejnarth, A., Tek. Tid. 72, 33 (1942).

The value of  $\Delta H_{f298}^{\circ}$  adopted was an average of the above values, excluding the results of Ruff and Hartmann  $^{153}$  and of Ditte.  $^{250}$  This average value is 35.340  $\pm$  0.250 Kcal/gfw. The error given was based on the spread in reported vapor pressures, and did not include uncertainties in condensed phase free-energy functions. The normal boiling point of magnesium was calculated to be 1377°  $\pm$  6°K. The uncertainty in the boiling-point value was estimated from an uncertainty of 0.21 e.u. in  $\Delta S_{v}^{\bullet}$  and an uncertainty of 0.40 Kcal/gfw in  $\Delta H_{v}^{\circ}$  at the normal boiling point where  $\Delta H_{v}$  equals 30.740 Kcal/gfw.

# 5) Thermodynamic functions

The reference state thermodynamic functions of magnesium are given in Table XXIV. The ideal monatomic gas thermodynamic functions of magnesium given in Table XXV were calculated using all the energy levels listed by Moore.  $^{52}$  Uncertainty estimates are summarized on the back of the tables.  $\rm H_{298}^{\circ}-\rm H_{0}^{\circ}$  was found to be 1,481 cal/mole for the ideal gas.

Mg

Reference State for Calculating ΔH<sup>o</sup>, ΔF<sup>o</sup>, and Log K<sub>p</sub>: Solid from 298.15° to 923° K, Liquid from 923° to 1377° K, Gas from 1377° to 6000° K.

gfw = 24.32m.p. = 923° ± 3°K b. p. = 1377\* + 6\* K -cal/oK gfw -Kcal/gfw ...  $-(F_{T}^{o} - H_{298}^{o})/T$ C. ST HT - H298 T, °K Infinite 7,800 7,800 0,000 0.000 -1.195 298.15 7,800 7,836 0.000 5.951 300 5.957 0.011 8.037 400 6.212 9.587 0.620 500 6.490 11.001 1,254 9,013 1.919 600 6.808 700 7.137 7.470 13, 286 9.548 10.077 2.616 3.347 800 14,261 10,593 10,709 900 7.807 15, 160 4.110 15.358 923 7.885 4.291 7.800 17,662 10.709 6.418 11.268 1000 7,800 18.287 7.019 11.940 19.030 1100 7.800 7.799 7.800 19.709 12,560 1300 7.800 20, 333 13, 134 9.359 7.800 9.960 1377 1377 4.968 43.102 13.545 40,700 4.968 14.035 40.814 1400 1500 4.968 43,531 15.990 41.311 17, 721 1600 4.968 43.851 41.808 4.968 19.268 44, 153 42,305 1700 44.437 44.705 1800 4.968 20.659 42,801 21.917 43, 298 1900 4.968 2000 4.969 44.960 43,795 2100 45.202 24, 111 44.292 4.970 4.972 45.434 45.655 44.789 45.286 2200 25,075 2300 25.965 2400 4.974 45,866 26, 790 45 783 27.557 2500 46.069 46.281 4.978 28.273 2600 4.983 46, 265 46,779 28. 943 29. 571 47.278 47.777 2700 4.989 46.453 2800 4.998 46,634 48.277 3000 5,023 46, 980 30,720 48.779 47, 145 11.248 3100 5.040 49.282 3200 5.060 3 30 0 5,085 47,461 32, 220 50.294 47,614 50.804 3400 5.114 3500 5.148 47.762 33.100 51.317 33,510 3600 5.186 47.908 51.834 33.901 52, 354 3700 48.051 5, 229 3800 5.278 48.191 34.275 52,880 3900 5.332 48.328 34.634 53,410 53.946 5.457 35.308 54.489 5.528 5.604 48.730 48.861 35.626 35.933 55.038 55.594 4200 4 300 4400 5,686 48.991 36, 228 56.159 4500 5.773 49, 120 36.513 56.732 5.866 49.248 57.314 4600 4700 5.964 6.067 49, 375 49, 502 37.055 37.313 57, 905 58, 507 4800 4900 6.176 49.628 37, 563 59.119 5000 6.289 49,754 37,806 59.742 6.407 49, 879 38,040 60.377 5100 6,530 5200 50,005 38.270 61.024 5 300 50, 131 38,493 18,709 61.683 6.790 62.355 5500 6.927 50.382 18, 920 63.041 50.508 7,069 39, 126 63,741 5600 39, 327 39, 522 39, 715 64, 455 65, 184 65, 929 50, 635 50, 761 5700 7,215 5800 7, 366 5900 6000 7.682 51.016 39.901 66,689

MAGNESIUM REFERENCE STATE

	a	1/°K gfv			Kcal/	<b>/-</b>	$\overline{}$
T, E	ς <b>,</b>	S <sub>T</sub>	$-(F_{T}^{\bullet} - H_{290}^{\bullet})/T$	$H_T^n-H_{290}^n$	AH?	AF (	Log Kp
298, 15	±.030	±,030	±,030	±.000			
923	±.060	±.0b0	±.020	±.040			
923	±.160	±.090	±.020	±.070			
1377	±.600	±.210	±.070	±.200			
1377	±.000	±.002					
2000	±.000	±.002					
3000	±.001	±.002					
4000	±,002	±.003					
5000	±,002	±.003					
6000	±.002	±.003					

Reference State for Calculating ΔH°, ΔF°, and Log K : Solid from 298, 15° to 923° K, Liquid from 923° to 1377° K, Gas from 1377° to 6000° K.

gfw = 24, 32 m. p. = 923° ± 3° K b. p. = 1377° ± 6° K

IW = 24.32			m.p. = 923	. 1 2. V			13/1, + 9. K
T,*E	c <sub>p</sub> °	cal/°K gfv	-(F <sub>T</sub> -H <sub>290</sub> )/T	H <sub>T</sub> - H <sub>290</sub>	AH? Keal/gfw "	ΔF	Log K,
0		0.000		-1.481	35.054	35.054	
298.15	0.000 4.968	35.504	Infinite 35, 504	0.000	35. 340	27.080	Infinite
300	4.968	35, 535	35.504	0.009	35, 338	27.029	-19.849 -19.690
400	4.968	36, 964	35.699	0.506	35. 226	24. 275	-19, 690
500	4.968	38.073	36.067	1.003	35.089	21,553	-9. 420
400		10.000	14 470	1.500	24 221	10.040	
600 700	4.968	38. 978 39. 744	36. 479 36. 892	1.500	34. 921 34. 720	18.860 16.199	-6.869 -5.057
800	4. 968	40.408	37. 291	2.493	34. 486	13.569	-3, 707
900	4.968	40.993	37.671	2.990	34, 220	10.970	-2.664
923	4. 968	41, 118	37.755	3, 104	34, 153	10. 377	-2, 457
923	4. 968	41.118	37. 755	3.104	32.026	10.377	-2, 457
1000	4.968	41.516	38.029	3.487	31.808	8.580	-1.875
1100	4.968	41.990	38, 368	3.984	š1.525	6. 269	-1, 245
1200	4.968	42,422	38.688	4.481	31, 242	3. 986	-0.726
1300	4. 968	42.620	38, 991	4.977	30. 959	1.726	-0. 290
1377	4. 968	43, 102	39. 210	5. 360	30.740	0.000	
1377				5. 360	30. 140	0.000	0.000
	4.968	43, 102	39, 210				
1400	4, 968	43.188	39. 278	5.474			
1500	4.968	43, 531	39, 550	5.971			
1600	4. 968	43, 851	39.809	6,468			
1700	4.968	44, 153	40,056	6,965			
1800	4.968	44.437	40, 291	7.461			
1900	4.968	44.705	40.517	7.958			
2000	4.969	44.960	40.732	8.455			
1100	4 040	45, 202	40.940	8.952			
2100 2200	4.969	45, 434	41, 139	9.449			
	4,970	45, 655	41, 139				
2300 2400	4.972			9.946			
2400 2500	4.974	45, 866 46, 069	41.515 41.693	10.443			
	.,,,,	-31,007	,,	,			
600	4,983	46, 265	41.865	11.439			
700	4.989	46.453	42.032	11.938			
2800	4.998	46.634	42.193	12,437			
900	5.009	46.810	42.349	12.937			
1000	5.023	46.980	42.500	13,439			
100	5.040	47,145	42, 648	13.942			
200	5.060	47, 305	42,791	14.447			i
300	5.085	47,461	42, 930	14.954			
400	5.114	47,614	43.965	15,464			
500	5.148	47,762	43, 197	15.977			
600	5. 186	47.908	43 324	16,494			
700	5, 229	48.051	43, 326 43, 452	17.014			
800			43, 575				
	5, 278	48, 191	43, 575	17.540			
900 000	5. 332 5. 392	48, 328 48, 464	43, 695 43, 813	18.070 18.606			
100	5.457	48.598	43.928	19.149			
200	5.528	48.730	14.040	19,698			
300	5.604	48,861	44, 151	20, 254			
400	5,686	48, 991	44, 260	20,819			
500	5,773	49.120	44. 366	21, 392			
600	5.866	49, 248	44, 471	21.974			
700	5. 964	49.375	44.574	22.565			
800	6.067	49, 502	44, 675	23.167			
900	6.176	49.628	44.775	23.779			
000	6.289	49.754	44.873	24.402			
100	6.407	49.879	44.970	25,037			
200	6.530	50.005	45,066	25,684			
300		50.131	45, 160	26.343			
100	6.658	50. 151	45, 253	27.015			
300	6.927	50, 382	45. 346	27,701			
500	7.069	50, 508	45.437	28.401			
700	7, 215	50,635	45, 527	29.115			
800	7.366	50.761	45.616	29.844			
900	7.522	50, 889	45,704	30.569			
000	7.682	51.016	45.792	31.349			

#### MAGNESIUM IDEAL MONATOMIC GAS

		ul/*K gfe			Kcal/	g/v	· ·
T, °K	c <b>,</b>	s*T	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	AH o	ΔF	Log Kp
298. 15	±,000	±.002	±.000	±.000	±, 250	±.260	±.190
923					±.290	±, 270	±.060
923					±.320	±.270	±.060
1000	±.000	±.002	±.002	±.000			
1377					±.450	±.350	±.060
2000	±,000	±.002	±.003	±.001			
3000	±.001	±.002	±.003	±.001			
4000	±.002	±.003	±.003	±.002			
5000	±.002	±.003	±.003	±,004			
6000	±,002	±.003	±.003	±,005			

gfw = 54, 94

		el/ok sta			Kcal/gfw		
T, *K	c <b>,</b>	ST	$-(F_{T}^{a} - H_{296}^{o})/T$	H <sub>T</sub> H <sub>298</sub>	ΔH <sup>o</sup> .	ΔF	Log K
•	0.000	0,000	Tuella da				
298.15	4.968	41.494	Infinite 41.494	0.000			Infini
300	4.968	41.525	41, 494	0.009			
400	4. 968	42, 954	41.689	0.506			
500	4, 968	44.063	42.057	1.003			
600	4.968	44.968	42.469	1.500			
700	4.968	45,734	42.882	1.996			
800	4.968	46.398	43, 281	2.493			
900	4.968	46. 983	43,660	2.990			
1000	4, 968	47.506	44.019	3.487			
100	4.968	47.980	44. 358	3. 984			
200	4.968	48,412	44.678	4.481			
300	4.968	48.810	44.981	4.977			
400	4.968	49.178	45.268	5.474			
500	4.968	49.521	45,540	5.971			
400	4 040	40.041	45. 200				
600 700	4.969	49.841	45,799	6.468			
800	4.969 4.971	50.143	46.046	6, 965			
900	4.973	50. <b>42</b> 7 50. 695	46, 281 46, 507	7.462			
000	4. 977	50.951	46.722	7.959 8.456			
	•• ••	30, 731	10	0.450			
100	4.982	51.194	46.930	8.954			
200	4.991	51,426	47, 129	9.453			
300	5.002	51.648	47.320	9.953			
400	5.018	51.861	47.505	10.454			
500	5.040	52,066	47.684	10.956			
600	5.067	52, 264	47.856	11 463			
700	5, 101	52, 456	48.023	11.462 11.970			
800	5.142	52.642	48.184	12.482			
900	5. 193	52.824	48, 341	12.999			
000	5, 253	53.001	48.494	13.521			
				******			
100	5. 322	53, 174	48.642	14.050			
200	5,403	53.344	48,766	14.586			
300	5.495	53, 512	48.927	15, 131			
400	5.598	53.677	49.064	15,685			
500	5, 713	53.841	49.198	16.251			
600	5.841	54.004	49. 330	16.828			
700	5. 951	54, 166	49.458	17.419			
800	6. 133	84. 327	49.584	18.025			
900	4.297	84, 489	49.708	18.646			
000	6,473	54,650	49.829	19, 285			
100	6.661	84.813	40.040	18.641			
100	4.857	54. 975	49.949 50.067	19.941			
100	7.068	55, 139	50, 183	21, 313			
100	7. 287	55. 304	50. 297	22.031			
00	7.515	55.471	50.410	22.771			
00	7.751	-55, 634	50, 522	23, 534			
00	7.995	55.806	50.633	24, 322			
00	8, 244	55.979	50.742	25.134			
00	8.500 8.759	56, 151 56, 325	50.851 50.959	25, 971 26, 834			
•			301,737				
00	9.022	56, 502	51.066	27,723			
00	9. 288	56, 679	51.172	28.638			
00	9. 554	56.859	51.276	19.580			
00	9.821	87,040	51, 383	30.545			
00	10.088	57, 221	51,487	51.545			
00	10.362	57.407	51,591	32.567			
00	10,614	87, 892	\$1.695	33, 616			
00	10.873	\$7.779	81.798	34,689			
00	11.127	87.967	wi. 901	38.789			
00	11, 376	88, 186	52,004	36.916			
					5		

MANGANESE IDEAL MONATOMIC GAS

	cal/ok gfv				Kcal/	ri -		
T, °K	C.	s <sub>T</sub>	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	VH 0	ΔF	Log K	
298.15	±.000	±.002	±.002	±.000				
1000	±.000	±.002	±.002	±.000				
2000	±.000	±.002	±.003	±.000				
3000	±.000	±,002	±.003	±.001				
4000	±.001	±.003	÷.003	±.001				
5000	±.002	±.003	±.003	±.002				
6000	± 003	±.003	±.003	±.004				

# 9. Manganese

The ideal gas thermodynamic functions in Table XXVI were calculated with the energy levels given by Moore<sup>253</sup> and the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

<sup>253</sup> Moore, C.E., Nat. Bur. Stds. Circ. 467, vol 2 (15 August 1952).

# 10. Molybdenum

The stable form of solid molybdenum at 25 °C is the body-centered cubic crystal.  $^{254-256}$  There appears to be no conclusive evidence for solidstate transitions although the existence of a face-centered cubic modification has been reported.  $^{257}$  The body-centered cubic form has been taken as the stable form from room temperature to the melting point in the present work. The melting point of molybdenum is  $2617^{\circ} \pm 10^{\circ}$ C, and the estimated standard boiling point is  $4692^{\circ} \pm 300^{\circ}$ C.

### a. The Melting Point of Molybdenum

The absolute value of the melting point of molybdenum has been somewhat in doubt, but the "best" value has been taken to be  $2617^{\circ}\pm10^{\circ}\text{C}$  by several workers.  $^{76}$ ,  $^{77}$ ,  $^{56}$  The most exhaustive study of the melting point appeared to be that of Worthing  $^{258}$ ,  $^{259}$  who reported a value of  $2622^{\circ}\pm10^{\circ}\text{C}$ . Worthing  $^{259}$  discussed the results of earlier workers whose values ranged from  $2562^{\circ}$  to  $2597^{\circ}\text{C}$ . Melting-point values were also discussed in two recent general works dealing with molybdenum.  $^{254}$ ,  $^{256}$ 

The heat of fusion has not been directly established. Estimated values found in the literature included the following:

6660 cal/g atom	(Ref.	191)
6650 cal/g atom	(Ref.	56)
6600 cal/g atom	(Ref.	77)
3000 cal/g atom	(Ref.	256)
4800 cal/g atom	(Ref.	254)
6650 cal/g atom	(Ref.	76)
6700 cal/g atom	(Ref.	260)
8380 cal/g atom	(Ref.	261)

<sup>254</sup>Northcott, L., Molybdenum, Butterworths, London (1956).

<sup>255</sup> Lu, S.S. and Y.L. Chang, Proc. Phys. Soc. (London) 53, 517 (1941).

<sup>256</sup> Agte, C. and J. Vacek, Wolfram and Molybdan, Akademic Verlag, Berlin (1959).

<sup>&</sup>lt;sup>25</sup> Aggarwal, P.S. and A. Goswami, Proc. Phys. Soc. (London) <u>708</u>, 708 (1957).

<sup>258</sup> Worthing, A.G., J. Franklin Inst. 199, 549 (1925).

<sup>&</sup>lt;sup>259</sup>Worthing, A.G., Phys. Rev. <u>25</u>, 846 (1925).

<sup>&</sup>lt;sup>260</sup>Molybdenum Metal, Climax Molybdenum Co., New York (1960).

<sup>&</sup>lt;sup>261</sup>Jones, H.A., I. Langmuir, and G.M. J. MacKay, Phys. Rev. <u>30</u>, 201 (1927).

In the absence of conclusive experimental data, an estimated  $\Delta H$  of fusion of 6650 cal/g atom was chosen for the present compilation. This value was based on an assumed entropy of fusion of 2.3 e.u. An uncertainty of  $\pm 1000$  cal/g atom was arbitrarily assigned to the  $\Delta H$  of fusion at the melting point.

# b. The Standard Heat of Formation at 298.15 °K ( $M_{208}^{\circ}$ )

Vapor pressure measurements for solid molybdenum have been reported by Jones, Langmuir, and MacKay,  $^{261}$  by Norris and Worthing,  $^{262}$  and by Edwards, Johnston, and Blackburn.  $^{263}$  A  $_{\Delta H^{\circ}_{f298}}$  value of 158,200  $\pm$  800 cal/g atom was calculated using the vapor pressure values of Edwards and co-workers,  $^{263}$  and the free-energy functions from the present compilation. Norris and Worthing  $^{262}$  did not report actual experimental vapor pressure values, and the data of Jones and co-workers  $^{261}$  led to a rather marked temperature dependence of  $^{\Delta H^{\circ}_{f298}}$ . The latter two studies were therefore given no weight in evaluating  $^{\Delta H^{\circ}_{f298}}$ .

#### c. The Boiling Point of Molybdenum

The boiling point of molybdenum had not been clearly established. Estimated and/or quoted values ranged from 3650° to 5697°C; e.g.:

3560 °C	(Ref.	264)
3700 °C	(Ref.	256)
4651 °C	(Ref.	76)
4804 °C	(Ref.	191)
4827 °C	(Ref.	77)
5560 °C	(Ref.	260)
5687 °C	(Ref.	261)

From a calculated  $\Delta H_{1298}^{\circ}$  value of 158,200 ±800 cal/g atom and free-energy functions for the gas and condensed phases from the present compilation, a standard boiling point of 4692° ±300°C was calculated in the present work.

<sup>&</sup>lt;sup>202</sup>Norris, L. and A.G. Worthing, Phys. Rev. <u>44</u>, 323 (1933).

<sup>&</sup>lt;sup>263</sup>Fdwards, J.W., H.L. Johnston, and P.F. Blackburn, J. Am. Chem. Soc., <u>"4</u>, 1539 (1952).

<sup>204</sup> Sidgwick, N.V., Chemical Flements and Their Compounds, vol. 2, Oxford University Press, London (1950).

The heat of vaporization at the standard boiling point was then estimated from the above value of  $\Delta H_{f298}^{\circ}$  and the enthalpy functions for the gaseous and condensed phases at the standard boiling temperature. The value thus calculated was 141,300  $\pm$  10,000 cal/g atom.

In Table XXVII are summarized the heats of transformation for the various phase changes of molybdenum.

# TABLE XXVII TRANSFORMATION DATA FOR MOLYBDENUM

Transition	Temperature (°K)	ΛΗ (cal/g atom)
solid liquid	2890 ± 10	6650 ± 1000
liquid → gas	4965 ± 300	141,300 ± 10,000
solid —— gas	298.15	158,200 ± 800

d. Calculation of Thermodynamic Functions for Condensed Phases of Molybdenum

Recent compilations of the thermodynamic functions of solid and liquid molybdenum included those of Stull and Sinke, <sup>77</sup> Hultgren, <sup>76</sup> and Kelley. <sup>56</sup> Those three compilations were in essential agreement but did not take into account the recent heat capacity measurements of Rasor and McClelland <sup>27, 157</sup> in the temperature range from about 1500 °K to the melting point. The values of enthalpy and entropy at 298.15 °K were as follows:

$$H_{298}^{\circ} - H_{0}^{\circ} = 1092 \text{ cal/g atom}$$
 (Refs. 76, 77)  
 $S_{298}^{\circ} = 6.83 \text{ e.u.}$  (Refs. 76, 77, 265).

For purposes of discussion, the thermodynamic properties of solid molybdenum will be considered first over the temperature range from 298.15° to about 1500°K, and then from about 1500°K to the melting point.

<sup>265</sup> Clusius, K. and P. Franzosini, Z. Naturforsch. A14, 99 (1959).

The enthalpy functions for solid molybdenum (i.e.,  $H_T^{\circ} - H_{298}^{\circ}$ ), for the temperature range from 298.15° to 1500°K in the present table, were those of Stull and Sinke; <sup>77</sup> they are almost identical to those of Hultgren <sup>76</sup> and Kelley. <sup>56</sup> The tabular entropy values,  $S_T^{\circ}$ , were

calculated by the method of Kelley. 56 Values for  $-\left(\frac{F_T^{\circ} - H_{298}^{\circ}}{T}\right)$  were

then calculated from equation (108).

The tabular values of  $\rm C_p^o$  over this temperature range were those of Stull and Sinke  $^{77}$  and Hultgren.  $^{76}$ 

For the temperature range from 1500 °K to the melting point, other compilers  $^{56}$ ,  $^{76}$ ,  $^{77}$  chose a linear function of  $^{\circ}$ C° based on enthalpy measurements of Kothen  $^{266}$  and Redfield and Hill  $^{267}$  over portions of this temperature range. However, Rasor and McClelland  $^{27}$ ,  $^{157}$  have measured  $^{\circ}$ C° values over the whole temperature range and reported an appreciable deviation from linearity. The heat capacity values of Rasor and McClelland gave a poor "fit" with a  $^{\circ}$ C° (T) function of the form

$$A + BT + CT^{-2}$$

but gave a very good "fit" with a function of the form

$$A + BT + CT^2$$
.

The equation employed herein was

$$C_p^{\circ} = 6.026 - 0.217 \times 10^{-3} \,\mathrm{T} + 0.0880 \times 10^{-5} \,\mathrm{T}^2$$
 (145)

This equation gave  $C_p^o$  values which join those of the low range (298.15° to 1500°K) smoothly at 1500°K.

Tabular values of  $C_p^o$  were calculated with equation (145). The equation was then used to calculate tabular values of entropy and enthalpy over the temperature range from 1600 °K to the melting point. The entropy and enthalpy equations were

$$S_{\rm T}^{\circ} = 6.026 \ln T - 0.217 \times 10^{-3} \, \text{T} + 0.440 \times 10^{-5} \, \text{T}^2 - 27.5066$$
, (146)

<sup>266</sup>Kothen, C., The High Temperature Heat Contents of Molybdenum and Titanium and the Low Temperature Heat Capacities of Titanium, Ph.D. Thesis, Ohio State Univ. (1952); Dissertation Abstracts 17, 2842 (1957); Univ. Mich., Microfilm, Ann Arbor, Pub. No. 23697.

<sup>267</sup> Redfield, T.A. and J.H. Hill, U.S. Atomic Energy Commission, Rept. ORNL-1087, Oak Ridge National Lab. (24 September 1951).

$$H_T^{\circ} - H_{298}^{\circ} = 6.026 \,\mathrm{T} - 10.85 \times 10^{-5} \,\mathrm{T}^2 + 29.333 \times 10^{-8} \,\mathrm{T}^3 - 1785.$$
 (147)

The values of the last constants in the above equations were evaluated from the tabular values of S<sub>T</sub> and H<sub>T</sub> - H<sub>298</sub> at 1500 •K. The free-energy function for solid molybdenum in this temperature range was then calculated using equation (108).

The heat capacity of liquid molybdenum was taken to be a constant value of  $10.00 \text{ cal/}^{\circ} \text{ Kg}$  atom. This value was an estimate  $^{76}$  since an experimental determination did not appear to have ever been made. Entropy and enthalpy values for liquid molybdenum were calculated using this value of  $C_{p}^{\circ}$  according to equations (138) and (139).

The values of the constants  $C_1$  and  $C_2$  in equations (138) and (139) were evaluated from the tabular values of  $S_T^o$  and  $H_T^o - H_{298}^o$  for liquid molybdenum at the melting point. The free-energy function for liquid molybdenum was evaluated in the same manner as that used for the corresponding function of solid molybdenum.

### e. Calculation of Thermodynamic Functions for Gaseous Molybdenum

Thermodynamic properties for the ideal monatomic gas were calculated using the spectroscopic energy levels listed by Moore. <sup>52</sup> Energy levels and J values not definitely established in these tables were estimated. The equations employed in these calculations have been discussed in two recent publications <sup>75</sup>, <sup>51</sup> and are summarized in section III-D.

The  $\Delta H_f^o$  ,  $\Delta F_f^o$  , and  $log_{10}K_p$  functions of gaseous molybdenum were calculated by the methods in section III-D.

#### f. Uncertainty in Condensed Phase Functions

The basic data for molybdenum included both heat capacity and enthalpy measurements.  $^{173}$ ,  $^{194}$ ,  $^{243}$ ,  $^{27}$  Heat capacities could be calculated from measured enthalpies; therefore, for the present compilation, uncertainties were assigned to  $C_p^o$  values and these uncertainties then used in calculating uncertainties in the other thermodynamic functions. These uncertainty estimates are summarized on the back of Table XXVIII.

#### REFERENCE STATE

Reference State for Calculating OH?, AF?, and Log Kp: Solid from 298.15° to 2890°K, Liquid from 2890° to 4965°K, Gas from 4965° to 6000°K.

aiw.	95.	95

200 300 400 500	C*P 0.000 5.680 5.690 5.970 6.150 6.280 6.350 6.440 6.550 6.700 6.860 7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112 9.451 9.808	0.000 6.830 6.865 8.545 9.905 11.035 12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	-(F <sub>T</sub> - H <sup>o</sup> <sub>298</sub> )/T Infinite 6.830 6.830 7.057 7.499 7.993 8.499 8.993 9.467 9.919 i0.349 i0.761 i1.154 i1.531 i1.894	H <sub>T</sub> - H <sub>298</sub> -1.092 0.000 0.011 0.595 1.203  J.825 2.460 3.100 3.750 4.410  5.090 5.790 6.510	AH°	ΔF	Log K <sub>p</sub>
298.15 300 400 500 600 700 800 900 1100 1200 1300 400 1500 600 700 800 900 1000 1100 1200 1300 1400 1500 1600 1700 1800 1800 1800 1800 1800 1800 18	5.680 5.690 5.970 6.150 6.280 6.350 6.440 6.550 6.700 6.860 7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112	6.830 6.865 8.545 9.905 11.035 12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	6.830 6.830 7.057 7.499 7.993 8.499 8.993 9.467 9.919 10.349 10.761 11.154	0.000 0.011 0.595 1.203 1.825 2.460 3.100 3.750 4.410 5.090 5.790 6.510			•
300 400 500 600 700 800 900 1100 1200 800 900 1000 1100 12200 1300 1400 1500 600 600 600 600 600	5.690 5.970 6.150 6.280 6.350 6.350 6.700 6.860 7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112	6.865 8.545 9.905 11.035 12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	6.830 7.057 7.499 7.993 8.499 8.993 9.467 9.919 10.349 10.761 11.154 11.531	0.011 0.595 1.203 J.825 2.460 3.100 3.750 4.410 5.090 5.790 6.510			
400 500 600 700 800 900 1000 1100 1200 1300 1400 1500 1600 1000	5.970 6.150 6.280 6.350 6.440 6.550 6.700 6.860 7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112	8.545 9.905 11.035 12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	7.057 7.499 7.993 8.499 8.993 9.467 9.919 10.349 10.761 11.154 11.531	0.595 1.203 J.825 2.460 3.100 3.750 4.410 5.090 5.790 6.510			•
500  600 700 800 900 1100 1200 1300 1400 1500 600 700 800 900 100 600 890 890 900 100 100 100 100 100 100 100 100 1	6.150 6.280 6.350 6.440 6.550 6.700 6.860 7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112 9.451 9.808	9.905 11.035 12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	7. 499 7. 993 8. 499 8. 993 9. 467 9. 919 10. 349 10. 761 11. 154 11. 531	1. 203 J. 825 2. 460 3. 100 3. 750 4. 410 5. 090 5. 790 6. 510			
600 700 800 900 1000 1100 1200 1300 1400 1500 600 700 800 900 900 100 2200 3300 4400 6500 6600 700 890 900 900 900 900 900 900 900 900 9	6. 280 6. 350 6. 440 6. 550 6. 700 6. 860 7. 050 7. 450 7. 680 7. 932 8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	11.035 12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	7.993 8.499 8.993 9.467 9.919 10.349 10.761 11.154	1.825 2.460 3.100 3.750 4.410 5.090 5.790 6.510			
700 800 900 900 1100 1200 1300 400 1500 800 900 100 100 800 890 890 890 900 100 200 300 400 500	6. 350 6. 440 6. 550 6. 700 6. 860 7. 050 7. 240 7. 450 7. 680 7. 932 8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	8.499 8.993 9.467 9.919 10.349 10.761 11.154 11.531	2. 460 3. 100 3. 750 4. 410 5. 090 5. 790 6. 510			
700 800 900 900 1100 1200 1300 400 1500 800 900 100 100 800 890 890 890 900 100 200 300 400 500	6. 350 6. 440 6. 550 6. 700 6. 860 7. 050 7. 240 7. 450 7. 680 7. 932 8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	12.013 12.868 13.633 14.329 14.977 15.586 16.162 16.710 17.227	8.499 8.993 9.467 9.919 10.349 10.761 11.154 11.531	2. 460 3. 100 3. 750 4. 410 5. 090 5. 790 6. 510			
800 900 1100 1200 1300 1400 1500 1600 700 800 900 100 2200 890 890 890 890 900 100 200 300 400 600 600	6. 440 6. 550 6. 700 6. 860 7. 050 7. 240 7. 450 7. 680 7. 932 8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	12. 868 13. 633 14. 329 14. 977 15. 586 16. 162 16. 710 17. 227	8.993 9.467 9.919 10.349 10.761 11.154 11.531	3.100 3.750 4.410 5.090 5.790 6.510			
900 1000 1100 1200 1300 1400 1500 1600 7700 800 900 1000 1000 890 890 890 890 1000 100	6.550 6.700 6.860 7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112 9.451 9.808	13.633 14.329 14.977 15.586 16.162 16.710 17.227 17.731 18.220	9.467 9.919 10.349 10.761 11.154 11.531	3.750 4.410 5.090 5.790 6.510			
1000 1100 1200 1300 1400 1500 1600 1600 1000 1000 1000 1000 10	6.700 6.860 7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112 9.451 9.808	14. 329 14. 977 15. 586 16. 162 16. 710 17. 227 17. 731 18. 220	9.919 10.349 10.761 11-154 11.531	4.410 5.090 5.790 6.510			•
1200 1300 1400 1500 1600 1700 1800 1900 1000 1100 1200 1300 1400 1500 1600 1700 1800	7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112 9.451 9.808	15.586 16.162 16.710 17.227 17.731 18.220	10.761 11.154 11.531	5.790 6.510			
1200 1300 1400 1500 1600 1700 1800 1900 1000 1100 1200 1300 1400 1500 1600 1700 1800	7.050 7.240 7.450 7.680 7.932 8.200 8.486 8.791 9.112 9.451 9.808	15.586 16.162 16.710 17.227 17.731 18.220	10.761 11.154 11.531	5.790 6.510			
1300 400 1500 1600 700 800 900 100 100 100 100 100 100 1	7. 240 7. 450 7. 680 7. 932 8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	16. 162 16. 710 17. 227 17. 731 18. 220	11.154 11.531	6.510			
1400 1500 1600 700 800 800 1000 1100 1200 1300 1400 1500 1600 1700 180	7. 450 7. 680 7. 932 8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	16.710 17.227 17.731 18.220	11.531				
1500  1600  700  800  900  1000  2100  3300  400  500  1000  300  1000  300  400  500	7.680 7.932 8.200 8.486 8.791 9.112 9.451 9.808	17. 227 17. 731 18. 220					
600 700 800 900 1000	7. 932 8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	17.731 18.220	11.074	7.250			
700 800 9900 1000 1000 890 1000 2000 300 400 500 6600	8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	18.220		8.000			
700 800 9900 1000 1000 890 1000 2000 300 400 500 6600	8. 200 8. 486 8. 791 9. 112 9. 451 9. 808	18.220	12.244	8.780			
800 900 1000 2200 2300 2300 4400 5500 6600 890 890 900 000 100 2200 3300 4400 5500	8.486 8.791 9.112 9.451 9.808		12.580	9.587			
900 1000 1100 1200 1300 1400 1500 1600 1700 1890 1890 1900 100 100 100 100 100 100	8.791 9.112 9.451 9.808	18.697	12.907	10.421			
2000 2100 2200 3300 4400 5500 600 700 890 890 900 900 100 200 300 400 600	9-112 9-451 9-808	19.163	13.224	11.285			
2100 2200 3300 400 5500 600 700 890 890 900 000 100 2200 3300 400 600	9.451 9.808	19.622	13.532	12.180			
2200 3300 4400 5500 6600 7700 8890 8990 9900 0000 1000 2000 3000 4000 5500	9.808						
300 400 5500 600 700 890 890 900 000 100 200 300 400 600		20.075	13.833	13.108			
400 500 600 700 890 890 900 000 100 200 300 400 500		20.523	14.127	14.071			
600 700 800 890 900 000 100 200 300 400 500	10.182	20.967	14.415	15.070			
600 700 800 890 990 000 100 200 300 400 500	10.574	21.409	14.697	16. 107			
70C 800 890 900 000 100 200 300 400 500	10.983	21.849	14.975	17.185			
70C 800 890 900 000 100 200 300 400 500	11 311	22 200	15.247	18.305			
890 890 900 000 100 200 300 400 500	11.411	22.288 22.727	15.516	19.468			
890 990 000 100 200 300 400 500	12.317	23. 166	15.782	20.676			
890 900 000 100 200 300 400 500	12.749	23. 563	16.018	21.804			
900 000 100 200 300 400 500	10.000	25.864	16.018	28. 454			
000 100 200 300 400 500	10.000	25.899	16.053	28.554			
100 200 300 400 500	10.000	26. 238	16.387	29.554			
200 300 400 500							
300 400 500	10.000	26.566	16.710	30.554			
<del>4</del> 00 500 600	10.000	26.883	17.022	31.554			
500 600	10.000	27.191	17.326	32.554	•		
600	10.000	27.489	17.620	33.554			
	10.000	27.779	17.906	34. 554			
	10.000	30 061	10 105	16 164			
700	10.000	28.061 28.335	18.185 18.456	35.554 36.554			
	10.000	28.602	18.719	37.554			
	10.000	28.861	18.975	38.554			
	10.000	29.115	19.226	39.554			
			.,				
100	10.000	29.361	19.470	40.554			
	10.000	29.602	19.708	41.554			
	10.000	29.838	19.942	42.554			
	10.000	30.068	20.169	43.554			
300	10.000	30.292	20.391	44. 554			
500	10.000	10 412	20.609	45.554			
	10.000	30.512 30.727	20.809	46.554			
	10.000	30.938	21.031	47.554			
	10.000	31.144	21.235	48.554			
	10.000	31.276	21.366	49.204			
65	12.401	59.735	21.366	190.501			
00	12.500	59.822	21.635	190.936			
	12.775	60.072	22.386	192.200			
	13.033	60.322	23.112	193.491			
	13.275	60.573	23.817	194.806			
	13.498 13.703	60. <b>823</b> 61.073	24.500 25.163	196.145 197.505			
• •		01.073	(3.10)	1711303			
00 1	13.889	61.321	25.806	198.885			
	14.056	61.569	26.432	200.203			
	14. 204	61.815	27.040	201-696			
	14. 334	62.058	27.630	203.123			
00 1	14.444	62.300	28. 206	204. 562			
						• • •	

#### MOLYBDENUM REFERENCE STATE

ſ ,	a	I/°K gfu			Kcal/	y(=	<u> </u>
T,°K	C <sub>p</sub>	s <sub>T</sub>	$-(F_T^{\circ} - H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>2</sup>	ΛF	Log Kp
298.15	± .300	± .100	± .100	t .000			
1000	± .500	± .600	± .320	± .280			
2000	± .800	±1.050	± .580	± .930			
2890	± 2.000	±1.570	± .320	± 2.180			
2890	± 2.000	±1.920	± .820	± 3.180			
3000	± 2.000	±1.990	± .860	± 3.400			
4000	± 3.000	± 2.710	±1.240	± 5.900			
4465	± 4.000	± 3.470	±1.600	±9.270			
4965	± .004	± .003					
5000	± .004	± .003					
6000	± .005	± .004					

#### 1) Heat capacity

Heat capacity values reported near room temperature ranged from  $5.6^{139}$  to  $6.3^{173}$  with most values near  $5.7^{268}$ , 270,274,275,276. The uncertainty in  $C_p^{\circ}$  at 298.15 °K was therefore taken to be  $\pm 0.3$  cal/° K g atom. Comparison of reported values in a graphical fashion at  $1000^{\circ}$  K  $^{277}$  indicated an uncertainty of  $\pm 0.5$  cal/° K g atom. A similar comparison at  $2000^{\circ}$ K led to an uncertainty of  $\pm 0.8$  cal/° K g atom. From  $2000^{\circ}$ K to the melting point, the data of Rasor and McClelland  $^{27}$ ,  $^{157}$  showed a rather rapid rise with temperature while the data of Kothen  $^{266}$  showed an almost linear rise with temperature. The uncertainty may therefore be as large as 2.0 cal/° K g atom at the melting point of  $2890^{\circ}$ K.

The heat capacity of liquid molybdenum had apparently never been experimentally measured; therefore, a rather large overall uncertainty was arbitrarily assigned to it. Particular uncertainties assigned were as follows:

```
\pm 2.0 cal/° K g atom at m.p. (2890 °K)
```

 $<sup>\</sup>pm$  2.0 cal/° K g atom at 3000 °K

 $<sup>\</sup>pm$  3.0 cal/° K g atom at 4000 °K

 $<sup>\</sup>pm$  4.0 cal/° K g atom at b.p. (4965 °K).

<sup>268</sup> Bronson, H.L. and H.M. Chisholm, Proc. Nova Scotia Inst. Sci. 17, 44 (1929).

<sup>&</sup>lt;sup>269</sup>Bronson, H.L., H.M. Chisholm, and S.M. Dockerty, Can. J. Res. <u>8</u>, 282 (1933).

<sup>&</sup>lt;sup>270</sup>Cooper, D. and G.O. Langstroth, Phys. Rev., 33, 243 (1929).

<sup>&</sup>lt;sup>271</sup>Defacqz, E. and M. Guichard, Ann. Chim. Phys. <u>24</u>, 139 (1901).

<sup>272</sup> Jaeger, F.M. and W.A. Veenstra, Proc. Acad. Sci. (Amsterdam) 37, 61 (1934).

<sup>&</sup>lt;sup>273</sup> Jaeger, F.M. and W.A. Veenstra, Rec. Trav. Chim. 58,.677 (1934).

<sup>&</sup>lt;sup>274</sup>Stern, T.E., Phys. Rev. 32, 298 (1928).

<sup>&</sup>lt;sup>275</sup>Fieldhouse, I., J. Hedge, J. Lange, A. Takata, and T. Waterman, Tech. Rep. 55-495, WADC (3 August 1956).

<sup>&</sup>lt;sup>276</sup>Simon, F. and W. Zeidler, Z. Physik. Chem. 133, 383 (1926).

<sup>277</sup> Goldsmith, A., T.E. Waterman, and H.G. Hirschhorn, Thermophysical Properties of Solid Materials, vol. I, Elements, TR-58-476, WADC (January 1960).

#### 2) Entropy

Uncertainties in entropy values were calculated from assigned uncertainties in  $C_p^\circ$  values (assuming that uncertainties in  $C_p^\circ$  were not functions of temperature and using average uncertainties over a temperature range) and assigned values of uncertainties for  $\Delta H's$  of transitions. The equations employed were as follows:

a) · For single-phase regions

$$s_{T_2} = s_{T_1} + \delta C_p \ln \frac{T_2}{T_1}$$
, (148)

where

 $s_{T_2}$  = entropy uncertainty at  $T_2$ ,

 $s_{T_1}$  = entropy uncertainty at  $T_1$ ,

 $\delta C_p^o$  = average uncertainty in  $C_p^o$  over the temperature range  $T_1 < T < T_2$  .

b) At transitions

$$s_B = s_A + \frac{\delta \Delta H_t}{T_t} , \qquad (149)$$

where

s<sub>B</sub> = entropy uncertainty for phase B at temperature of transition T<sub>t</sub>,

s<sub>A</sub> = entropy uncertainty for phase A at temperature of transition T<sub>t</sub>,

 $\delta \Delta H_t$ = uncertainty in  $\Delta H$  of transition.

The uncertainty in  $S_{298}^{\circ}$  was taken to be  $\pm$  0.1 e.u. in view of the rather large uncertainty in  $C_p^{\circ}$  near room temperature.

#### 3) Enthalpy

Uncertainties in enthalpy values were calculated from  $C_p^\circ$  on-certainties and assigned values of  $\Delta H$ -of-transition uncertainties. The equations used for single-phase regions and transitions were

$$h_{T_2} = h_{T_1} + \delta C_p^{\circ} (T_2 - T_1)$$
 (150)

and

$$h_{\mathbf{B}} = h_{\mathbf{A}} + \delta \Delta H_{\mathbf{c}} \quad . \tag{151}$$

# 4) Free energy

The uncertainty in the free energy function was calculated from calculated uncertainties in  $S_T^{\circ}$  and  $H_T^{\circ} - H_{298}^{\circ}$  by means of equations (119) and (120).

#### g. Uncertainty in Gas Phase Functions

Uncertainties in the thermodynamic functions at the specified temperatures were computed as explained in section III-D2. They are summarized on the back of Table XXIX.

The uncertainties in  $\Delta H_f^\circ$ ,  $\Delta F_f^\circ$ , and  $\log_{10} K_p$  were calculated by means of equations (46), (47) and (48).

h. Other References Pertaining to Thermodynamics of Molybdenum

Heat capacity measurements at low temperatures have been reported and discussed by Boosz,  $^{278}$  Wolcott,  $^{204}$  Rayne,  $^{279}$  Horowitz and Daunt,  $^{280}$  and Simon and Zeidler,  $^{276}$  Recent work on heat capacities at higher temperatures has been that of Boggs and Wiebelt,  $^{281}$ 

Vapor pressure data have also been reported by van Liempt. 282

Useful annotated bibliographies on molybdenum were those of Goodwin, 209

<sup>&</sup>lt;sup>278</sup>Boosz, H.J. Metall. <u>11</u>, 22 (1957).

<sup>279</sup> Rayne, J.A., Phys. Rev. 95, 1428 (1954).

<sup>280</sup> Horowitz, M. and J.G. Daunt, Phys. Rev. 91, 1099 (1953).

<sup>281</sup> Boggs, J.H. and J.A. Wiebelt, Rept. AECU-4473, U.S. Atomic Energy Commission (November 1959).

<sup>&</sup>lt;sup>282</sup>van Liempt, J.A.M., Z. Anorg. u. Allgem. Chem. 114, 105 (1920).

and of Richert, Beckett, and Johnston. <sup>283</sup> A recent review article of Argent and Milne <sup>284</sup> was examined but not used since it did not provide any new data.

i. Thermodynamic Functions

The reference state thermodynamic functions of molybdenum are given in Table XXVIII. The ideal monatomic gas thermodynamic functions of molybdenum in Table XXIX were calculated using the energy levels given by Moore.  $^{52}$   $_{298}$  - $_{0}^{6}$  was found to be 1,481 cal/mole for the ideal gas.

<sup>283</sup> Richert, E., C.W. Beckett, and H.L. Johnston, Cryogenic Lab., Ohio State Univ. Tech. Rept. No. 102-AC49/12-100, Astia No. ATI 111-799 (1949).

<sup>&</sup>lt;sup>284</sup>Argent, B.B. and C.J.C. Milne, J. Less Common Metals <u>2</u>, 154 (1960).

Reference State for Calculating ΔH<sup>o</sup><sub>2</sub>, ΔF<sup>o</sup><sub>2</sub>, and Log K<sub>p</sub>: Solid from 298.15° to 2890°K, Liquid from 2890° to 4965°K, Gas from 4965° to 6000°K.

(w = 95.95		al 'ok giv	т.р 20	990 * ± 10 *K	Kcal/gt		4965° ± 300
T, °K	c,	ST	-(F <sub>T</sub> " H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH "	$\Delta F_I^{\circ}$	Log Kp
0	0.000	0.000	Infinite	-1.481	157.811	157.811	Infinite
298.15	4.968	43.462	43.462	0.000	158.200	147.278	-107.95
300	4.968	43.493	43.463	0.009	158.198	147.210	-107.23
400	4.968	44.922	43.657	0.506	158.111	143.560	-78, 43
500	4.968	46.031	44.025	1.003	158.000	139.937	-61.16
600	4.968	46.937	44.437	1.500	157.875	136.334	-49.65
700	4.968	47.703	44.851	1.996	157.736	132.754	-41-44
800	4.968	48.366	45.249	2.493	157-593	129.195	-35.29
900	4.968	48.951	45.629 45.988	2.990 3.487	157. 440 157. 277	125.65 <b>4</b> 122.131	-30.51 -26.69
1000	4. 700	49.475	13.700	3. 407	131.211	122.131	- 20. 070
1100	4.969	49.948	46.327	3.984	157.094	118.624	- 23. 567
1200	4.970	50.381	46.647	4.481	156.891	115.136	- 20. 961
1300	4.972	50.778	46.949	4.978	156.668	111.666	-18.77
1400	4.977	51.147	47.236	5.475	156-425	108.213	-16.89
1500	4.985	51.491	47.509	5.973	156.173	104.778	-15.265
1600	4.998	51.813	47.768	6.472	155.892	101.362	-13.845
1700	5.017	52.116	48.015	6.973	155.586	97.961	- 12. 593
1800	5.043	52.404	48.251	7.476	155. 255	94.581	-11.483
1900	5.079	52.677	48.476	7.982	154.897	91.221	-10.492
2000	5.125	52.939	48.693	8.492	154.512	87.878	-9.60
2100	5.183	53.190	48.901	9.007	154-099	84.557	-8.799
2200	5. 255	53.433	49.102	9.529	153.658	81.299	-8.076
2300	5. 340	53.669	49.295	10.059	153.189	77.977	-7.409
400	5. 440	53.898	49.482	10.598	152.691	74.717	-6.804
500	5.556	54.122	49.663	11.147	152.162	71.480	-6.327
600	5.689	54.343	49.839	11.710	151.605	68.260	-5.738
700	5.839	54.560	50.010	12. 286	151.018	65.067	-5.267
800	6.006	54.776	50.176	12.878	150.402	61.897	-4.831
890	6.171	54.968	50.323	13. 426	149.822	59.057	-4.466
890	6. 171	54.963	50.323	13.426	143.172	59.057	-4.466
900	6.190 6.392	54.989 55.203	50.339 50.497	13.487 14.116	143.133 142.762	58.771 55.869	-4.429 -4.070
1000	0.392	55, 203	30.497	14.110	192.702	22.004	-4.070
100	6.611	55.416	50.652	14.766	142-412	52.979	- 3. 735
200	6.847	55.629	50.805	15.439	142.085	50.096	-3.421
300	7.099	55.844	50.954	16.136	141.782	47.226	-3.128
400	7.367	56.060	51.101	16.860	141.506	44.363	-2.852
500	7.650	56.277	51.246	17.610	141.256	41.510	- 2. 592
600	7.946	56.497	51.389	18.390	141.036	38.664	-2.347
700	8.254	56.719	51.530	19.200	140.846	35.827	- 2. 116
800	8.573	56.943	51.669	20.041	140.687	32.992	-1.897
900 000	8.901 9.235	57.170 57.400	51.807 51.944	20.915 21.822	140.561 140.468	30.155 27.328	-1.690 -1.493
000	9.233	37.400	31. 747	21.022	140.400	21.320	-1-473
100	9.575	57.632	52.080	22.762	140.408	24.498	-1.306
200	9.917	57.867	52.215	23.736	140.382	21.672	-1.128
300	10.260	58.104	52.349	24.745	140.391	18.7851 *	-0.958
400	10.601	58.344	52.483	25.788	140.434	16.020	-0.796
500	10.939	58.586	52.616	26.865	140.511	13.190	-0.641
600	11. 271	58.830	52.748	27.976	140.622	10.359	-0.492
700	11.595	59.076	52.880	29.119	140.765	7.529	-0.350
900	11.909	59.323	53.012	30. 295	140.941	4.690	-0.214
900	12.211	59.572	53.143	31.501	141.147	1.852	-0.083
765	12.401	59.735	53.229	32. 301	141.297	0.000	0.000
765 000	12.401	59.735 59.822	53.229 53.274	32.301 32.736			
700	12. 100	17.04.2	33.214	72.750			
100	12.775	60.072	53.405	34.000			
200	13.033	60.322	53.536	35. 291			
300	13.275	60.573	53.666	36.606			
100	13.498	60.821	53.796	37.945			
500	13.703	61.073	53.926	19. 105			
-00	11 990	61 221	£4 054	40 495			
500 700	13.889	61.321	54.056 54.186	40.685			
300	14.204	61.815	54.315	43.496			
100	14.334	62.058	54.444	44.923			
000	14.444	62.300	54.573	46. 362			
			,				
		•					

MULYBDENUM IDEAL MONATOMIC GAS

	cal	/°K gfw			Kcal/	`	
T, <b>°K</b>	c.	s <sub>T</sub>	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	AH o	ΔF	Log Kp
298.15	±.000	±.002	±.002	±.000	± .800	± .830	±.610
1000	±.000	±.002	±.002	±.000	±1.080	±1.120	±.240
2000	±.000	±.002	±.003	±.000	±1.730	±1.970	±.220
2800	±.001	±.003	±.003	±.001	± 2.980	± 3.180	±.240
2890	±.001	±.003	±.003	±.001	±3.980	± 3.180	± . 240
3000	±.001	±.003	±.003	±.001	±4.200	± 3.390	± . 250
4000	± . 002	±.003	±.003	±.002	±6.700	± 5.770	±.320
4965	±.004	±.003	±.003	±.004	±10.070	±8.760	±.390
4965	± · 004	±.003	±.003	±.004			
5000	±.004	±.003	±.003	±.004			
6000	±.005	±.004	±.003	±.008			

-6... - 02 O

		al/°K gfw			Kcal/gf	•	1
T, °K	c°p	scr	$-(F_{T}^{\circ}-H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>o</sup>	ΔF	Log
0	0.000	0.000	Infinite	1117			
298.15	7.208	44.492	44. 492	0.000			
300	7.208	44.537	44. 492	0.013			
400	7.086	46.597	44.774	0.729			
500	6.893	48.157	45.301	1.428			
600	6.704	49.397	45.884	2.108			
700	6.541	50.418	46.461	2.770			
800	6.402	51.282	47.001	3.417			
900	6.285	52.029	47.528	4.051			
000	6.186	52.686	48.012	4.674			
100	6.103	53.272	48.464	5-289			
200	6.035	53.800	48.887	5.895			
300	5.981	54.280	49.283	6.496			
400	5.941	54.722	49.656	7.092			
500	5.915	55.131	50.008	7.685			
600	5.903	55.512	50.340	8.276			
700	5.904	55-870	50.655	8.866			
800	5.918	56.208	50.954	9.457			
900	5.945	56.528	51.239	10.050			
000	5.984	56.834	51.511	10.646			
100	6.034	57.127	51.772	11.247			
200	6.094	57.409	52.022	11.853			
300	6.164	57.682	52. 262	12.466			
400	6.242	57.946	52.493	13.086			
500	6.328	58.2GZ	52.716	13.715			
500	6.419	58.452	52.932	14.352			
700	6.516	58.696	53.141	14.999			
300	6.616	58.935	53.344	15-655			
900	6.719	59.169	53.541	16.322			
000	6.825	59.399	53.732	16.999			
100	6.931	59.624	53.919	17.687			
200	7.038	59.846	54.100	18.385			
300	7.144	60.064	54.278	19.095			
100	7.250	60.279	54.451	19.814			
500	7.354	60.491	54.621	20.545			
500	7.456	60.699	54.787	21.285			
700	7.555	60.905	54.949	22.036			
300	7.652	61.108	55.109	22.796			
300	7.747	61.308	55.265	23.566			
000	7.838	61.505	55.419	24. 345			
100	7 026	(1.700		25.133			
	7.926	61.700 61.892	55.569 55.718	25.930			
200	8.011 8.093			26.736			
300		62.081	55.863	27.549			
100 100	8.172 8.247	62. 268 62. 453	56.007 56.148	28.370			
100	0.24/	02. 433	30.140	20.310			
00	8.320	62.635	56.287	29.198			
00	8.390	62.814	56.424	30.034			
100	8.456	62.992	56.559	30.876			
000	8.520	63.167	56.692	31.725			
100	8.581	63.339	56.823	32.580			
-							
00	8.640	63.510	56.953	33.441			
00	8,695	63,678	57.081	34,308			
00	8.749	63.844	57.207	35.180			
00	8.800	64.008	57.331	36.057			
00	8.848	64.170	57.454	36. 740			
-			2.1171	70. 710			
00	8.894	64.330	57.575	37.827			
00	8.939	64.488	57.695	18.7.9			
0.0	8. 781	64.644	57.814	39.615			
00	2.021	64.798	57.931	40.515			
100	9,059	64.950	58.046	41.419			

#### NIOBIUM IDEAL MONATOMIC GAS

		J∕°K gf <del>v</del>		Kcal/	$\overline{}$		
T, °K	c*	s <del>*</del> T	$-(F_{T}^{\circ} - H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	AH o	ΔF <sub>1</sub>	Log Kp
298-15	±.001	±.002	±.003	±.000			
1000	±.000	±.003	±.003	±.000			
2000	±.000	±.003	±.003	±.001			
3000	±.001	±.003	±.003	±.001			
4000	±.002	±.003	±.003	±.002			
5000	±.002	±.004	±.003	±.004			
6000	± .003	±.004	±.003	±.006			

# 11. Niobium

The ideal monatomic gas thermodynamic functions of niobium in Table XXX were calculated with the energy levels given by Moore 253 using the computer program described in section III-D. Uncertainty estimates are summarized on the back of the table.

#### 12. Nitrogen

#### a. Molecular Nitrogen

Machine computations based on the treatment of the diatomic molecule outlined in section III-E of this report, were made of the thermody-namic functions of molecular nitrogen.

The  $\underline{x}$   ${}^{1}\Sigma_{g}^{+}$  ground state and  $\underline{A}$   ${}^{3}\Sigma_{u}^{+}$  and  $\underline{B}$   ${}^{3}\Pi_{g}$  excited states of nitro-

gen were included in the calculation. The spectroscopic constants of Lofthus  $^{285}$  were used for the ground state of  $N_2^{14}$ . He combined his observations of the near-ultraviolet part of the emission spectrum of nitrogen with the Raman spectrum results on nitrogen obtained by Stoicheff.  $^{286}$  The resulting spectroscopic constants were slightly different from the ones listed by Herzberg.  $^{54}$  Wilkinson and Houk  $^{287}$  have also recently given constants for the ound state, which were later slightly modified by Wilkinson.  $^{288}$  e constants listed by Herzberg  $^{54}$  were used herein for the A and B states.

The spectroscopic constants adopted were corrected to correspond to the naturally occurring mixture of isotopic molecules although in the case of nitrogen, the resulting shift was less than the uncertainties assigned to the constants. According to custom for a process which does not involve separation of isotopes, the entropy of mixing of isotopes was not included. The entropy of nuclear spin was likewise omitted. No correction was necessary for the symmetry number of the heteronuclear isotopic molecule N $^{14}$ N $^{15}$  since this correction has been shown to be unnecessary by Giauque and Overstreet.  $^{289}$ 

The effect of the presence of isotopic molecules was accounted for by the use of the average molecular weight on the chemical scale in the calculation of translational entropy and the use of averages of the spectroscopic constants of the isotopes weighted according to composition. The procedure given by Herzberg  $^{54}$  was used to calculate the spectroscopic constants of  $N^{15}N^{15}$  and  $N^{14}N^{15}$  from those of  $N^{14}N^{14}$ .

<sup>285</sup> Lofthus, A., Can. J. Phys. 34, 780 (1956).

<sup>&</sup>lt;sup>286</sup>Stoicheff, B. P., Can. J. Phys. 32, 630 (1954).

<sup>287</sup> Wilkinson, P. G. and N. B. Houk, J. Chem. Phys. 24, 528 (1956).

<sup>288</sup> Wilkinson, P. G., Astrophys. J. 126, 1 (1957).

<sup>&</sup>lt;sup>289</sup>Giauque, W. F. and R. Overstreet, J. Am. Chem. Soc. <u>54</u>, 1731 (1932).

For discussion purposes, the properties of an isotopic molecule differing from those of the ordinary molecule are designated by the superscript i. If the parameter  $\rho$  is defined as

$$\rho = \sqrt{\mu/\mu^{i}} , \qquad (152)$$

where  $\mu$  is the reduced mass, then to a good approximation, the spectroscopic constants are related by equations (153)

$$\omega_e^i = \rho \omega_e$$
,  $\omega_e^i \mathbf{x}_e^i = \rho^2 \omega_e \mathbf{x}_e$ ,  $\omega_e^i \mathbf{y}_e^i = \rho^3 \omega_e \mathbf{y}_e$ ,  $B_e^i = \rho^2 B_e$ ,
$$\alpha_e^i = \rho^3 \alpha_e$$
, and  $D_e^i = \rho^4 D_e$ . (153)

The values of  $\rho$  for the pairs  $N^{14}N^{14}$ ,  $N^{14}N^{15}$  and  $N^{14}N^{14}$ ,  $N^{15}N^{15}$  were 0.983243 and 0.966195, respectively, using the isotopic masses tabulated by Stehn and Clancy. 290 The fractions of  $N^{14}N^{14}$ ,  $N^{14}N^{15}$ , and  $N^{15}N^{15}$  in naturally occurring molecular nitrogen were calculated from the isotopic abundances 291 by assuming that the equilibrium constant for the exchange process,

$$N^{14}N^{14} + N^{15}N^{15} \Longrightarrow 2N^{14}N^{15}, \tag{154}$$

equaled 4; i.e., the distribution among the isotopic species was random.

The corrected spectroscopic constants and the assigned uncertainties (in cm<sup>-1</sup>) which were used in the machine computations were as follows:

State	E	$\omega_{e}$	ω <sub>c</sub> x <sub>e</sub>	ω <sub>e</sub> y <sub>e</sub>	B <sub>e</sub>	a <sub>e</sub>	$y_e \times 10^5$	D <sub>e</sub> × 10 <sup>6</sup>
$X^{-1}\Sigma_g^+$	0.0	2357.93 ±0.4	14.186 ±0.12	-0.0124 ±0.008	1.9981 ±0'.001	0.01709 ±0.001	-4.6 ±2.0	6 ±0.5
$A^{-3}\Sigma_{u}^{+}$	49757.2 ± 2.0	1460.19 ±0.5	13.888	-0.025	1.440	0.013		5.6
$B^{-3}H_{g}$	59314.2 ±2.0	1733.89 ±0.5	14.47		1.6376	0.0184		5.8

<sup>&</sup>lt;sup>290</sup>Lange, N. (ed.), <u>Handbook o. Chemistry</u>, 9th ed., Handbook Publ., Sandusky, Ohio (1956), p 113.

<sup>&</sup>lt;sup>291</sup>Strominger, D. J. M. Hollander and G. T. Seaborg, Rev. Mod. Phys. 30, 585 (1958).

The calculated thermodynamic functions of molecular nitrogen are given in Table XXXI. The indicated uncertainties in the spectroscopic constants made a difference of 0.0005 units in the entropy at 6000° K. The uncertainty estimates summarized on the back of the table reflect primarily the uncertainty in the value of the gas constant R.

No attempt was made to assess the uncertainties introduced by the approximations made here in the evaluation of the partition function of the diatomic molecule. However, values of the heat content and free-energy functions from the present calculation are compared immediately below at several temperatures with data from other sources to give an indication of the effect of the approximations.

Temp.	(H° - H° ) T 298 Kcal/gfw			-(F° - H° )/T T 298 cal/% gfw				
	Avco	NBSa	JANAF <sup>b</sup>	Avco	NBS <sup>a</sup>	JANAF <sup>b</sup>		
298.15	0.000	0.000	0.000	45.771	45. 763	45.770		
1000	5.130	5.130	5.129	49.380	49.373	49.378		
2000	13.418	13.418	13.418	53.515	53.508	53.513		
3000	22.160	22.159	22.165	56.378	56.372	56.376		
4000	31.075	31.080	31.089	58.560	58, 554	58.559		
5000	40.089	40.098	40.119	60.322	60.316	60.322		
6000	49.179		49.237	61.801		61.802		

<sup>&</sup>lt;sup>a</sup>Re-calculated from National Bureau of Standards values in Circ. 564 to a reference temperature of 298.15° K.

The NBS table was based largely on calculations of Goff and Gratch  $^{292}$  (60° to 2800° K) and was extended to 5000° K by NBS using the same spectroscopic data. The spectroscopic data used were essentially those listed by Herzberg  $^{54}$  except for somewhat smaller values of Be and  $a_e$ . The JANAF table was a modification of the calculations of

<sup>&</sup>lt;sup>b</sup>From JANAF Thermochemical Tables (31 March 1961). ("White sheet") provided in advance of publication through the courtesy of Dr. D. R. Stull.)

<sup>&</sup>lt;sup>292</sup>Goff, J. A. and S. Gratch, Trans. Am. Soc. Mech. Engrs. <u>72</u>, 741 (1950).

### REFERENCE STATE

Reference State for Calculating AH7,  $\Delta F_f^o$ , and  $\log K_p$ : Diatomic Gas from 298.15° to 6000°K.

gfw = 28.016

		cal/oK gfv			Kcal/gfw -		
T, ° <b>K</b>	C <sub>P</sub>	Scr	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF (	Log Kp
0	0.000	0.000	Infinite	-2.072			
298.15	6.961	45.771	45.771	0.000			
300 400	6.961 6.991	45.814 47.820	45.771 46.045	0.013 0.710			
500	7.070	49.388	46. 562	i.413			
600	7. 197	50.687	47.144	2.126			
700	7.351	51.808	47.732	2.853			
900	7.513 7.670	52.800 53.695	48.305 48.855	3. 596 4. 356			
1000	7.815	54.510	49.380	5. 130			
1100	7.945	55. 261	49.881	5.918			
1200	8.061	55.958	50.359	6.719			
1300	8.162	56.607	50.815	7.530			
1400	8.250	57. 215	51.251	8.351			
1500	8.328	57.787	51.667	9.180			
1600	8, 396	58.327	52.067	10.016			
1700	8.456	58.838	52.450	10.858			
1800	8.509	59.322	52.819	11.707			
1900	8.555	59.784	53.173	12.560			
2000	8.597	60.224	53.515	13.418			
2100	8.635	60.644	53.844	14. 279			
2200	8.668	61.047	54.163	15.144			
2300	8.698	61.433	54. 471	16.013			
2400	8.726	61.803	54.768	16.884			
2500	8.751	62. 160	55.057	17.758			
2600	8.774	62.504	55.337	18.634			
2700	8.795	62.835	55.608	19.513			
800	8.814	63.156	55.872	20.393			
900 8000	8.832 8.849	63.465 63.765	56.129 56.378	21. 276			
.000	0.047	03.703	30.310	22. 160			
100	8.865	64.055	56.621	23.045			
200	8.879	64.337	56.858	23.933			
300	8.893	64.610	57.089	24.821			
1400 1500	8.906 8.918	64.876	57.314 57.534	25.711 26.602			
,,,,	3.,.0		310331	20.002			
600	8.930	65.386	57.748	27.495			
700 800	8.941 8.951	65.631	57.958	28.388			
900	8.961	65.869 66.102	58. 163 58. 364	29. 283 30. 178			
1000	8.971	66.329	58.560	31.075			
100	0.000	** ***					
100	8.980 8.959	66. 551 66. 767	58.752 58.941	31.973 32.871			
300	8.998	66.979	59.125	33.770			
400	9.006	67.186	59.306	34.671			
500	9.014	67.388	59. <b>4</b> 83	35. 572			
600	9.022	67.587	59.657	36. 474			
700	9.030	67. 781	59.828	37. 376			
800	9.038	67.971	59.996	38.280			
900	9.045	68.157	60.161	39.184			
000	9.053	68.340	60.322	40.089			
100	9.060	68.520	60.481	40.994			
200	9.058	68.696	60.638	41.901			
300	9.075	68.868	60.792	42.808			
400 500	9.083	69.038 69.205	60.943 61.091	43.716 44.624			
			******				
600	9.098	69.369	61.238	45.534			
700	9.105	69.530	61.382	46. 444			
800 900	9.113	69.689	61.524	47.355 48.267			
000	9.130	69.998	61.801	49.179			
			- ·				

### NITROGEN REFERENCE STATE

		ul/°K gf <del>u</del>			Kcal/	d -	$\overline{}$
T, ° <b>K</b>	C.	s <b>°</b> T	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>299</sub>	VH.	$\Delta F_f$	Log K
298.15	±.000	±.002	±.002	±.000			
1000	±.000	±.003	±.002	±.000			
2000	±.000	±.003	±.003	±.001			•
3000	±.000	±.004	±.003	±.001			
4000	±.000	±.004	±.003	±.001			
5000	±.000	±.004	±.003	±.001			
6000	±.000	±.004	±.003	±.001			

Reference State for Calculating AH? , AF? , and Log K  $_p$  : Diatomic Gas from 298.15° to 6000°K.

gfw = 14.008

		al/°K gfv			Kcal.	•	
T, *E	C <sub>p</sub>	s <b>4</b>	$-(F_{T}^{e} - H_{296}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>e</sup>	AF :	Lag I
0	0.000	0.000	Infinite	-1.491	112.536	112.536	Infinit
298.15	4.968	36.615	36.615	0.000	112.980	108.887	-79.8
300	4.968	36.645	36.615	0.009	112.983	108.861	-79.3
400	4.968	38.074	36.809	0.506	113.131	107.465	-58.7
500	4.968	39. 183	37.177	1.003	113.277	106.032	-46.3
						101 510	•••
600	4.968	40.089	37.590	1.500	113.417	104. 569	-38.0
700	4.968	40.855	38.003	1.996	113.550	103.084	-32.1
800 900	4.968 4.968	41.518 42,103	38.402 38.781	2. <b>4</b> 93 2. <b>9</b> 90	113.675 113.792	101.580 100.061	- 27. 7. - 24. 2
000	4.968	42.627	39.140	3.487	113.792	98.530	-21.5
100	4.968	43.100	39.479	3.984	114.005 114.101	96.987	-19.2 -17.3
200 300	4.968	43.533 43.930	39.799 40.101	4.481	114. 192	95. 437 93. 879	-17.3
400	4. 968	44. 298	40. 388	5.474	114. 278	92.312	-14.4
500	4. 968	44.641	40.661	5.971	114.361	90.740	-13.2
		44.043	40.010				
600	4.968	44.962	40.919	6.468	114.440	89.164	-12.17
700	4.968	45. 263	41.166	6.965 7.461	114.516 114.587	87.580	-11.29
800 900	4.968	45.547	41.402 41.627	7.958	114.658	85, 993 84, 402	-10.44 -9.70
000	4.969 4.969	45.816 46.070	41.843	8.455	114.726	82.810	-9.04
100	4.970	46.313	42.050	8.952 9.449	114.792	81.211	-8.4
200 300	4.971	46. 544 46. 765	42. 249 42. 441	9.946	114.857 114.920	79.610 78.006	-7.91 -7.4
100	4.975	46.977	42.625	10.444	114.982	76.402	-6.9
500	4.978	47.180	42.803	10.941	115.042	74, 792	-6.53
600 700	4.982	47.375	42.976	11.439	115.102	73.179 71.567	-6.15
700 B00	4. 987 4. 993	47.563 47.745	43.142 43.303	11.938 12.437	115.162 115.221	69.952	-5.79 -5.46
900	5.001	47.920	43.459	12.936	115. 278	68.334	-5.15
000	5.010	48.090	43.611	13.437	115.337	66.714	-4.86
100	5. 022	48.254	43.758	13.938	115.397	65.091	-4.58
200	5. 035	48.414	43.901	14.441	115.455	63.469	-4.33 4.00
300 400	5. 050 5. 066	48.569 48.720	44. 040 44. 176	14.945 15.451	115.515 115.575	61.843 60, 215	-4.09 -3.87
500	5. 085	48.867	44.308	15.959	115.638	58. 584	-3.65
500	5. 107	49.011	<b>44. 43</b> 6 <b>44.</b> 562	16.468 16.980	115.700 115.766	56. 956 55. 323	-3.45 -3.26
700 800	5.130 5.155	49, 151 49, 288	44.684	17. 494	115.833	53.691	-3.08
900	5. 183	49.422	44, 804	18.011	115.902	52. 054	-2.91
000	5. 213	49.554	44.921	18.531	115.973	50.416	- 2. 75
100	5. 244	49.683	45.036	19.054	116.048	48.774	- 2. 60 - 2. <b>4</b> 5
200 300	5. 278	49.810 49.935	45. 148 45. 258	19.580 20.110	116.124 116.205	47. 132 45. 487	-2.31
100	5.314 5.351	50.057	45.366	20.643	116. 287	43.843	-2.17
00	5. 390	50.178	45. 471	21.180	116. 374	42. 195	- 2. 04
						40.744	
00	5. 431	50. 297	45. 575	- 21.721	116.465	40.544	-1.92
00	5. 473	50.414	45.676	22. 266 22. 816	116.558	38.899	-1.80
00	5.517 5.562	50.530	45.776 45.875	22.816	116.656	37. 246 35. 584	-1.69 -1.58
00	5.608	50. <b>644</b> 50. <b>7</b> 57	45.971	23. 928	116.864	33.930	-1.36
00	5. 65 <b>4</b> 5. 702	50.868 50.978	46.066 46.159	24. 491 25. 059	116.974 117.089	32.267 30.607	-1.38 -1.28
00	5. 751	51.088	46. 251	25.632	117. 208	28.948	-1.19
00	5.800	51.195	46. 342	26. 209	117.332	27. 277	-1.10
00	5.850	51.302	46. 431	26.792	117.460	25.612	-1.01
00	F 000	61 400	46 510	17 170	117 502	21 040	0.03
00	5.899 5.950	51.408 51.513	46.519 46.606	27.379 27.971	117.592	23.940 22.266	- 0. 93 - 0. 85
00	6.000	51.617	46.691	28. 569	117.872	20.592	-0.77
00	6.050	51.720	46.776	29.171	118.019	18.910	-0.70
00	6.100	51.822	46.859	29.779	118.170	17.226	-0.6.
			2				

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NITROGEN IDEAL MONATOMIC GAS

	c	ul/°K gtu			Kcal	Kcal/gfw		
T, ° <b>K</b>	C.	ST	$-(F_{T}^{o}-H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	AH ?	ΔF	Log K	
298.15	±.000	±.002	±.002	±.000	±.100	±.100	<b>1</b> .070	
1000	±.000	±.002	±.002	±.000	±.100	±.100	±.020	
2000	±.000	±.002	±.002	±.000	±.100	±.110	±.010	
3000	1,000	±.002	±.002	±.001	±.100	±.110	±.010	
1000	±.000	±.002	±.002	±.001	±.100	±.120	±.005	
5000	±.001	±.002	±.002	±.001	±.100	±.120	±.005	
6000	±.001	±.002	±.003	±.002	±.100	±.130	±.005	

Glatt, Belzer, and Johnston, <sup>293</sup> who had used the spectroscopic distagiven by Herzberg. <sup>54</sup> The modifications in the JANAF tables were the addition of -Rln 9 to the entropy to remove the effect of naclear spin included by Glatt, Belzer, and Johnston<sup>293</sup> and 0.012 e.u. to convert to the spectroscopic data of Stoicheff. <sup>286</sup> The vibrational constants used herein for the ground state were slightly different from those given by Stoicheff, <sup>286</sup> but that difference was within the uncertainties summarized above.

 $(H_{298}^{\circ} - H_{0}^{\circ})$  for molecular nitrogen was calculated to be 2072.3 cal/gtw.

### b. Monatomic Nitrogen

# 1) Dissociation energy of nitrogen

The dissociation energy of molecular nitrogen was a subject of dispute for many years. A set of possible values resulted from differences between the dissociation limits obtained from the predissociation of various excited states, particularly the C 311g state, and the energies of various combinations of three possible lowlying states of the atomic dissociation products. 3 From this set, the alternative values of 9.76 and 7.38 ev appeared most likely, and a great amount of work has been done to confirm one or the other value. The subject was reviewed by Gaydon<sup>294</sup> in 1953, and by Brewer and Searcy 295 in 1956. Several other papers 285, 287, 296-300 have appeared since Brewer and Searcy's review. There has been achieved a virtually unanimous agreement that the higher value is correct. The dissociation energy of  $N_2^{-14}$  was therefore taken to be 225.07  $\pm$ 0.1 Kcal/gfw from Brewer and Searcy's recommended value of 78717  $\pm$  40 cm<sup>-1</sup> (1 cm<sup>-1</sup> = 2.85927 cal/gfw). The correction to convert this to the naturally occurring isotopic mixture is negligible. 294

#### 2) Thermodynamic functions of monatomic nitrogen

The ideal gas thermodynamic functions in Table XXXII were calculated with the energy levels given by Moore  $^{52}$  and the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table. H $^{\circ}_{298}$  - H $^{\circ}_{0}$  was found to be 1, 481 cal/mole.

<sup>293</sup> Glatt, L., J. Belzer, and H. L. Johnston, Ohio State Univ. Research Found., Proj. 316, Rep. 9 (1953).

<sup>294</sup> Gaydon, A. G., Dissociation Energies and Spectra of Diatomic Molecules, 2nd ed., Rev., Chapman and Hall, London (1953).

<sup>&</sup>lt;sup>205</sup>Brewer, L. and A. W. Searcy, Ann. Rev. Phys. Chem. <u>8</u>, 259 (1956).

<sup>&</sup>lt;sup>296</sup>Frost, D. C. and C. A. McDowell, Proc. Roy. Soc. (London) A236, 278 (1956).

<sup>&</sup>lt;sup>20</sup> Thorburn, R. and J. D. Craggs, Proc. Phys. Soc. (London) 69B, 682 (1956).

<sup>&</sup>lt;sup>208</sup>Lofthus, A., Nature <u>186</u>, 302 (1960).

Toennies, J. P. and F. F. Greene, J. Chem. Phys. <u>26</u>, 655 (1957).

<sup>300</sup> Wilkinson, P. G., J. Chem. Phys. 30, 773 (1959).

# 13. Osmium

The ideal monatomic gas thermodynamic functions of osmium in Table XXXIII were calculated from the energy levels given by Moore <sup>221</sup> with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

gfw = 190.2

		cal/°K atv			Keal/gfw -		`
T, *K	c,	s <b>4</b>	$-(F_{T}^{0}-H_{298}^{0})/T$	$H_T^0 - H_{298}^0$	ΔH°	ΔF ,	Log Kp
0	0.000	0.000	Infinite				Infinit
298.15	4.968	46.002	46.002	0.000			
300	4.969	46.032	46.002	0.009			
400	4.974	47.462	46. 197	0.506			
500	4,996	48.574	46. 565	1.005			
600 700	5.044 5.122	49.489 50.272	46.978	1.506 2.014			
800	5. 231	50.962	47.394 47.798	≥ 2.532			
900	5. 367	51.586	48. 185	3.061			
000	5. 522	52. 159	48.554	3.606			
100 200	5.691 5.867	52.694	48.906	4.166			
300	6.042	53. 196 53. 673	49. 243 49. 565	4.744 5.340			
400	6. 211	54. 127	49.875	5.952			
500	6.372	54. 561	50.173	6. 582			
600	6.521	54.977	50.460	7. 226			
700 800	6.658 6.782	55.376	50.738	7.885			
900	6.895	55.761 56.130	51.006 51.266	8.558 9.241			
000	6. 998	56.487	51.519	9.936			
100	7.091	56.830	51.763	10.641			
200	7.177	57. 162	52.001	11.354			
300 400	7. 257	57.483	52, 233	12.076			
500	7.332 7.403	57.794 58.094	52 <b>. 4</b> 58 52 <b>.</b> 677	12.805 13.542			
500	1.403	30.074	54.077	15.542			
600	7.472	58.386	52.891	14. 286			
700	7.538	58.669	53.100	15.036			
900	7.603	58.945	53.304	15.794			
900	7.667	59. 213	53, 503	16.557			
000	7.730	59.474	53.698	17.327			
100	7.792	59.728	53.888	18.103			
200	7.853	59.976	54.075	18.885			
300	7.914	60.219	54.257	19.674			
100	7.974	60.456	54.436	20.468			
500	8.033	60.688	54.611	21. 269			
500	9 000	(0.015	£4.203	22 075			
700	8.090 8.147	60.915 61.138	54.783 54.952	22.075 22.887			
100	8. 203	61.356	55.118	23.704			
00	8. 257	61.569	55. 280	24.527			
000	8.309	61.779	55.440	25.355			
	0.2/0	41.005					
00	8.360 8.410	61.985 62.187	55.597	26.189 27.027			
00	8. 457	62. 385	55.752 55.904	27.871			
00	8.503	62.580	56. 053	28.719			
00	8.547	62.772	56. 201	29.571			
00	8.590	62.960	56.345	30. 428			
00 00	8.631	63.145	56.488 56.629	31. 289 32. 154			
00	8.670	63.328 63.507	56.767	33.023			
00	8.743	63.683	56.904	33.896			
00	8.777	63.856	57. 039	34.772			
00	8.810	64.027	57.171	35.651			
00 00	8.841	64.195 64.361	57.302 57.431	36.534 37.419			
00	8.899	64.524	57.559	38.308			
	11127.5						
00	8.926	64.685	57.685	39.199			
00	8.952	64.843	57.809	40.093			
00 00	9.977	64. 999 65. 152	57.932 58.053	40.989 41.888			
00	9.024	65.304	58. 172	42.790			

OSMIUM IDEAL MONATOMIC GAS

		ul/°K afe			Kcal/	ri •	
T, °K	c. <mark>b</mark>	s <sup>o</sup> T	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	∆H d	ΔF	Log Kp
298.15	±.000	±.002	±.002	±.000			
1000	±.000	±.002	±.003	±.000			
2000	£.002	±.003	±.003	±.001			
3000	±.008	±.004	±.003	±.005			
4000	±.013	±.007	±.004	±.016			
5000	±.010	±.010	±.005	±.027			
6000	±.004	±.011	±.006	±.034			

# 14. Oxygen

### a. Molecular Oxygen

The thermodynamic functions of molecular oxygen were calculated with a computer program based on the treatment of the diatomic molecule outlined in section III-E of this report.

The electronic states and spectroscopic constants used for the oxygen molecule are given below with the assigned uncertainties:

Constant	$x^{3}\Sigma_{g}^{-}$	a <sup>1</sup> $\Delta_{g}$	b <sup>1</sup> Σ <sub>g</sub> <sup>+</sup>	$\Lambda^{3}\Sigma_{u}^{+}$	$1_{\Sigma_{\mathbf{u}}^{-}}$	B <sup>3</sup> ∑ =
E	- 0.244 + 0.2	7882.36 <u>+</u> 1.0	13120.917 <u>+</u> 1.0	35008.0 + 100.	36212.8 +1000.	49357.6 + 10.
ω <sub>e</sub>	1580. 1622 <u>+</u> 0. 4	1509.1 <u>+</u> 1.0	1432.507 + 0.4	801.0	650.41	709. 4
ω <sub>e</sub> x <sub>e</sub>	12,07 + 0.01	12.9 <u>+</u> 0.4	13.9466 + 0.02	15.0	17.03	8.0
ω <sub>e</sub> y <sub>e</sub>	0.0546 + 0.005		- 0.01075 + 0.01		-0.106	-0.375
B <sub>e</sub>	1.44531 <u>+</u> 0.001	1.4260 <u>+</u> 0.004	1.40007 <u>+</u> 0.005	0.91	0.826	0.819
a <sub>e</sub>	0.01579 + 0.0001	0.0171 + 0.006	0.01817 + 0.0001	0.015	0.0205	0.011
γ <sub>e</sub> (×10 <sup>5</sup> )			- 4.3 <u>+</u> 4.0		-83.0	~
D <sub>e</sub> (x10 <sup>6</sup> )	4.96 <u>+</u> 0.1	5. 1 <u>+</u> 0. 6	5. 36 <u>+</u> 0. 5	3.4	5.3	4.4
g	3	2	1	3	7*	3

<sup>\*</sup> Includes the  $^3\Delta_u$  state on the assumption that its spectroscopic constants are the same as those of the  $^1\Sigma_u^-$  state.

Constants adopted for  $0\frac{16}{2}$  were converted to those appropriate to a naturally occurring isotopic mixture by the procedure discussed in section IV-A12, using data for the isotopic masses and abundances from the same sources.

Constants used for the X, a, and b states of  $O_2^{16}$  were those listed by Herzberg. <sup>54</sup> The rotation and vibration-rotation interaction constants of the ground state have received recent confirmation in the Raman spectroscopic results of Weber and McGinnis. <sup>301</sup> Woolley's <sup>55</sup> additive correction of -0.244 cm<sup>-1</sup> was used to account for the effect of the triplet splitting of the ground state. Constants for the A state were from the modification of Herzberg's <sup>302</sup> results by Broida and Gaydon. <sup>303</sup>

Herzberg  $^{304}$  reported two new states for molecular oxygen which have not been included in previous calculations of the thermodynamic functions. He gave constants for the  $^1\Sigma_{\bf u}^-$  state, which were adopted here, but noted that the constants were based on the assumption of a vibrational numbering which might have to be revised. Much less is known about the  $^3\Delta_{\bf u}$  state as the data are fragmentary. Moffit  $^{305}$  had previously predicted the positions of these then unknown states, and concluded that they should be separated by less than 0.2 ev (1600 cm $^{-1}$ ) from the A state. Chamberlain  $^{306}$  stated that the  $^3\Delta_{\bf u}$  state probably lies slightly above the A state. Later theoretical calculations relating to the  $^1\Sigma_{\bf u}^-$  and  $^3\Delta_{\bf u}$  states were discussed by Itoh and Kimio.  $^{308}$  For the present calculation, the energies of the O-O bands of the two new states and their other spectroscopic constants were assumed identical. A total multiplicity of 7 was used. An uncertainty of 1000 cm $^{-1}$  was assigned to the common electronic levels.

Spectroscopic constants for the B state were taken from Brix and Herzberg.  $^{307}$ 

The results of the computations of the thermodynamic functions of molecular oxygen are given in Table XXXIV. The entropies of isotopic mixing and nuclear spin were not included. The calculations of Woolley have been almost universally accepted for recent compilations of thermodynamic functions. 77, 156, 309 Woolley broke off summation of rotational levels for a given vibrational level at the top of the dissociation or pre-dissociation applying to the vibrational level. In the

 $<sup>^{301}</sup>$  Weber, A. and E. A. McGinnis, J. Mol. Spectroscopy  $\underline{4},\ 195\ (1960).$ 

<sup>302</sup> Herzberg, G., Can. J. Phys. 30, 185 (1952).

<sup>303</sup> Broida, H. P. and A. G. Gaydon, Proc. Roy. Soc. (London) A222, 181 (1954).

<sup>&</sup>lt;sup>304</sup>Herzberg, G., Can. J. Phys. <u>31</u>, 657 (1953).

<sup>305</sup> Moffitt, W., Proc. Roy. Soc. (London) A210, 245 (1951).

<sup>306</sup> Chamberlain, J. W., Astrophys. J. 128, 713 (1958).

<sup>307</sup>Brix, P. and G. Herzberg, Can. J. Phys. 32, 110 (1954).

<sup>308</sup> Itoh, T. and O. Kimio, J. Chem. Phys. 25, 1098 (1956).

<sup>&</sup>lt;sup>309</sup>Dergazarian <u>et al, JANAF Thermochemical Tables, The Thermal Laboratory, Dow Chemical Co. (31 March 1961).</u>

REFERENCE STATE

02

Reference State for Calculating AHP, AFP, and Log Kp; Diatomic Gas from 298.15° to 6000°K.

gfw = 32.000

7 0-		۱/°K واه	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	ΔH	— Keal∕gfv .°	•	1 40 8
T, °K	c,	ST	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	ΔН	1	ΔF	Log E
0	0.000	0.000	Infinite	-2.075				
298.15	7. 021	49.007	49.007	0.000				
300	7.024	49.051	49.007	0.013				
100	7.196	51.092	49. 284	0.723				
500	7.431	52.723	49.814	1.454				
600	7.670	54.099	50.417	2.210				
700	7.884	55. 298	51.030	2.987				
800	8.064	56.363	51.631	3.785				
900	8.213	57.321	52, 211	4.599				
000	8.336	58. 193	52.767	5.427				
100	8.439	58.993	53. 297	6. 266				
200	8.527	59.731	53.803	7.114				
300	8.604	60.417	54. 285	7.971				
400	8.674	61.057	54.746	8.835				
500	8.738	61.657	55. 187	9.705				
600	8.799	62. 223	55.609	10.582				
700	8.858	62.759	56.014	11.465				
800	8.915	63. 267	56. 403	12.354				
900	8.972	63.750	56.777	13. 248				
000	9.028	64. 212	57.138	14.148				
			227.44					
100	9.083	64.654	57.485	15.054				
200 300	9.138	65.077	57.821	15-965				
100	9.193	65.485 65.877	58. 145 58. 459	16.881 17.803				
500	9. 246 9. 299	66.256	58.763	18.731				
	,,,,,	***************************************	301.103	101151				
00	9.351	66.622	59.059	19.663				
00	9.402	66.975	59.345	20.601				
00	9.451	67.318	59.624	21.543				
00	9.499	67.651	59.895	22.491				
	9.546	67.974	60.159	23.443				
00	9.591	68. 288	60.417	24.400				
00	9.635	68.593	60.667	25.362				
00	9.677	68.890	60.912	26.327				
100	9.718	69.180	61.151	27. 297				
00	9.758	69.462	61.385	28.271				
00	9.796	69.738	61.613	29.249				
00	9.833	70.007	61.836	30.230				
00	9.869	70. 269	62.055	31.215				
00	9.905	70.526	62. 269	32, 204				
00	9.940	70.778	62.479	33.196				
00	9.976	71.024	62.684	14 102				
00	10.012	71.024 71.265	62.886	34, 192 35, 192				
00	10.049	71.501	63.084	36. 195				
00	10.088	71.733	63.278	37. 203				
00	10.130	71.960	63.468	38.214				
			12.454					
00	10.176	72.184	63.656	39. 230				
00	10.226	72.404	63.840	40. 251				
00 00	10. 283 10. 347	72.620 72.834	64.021 64.199	41, 278 42, 311				
00	10.421	73.044	64. 374	43.352				
00	10.506	73. 252	64. 546	44. 402				
00	10.607	73.459	64.716	45.462				
00 00	10.724 10.863	73.663 73.867	64.883 65.048	46.535				
00	11.027	74, 070	65. 211	48.728				
00	11.222	74. 274 74. 479	65.371 65.530	49.855 51.007	•			
00 00	11.453 11.727	74.685	65.687	52. 191				
00	12.052	74.895	65.842	53.412				
00	12. 439	75.109	65.996	54.677				

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#### OXYGEN REFERENCE STATE

	c	d/°K gf+ —			Kcal/j	d =	`
T, "K	C <sub>p</sub>	s <sub>T</sub>	$-(F_{T}^{\circ} - H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF	Log K
298.15	±.000	±.003	±.003	±.000			
1000	±.001	±.004	±.004	±.001			
2600	±.002	±.005	±.004	±.002			
3000	±.005	±.007	±.004	±.005			
4000	±.014	±.009	±.006	±.014			
5000	±.089	±.018	±.007	±.057			
6000	±.673	±.081	±.013	±.407			

present work, the sum has been taken to infinite energy. The effect of the alternative procedures will be evident only at the higher temperatures. Thus, at 5000°K, Woolley's 55 free-energy function would have been increased by 0.0003 cal/oK gfw had he summed to infinite energy, and his heat content would have been 14 cal/gfw greater. If levels for the two new states had been included, the differences in the two calculations for the free-energy function and heat content would have been 0.0005 cal/OK gfw and 30 cal/gfw, respectively, at 5000 K. Although some procedure for taking into account the effect of dissociation or pre-dissociation on the thermodynamic functions is certainly valid, it was preferred here to retain the simplicity of the present procedure. The uncertainty in the thermodynamic functions of oxygen which results is far less than the uncertainty in the functions of other substances with which the oxygen data will be combined. The uncertainties in the thermodynamic functions summarized on the back of Table XXXIV do not include a contribution from a summation to infinite energy.

The results of the present calculation are compared below with those in the JANAF compilation  $^{309}$  at selected temperatures:

Temp. <sup>O</sup> K		– H <sub>298</sub> ) l/gfw	–(F <sub>T</sub> – H <sub>298</sub> )/Т cal/ <sup>0</sup> К gfw		
	Avco	JANAF	Avco	JANAF	
298.15	0.000	0.000	49.007	49.004	
1000	5. 427	5. 427	52. 767	52. 765	
2000	14.148	14. 149	57. 138	57. 136	
3000	23. 443	23.446	60. 159	60. 157	
4000	33. 196	33. 201	62. 479	62.476	
5000	43. 352	43.257	64. 374	64. 368	
6000	54. 677	53. 479	65. 996	65. 970	

The JANAF table was taken from Woolley, <sup>55</sup> with a reduction of the entropies by 0.0065 cal/<sup>o</sup>K gfw. This amount had been added by Woolley <sup>55</sup> to account for the difference in symmetry number between heteronuclear and homonuclear isotopes.

 $(H_{298}^{o} - H_{0}^{o})$  was calculated to be 2074.7 cal/gfw.

### b. Monatomic Oxygen

# Dissociation energy of oxygen

The dissociation energy of  $O_2^{16}$  was taken to be 117.973  $\pm$  0.04 Kcal/gfw (41260  $\pm$  15 cm<sup>-1</sup>) from Brixand Herzberg. <sup>310</sup> The correction to a naturally occurring isotopic mixture was negligible.

# 2) Ideal monatomic gas thermodynamic functions

The ideal monatomic gas thermodynamic functions of oxygen in Table XXXV were calculated with the energy levels given by Moore 52 and the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table. H<sub>298</sub> - H<sub>0</sub> was found to be 1,607.50 cal/mole for the ideal monatomic gas.

<sup>310</sup>Brix, P. and G. Herzberg, J. Chem. Phys. 21, 2240 (1953).

# IDEAL MONATOMIC GAS

0

Reference State for Calculating  $\Delta H_f^a$  ,  $\delta F_f^{\mu\nu}$  , and  $L_{0g}~K_p$  : Diatomic Gas from 298, 15° to 6000  $^5$  K.

gfw = 16.000

298, 15 5, 237 38, 469 38, 469 0, 000 59, 557 55, 33, 300 5, 235 38, 501 38, 469 0, 000 59, 557 55, 33, 300 5, 235 38, 501 38, 469 0, 010 59, 561 55, 34 400 5, 135 39, 992 38, 673 0, 528 59, 724 53, 9 500 5, 081 41, 131 39, 055 1, 038 59, 868 52, 44 600 5, 049 42, 054 39, 460 1, 544 59, 996 52, 44 600 5, 029 42, 831 39, 905 2, 048 60, 111 49, 41 680 5, 015 43, 502 40, 701 3, 052 60, 309 46, 41 79, 900 5, 006 44, 092 40, 701 3, 052 60, 309 46, 47, 99 600 5, 006 44, 092 40, 701 3, 052 60, 309 46, 41 79, 900 5, 006 44, 092 40, 701 3, 052 60, 309 46, 41 79, 900 45, 529 41, 737 4, 551 60, 550 41, 731 3100 4, 994 45, 095 41, 737 4, 551 60, 550 41, 731 3100 4, 994 45, 299 42, 315 5, 548 60, 688 38, 61 5100 4, 981 46, 298 42, 335 5, 548 60, 688 38, 61 5100 4, 982 46, 642 42, 611 6, 046 60, 750 37, 01 6100 4, 991 47, 265 41, 121 7, 042 60, 886 33, 81 8100 4, 979 47, 265 41, 121 7, 042 60, 886 33, 81 8100 4, 978 47, 819 41, 888 8, 018 60, 971 30, 61 8100 4, 978 47, 819 41, 888 8, 018 60, 971 30, 61 8100 4, 978 48, 074 41, 806 4, 978 47, 819 41, 806 4, 978 47, 819 41, 806 4, 978 47, 819 41, 806 4, 978 48, 074 41, 806 4, 978 48, 074 41, 806 4, 978 48, 979 47, 550 41, 121 7, 042 60, 886 33, 81 800 4, 978 48, 074 41, 806 4, 981 49, 982 44, 199 41, 816 44, 799 47, 550 41, 110 60, 40, 978 48, 074 41, 806 48, 516 61, 019 29, 00 49, 978 48, 074 41, 806 48, 516 61, 019 29, 00 49, 978 48, 074 41, 806 48, 516 61, 019 29, 00 49, 978 48, 074 41, 806 48, 516 61, 019 29, 00 49, 984 49, 186 44, 775 41, 10, 025 61, 107 25, 88 80, 00 49, 994 49, 926 44, 410 61, 0.029 61, 145 61, 107 25, 88 80, 10, 10, 10, 10, 10, 10, 10, 10, 10, 1	.*x	c,	cai/°K gfv	-(FT -H298)/T	H <sub>T</sub> - H <sub>296</sub>	———— Keal/gfv ΔΗ <sup>°</sup> <sub>t</sub>	ΔF	Lo
298, 15 5, 237 38, 469 36, 469 0, 000 59, 557 55, 35, 300 5, 235 38, 501 38, 469 0, 010 59, 561 55, 3 400 5, 135 39, 992 38, 673 0, 528 59, 724 53, 9 500 5, 081 41, 131 39, 055 1, 038 59, 868 52, 4 660 5, 049 42, 054 39, 460 1, 544 59, 996 52, 4 660 5, 049 42, 054 39, 460 1, 544 59, 996 50, 9 700 5, 029 42, 831 19, 905 2, 048 60, 111 49, 4 680 5, 015 43, 502 40, 314 2, 550 60, 214 47, 9 900 5, 006 44, 092 40, 701 3, 052 60, 309 46, 4 77, 990 44, 619 41, 067 3, 552 60, 395 44, 8 100 4, 994 45, 529 41, 737 4, 551 60, 550 41, 7 300 4, 997 45, 529 41, 737 4, 551 60, 550 41, 7 300 4, 992 46, 642 42, 611 6, 046 60, 750 37, 0 500 4, 982 46, 642 42, 611 6, 046 60, 750 37, 0 600 4, 981 46, 963 42, 315 5, 548 60, 688 38, 6 600 4, 981 46, 963 42, 315 7, 042 60, 866 33, 8 800 4, 979 47, 265 43, 123 7, 042 60, 866 33, 8 800 4, 978 47, 899 43, 888 8, 018 60, 971 30, 67 700 4, 978 47, 891 43, 888 8, 018 60, 971 30, 67 800 4, 981 48, 991 44, 216 9, 512 60, 970 32, 22 800 4, 980 49, 88 42, 315 88 8, 018 60, 971 30, 67 800 4, 981 48, 991 44, 216 9, 512 61, 107 25, 88 800 4, 978 47, 891 44, 1016 10, 1029 61, 145 24, 28 800 4, 978 48, 197 44, 116 9, 512 61, 107 25, 88 800 4, 978 48, 197 44, 116 9, 512 61, 107 25, 88 800 4, 980 48, 770 44, 410 10, 1029 61, 145 24, 22, 26 800 4, 980 48, 770 44, 410 10, 1029 61, 145 24, 22, 26 800 4, 980 48, 770 44, 410 10, 1029 61, 145 24, 22, 26 800 4, 980 48, 770 44, 410 10, 1029 61, 145 24, 22, 26 800 4, 980 49, 186 44, 775 11, 1026 61, 128 21, 107 800 5, 010 5, 010 50, 260 45, 736 14, 522 61, 1307 16, 24 800 5, 010 5, 010 50, 066 45, 588 13, 522 61, 1307 16, 24 800 5, 010 5, 010 50, 026 45, 736 14, 522 61, 1307 16, 24 800 5, 010 5, 010 50, 026 45, 736 14, 023 61, 380 11, 42 800 5, 010 5, 010 50, 026 47, 785 22, 11, 126 61, 137 9, 14, 14, 14, 14, 14, 14, 14, 14, 14, 14			•					
100							58,986	Inf
\$ 1.95 \$ 1.95 \$ 1.95 \$ 1.96 \$ 1.97 \$ 1.98 \$ 2.98 \$ 3.99 \$ 2.98 \$ 3.99 \$ 4.89 \$ 4.99 \$ 4.89 \$ 4.99 \$ 4.89 \$ 4.99 \$ 4.89 \$ 4.99 \$ 4.89 \$ 4.99 \$ 4.89 \$ 4.99 \$							55. 393	-40
500         5,081         41,131         39,055         1,038         59,868         52,44           600         5,049         42,054         39,480         1,544         59,996         50,99         60,77         700         5,029         42,831         39,955         2,048         60,111         49,44         49,990         5,006         44,092         40,701         3,052         60,399         46,4         47,999         46,4092         40,701         3,052         60,395         44,81         99,90         5,006         44,092         40,701         3,052         60,395         44,81         40,701         3,052         60,395         44,81         40,701         3,052         60,395         44,81         40,701         3,052         60,395         44,81         46,41         41,71         4,91         46,42         44,81         41,71         4,951         60,45         41,71         40,11         40,11         41,71         40,11         40,11         41,71         40,11         40,11         41,71         40,11         40,11         41,71         40,11         40,11         41,71         40,11         41,71         40,11         41,71         40,11         41,71         40,11         41,71         40,11 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>55. 367</td> <td>-40</td>							55. 367	-40
100   1,049   42,054   39,480   1,544   59,996   50,970   50,029   42,831   39,905   2,048   60,111   49,48   60,000   4,999   44,599   40,701   3,052   60,309   46,48   60,000   4,999   44,619   41,067   3,552   60,395   44,88   60,000   4,999   44,619   41,067   3,552   60,395   44,88   60,000   4,994   45,095   41,412   4,051   60,475   43,31   400   4,987   45,299   42,045   5,049   60,621   40,11   400   4,984   46,288   42,335   5,548   60,688   38,6   6500   4,982   46,642   42,611   6,046   60,750   37,00   4,972   46,642   42,611   6,046   60,750   37,00   4,979   47,550   43,361   7,540   60,621   40,11   49,40   49,799   47,550   43,361   7,540   60,920   32,27   60,000   4,979   47,550   43,361   7,540   60,920   32,27   60,000   4,978   48,074   41,866   8,516   61,019   29,06   40,979   47,810   44,216   9,034   61,064   27,48   400   4,978   48,074   41,866   8,516   61,019   29,06   40,979   47,810   44,216   9,034   61,064   27,48   400   4,978   48,770   44,216   9,034   61,064   27,48   400   4,978   48,770   44,410   10,029   61,145   24,28   400   4,981   48,982   44,596   10,527   61,182   22,67   61,007   61,490   49,780   49,786   49,186   44,775   11,026   61,218   21,07   600   5,004   50,096   45,588   13,522   61,307   61,280   600   5,004   50,096   45,588   13,522   61,307   61,280   600   5,004   50,096   45,588   13,522   61,307   61,280   600   5,005   51,102   46,418   16,537   61,470   3,35   61,280   51,100   5,005   51,102   46,418   16,537   61,470   3,35   61,280   51,100   5,005   51,102   46,418   16,537   61,470   3,35   61,280   51,100   5,005   51,102   46,418   16,537   61,470   3,35   60,000   5,104   50,000   5,114   51,795   47,132   19,566   61,479   61,485   61,590   61,557   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   61,596   61,597   6							53, 945	- 29
700	)0	5.081	41, 131	39, 055	1.038	59.868	52.483	- 2.
800 5.015 43.502 40.314 2.550 60.214 47.97 900 5.006 44.092 40.701 3.052 60.395 44.87 900 4.999 44.619 41.067 3.552 60.395 44.87 100 4.999 45.095 41.412 4.051 60.475 43.37 200 4.990 45.529 41.737 4.551 60.550 41.77 300 4.987 45.529 41.737 4.551 60.550 41.77 300 4.987 45.529 41.737 4.551 60.550 41.77 300 4.987 45.529 42.045 5.049 60.621 40.11 400 4.984 46.288 42.355 5.548 60.688 38.6 500 4.981 46.963 42.873 6.544 60.810 35.44 700 4.999 47.655 43.123 7.042 60.866 33.86 800 4.999 47.655 43.123 7.042 60.866 33.88 800 4.979 47.550 43.361 7.540 60.920 32.27 900 4.978 48.074 43.808 8.536 61,019 29.00 100 4.978 48.074 43.808 8.536 61,019 29.00 100 4.978 48.94 44.216 9.532 61.107 25.88 300 4.990 48.770 44.410 10.029 61.145 24.28 400 4.981 48.982 44.596 10.527 61.182 22.67 800 4.990 49.589 45.116 12.023 61.282 12.07 800 4.990 49.786 49.186 44.775 11.026 61.218 21.07 800 4.990 49.559 45.116 12.023 61.280 17.86 800 4.994 49.186 44.775 11.026 61.218 12.07 800 4.990 49.559 45.116 12.023 61.280 17.86 800 4.994 49.551 45.279 12.522 61.307 16.24 900 4.990 49.559 45.116 12.023 61.280 17.86 800 4.994 49.551 45.279 12.522 61.307 16.24 900 4.990 49.559 45.116 12.023 61.280 17.86 800 4.990 49.995 45.486 13.022 61.331 14.64 800 5.010 50.026 45.736 14.023 61.380 17.42 800 5.017 50.419 45.880 14.524 61.400 9.81 800 6.999 49.956 45.588 13.522 61.357 13.00 800 5.017 50.419 45.880 14.524 61.400 9.81 800 5.017 50.419 46.289 16.033 61.455 4.99 800 5.017 50.419 46.589 16.033 61.455 4.99 800 5.017 50.419 47.558 21.641 61.583 -1.49 800 5.010 50.25 50.574 46.020 15.026 61.419 8.19 800 5.011 50.870 46.289 16.033 61.455 4.99 800 5.012 50.459 47.558 21.641 61.559 61.438 6.55 800 5.014 50.870 46.289 16.033 61.455 4.99 800 5.015 50.25 50.574 46.020 15.026 61.419 6.155 4.99 800 5.010 50.25 50.574 46.020 15.026 61.419 6.155 4.99 800 5.010 50.25 50.574 46.020 15.026 61.419 6.155 4.99 800 5.010 50.25 50.574 46.020 15.026 61.515 4.99 800 5.010 50.25 50.574 46.020 15.026 61.515 4.99 800 5.114 50.195 47.755 80.419 80.610 51.556 61.577 -7.95 800 5.120 52.26	00	5.049	42,054	39,480	1.544	59.996	50.994	- 18
800 5.015 43.502 40.314 2.550 60.214 47.97 900 5.006 44.092 40.701 3.052 60.395 44.87 1000 4.999 44.619 41.067 3.552 60.395 44.87 1100 4.994 45.095 41.412 4.051 60.475 43.37 1200 4.997 45.529 41.737 4.551 50.550 41.77 1300 4.987 45.529 41.737 4.551 50.550 40.886 13.60 4.984 46.288 42.355 5.548 60.888 38.67 14.982 46.642 42.611 6.046 60.750 37.07 14.992 46.642 42.873 6.544 60.810 35.44 14.990 4.984 46.288 42.355 5.548 60.888 38.67 14.990 4.998 47.819 47.855 43.123 7.042 60.866 33.87 18.00 4.999 47.655 43.123 7.042 60.866 33.87 18.00 4.979 47.555 43.123 7.042 60.866 33.87 18.00 4.978 48.074 43.806 8.536 61.019 29.00 19.00 4.978 48.074 33.808 8.038 60.971 30.67 19.00 4.978 48.974 44.216 9.532 61.107 25.88 19.00 4.981 48.982 44.596 10.527 61.182 22.67 19.00 4.984 49.186 44.775 11.026 61.218 21.07 19.00 4.984 49.186 44.775 11.026 61.218 21.07 19.00 4.990 49.559 45.116 12.023 61.282 17.07 10.00 4.990 49.559 45.116 12.023 61.280 17.86 10.00 4.991 49.559 45.116 12.023 61.280 17.86 10.00 4.994 49.751 45.279 12.522 61.307 16.24 10.00 5.010 50.260 45.736 46.200 15.026 61.419 8.19 10.00 5.004 50.096 45.588 13.522 61.357 13.00 10.00 5.004 50.096 45.588 13.522 61.357 13.00 10.00 5.004 50.096 45.588 13.522 61.357 13.00 10.00 5.005 50.04 50.096 45.588 13.522 61.357 13.00 10.00 5.000 5.004 50.096 45.588 13.522 61.357 13.00 10.00 5.000 5.004 50.096 45.588 13.522 61.357 13.00 10.00 5.000							49.484	- 1
900							47.959	-1.
1000   4,999   44,619   41,067   3,552   60,395   44,81							46.421	-1
1200							44.873	-
1200	00 .	4 994	45 005	41 412	4 051	60 475	43 317	-1
1300							41.754	
							40, 184	-1
4,982         46,642         42,611         6,046         60,750         37,03           600         4,981         46,963         42,873         6,544         60,810         35,44           700         4,979         47,265         43,123         7,042         60,866         33,81           800         4,979         47,550         43,361         7,540         60,920         32,21           900         4,978         47,819         43,588         8,038         60,971         30,61           1000         4,978         48,074         43,806         8,536         61,094         27,48           2000         4,978         48,317         44,016         9,034         61,064         27,48           2000         4,979         46,549         44,216         9,532         61,107         25,88           3000         4,980         48,770         44,410         10,029         61,145         24,28           400         4,981         48,982         44,594         10,527         61,182         22,07           500         4,984         49,186         44,775         11,026         61,218         21,07           600         4,944         49							38, 610	-1
1700							37.031	- 9
1700			46.063	43.073		(0.010	25 440	
1800								
990								
1000         4,978         48,074         43,806         8,536         61,019         29,08           1100         4,978         48,317         44,016         9,034         61,064         27,48           1200         4,979         48,549         44,216         9,532         61,107         25,88           1300         4,980         48,770         44,410         10,029         61,145         24,28           1400         4,981         48,982         44,596         10,527         61,182         22,67           1500         4,984         49,186         44,775         11,026         61,218         21,07           1600         4,986         49,381         44,949         11,524         61,249         19,47           1600         4,994         49,751         45,279         12,522         61,307         16,24           1700         4,999         49,926         45,436         13,022         61,334         14,64           100         5,010         50,260         45,736         14,023         61,380         11,42           200         5,017         50,419         45,880         14,524         61,400         9,81           300								- :
100								- :
1200   4,979   48,549   44,216   9,532   61,107   25,88	10 1	a. 9/8	48.074	43.806	8.536	91.014	29.083	- 3
300	00	4.978	48.317	44.016	9.034		27.484	- 2
400 4,981 48,982 44,596 10,527 61,182 22,67 500 4,984 49,186 44,775 11,026 61,218 21,07 600 4,986 49,381 44,949 11,524 61,249 19,46 600 4,990 49,569 45,116 12,023 61,280 17,86 800 4,990 49,569 45,116 12,023 61,280 716,24 900 4,999 49,926 45,436 13,022 61,334 14,64 900 5,004 50,096 45,588 13,522 61,357 13,03 100 5,010 50,260 45,736 14,023 61,380 11,42 200 5,017 50,419 45,880 14,524 61,400 9,81 300 5,025 50,574 46,020 15,026 61,419 8,19 400 5,033 50,724 46,156 15,529 61,438 6,58 500 5,041 50,879 46,289 16,033 61,455 4,96 600 5,050 51,012 46,418 16,537 61,470 3,35 700 5,060 51,150 46,544 17,043 61,485 1,74 800 5,070 51,285 46,667 17,549 61,498 0,12 900 5,081 51,417 46,787 18,057 61,512 -1,49 900 5,091 51,546 46,905 18,565 61,576 -11,181 200 5,114 51,795 47,132 19,586 61,547 -6,33 300 5,126 51,916 47,242 20,098 61,557 -7,95 600 5,186 52,149 47,455 21,126 61,589 -14,411 800 5,138 52,033 47,349 20,611 61,567 -9,56 800 5,162 52,262 47,558 21,641 61,583 -12,80 800 5,164 52,481 47,758 22,676 61,594 -16,03 800 5,164 52,282 47,558 21,126 61,594 -16,03 800 5,164 52,481 47,758 22,676 61,594 -16,03 800 5,266 52,481 47,758 22,676 61,594 -16,03 800 5,266 52,481 47,758 22,676 61,594 -16,03 800 5,266 53,194 48,046 24,237 61,593 -12,661 800 5,266 53,194 48,046 24,237 61,594 -16,03 800 5,266 53,194 48,046 24,237 61,593 -12,661 800 5,266 53,194 48,046 24,237 61,593 -12,661 800 5,266 53,194 48,046 24,237 61,593 -20,881 800 5,266 53,194 48,046 24,237 61,593 -12,661 800 5,266 53,194 48,046 24,237 61,593 -22,493 800 5,266 53,194 48,046 26,335 61,545 -3,100 800 5,269 53,194 48,046 26,335 61,493 -28,895 800 5,269 53,194 48,046 26,335 61,493 -28,895 800 5,269 53,194 48,406 26,335 61,493 -28,895 800 5,269 53,194 48,406 26,335 61,493 -28,895 800 5,269 53,194 48,406 26,335 61,493 -28,895 800 5,260 53,475 48,661 27,921 61,383 -22,600 800 5,260 53,475 48,661 27,921 61,383 -22,600 800 5,260 53,475 48,661 27,921 61,383 -22,800 800 5,260 53,475 48,661 27,921 61,383 -22,800 800 5,260 53,475 48,661 27,921 61,383 -22,800	10	4.979	48,549	44.216	9.532	61.107	25,884	- 7
4.981					10.029	61, 145	24.282	- 2
500         4,984         49,186         44,775         11,026         61,218         21,07           600         4,986         49,381         44,949         11,524         61,249         19,46           700         4,990         49,569         45,116         12,023         61,280         17,86           800         4,994         49,751         45,279         12,522         61,307         16,24           900         4,999         49,926         45,436         13,022         61,334         14,64           900         5,004         50,096         45,588         13,522         61,357         13,03           100         5,010         50,260         45,736         14,023         61,380         11,42           200         5,017         50,419         45,880         14,524         61,400         9,81           300         5,025         50,574         46,020         15,026         61,419         8,19           400         5,033         50,724         46,156         15,529         61,418         6,58           500         5,041         50,879         46,289         16,033         61,455         4,96           600         5,05							22.679	- 2
700	10	4.984	49.186	44.775	11.026	61.218	21.075	- 1
700	10 ,	4 996	49 381	44 949	11 524	61 249	19 468	- !
800								-1
900								-1
000         5,004         50,096         45,588         13,522         61,357         13.03           100         5,010         50,260         45,736         14,023         61,380         11,42           200         5,017         50,419         45,880         14,524         61,400         9,81           300         5,025         50,574         46,020         15,026         61,419         8,19           400         5,033         50,724         46,156         15,529         61,438         6,58           500         5,041         50,879         46,289         16,033         61,455         4,96           600         5,050         51,012         46,418         16,537         61,470         3,35           700         5,060         51,150         46,544         17,043         61,485         1,74           800         5,070         51,285         46,667         17,549         61,498         0,12           900         5,081         51,417         46,787         18,565         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,524         -3,10           100         5,103 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>-1</td>								-1
100							13.033	- 0
200         5,017         50,419         45,880         14,524         61,400         9,81           300         5,025         50,574         46,020         15,026         61,419         8,19           400         5,033         50,724         46,156         15,529         61,438         6,58           500         5,041         50,879         46,289         16,033         61,455         4,96           600         5,050         51,012         46,418         16,537         61,470         3,35           700         5,060         51,150         46,544         17,043         61,485         1,74           800         5,070         51,285         46,667         17,549         61,498         0,12           900         5,081         51,417         46,787         18,057         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,524         -3,10           100         5,103         51,672         47,019         19,075         61,536         -4,71           200         5,114         51,795         47,132         19,586         61,547         -6,33           300         5,126 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>								
300         5,025         50,574         46,020         15,026         61,419         8,19           400         5,033         50,724         46,156         15,529         61,438         6,58           500         5,041         50,879         46,289         16,033         61,455         4,96           600         5,050         51,012         46,418         16,537         61,470         3,35           700         5,060         51,150         46,544         17,043         61,485         1,74           880         5,070         51,285         46,667         17,549         61,498         0,12           900         5,081         51,417         46,787         18,057         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,524         -3,10           100         5,103         51,672         47,019         19,075         61,536         -4,71           200         5,114         51,795         47,132         19,586         61,547         -6,33           300         5,126         51,916         47,242         20,098         61,557         -7,95           400         5,138<							11.420	- C
400         5,033         50,724         46,156         15,529         61,438         6,58           500         5,041         50,879         46,289         16,033         61,455         4,96           600         5,050         51,012         46,418         16,537         61,470         3,35           700         5,060         51,150         46,544         17,043         61,485         1,74           800         5,070         51,285         46,667         17,549         61,498         0,12           990         5,081         51,417         46,787         18,057         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,536         -4,71           200         5,114         51,795         47,132         19,586         61,547         -6,33           300         5,126         51,916         47,242         20,098         61,557         -7,95           400         5,138         52,033         47,349         20,611         61,567         -9,56           500         5,162								- 0
500         5,041         50,870         46,289         16,033         61,455         4,96           600         5,050         51,012         46,418         16,537         61,470         3,35           700         5,960         51,150         46,544         17,043         61,485         1,74           800         5,070         51,285         46,667         17,549         61,498         0,12           900         5,081         51,417         46,787         18,057         61,512         -1,49           900         5,081         51,417         46,787         18,057         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,512         -1,49           900         5,133         51,672         47,019         19,075         61,536         -4,71           200         5,114         51,795         47,132         19,586         61,547         -6,33           300         5,126         51,916         47,242         20,098         61,557         -7,95           400         5,138         52,333         47,349         20,611         61,567         -9,56           500         5,16								-0
6000         5,050         51,012         46,418         16,537         61,470         3,35           700         5,050         51,150         46,544         17,043         61,485         1,74           800         5,070         51,285         46,667         17,549         61,498         0,12           900         5,081         51,417         46,787         18,057         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,512         -1,49           900         5,091         51,546         46,905         18,565         61,536         -4,71           100         5,103         51,672         47,019         19,075         61,536         -4,71           200         5,114         51,795         47,132         19,586         61,547         -6,33           300         5,126         51,916         47,242         20,098         61,557         -7,95           400         5,138         52,033         47,349         20,611         61,567         -9,56           500         5,150         52,149         47,455         21,126         61,576         -11,18           600         5								- 0 - 0
700	,	3.041	30,073	40, 20)	10.035	01, 433	4. 701	-0
800         5,070         51,285         46,667         17,549         61,498         0,12           900         5,081         51,417         46,787         18,057         61,512         -1,49           900         5,091         51,546         46,705         18,565         61,512         -1,49           100         5,003         51,672         47,019         19,075         61,536         -4,71           200         5,114         51,795         47,132         19,586         61,547         -6,33           300         5,126         51,916         47,242         20,098         61,557         -7,95           400         5,138         52,033         47,349         20,611         61,567         -9,56           500         5,150         52,149         47,455         21,126         61,576         -11,18           600         5,162         52,262         47,558         21,641         61,583         -12,80           700         5,174         52,374         47,659         22,158         61,589         -14,41           800         5,186         52,483         47,758         22,676         61,594         -16,03           900         <							3, 354	-0
900 5.081 51.417 46.787 18.057 61.512 -1.49 000 5.091 51.546 46.905 18.565 61.524 -3.10  100 5.103 51.672 47.019 19.075 61.536 -4.71 200 5.114 51.795 47.132 19.586 61.547 -6.33 300 5.126 51.916 47.242 20.098 61.557 -7.95 400 5.138 52.033 47.349 20.611 61.567 -9.56 500 5.150 52.149 47.455 21.126 61.576 -11.186  800 5.162 52.262 47.558 21.641 61.583 -12.80  700 5.174 52.374 47.659 22.158 61.589 14.41  800 5.186 52.483 47.758 22.676 61.594 -16.03  900 5.186 52.483 47.758 22.676 61.594 -16.03  900 5.198 52.590 47.856 23.195 61.596 -17.656  100 5.210 52.695 47.952 23.715 61.596 -17.656  100 5.222 52.798 48.046 24.237 61.593 -20.889  100 5.246 52.900 48.138 24.760 61.586 -22.499  100 5.258 53.098 48.318 25.809 61.555 -24.73  100 5.269 53.194 48.406 26.335 61.528 -27.346  100 5.260 5.269 53.194 48.406 26.335 61.528 -27.346  100 5.280 53.289 48.492 26.863 61.493 -28.957  100 5.292 53.383 48.577 27.392 61.445 -30.579  100 5.292 53.383 48.577 27.392 61.445 -30.579  100 5.292 53.383 48.577 27.392 61.445 -30.579  100 5.292 53.383 48.577 27.392 61.445 -30.579  100 5.292 53.383 48.577 27.392 61.445 -30.579  100 5.292 53.383 48.577 27.392 61.445 -30.579							1,741	- 0
000         5,091         51,546         46,905         18,565         61,524         -3,10           100         5,103         51,672         47,019         19,075         61,536         -4,71           200         5,114         51,795         47,132         19,586         61,547         -6,33           300         5,126         51,916         47,242         20,098         61,557         -7,95           400         5,138         52,033         47,349         20,611         61,567         -9,56           500         5,150         52,149         47,455         21,126         61,576         -11,18           600         5,162         52,262         47,558         21,641         61,583         -12,80           700         5,174         52,374         47,659         22,188         61,589         -14,41           800         5,186         52,483         47,758         22,676         61,594         -16,03           900         5,198         52,590         47,856         23,195         61,596         -17,656           100         5,222         52,798         48,046         24,237         61,596         -19,261           100							0,125	- 0
100							-1.490	0
200         5,114         51.795         47,132         19,586         61,547         -6.33           300         5,126         51.916         47,242         20.098         61,557         -7.95           400         5,138         52.033         47,349         20,611         61,567         -9.56           500         5,150         52,149         47.455         21,126         61.576         -11.18           600         5,162         52,262         47.558         21,641         61.583         -12.80           700         5,174         52,374         47.659         22,188         61,589         -14.41           800         5,186         52,483         47.758         22,676         61.594         -16.03           900         5,198         52,590         47.856         23,195         61.596         -17.65           900         5,210         52,695         47.952         23.715         61.596         -17.65           100         5,222         52,798         48,046         24,237         61.593         -20.88           200         5,244         52,999         48.229         25.284         61.574         -24.11           800	0 5	5.091	51,546	46.905	18.565	61.524	- 3, 107	0
300 5,126 51,916 47,242 20,098 61,557 -7,95 400 5,138 52,033 47,349 20,611 61,567 -9,56 500 5,150 52,149 47,455 21,126 61,567 -9,56 600 5,162 52,262 47,558 21,641 61,583 -12,80 700 5,174 52,374 47,659 22,158 61,589 -14,41 800 5,186 52,483 47,758 22,676 61,594 -16,03 800 5,198 52,590 47,856 23,195 61,596 -17,655 800 5,210 52,695 47,952 23,715 61,596 -17,655 800 5,222 52,798 48,046 24,237 61,593 -20,881 800 5,246 52,999 48,138 24,760 61,586 -22,493 800 5,246 52,999 48,229 25,284 61,574 -24,114 800 5,258 53,098 48,318 25,809 61,555 -25,731 800 5,269 53,194 48,406 26,335 61,528 -27,346 800 5,280 53,289 48,492 26,863 61,493 -28,957 800 5,240 53,383 48,577 27,392 61,445 -30,571 800 5,242 53,383 48,577 27,392 61,445 -30,571 800 5,242 53,383 48,577 27,392 61,445 -30,571 800 5,242 53,383 48,577 27,392 61,445 -30,571 800 5,302 53,475 48,661 27,921 61,383 -32,186 800 5,313 53,566 48,743 28,452 61,303 -33,793	C 5	5.103	51,672	47.019	19.075	61,536	-4.719	0
400 5, 138 52,033 47, 349 20,611 61,567 -9,56 600 5,150 52,149 47,455 21,126 61,576 -11,18i 600 5,152 52,262 47,558 21,641 61,583 -12,80 700 5,174 52,374 47,659 22,158 61,589 14,411 800 5,186 52,483 47,758 22,676 61,594 -16,03 800 5,186 52,483 47,758 22,676 61,594 -16,03 800 5,198 52,590 47,856 23,195 61,596 -17,65i 800 5,222 52,798 48,046 24,237 61,596 -17,65i 800 5,222 52,798 48,046 24,237 61,593 -20,88i 800 5,246 52,999 48,229 25,284 61,574 -24,114 800 5,258 53,098 48,318 25,809 61,555 -24,73 800 5,269 53,194 48,406 26,335 61,528 -27,346 800 5,280 53,289 48,492 26,863 61,493 -28,95i 800 5,292 53,383 48,577 27,392 61,445 -30,57i 800 5,292 53,383 48,577 27,392 61,445 -30,57i 800 5,292 53,475 48,661 27,921 61,383 -32,186 800 5,113 53,566 48,743 28,452 61,303 -33,79;	0 5	5.114	51.795	47.132		61.547	-6.337	0
500         5,150         52,149         47,455         21,126         61,576         -11,186           600         5,162         52,262         47,558         21,641         61,583         -12,80           700         5,174         52,374         47,659         22,158         61,589         -14,41           800         5,186         52,483         47,758         22,676         61,594         -16,03           900         5,198         52,590         47,856         23,195         61,596         -17,65           900         5,210         52,695         47,952         23,715         61,596         -17,65           100         5,222         52,798         48,046         24,237         61,593         -20,881           200         5,234         52,900         48,138         24,760         61,586         -22,49           300         5,246         52,999         48,229         25,284         61,574         -24,11-4           800         5,258         53,098         48,318         25,809         61,555         25,734           800         5,280         53,194         48,406         26,335         61,528         -27,346           800 </td <td>0 5</td> <td>5, 126</td> <td>51.916</td> <td>47, 242</td> <td>20.098</td> <td>61.557</td> <td>-7.953</td> <td>0</td>	0 5	5, 126	51.916	47, 242	20.098	61.557	-7.953	0
6000         5, 162         52, 262         47, 558         21, 641         61, 583         -12, 80           700         5, 174         52, 374         47, 659         22, 158         61, 589         -14, 41           800         5, 186         52, 483         47, 758         22, 676         61, 594         -16, 03           900         5, 198         52, 590         47, 856         23, 195         61, 596         -17, 65           900         5, 210         52, 695         47, 952         23, 715         61, 596         -17, 26           100         5, 222         52, 798         48, 046         24, 237         61, 593         -20, 88           200         5, 234         52, 990         48, 138         24, 760         61, 586         -22, 49           300         5, 246         52, 999         48, 229         25, 284         61, 574         -24, 11           400         5, 258         53, 098         48, 318         25, 809         61, 555         -25, 73           500         5, 280         53, 194         48, 406         26, 335         61, 528         -27, 346           500         5, 280         53, 289         48, 577         27, 392         61, 445 <td>0 5</td> <td>5.138</td> <td>52.033</td> <td>47, 349</td> <td>20,611</td> <td>61.567</td> <td>- 9. 567</td> <td>Ð</td>	0 5	5.138	52.033	47, 349	20,611	61.567	- 9. 567	Ð
700 5,174 52,374 47,659 22,158 61,589 -14,416 800 5,186 52,483 47,758 22,676 61,594 -16,03 900 5,198 52,590 47,856 23,195 61,596 -17,65; 900 5,210 52,695 47,952 23,715 61,596 -19,26; 100 5,222 52,798 48,046 24,237 61,593 -20,88; 100 5,224 52,900 48,138 24,760 61,586 -22,49; 100 5,234 52,900 48,138 24,760 61,586 -22,49; 100 5,258 53,098 48,138 25,809 61,555 -24,73; 100 5,258 53,194 48,406 26,335 61,528 -27,346; 100 5,269 53,194 48,406 26,335 61,528 -27,346; 100 5,280 53,289 48,492 26,863 61,493 -28,95; 100 5,292 53,183 48,577 27,392 61,445 -30,57; 100 5,292 53,183 48,577 27,392 61,445 -30,57; 100 5,102 53,475 48,661 27,921 61,383 -12,186; 100 5,113 53,566 48,743 28,452 61,303 -33,79;	0 5	5.150	52.149	47.455	21.126	61.576	-11,168	0
700 5,174 52,374 47,659 22,158 61,589 -14,416 800 5,186 52,483 47,758 22,676 61,594 -16,03 900 5,198 52,590 47,856 23,195 61,596 -17,65; 900 5,210 52,695 47,952 23,715 61,596 -19,26; 100 5,222 52,798 48,046 24,237 61,593 -20,88; 100 5,224 52,900 48,138 24,760 61,586 -22,49; 100 5,234 52,900 48,138 24,760 61,586 -22,49; 100 5,258 53,098 48,138 25,809 61,555 -24,73; 100 5,258 53,194 48,406 26,335 61,528 -27,346; 100 5,269 53,194 48,406 26,335 61,528 -27,346; 100 5,280 53,289 48,492 26,863 61,493 -28,95; 100 5,292 53,183 48,577 27,392 61,445 -30,57; 100 5,292 53,183 48,577 27,392 61,445 -30,57; 100 5,102 53,475 48,661 27,921 61,383 -12,186; 100 5,113 53,566 48,743 28,452 61,303 -33,79;	n <b>s</b>	5 162	52 262	47 558	21 641	61 583	-12 801	0
300         5,186         52,483         47,758         22,676         61,594         -16,03           300         5,198         52,590         47,856         23,195         61,596         -17,65           300         5,210         52,595         47,952         23,715         61,596         -19,26           100         5,222         52,798         48,046         24,237         61,593         -20,88           200         5,234         52,900         48,138         24,760         61,586         -22,49           300         5,246         52,999         48,229         25,284         61,574         -24,11           300         5,258         53,098         48,318         25,809         61,555         -24,731           300         5,269         53,194         48,406         26,335         61,528         -27,346           300         5,280         53,289         48,492         26,863         61,493         -28,951           300         5,280         53,383         48,577         27,392         61,445         -30,571           300         5,242         53,383         48,577         27,392         61,445         -30,571           300 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>o</td>								o
900 5,198 52,590 47,856 23,195 61,596 -17,656 000 5,210 52,695 47,952 23,715 61,596 -19,261 100 5,222 52,798 48,046 24,237 61,593 -20,889 200 5,234 52,900 48,138 24,760 61,586 -22,499 300 5,246 52,999 48,229 25,284 61,574 -24,114 400 5,258 53,098 48,318 25,809 61,555 -25,731 500 5,269 53,194 48,406 26,335 61,528 -27,346 100 5,280 53,289 48,492 26,863 61,493 -28,951 100 5,242 53,383 48,577 27,392 61,445 -30,571 100 5,302 53,475 48,661 27,921 61,383 -32,182 100 5,313 53,566 48,743 28,452 61,303 -33,793								0
5,210         52,695         47,952         23,715         61,596         -19,26           100         5,222         52,798         48,046         24,237         61,593         -20,88           100         5,234         52,900         48,138         24,760         61,586         -22,49           100         5,246         52,999         48,229         25,284         61,574         -24,11-2           100         5,258         53,098         48,318         25,809         61,555         -21,734           100         5,269         53,194         48,406         26,335         61,528         -27,346           100         5,280         53,289         48,492         26,863         61,493         -28,951           100         5,292         53,383         48,577         27,392         61,445         -30,571           100         5,102         53,475         48,661         27,921         61,383         -32,186           100         5,113         53,566         48,743         28,452         61,303         -33,793								0
200     5, 234     52, 900     48, 138     24, 760     61, 586     -22, 499       100     5, 246     52, 999     48, 229     25, 284     61, 574     -24, 114       100     5, 258     53, 098     48, 318     25, 809     61, 555     -25, 73       100     5, 269     53, 194     48, 406     26, 335     61, 528     -27, 346       100     5, 280     53, 289     48, 492     26, 863     61, 493     -28, 951       100     5, 242     53, 383     48, 577     27, 392     61, 445     -30, 571       100     5, 102     53, 475     48, 661     27, 921     61, 383     -12, 182       100     5, 113     53, 566     48, 743     28, 452     61, 303     -33, 793							-19.268	0
200     5, 234     52, 900     48, 138     24, 760     61, 586     -22, 499       100     5, 246     52, 999     48, 229     25, 284     61, 574     -24, 114       100     5, 258     53, 098     48, 318     25, 809     61, 555     -25, 73       100     5, 269     53, 194     48, 406     26, 335     61, 528     -27, 346       100     5, 280     53, 289     48, 492     26, 863     61, 493     -28, 951       100     5, 242     53, 383     48, 577     27, 392     61, 445     -30, 571       100     5, 102     53, 475     48, 661     27, 921     61, 383     -12, 182       100     5, 113     53, 566     48, 743     28, 452     61, 303     -33, 793								
5,246     52,999     48,229     25,284     61,574     -24,11-2       100     5,258     53,098     48,318     25,809     61,555     -24,73-2       100     5,269     53,194     48,406     26,335     61,528     -27,34E       100     5,280     53,289     48,492     26,863     61,493     -28,95-1       100     5,292     53,303     48,577     27,392     61,445     -30,57-1       100     5,102     53,475     48,661     27,921     61,383     -32,182-1       100     5,113     53,566     48,743     28,452     61,303     -33,793-1							-20,885	0
5,258     53,098     48,318     25,809     61,555     -25,731       5,269     53,194     48,406     26,335     61,528     -27,346       500     5,280     53,289     48,492     26,863     61,493     -28,957       100     5,242     53,383     48,577     27,392     61,445     -30,571       100     5,302     53,475     48,661     27,921     61,383     -32,182       100     5,113     53,566     48,743     28,452     61,303     -33,793								0
500     5,269     53,194     48,406     26,335     61,528     -27,346       500     5,280     53,289     48,492     26,863     61,493     -28,951       700     5,292     53,383     48,577     27,392     61,445     -30,571       800     5,302     53,475     48,661     27,921     61,383     -32,182       900     5,313     53,566     48,743     28,452     61,303     -33,791								0
500 5,280 53,289 48,492 26,863 61,493 -28,951 100 5,292 53,383 48,577 27,392 61,445 -30,571 100 5,302 53,475 48,661 27,921 61,383 -32,182 100 5,313 53,566 48,743 28,452 61,303 -33,793							-27, 348	1.
100     5,242     53,383     48,577     27,392     61,445     -30,571       800     5,302     53,475     48,661     27,921     61,383     -32,182       900     5,313     53,566     48,743     28,452     61,303     -33,793								
300 5,302 53,475 48,661 27,921 61,383 -32,182 900 5,313 53,566 48,743 28,452 61,303 -33,793							- 28, 957	1.
000 5, 313 53, 566 48, 743 28, 452 61, 303 - 33, 793								1.
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1, 12, 23, 25, 190, 664 66, 464 61, 202 - 35, 39°								1.
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#### OXYGEN IDEAL MONATOMIC GAS

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T, °E	C.	s <sub>7</sub>	$-(F_{T}^{\circ} - H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	AH °	ΔF	Log Kp
498. 15	±,000	±.002	±.002	±.000	±,020	±.021	t.015
1000	±.000	±.002	±.002	±.000	±.021	±.024	±.005
2000	±.000	±.002	±,002	±.000	±.022	±.028	±.003
3000	±.000	±.002	±.002	±,000	±.025	±.032	±.002
4000	±.000	±.002	±.003	±.001	±.035	±.044	±.002
5000	±.000	±.002	±.003	±.001	±.078	±.053	±.002
6000	±.000	±,002	±,003	±.001	±.428	±.077	±.003

gfw = 195.09

		al/°K gfv			Kcal, gfw		
T, °K	c <mark>,</mark>	sc <sub>t</sub>	$-(F_{T}^{0}-H_{298}^{0})/T$	Н <sub>Т</sub> - Н <sub>298</sub>	AH j	AF	i.og K
0	0.000	6, 600	Infinite				1.6
298.15	6. 102	45. 962	45. 962	0.000			la finit
300	6.113	45. 999	45. 962	0.011			
400	6.459	47.817	46, 207	0.644			
500	6. 435	49.260	46.679	1.291			
		.,	******				
600	6.260	50.419	47,209	1.926			
700	6.059	51.369	47,738	2.542			
800	5.877	52.166	48, 243	3, 138			
900	5.728	52,849	48.717	3.718			
000	5.609	53.446	49, 161	4.285			
100	5.517	53, 976	49.575	4,841			
200	5.447	54,453	49, 962	5.389			
300	5.395	54.887	50, 325	5.931			
400	5, 358	55. 285	50.665	6.469			
500	5,333	55.654	50, <del>9</del> 85	7.003			
400	6 310	E E 000	C1 200	7 526			
600	5, 318	55.998	51,288	7.536			
700	5,311	56.320	51,575	8.067			
800 9 <b>0</b> 0	5.310 5.316	56.623 56.911	51.847 52,106	8.598 9.129			
900	5, 316	56, 911 57, 184	52, 106	9.661			
	J. J&C	57, 104	Ju. 333	7,001			
100	5.340	57, 444	52, 589	10 195			
200	5. 356	57.693	52.816	10.729			
300	5.376	57, 931	53,033	11,266			
400	5. 397	58. 160	53, 242	11.805			
500	5. 421	58, 381	53.443	12, 346			
		- 3					
600	5.445	58,594	53, 637	12.889			
700	5.470	58.800	53,824	13.435			
800	5,496	59.000	54.006	13.983			
900	5,523	59.193	54.181	14.534			
000	5.549	59. 381	54.351	15.087			
100	5.576	59.563	54.517	15.644			
200	5.603	59.740	54.677	16.203			
300	5.629	59, 913	54.833	16.764			
400	5.655	60.082	54. 985	17. 328			
500	5.681	60.246	55, 133	17.895			
400	£ 707	60.406	CC 177	18.465			
600 700	5.707	60,406 60,563	55.277 55.418	19,037			
800	5.732 5.756	60,716	55, 555	19.611			
900	5. 780	60.866	55.690	20, 188			
000	5.804	61.013	55, 821	20.767			
	3,001	01.015	33,021				
100	5.827	61.156	55.949	21.349			
200	5.850	61.297	56,075	21.932			
300	5.873	61,435	56.198	22.519			
400	5.895	61.570	56. 319	23, 107			
500	5.917	61,703	56. 437	23,698			
600	5.939	61,833	56, 553	24.290			
700	5.960	61.961	56.666	24.885			
300	5.982	62,087	56, 778	25,483			
900	6,003	62, 210	56,888	26.082			
000	6.024	62.332	56. 995	26.683			
		7.					
100	6.046	62, 451	57, 101	27, 287			
200	6.067	62,569	57. 205	27.892			
300	6.089	62, 685	57. 307	28.500			
100	6, 111	62,799	57.408 57.507	29.110 29.722			
300	6. 133	62.911	57.507	27.126			
. 600	6. 155	63,022	57.605	30.337			
700	6.178	63. 131	57. 701	30.953			
900	6, 202	63, 239	57.795	31.572			
900	6. 225	63.345	57,888	32.194			
000	6, 250	63,450	57.980	32.817			
				m*			

#### PLATINUM IDEAL MONATOMIC GAS

		I/°K gfw			Kcal/	ef w	`
T, °K	C <sub>p</sub>	s <sup>e</sup> T	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	∆H°	ΔF	Log Kp
298.15	±.000	±.002	÷.003	±.000			
1000	±.000	±.003	±.003	±.000			
2000	±.000	±,003	±.003	±,000			
3000	±.000	±.003	±.003	±.001			
4000	±.000	± 003	±.003	±,001			
5000	±,001	±.003	±.003	±.001			
6000	±.001	±.003	±.003	±.002			

# 15. Platinum

The ideal monatomic gas thermodynamic functions of platinum in Table XXXVI were calculated from the energy levels given by Moore <sup>221</sup> with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

# 16. Rhenium

The ideal monatomic gas thermodynamic functions of rhenium in Table XXXVII were computed from the energy levels listed by Moore<sup>221</sup> with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

		/°K gfw			Kcal/	kt.#	
í. 'K	C.	s <sup>e</sup> T	-(FT - H298)/T	H <sub>T</sub> - H <sub>298</sub>	7H ,	ΔF <sub>1</sub>	Lot K
ų.	0.000	0,000	Infinite				Infinit
298.15	4.968	45, 133	45, 133	0.000			
	4.968	45. 163	45, 133	0.009			
300	4,968	46, 593	45. 328	0.506			
400	4.968	47.701	45.696	1.003			
500	1.700	41.701	43.070				
600	4.968	48,607	46.108	1.500			
700	4.968	49.373	46,521	1.996			
600	4.968	50.036	46.920	2,493			
900	4.968	50.622	47.299	2.990			
000	4.968	51, 145	47.658	3.487			
100	4,968	51,619	47, 997	3.984			
200	4.969	52, 051	48.317	4,481			
		52, 449	48.620	4,978			
300	4.971		48.907	5.475			
500	4.974 4.979	52,817 53,160	49, 179	5.972			
1600	4.989	53, 482	49.438	6.471			
700	5.004	53.785	49.685	6.970			
800	5.025	54,071	49.921	7.472			
900	5.056	54, 344	50.146	7.976			
000	5.097	54.604	50.363	8.483			
100	5.150	54, 854	50.571	8, 995			
200	5, 218	55. 095	50.771	9,514			
300	5, 301	55. 329	50.964	10.040			
400	5,401	55.557	51, 151	10.574			
500	5.518	55.779	51. 331	11.120			
600	5.655	55. 998	51.507	11.679			
700	5.810	56.215	51.677	12, 252			
800	5.984	56.429	51.843	12.841			
900	6.178	56, 642	52.005	13.449			
1000	6.390	56.855	52.163	14.078			
100	6.620	57.069	52,318	14.728			
3200	6.866	57, 283	52,469	15.402			
300	7.127	57.498	52.619	16, 101			
1400	7.402	57.715	52, 765	16,828			
500	7.688	57, 933	52.910	17.582			
		** ***		10.277			
3600	7.984	58.154	53.052	18, 366			
3700	8,288	58.377	53.193	19, 179			
3800	8.596	58,602	53, 333	20.023			
3900	8.908	58,829	53.471	20.899			
1000	9.220	59.059	53.608	21.805			
100	9.531	59.290	53,743	22,743			
200	9.838	59, 524	53.878	23.711			
300	10.138	59.759	54.012	24.710			
400	10.431	59.995	54, 145	25.739			
500	10.714	60.233	54.278	26.796			
600	10.986	60,471	54.410	27.881			
700	11.244	60.710	54, 542	28.993			
800	11.489	60, 950	54, 673	30,129			
900	11.719	61.189	54.803	31,290			
000	11.932	61,428	54. 933	32.473			
100	12.130	61.666	55.063	33,676			
200	12, 311	61.903	55, 192	34,898			
300	12,475	62. 139	55, 321	36.138			
400	12.623	62.374	55.450	37. 393			
500	12,754	62,607	55.578	38.662			
600	12.869	62,838	55.705	39.943	•		
700	12.968	63.066	55.832	41.235			
800	13.052	63, 293	55, 959	42.536			
900	13, 122	63.516	56.085	43.845			
000	13,178	63, 738	46.211	45,160			
	-						
			,				

# RHENIUM IDEAL MONATOMIC GAS

	Cal/oK gfv				el v	$\overline{}$	
T,°E	c <b>,</b>	$s_T^{\bullet}$	$-(F_{T}^{o} - H_{290}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF	Log K
298, 15	±.000	±.002	±.002	±.000			
1000	±.000	±.002	±.003	±.000			
2000	±,000	±.002	±,003	±.000			
3000	±.001	±.003	±.003	± 001			
4000	±.003	±.003	±,003	±.002			
5000	±.006	±.004	±.003	±.006			
6000	±.009	±.005	±.003	±.013			

/		al 'SK gfw			Keal bin		1
CEK	C°p	SΫ́T	-(FT -H298)/T	H <sub>T</sub> - H <sub>298</sub>	ΔH $\hat{l}$	ΔF	Log k
	-р	1	298	1 290	•	•	
	0.000	0,000	Infinite				1
245, 15	5,023	44, 388	44, 388	0.000			
3CD	5.025	44.419	44.388	0.009			
400	5,174	45.883	44.587	0.518			
500	5. 386	47.060	44. 967	1.046			
	3.300	*******	,	***			
500	5.618	48.062	45.402	1.596			
:00			45, 846	2.169			
	5.839	48.945					
800	6.034	49.738	46. 284	2,763			
900	6.198	50.458	46.708	3.375			
000	6.329	51.118	47.117	4.002			
100	6.430	51.727	47.508	4.640			
200	6.505	52.290	47.884	5.287			
300	6.558	52,812	48.243	5.940			
400	6.594	53.300	48,587	6.598			
500	6.617	53.756	48, 917	7.259			
			,				
600	6,629	54 183	49.232	7.921			
		54.183					
700	6.635	54, 585	49.536	8.584			
900	6.636	54.965	49.827	9.248			
900	6.634	55, 323	50.107	9.911			
000	6.631	55.663	50.376	10.575			
100	6.626	55.987	50,636	11.237			
200	6.623	56, 295	50,886	11,900			
300	6.620	56, 589	51.128	12.562			
100	6.618			13.224			
		56.871	51.361				
500	6.618	57. 141	51.587	13.886			
	6 630	67 401	61 007	14 640			
500	6.620	57, 401	51.806	14.548			
700	6.623	57,651	52.017	15.210			
300	6.627	57.892	52, 223	15.872			
900	6.634	58.124	52,422	16.535			
000	6.641	58, 349	52,616	17.199			
100	6.650	58.567	52.805	17,864			
200	6.660	58.779	52, 988	18.529			
300	6,671	58.984	53, 167	19.196			
400	6.683	59, 183	53, 341	19.863			
500	6, 695		53, 511	20.532			
500	0.073	59. 377	33, 311	20.332			
600	6.708	59.566	53.676	21.202			
700	6.721	59.750	53.838	21.874			
300	6.735	59.929	53.996	22.547			
900	6.749	60.104	54. 150	23, 221			
000	6.764	60.275	54.301	23.897			
100	6.778	60,442	54.449	24.574			
200	6.793	60.606	54, 594	25.252			
300	5,808	60.766	54.735	25.932			
00	6.823	60.923	54.874	26,614			
500	6.839	61.076	55.010	27.297			
	0.037	01.010	33,010	21,271			
00	6.854	61, 227	55 144	21 OP? .			
			55, 144	27,982		-	
00	6.870	61, 374	55, 275	28,668			
00	6.887	61.519	55, 403	29, 356			
00	6.903	61.661	55, 530	30,045			
00	6.920	61.801	55.654	30,736			
00	6.937	61.938	55.775	31.429			
.00	6. 955	62.073	55.895	32, 124			
00	6.973	62, 206	56.013	32.820			
00	6. 992	62, 336	56.129	33,518			
00	7.011	62.465	56, 243	34, 218			
		Ju. 403	30,643	31.410			
00	7.030	62.591	56. 355	34.921			
00	7.051	62, 716	56.466	35, 625			
00	7.072	62.838	56, 575	36. 331			
00	7.093	62, 960	56, 682	37.039			
00	7.115	63.079	56.787	37,749			
					•		

### RHODIUM IDEAL MONATOMIC GAS

	c	1/°K gfw			Kcal/	d v	
T,°K	c*	s <sup>o</sup> T	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>290</sub>	ΔH	ΔF	Los Kp
298.15	±.000	±.002	±,002	±.000			
1000	±.001	±.002	±,003	±.000			
2000	±.001	±.003	±.003	±.001			
3000	±.001	±.003	±.003	±.001			
4000	±.001	±.003	±,003	±.002			
5000	±.001	±.003	±.003	±.002			
6000	±.001	±.003	±.003	±,003			

# 17. Rhodium

The ideal monatomic gas thermodynamic functions of rhodium in Table XXXVIII were calculated from the energy levels listed by Moore<sup>221</sup> with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

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### 18. Scandium

### a. Crystal Structure, Transition Point and Melting Point

At room temperature, elemental scandium has a hexagonal, close-packed structure, 311,312,315,316. A face-centered cubic form reported by Meisel 313 has been attributed 311,314 to ScN. Spedding and Daane 315 reported an allotropic transition at 1608 °K. Mardon et al 316 found a thermal arrest corresponding to a transition at 1646 °± 10 °K. The last authors stated that the transition was expected to be to a bodycentered cubic structure by analogy with certain of the rare earth elements.

Spedding et al 311, 315 found the melting point of scandium to be 1812°  $\pm$  2°K. Mardon et al 316 reported a melting point of 1795°  $\pm$  5°K for metal which had picked up an "appreciable" but unspecified amount of tantalum. The transition and melting points adopted herein were those reported by Spedding et al 311, 315 Uncertainties of  $\pm$ 15° and  $\pm$ 5°K, respectively, were assigned. Other compilers 56,77 had recently assumed the melting point to be 1673°K.

#### b. Thermodynamic Properties

### 1) Heat of transition

The heat of transition of scandium at 1608 °K was estimated to be 350  $\pm\,100$  cal/gfw.

#### 2) Heat of fusion

The heat of fusion of scandium had not been measured. It was estimated herein to be  $3770 \pm 200 \text{ cal/gfw}$  on the assumption that

<sup>311</sup> Spedding, F. H., A. H. Daane, G. F. Wakefield, and D. H. Dennison, Trans. Met. Soc. AIME 218, 608 (1960).

<sup>312</sup> Spedding, F. H., K. W. Herrman, and A. H. Daane, Acta Cryst. 9, 559 (1956).

<sup>313</sup> Mersel, K., Naturwiss, 27, 230 (1939).

<sup>314</sup>Klemm, W., Anorganische Chemie 1, 48 (1948).

<sup>315</sup> Spedding, F. H. and A. H. Daane, Met. Revs. 5, 29 (1960).

<sup>316</sup> Mardon, P. G., J. L. Nichols, J. H. Pearce and D. M. Poole, Nature 189, 566 (1971).

#### REFERENCE STATE

Sc

Reference State for Calculating  $\Delta H_0^2$ ,  $\Delta F_1^2$ , and  $\log K_p$ : Solid from 298.15° to 1812°K, Liquid from 1812° to 3021°K, Gas from 3021° to 6000°K.

	c	al/°K gfv	8° ± 15°K	m.p. = 1812	Keal/gf		3021. +
T,°K	C <sub>P</sub>	ST	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>0</sub> <sup>T</sup> - H <sub>0</sub> <sup>298</sup>	ΔH °	ΔF	Log I
0	0.000	0.000	Infinite	- 1. 280			
298.15	6.000	9.000	9.000	0.000			
300	6.002	9.037	9.000	0.011			
400	6.110	10.778	9.236	0.617			
500	6.218	12.154	9.688	1.233			
600	6.326	13.297	10.197	1.860			
700	6.434	14. 280	10.711	2.498			
800	6.542	15.146	11.212	3.147			
900	6.650	15.923	11.693	3.807			
1000	6.758	16.629	12.152	4. 477			
1100	6.866	17.278	12.589	5.158			
1200	6.974	17.880	13.005	5.850			
1300	7.082	18.443	13.402	6.553			
1400	7.190	18.972	13.782	7. 267			
1500	7.328	19.471	14.144	7.991			
1/00	7 404	10.04/	14.403	0.734			
1600 1608	7 406	19.946	14.492	8.726 8.786			
	7.415	19.984	14.520				
1608 1700	8.000	20.202	14.520	9.136 9.872			
1800	8.000	20.647 21.104	14.840	10.672			
1812	8.000 8.000		15.175 15.215	10.072			
		21.158		14.538			
1812	8.000	23.238	15.215	15. 242			
2000	8.000 8.000	23.618 24.028	15.596 16.007	16.042			
	0.000	24.070	10.007	10.046			
2100	8.000	24.418	16.398	16.842			
2200	8.000	24.790	16.771	17.642			
2300	8.000	25.146	17.128	18.442			
400	8.000	25.486	17.468	19.242			
1500	8.000	25.813	17.796	20.042			
.,,	0.000	.,,,,,	,0	20.012			
600	8.000	26.127	18.111	20.842			
700	8.000	26.429	18.413	21.642			
800	8.000	26.720	18.705	22.442			
900	8.000	27.000	18.986	23. 242			
000	8.000	27.271	19.257	24.042			
021	8.000	27.326	19.312	24.210			
021	6.248	53.651	19.312	103.731			
100	6.397	53.815	20.193	104.229			
200	6.599	54.021	21.246	104.879			
300	6.810	54.227	22.242	105.549			
400	7.031	54.434	23.187	106.241			
500	7.259	43.641	24.082	106.955			
600	7.492	54.849	24.934	107.693			
700	7.730	55.057	25.745	108.454			
800	7.969	55.267	26.520	109.239			
900	8.208	55.477	27.260	110.048			
000	8.446	55.688	27.968	110.881			
100	8.680	55.899	28 444	111 717			
200		56.111	28.646	111.737			
	8.909		29.298	112.616			
300 400	9.132	56.323	29.923	113.518			
500	9.347	56.536 56.748	30.526 31.106	114.442 115.388			
	/24	70.110	311100				
500	9.750	56.960	31.666	116.353			
700	9.936	57.172	32.207	117.337			
300	10.111	57.383	32.729	118.340			
900	10.274	57.593	33.234	119.359			
000	10.425	57.802	33.723	120.394			
				* **** **** ****			
00	10.563	58.010	34.197	121.444			
00	10.689	58.216	34.657	126.506			
100	10.803	58.421	35.104	123.581			
100	10.905	58.624	35.538	124.667			
00	10.994	58.825	35.959	125.762			
0.0							
00	11 072	59.024	36. 370	126.865			
00	11.139	59.220	36.768	127.976			
100	11.196	59,415	37.158	129.093			
00	11 24,	50.606	37, 536	130.214			
00	11 279	59 746	17.906	131.341			

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### SCANDIUM REFERENCE STATE

	cal,	OK gto -		Kcal/gfv -			
T, °K	ς <b>,</b>	s <sub>T</sub>	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	VH &	ΔF į	Log Ep
0				± .040			
298.15	± .200	± .500	± .500	± .000			
1000	± .350	± .830	± .640	± -190			
1608	± .500	±1.090	± .800	± .460			
1608	±1.000	±1.150	± .800	± .560			
1812	±1.500	±1.300	± .850	± .810			
1812	± .400	±1.410	± .850	±1.010			
3021-	± 2.300	± 2.100	±1.220	± 2.640			
3021	± .001	± .002					
4000	± .002	± .003					
5000	± .002	± .003				1.5	
6000	± .002	± .003					

IDEAL MONATOMIC GAS

Sc

Reference State for Calculating  $\Delta H_q^a$ ,  $\Delta F_p^a$ , and  $\log K_p$ : Solid from 298.15° to 1812°K, Liquid from 1812° to 3021°K, Gas from 3021° to 6000°K.

gfw = 44.96

T<sub>t</sub> = 1608°± 15°K m.p. = 1812° ± 5°K b.p. = 3021° ± 140°K cal/oK gfw Kcal/efw ΔF ( T, °K s<sup>o</sup>t  $-(F_{T}^{o} - H_{298}^{o})/T$ H<sub>T</sub> - H<sub>298</sub> C<sub>P</sub> ΔH° Log Kp 0.000 0.000 Infinite -1.674 89.106 89.106 Infinite 41.750 41.750 79.736 79.665 -58. 445 -58. 033 298.15 5.283 41,750 0.000 89.500 5.279 41.783 0.010 89.499 300 400 5.148 43, 281 41.955 0.530 89.413 76.412 -41.748 500 5.085 1.042 44, 422 42.339 89.309 73.174 -31.983 42.765 600 45.346 5.049 1.548 89.188 69.959 -25, 480 5.028 46.122 43.191 2.052 89.054 66.763 -20.843 2,554 -17.371 -14.675 800 5.014 46, 793 43,600 88.907 63.590 43.988 3.055 60.434 1000 4.997 47.909 44.355 3.555 88. 578 57. 297 -12.522 1100 4.992 48.386 44.700 4.054 88.396 54.178 -10.764 48.820 4.989 45.025 4.553 88.203 1200 51.076 -9.302 4.988 5. 052 5. 551 87.999 87.784 47.990 44.921 1300 49.219 45.333 -8.067 49.589 1400 45.624 -7.012 1500 4.993 49.933 45.900 6.050 87.559 41.866 -6.100 1600 5,001 50.256 46, 162 6.550 87.324 38.828 -5.303 1608 5.002 50.280 46.182 6.590 87.304 38.587 -5. 244 1608 5.002 50.280 46.182 6.590 86.954 38.587 -5, 244 7.050 1700 5.014 50.559 46.412 86.678 35.828 -4.606 5.034 50.846 -3.988 1812 5.037 50.879 46.677 7.614 86.346 32.490 -3.919 50.879 7.614 -3.919 1900 5.062 51, 119 46.878 8.058 82. 316 30,064 -1.458 2000 5.099 51.380 47.097 8.566 27.320 82.024 -2.985 2100 5.148 51.630 47.307 9.078 81.736 24.591 - 2. 559 5. 208 5. 28 2 51.870 52.103 47.509 47.704 9.595 10.120 81.453 81.178 21.876 19.175 2200 -2.173 2300 -1.822 2400 5.369 52.330 47.892 10.652 80.910 16.482 -1.501 5.472 52.551 48.074 13.805 2500 11.194 80.652 -1.207 2600 5, 589 52,768 48, 250 11,747 11, 139 -0.936 80, 405 80.170 -0.686 5.828 2800 5.869 53.192 48.588 12.892 79.950 -0.455 6.032 79.745 3.184 -0.240 3000 6.208 53.608 48.909 14.099 79.557 0.544 -0.040 3021 6.248 53,651 48.941 14, 231 79.521 0.000 0.000 6. 248 53.651 14.231 3021 48.941 6.397 49.064 49.215 14.729 15.379 3100 53.815 3200 54.021 6.810 7.031 16.049 16.741 3300 54.227 49.364 3400 54.434 49.510 3500 7. 259 54.641 49.654 17.455 7.492 7.730 3600 54.849 49.795 18.193 3700 55.057 49.935 18.954 3800 7.969 55. 267 19.737 3900 8.208 55.477 50.208 20.548 4000 4100 8.680 55.899 50.475 22. 237 50.607 50.738 4200 8.909 56.111 23.116 4300 9.132 56. 323 24.018 4400 9. 147 56. 536 50.867 24.942 9.554 56.748 25.888 4500 50.995 4600 57.172 57.383 51.249 51.375 27.837 28.840 4700 9.936 4800 10.111 4900 10.274 57.593 51.499 29.859 5000 30.894 10.425 57.802 51.623 5100 58.010 51.747 31.944 10.563 10.689 58. 216 58. 421 51.869 51.991 5200 33.006 5300 34.081 5400 10.905 35.167 10.994 5500 58.825 52. 232 36. 262 5600 11.072 59.024 52. 351 37.365 52. 470 52. 588 5700 11.139 59.220 38.476 5800 11.196 59.415 39.593 5900 11.242 52.706 40.715 6000 11, 279 59.796 52.822 41.841

1-191

### SCANDIUM IDEAL MONATOMIC GAS

	c	u/ok gfo			Kcal/	$\overline{}$	
T, ° <b>K</b>	C <sub>p</sub>	s <sub>T</sub>	$-(F_{T}^{o} - H_{296}^{o})/T$	$H_T^{\circ} - H_{298}^{\circ}$	AH o	ΔF	Log Kp
298.15	±.000	±.002	±.002	±.000	± .500	± .650	±.480
1000	±.000	±.002	±.002	±.000	± .500	±1.060	±.230
1608	±-000 .	±.002	±.002	±.000	± .500	±1.790	±.240
1608	<b>±.000</b>	±.002	±.002	±.000	± .600	±1.790	±.240
1812	±.000	±.002	±.003	±.000	± .850	±1.940	±.230
1812	±.000	±.002	±.003	±.000	±1.050	±1.940	±.230
3021	±.001	±.002	±.003	±.001	±2.680	±3.690	±.270
3021	±.001	±.002	±.003	±.00]			
4000	±.002	x.003	±.003	±.002			
5000	±.002	±.003	±.003	±.004			
6000	±.002	±.003	±.003	±.005			

the entropy of transition plus the entropy of fusion was 2.3 cal/  $^{\circ}K$  gfw. The same entropy of transformation was adopted by Stull and Sinke  $^{77}$  and Kelley.  $^{56}$ 

### 3) Entropy and heat content at 298.15 °K

No data were available for the low temperature heat capacity of scandium. The estimate of Brewer  $^{317}$  of 9.0 cal/°K gfw was adopted. This was also listed by Kelley and King  $^{318}$  who assigned an uncertainty of 0.5 cal/°K gfw.  $^{\circ}_{298}$  -  $^{\circ}_{0}$  was estimated to be  $^{1280} \pm 40$  cal/gfw for the solid.

# 4) High-temperature heat content

In the absence of experimental data, Kelley's  $^{56}$  estimated heat capacity (in cal/ °K gfw) equation was used for the hexagonal-close-packed phase between 298.15° and 1608°K.

$$C_p^{\circ} = 5.68 + 1.08 \times 10^{-3} \text{T}$$
 (155)

For the high-temperature phase (presumably body-centered cubic), a constant heat capacity of  $8.00~\text{cal/}^{\circ}~\text{K}$  gfw was assumed. Kelley's  $^{56}$  estimate of  $8.00~\text{cal/}^{\circ}~\text{K}$  gfw was used for the heat capacity of liquid scandium.

# 5) Heat of sublimation, heat of vaporization, and boiling point

The vapor pressure of scandium was reported by Spedding et al. From their data and the free-energy functions tabulated here, the heat of sublimation at 298.15 °K was calculated to be 89.50  $\pm$  0.50 Kcal/gfw. The normal boiling point of scandium was calculated to be  $3021^{\circ} \pm 140^{\circ}$ K, and the heat of vaporization at the normal boiling point was found to be  $79.521 \pm 2.7$  Kcal/gfw. Stull and Sinke 77 had previously estimated the heat of sublimation at 298.15 °K to be 82.0 Kcal/gfw, the heat of vaporization to be 72.850 Kcal/gfw, and the normal boiling point to be 2750 °K.

#### 6) Thermodynamic functions

The reference state thermodynamic functions of scandium are given in Table XXXIX. The ideal monatomic gas thermodynamic functions of scandium given in Table XL were calculated from all the energy levels listed by Moore  $^{52}$  with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the tables.  $\rm H^{9}_{298}$ -  $\rm H^{0}_{0}$  was found to be 1,674 cal/mole for the ideal gas.

Brewer, L., Chemistry and Metallurgy of Miscellaneous Materials: Thermodynamics, Natl. Nuclear Energy Ser. IV-19B (L. L. Quill, ed.), McGraw-Hill, N.Y. (1950), chap. 3.

<sup>318</sup> Kelley, K. K. and E. G. King, Contributions to the Data on Theroetical Metallurgy, XIV. Entropies of Inorganic Substances, Bur. Mines Bull, 592 (to be published).

# 19. Silicon

The ideal monatomic gas thermodynamic functions of silicon given in Table XLI were calculated from the energy levels listed by  $\mathsf{Moore}^{52}$  with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

gfw = 28.09

	·	cel/°K gfw			Kcal/gfw		
T, *E	C <sub>p</sub>	sf	$-(F_{T}^{o}-H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH <sub>f</sub> °	ΔF	Log K
0	0.000	0.000	Infinite				Infinit
298.15	5.319	40-123	40.123	0.000			Initale
100	5.315	40.156	40.123	0.010			
00	5.166	41.662	40.330	0.533			
00	5.095	42.806	40.715	1.046			
500	5.056	43.731	41.143	1.553			
700	5.033	44.509	41.570	2.057			
800	5.019	45.180	41.980	2.560			
900	5.012	45.770	42.369	3.061			
000	5.012	46. 299	42.736	3.563			
100	5.017	46.776	43.082	4.064			
200	5.027	47.213	43.408	4.566			
300	5.043	47.616	43.717	5.070			
400	5.063	47.991	44.009	5.575			
500	5.087	48.341	44. 286	6.082			
600	5.113	48.670	44.550	6.592			
700	5.142	48.981	44.801	7.105			
800	5.172	49.276	45.042	7.621			
900	5.202	49. 556	45.272	8.139			
000	5. 232	49.824	45.493	8.661			
100	5.261	50.080	45.705	9.186			
200	5. 289	50.325	45.910	9.713			
300	5.316	50.561	46.107	10. 243			
100	5. 341	50.787	46. 297	10.776			
500	5.365	51-006	46.481	11.312			
500	5.386	51. 217	46.659	11.849			
100	5.406	51.420	46.832	12.389			
300	5. 424	51.617	46.999	12.930			
000	5.440	51.808	47.162	13.473			
000	5.454	51.993	47.320	14.018			
00	5.467	52.172	47.473	14.564			
00	5. 478	52. 345	47.623	15.111			
100	5. 487	52.514	47.769	15.660			
100	5.495	52.678	47.911	16.209			
00	5.502	52.837	48.049	16.759			
00	5.508	52. 99Z	48.184	17.309			
00	5.513	53.143	48.316	17.860			
100	5.516	53. 291	48. 445	18.412			
00	5.519	53.434	48.571	18.964			
00	5.521	53.574	48.695	19.515			
00	5.522	53.710	48.815	20.068			
00	5. 522	53.843	48.934	20.620			
00	5.522	53. 973	49.049	21.172			
00	5.522	54.100	49.163	21.724			
00	5.521	54. 224	49.274	22. 276			
00	5.520	54.345	49.383	22.829			
00	5.518	54.464	49.489	23.380			
00	5.517	54.580	49.594	23.932			
00 00	5.515	54.694	49.697	24. 484			
50	5.513	54.805	49.798	25.035			
00	5.512	54.915	49.898	25.587			
00	5.510	55.022	49.995	26.138			
00	5.509	55.126	50.091	26.689			
0	5.508	55. 229	50.185	27.239			
00	5.508	55.330	50.278	27.790			
	11						
00	5.507	55. 430	50.369	28.341			
00	5.508 5.509	55. 527	50.458	28.892			
00	5.511	55.623 55.717	50.547 . 50.634	29. <b>44</b> 3 29. 99 <b>4</b>			
99	5.514	55-810	50.719	30.545			
-			201117	201.3.3			

### SILICON IDEAL MONATOMIC GAS

		I/°K gf=	$\overline{}$	Kcal/g				
T, ° <u>K</u>	c <b>,</b>	s <sub>T</sub>	$-(F_{T}^{o} - H_{296}^{o})/T$	H <sub>7</sub> - H <sub>298</sub>	VH ,	ΔF	Log Kp	
298.15	±.000	±.002	±.002	±.000				
1000	±.000	±.002	± .002	±.000				
2000	±.000	±.002	±.002	±-000				
3000	±.000	±.002	±.003	±.001				
4000	±.000	±.002	±.003	±.001				
5000	±.000	± 002	±.003	±.001				
6000	±.001	±.003	±.003	±.002				

#### 20. Strontium

a. Crystal Structure, Transition Point, and Melting Point

Three allotropic modifications of elemental strontium have been reported.  $^{319-321,129,\,322}$  They are  $\alpha$ -Sr with a face-centered cubic structure,  $\beta$ -Sr with a hexagonal, close-packed structure, and  $\gamma$ -Sr with a body-centered structure. The transitions are summarized by equation (156):

$$\alpha - Sr \stackrel{T_1}{\rightleftharpoons} \beta - Sr \stackrel{T_2}{\rightleftharpoons} \gamma - Sr$$
 (156)

Rinck, <sup>319</sup> using thermal analysis, dilatometric studies, and electrical measurements, gave  $T_1$  as  $508^\circ K$  and  $T_2$  as  $813^\circ K$ . Sheldon and King, using high-temperature X-ray techniques, found  $T_1$  and  $T_2$  to be  $488^\circ \pm 10^\circ$  and  $878^\circ \pm 10^\circ$ ., respectively. Hirst, King, and Kanda <sup>321</sup> reported  $486^\circ \pm 10^\circ$  and  $881^\circ \pm 10^\circ K$  to be the two transition temperatures, and Schottmiller, King, and Kanda <sup>129</sup> give the temperatures as  $503^\circ \pm 6^\circ$  and  $894^\circ \pm 6^\circ K$ .

In view of Smith, Carlson, and Vest's  $^{124}$  demonstration that two of the four reported allotropic modifications of calcium were caused by impurities, it would not be surprising to find a similar situation with strontium. Kelley  $^{56}$  and Stull and Sinke  $^{77}$  used a single transition at  $862^{\circ}$ K in their compilations. However, the evidence for this transition temperature is not at all conclusive. It has been reported by Eastman, Cubicciotti, and Thurmond,  $^{323}$  and was tabulated by Kubaschewski et al  $^{79}$  in their review. The latter authors did not specify the source of the data, and Kubaschewski and Evans  $^{182}$  later listed the data of Rinck  $^{319}$  in their book. A single transition at  $^{862^{\circ}}$ K (face-centered cubic to body-centered cubic) has been adopted here and assigned an uncertainty of  $\pm 50\,^{\circ}$ K.

<sup>319</sup> Rinck, E., Compt. rend. 234, 845 (1952).

<sup>320</sup> Sheldon, F. A. and A. J. King, Acta Cryst. <u>6</u>, 100 (1953).

<sup>321</sup>Hirst, R. J., A. J. King, and F. A. Kanda, J. Phys. Chem. <u>60</u>, 302 (1956).

<sup>322</sup>Klemm, W. and G. Mika, Z. anorg. Chem. 248, 155 (1941).

<sup>323</sup> Eastman, E. D., D. D. Cubicciotti, and C. D. Thurmond, Chemistry and Metallurgy of Miscellaneous Materials: Thermodynamics, Natl. Nuclear Energy Ser. IV-19B (L. L. Quill, ed.), McGraw-Hill, N. Y. (1950), chap. 2.

The melting point of strontium was taken to be  $1045^{\circ} \pm 4^{\circ}$ K. The more reliable values in the literature <sup>132</sup>, <sup>129</sup>, <sup>321</sup> ranged from  $1041^{\circ}$  to  $1047^{\circ}$ K. Stull and Sinke <sup>77</sup> and Kelley <sup>56</sup> used  $1043^{\circ}$ K.

### b. Thermodynamic Properties

### 1) Heat of transition

The heat (or heats) of transition of strontium has not been measured. Stull and Sinke's 77 estimate of 200 cal/gfw for the single, assumed transition was adopted here. This estimate, arrived at by analogy with calcium, was assigned an uncertainty of 100 cal/gfw.

### 2) Heat of fusion

There were no measurements reported for the heat of fusion of strontium. Kubaschewski <u>et al</u>  $^{79}$  estimated the sum of the entropies of fusion and transition to be 2.12 cal/ $^{\circ}$ K gfw from regularities among the alkali and alkaline earth metals. The heat of fusion was then calculated to be 1970 cal/gfw and was assigned an uncertainty of  $\pm 150$  cal/gfw. Stull and Sinke  $^{77}$  and Kelley  $^{56}$  used 2200 cal/gfw for the heat of fusion of strontium from the same total entropy of transformation, but without subtracting the entropy of transition. Kubaschewski's values were were used herein.

### 3) Entropy and heat content at 298.15°K

The low-temperature heat capacity of strontium had not been measured. Kelley and King  $^{31\,8}$  estimated the entropy at 298.15°K to be 12.5  $\pm$  0.5 cal/°K gfw; this estimate was accepted here. Latimer  $^{324}$  and NBS Circular 500 reviewer estimated a value of 13.0 cal/°K gfw for this quantity. H $^{\rm o}_{298}$  - H $^{\rm o}_{0}$  for strontium was estimated to be 1550  $\pm$  150 cal/gfw from a plot of H $^{\rm o}_{298}$  - H $^{\rm o}_{0}$  versus S $^{\rm o}_{298}$  for the alkali and alkaline earth metals and the estimated value of S $^{\rm o}_{298}$  for strontium.

#### 4) High temperature heat content

No experimental data were available for the high-temperature heat capacity or heat content of strontium. Stull and Sinke  $^{77}$  and Kelley in their compilations assumed that these quantities for  $\alpha$ -Sr were essentially identical to those for  $\alpha$ -Ca, and extrapolated the  $\alpha$ -Ca data to the transition point of strontium.

<sup>324</sup> Latimer, W. M., Oxidation Potentials, 2nd ed., Prentice-Hall, N. Y. (1952).

Stull and Sinke  $^{77}$  extended this procedure for y-Sr. Kelley  $^{56}$  assumed a constant heat capacity of 9.16 cal/ $^{\circ}$ K gfw for y-Sr. The latter was an average of heat capacities obtained by the application of an equation for the heat capacity of y-Ca to y-Sr.

The present compilation for  $\alpha$ -Sr is based on assumed heat capacities (in cal/ $^{\circ}$ K gfw) over the range from 298.15 $^{\circ}$  to 862 $^{\circ}$ K given by equation (157).

$$C_p = 5.207 + 4.00 \times 10^{-3} \text{ T}$$
 (157)

This equation yields the adopted heat capacity of 6.400 cal/ $^{\circ}$ K gfw at 298.15 $^{\circ}$ K (compared with a heat capacity of 6.280 cal/ $^{\circ}$  K gfw for  $\alpha$ -Ca at the same temperature) and a temperature coefficient of the heat capacity about 10 percent greater than that for  $\alpha$ -Ca. The assigned uncertainties for the heat capacity of  $\alpha$ -Sr were about double the value of those used previously for  $\alpha$ -Ca.

Kelley's  $^{56}$  estimate of 9.16 cal/ $^{\circ}$ K gfw was adopted for the heat capacity of  $_{y-Sr}$  with increased uncertainties over those used for  $_{y-Ca}$ .

Stull and Sinke  $^{77}$  and Kelley  $^{56}$  assumed a constant heat capacity of 7.4 cal/ $^{\circ}$ K gfw for liquid strontium. The somewhat larger value of 7.8 cal/ $^{\circ}$ K gfw was used here with an assigned uncertainty which increases with temperature.

#### 5) Heat offermation of the monatomic gas

The free-energy functions tabulated here were used with vapor pressure data from the following sources to calculate the indicated heats of formation at 298.15°K using the Third Law Method:

Source	Temperature Range ( <sup>O</sup> K)	ΔH <sup>O</sup> f 298 (Kcal/gfw)
Hartmann and Schneider 148	1199-1379	39.490 4.0.110
Priselkov and Nesmeyanov 147	673- 873	38. 640 <u>+</u> 0. 400
Ruff and Hartmann 153	1217-1411	38.000 <u>+</u> 2.500

Unsmoothed vapor pressure data were used for these calculations.

An average of the first two values,  $39.070 \pm 0.500$  Kcal/gfw, was adopted for the heat of sublimation of strontium at 298.15°K.

The boiling point of strontium was calculated to be  $1641^{\circ} + 90^{\circ}$ K, and the heat of vaporization at the boiling point was found to be 33.012 + 1.05 Kcal/gfw.

# 6) Thermodynamic functions

The reference state thermodynamic functions of strontium obtained here are given in Table XLII. The ideal monatomic gas thermodynamic functions of stronium given in Table XLIII were calculated from all the energy levels listed by Moore 253 with the computer program described in section III-D. Uncertainty estimates are summarized on the back of the tables. H<sub>298</sub> - H<sub>0</sub> was found to be 1,481 cal/mole for the ideal gas.

#### REFERENCE STATE

Reference State for Calculating  $\Delta H_1^0$ ,  $\Delta F_1^0$ , and  $Log\,K_p$ : Solid from 298.15° to 1045°K, Liquid from 1045° to 1641°K, Gas from 1641° to 6000°K.

			*K * 50 *K	m.p. = 1045			= 1641° ± 9
T, °E	C.	el/°K gfv ——	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH? Keal/gfe	ΔF,	Log K,
0	0.000	0.000	Infinite	-1.550			
298.15	6.400	12.500	12.500	0.000			
300	6.407	12.540	12.501	0.012			
400	6.807	14.438	12.757	0.673			
500	7.207	15.999	13.253	1.373			
600	7.607	17.349	13.826	2.114			
700	8.007	18.551	14.416	2.895			
800	8.407	19.647	15.003	3.715			
862	8.655	20. 283	15.359	4. 244			
862	9.160	20.515	15.359	4. 444			
900	9.160	20.910	15.586	4.792			
1000	9.160	21.875	16.167	5.708			
1045	9-160_	22. 278	16.421	6.120			
1045	7.800	24. 163	16.421	8.090			
1100	7.800	24.563	16.818	8.519			
1200	7.800	25.242	17.493	9. 299			
1300	7.800	25.866	18.113	10.079			
1400	7.800	26.444	18.688	10.859			
1500	7.800	26.982	19.223	11.639			
1600	7.800	27.486	19.724	12.419			
1641	7.800	27.680	19.922	12.731			
1641	4.977	47.797	19.922	45.743			
1700	4.981	47.975	20.895	46.036			
1800	4-991	48. 260	22.407	46. 525			
1900	5.007	48.530	23.775	47.035			
2000	5.031	48.787	25.019	47.537			
2100	5.065	49.033	26.156	48.041			
2200	5.111	49.270	27.202	48.550			
2300	5.171	49.499	28.167	49.064			
2 <b>40</b> 0	5. 249	49.720	29.060	49.585			
2500	5.345	49.936	29.890	50.114			
	27.4		1.5				
2600	5.461	50.148	30.666	50.654			
2700	5.600	50.357	31.391	51.207			
2800	5.762	50.563	32.072	51.775			
2900	5.949	50.769	32.713	52.361			
3000	6.159	50.974	33.319	52.966			
3100	6.394	51.180	33.892	53. 593			
3200	6.653	51.387	34.435	54. 245			
3300	6. 933	51-596	34. 952	54. 924			
1400	7.235	51.807	35.444	55. 633			
3500	7.556	52.021	35.915	56. 372			
			24 246				
600	7.894	52. 239	36.365	57.144			
700	8.247	52.460	36.797	57.951			
800	8.611	52.685	37.213	58.794			
1900	8.984	52.913	37.612	59.674			
1000	9.364	53.145	37.997	60.591			
100	0 747	£2 10°	10 270	41 547			
100	9.747 10.131	53.381	38.370	61.547			
200		53.621	38.730	62.541			
1300 1400	10.513	53.864 54.110	39.080 39.418	63. 573 64. 643			
1500	11.262	54. 359	39.748	65.751			
	11. 202	37.337	37.190	03.131			
600	11.625	54.610	40.068	66.895			
700	11.979	54.864	40.380	68.076			
800	12.320	55.120	40.684	69. 291			
900	12.650	55.377	40.981	70.539			
000	12.965	55.636	41.272	71.820			
	, 0 5	22.030	******				
100	13.267	55.896	41.556	73.132			
200	13.554	56.156	41.833	74. 473			
300	13.826	56.417	42.107	75.842			
400	14.082	56.678	42.374	77.238			
500	14.324	56. 938	42.636	78.658			
		,,,,					
600	14.550	57.198	42.894	80.102			
700	14.762	57.458	43.148	81.568			
800	14.752	57.716	43.396	83.054			
900	15.141	57.974	43.642	84.559			
000	15.309	58.230	43.883	86.081			
	,	201 620					

STRONTIUM REFERENCE STATE

		/°K gfv			Keal/	¿. ———	`
T,°E	C*	s <sub>T</sub>	$-(F_{T}^{0}-H_{290}^{0})/T$	ห <sub>ื</sub> – ห <sub>290</sub>	AH?	ΔF <sub>f</sub>	Log Kp
0				±.150			
298.15	± .200	± .500	±.500	±.000			
862	± .300	± -610	±.540	±.060			
862	± .600	± .730	±.540	±.160			
1045	±1.000	± .760	±.580	±.190			
1045	± .500	± .910	±.580	± · 340			
1641	±1.500	±1.130	±.740	±.640			
1641	± .000	± .002					
2000	± .000	± .002					
3000	± .001	± .002					
4000	± .002	± .003					
5000	± .003	± .003					
6000	± .003	± .003					

#### IDEAL MONATOMIC GAS

Reference State for Calculating AH?, AF?, and Log K<sub>p</sub>: Solid from 298.15° to 1045°K,
Liquid from 1045° to 1641°K, Gas from 1641° to 6000°K.

		al/°K gf=			Kcel/gf	•	
T, °E	c,	s <sub>t</sub>	$-(F_{T}^{o} - H_{298}^{o})/T$	н <sub>т</sub> – н <sub>298</sub>	ΔH°	ΔF	Log Kp
0	0.000	0.000	Infinite	-1.481	39.139	39. 139	Infinite
298.15	4.968	39.325	39.325	0.000	39.070	31.072	-22.775
300	4.968	39.356	39. 325	0.009	39.067	31.023	-22.599
400	4.968	40.785	39.520	0.506	38.903	28. 365	-15.497
500	4.968	41.894	39.888	1.003	38.700	25.752	-11.256
600	4.968	42.799	40.300	1.500	38. 456	23. 186	-8.445
700	4.968	43.565	40.713	1.996	38. 171	20.662	-6.451
800	4.968	44. 229	41.112	2.493	37.848	18. 183	-4.967
862	4.968	44.600	41.350	2.801	37.627	16.666	-4. 225
862	4.968	44.600	41,350	2.801	37.427	16,666	-4. 225
900	4.968	44.814	41.492	2.990	37. 268	15.755	-3.826
1000	4.968	45.337	41.850	3.487	36.849	13.387	-2.926
1045	4.968	45.556	42.005	3.711	36.661	12 116	-2.580
1045	4.968	45. 556	42.005	3.711	34.691	12.335	-2.580
1100	4.968	45.811	42.189	3.984	34. 535	11.162	-2.218
1200	4.968	46. 243	42.509	4.481	34. 252	9.051	-1.648
1300	4.969	46.641	42.812	4.977	33.968	6.961	-1.170
1400	4.969	47.009	43. 099	5.474	33.685	4.895	-0.764
1500	4.971	47.352	43. 371	5.971	33.402	2.848	-0.415
1600	4 076	47 471	42 420	4 440	11 110	0.830	0.112
1641	4.975	47.673 47.797	43.630 43.731	6. <b>4</b> 69 6. 673	33.120 33.012	0.820 0.000	-0.112 0.000
1641	4.977	47.797	43.731	6. 673			3. 000
1700	4.981	47.975	43.877	6.966			
1800	4.991	48.260	44.112	7.465			
1900	5.007	48.530	44. 338	7.965			
2000	5.031	48.787	44.554	8.467			
2100	5.065	40.033	44 741	0.071			
2200	5.111	49.033 49.270	44.761 44.961	8.971			
2300	5. 171	49.499	45. 153	9.480			
2400				9.994			
2500	5. 249	49.720	45. 339	10.515			
2300	5.345	49.936	45.519	11.044			
2600	5.461	50, 148	45.693	11.584			
2700	5.600	50.357	45.862	12.137			
2800	5.762	50.563	46.026	12.705			
2900	5.949	50.769	46. 186	13. 291			
3000	6.159	50.974	46.342	13.896			
100	6. 394	51.180	46. 495	14.523			
3200	6.653	51.387	46.644	15. 175			
3300	6.933						
3400	7. 235	51.596 51.807	46.791 46.936	15.854			
500	7.556	52. 021	47.078	16.563 17.302			
600	7.894	52. 239	47.218	18.074			
700	8. 247	52.460	47.357	18.881	_		
800	8.611	52.685	47.494	19.724			
900	8.984	52.913	47.630	20.604			
000	9.364	53.145	47.765	21.521			
100	9.747	53.381	47.899	22.477			
200	10.131	53.621	48.033	23.471			
300	10.513	53.864	48.165	24.503			
400	10.891	54.110	48. 298	25.573			
500	11.262	54.359	48.430	26.681			
600	11.625	54.610	48.561	27.825			
700	11.023	54.864	48.693	29.006			
800	12. 320	55.120	48.824	30. 221			
900	12.650	55.377	48.955	31.469		_	
000	12.965	55. 636	49.086	32.750		_	
100	11 1/2						
100 200	13.267 13.554	55.896 56.156	49.217 49.348	34.062 35.403			
300	13.826	56.417	49.479	36.772			
400	14.082	56.678	49.610	38.168			
500	14. 324	56.938	49.741	39.588			
600	14.550	57. 198	49.871	41.032			
700	14.762	57.458	50.002	42.498			
900	14.959	57.716	50. 133	43.984			
900 -	15.141 15.309	57.974 58.230	50. 264 50. 394	45.489 47.011			
700	13.309	30. 230	39. 374	47.011			

STRONTIUM IDEAL MONATOMIC GAS

		d/°K gfu ──			Kcal/	g/ v	$\overline{}$
T,°K	c,	S <sub>T</sub>	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH o	ΔF <sub>f</sub>	Log K
298.15	±.000	±.002	<b>±.</b> 002	±.000	± .500	± .560	±.410
862	±.000	±.002	±.002	±.000	± .500	±1.000	±.250
862	±.000	±.002	±.002	±.000	± .500	±1.000	±.250
1045	±.000	±.002	±.002	±.000	± .600	±1.200	±.250
1045	±.000	±.002	±.002	±.000	± .750	±1.200	±.250
1641	±.000	±.002	±.002	±.000	±1.050	±1.800	±,240
1641	±.000	±.002	±.002	±.000			
2000	±.000	±.002	.t. 002	±.000			
3000	±.001	±.002	±.002	±.001			
1000	±.002	±.003	±.003	±.002			
5000	±.003	±.003	±.003	±.004			
6000	±.003	±.003	±.003	±.006			

gfw = 180.95

		cal/oK gfw			Kcal/gf	•	
T, °K	C <sub>p</sub>	ST	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> ~ H <sub>290</sub>	AH e	ΔF	Log I
^	0.000	0.000	7-61-14-				
0 298.15	4.985	0.000 44.243	Infinite 44.243	0.000			Infin
300	4. 986	44. 274	44. 243	0.009			
400	5.081	45.719	44.440	0.512			
500	5. 278	46.872	44.815	1.029			
	• -1:						
600	5.541	47.857	45.241	1.570			
760	5.827	48.733	45.679	2.138			
800	6.110	49.530	46.111	2.735			
900	6.376	50.265	46.532	3.359			
000	6.621	50.949	46.940	4.009			
100	6.844	51.591	47.334	4.683			
200	7.044	52. 195	47.714	5.377			
300	7.221	32.766	48.081	6.091			
400	7.377	53.307	48.435	6.821			
500	7.514	53.821	48.777	7.565			
600	7.633	54.310	49.108	8.323			
700	7.739	54.776	49.428	9-092			
800	7.832	55. 221	49.737	9.870			
900	7.916	55.647	50.037	10.658			
000	7.993	56.055	50-328	11.453			
100	8.064	56.446	50.610	12. 256			
200	8.132	56.823	50-884	13.066			
300	8.196	57.186	51.150	13.882			
400	8. 258	57.536	51.409	14.705			
500	8.319	57.874	51.661	15.534			
600	8.378	58. 202	51.906	16.369			
700	8.437	58.519	52.145	17.210			
300	8.495	48.827	52.378	18.056			
900	8.552	49.126	52.606	18.909			
000	8.610	59.417	52.828	19.767			
00	8.667	59.700	53.045	20.631			
200	8.725	59.976	53.258	21.500			
100	8.783	60.246	53.465	22.376			
100	8.841	60.509	53.669	23. 257			
500	8.900	60.766	53.868	24, 144			
500	8.959	61.018	54.063	25.037			
700	9.019	61.264	54.254	25.936			
300	9.079	61.505	54.442	26.841			
900	9.139	61.742	54.626	27.752			
000	9. 200	61.974	54.807	28.668			
100	0.241	62. 202	54.984	29.592			
200	9. 261 9. 322	62.426	55.159	30.521			
000	9.383	62.646	55.330	31.456			
100	9.444	62.862	55.499	32. 397			
00	9.504	63.075	55.665	33. 345			
••		40.305		14 200			
00	9.564	63. 285	55.829	34. 298			
00	9.623	63.491 63.694	55-989 56-148	35. 258 36. 223			
00	9.680 9.737	63.894	56.304	37.194			
00	9.792	64.092	56.458	38.170			
		44 204		10 161			
00 00	9.846 9.897	64. 286 64. 478	56.609 56.759	39.152 40.139			
00	9. 947	64.667	56.906	41.131			
00	9.995	64.853	57.052	42.128			
00	10.040	65.037	57.195	43.130			
00	10.083	65.218	57.337	44. 136			
00	10.124	65. 397	57. <b>4</b> 77	45.147			
00	10.161	65.573	57.615	46.161			
00	10.197	65.747	57.751	47.179			
00	10.229	65.919	57.886	48.200			
	•						

TANTALUM IDEAL MONATOMIC GAS

	(38	I/ok stw			Kcal/	div -	`
T, °E	c,	s <sub>T</sub>	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	VH.	ΔF	Log Kp
298.15	1.000	±.002	±.002	±.000			
1000	±.001	±.002	±.003	±.000			
2000	±.002	±.003	±.003	±.001			
3000	±.006	±.004	±.003	±.004			
4000	±.012	±.006	±.004	±.012			
5000	±.016	±.009	±.004	±.026			
6000	±.013	±.012	±.005	±.041			

# 21. Tantalum

The ideal monatomic gas thermodynamic functions of tantalum in Table XLIV were calculated from the energy levels listed by Moore<sup>221</sup> with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

# 22. Technetium

The ideal monatomic gas thermodynamic functions of technetium in Table XLV were calculated from the energy levels listed by Moore <sup>221</sup> with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

gfw = 99 (Isotope of Longest Known Half-Life)

T, °T C, °T C, °T - (F, T - H, 200)/T H, T - H, 200 AH, ° AF, ° I I  0 0,000 0,000 Infinite			al/oK gfw			Kcal/g	f w	
0 0.000 0.000 1.00	T, °K			$-(F_{T}^{0}-H_{208}^{0})/T$	HT - H200	ΔH°	ΔF,	Log E,
298.15 4.970 41.250 43.250 0.000 300 4.970 43.280 43.250 0.009 400 4.999 44.713 43.445 0.507 500 5.106 45.838 43.815 1.012 600 5.328 46.787 44.233 1.552 700 5.660 47.632 44.659 2.081 800 6.060 48.413 45.080 2.667 900 6.477 49.151 45.492 3.294 900 6.6477 49.151 45.492 3.294 900 6.683 49.894 43.893 3.3961 100 7.184 50.524 46.284 4.664 200 7.424 51.160 46.664 5.395 500 7.663 52.326 47.931 6.709 500 7.663 52.326 47.931 6.709 500 7.663 52.326 47.931 6.709 500 7.663 52.326 47.931 6.709 500 7.657 53.151 48.074 8.444 7700 7.597 53.814 48.998 9.207 900 7.426 46.60 49.711 9.963 900 7.426 46.60 49.013 10.710 900 7.426 46.60 49.013 10.710 900 7.726 55.718 49.857 12.176 100 7.332 55.028 49.304 11.448 100 7.726 55.718 49.857 12.896 100 7.680 56.035 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 17.015 65.335 50.118 13.608 18.600 6.866 57.403 51.302 17.083 18.600 6.866 57.403 51.302 17.083 18.600 6.866 57.403 51.302 17.083 18.600 6.864 53.813 52.137 10.814 18.600 7.186 60.055 53.680 21.296 18.600 7.186 60.055 53.680 21.296 18.700 7.144 59.878 53.522 25.420 18.700 7.144 59.878 53.522 25.420 18.700 7.144 61.054 54.558 30.528 18.700 7.144 61.054 54.558 30.528 18.000 7.403 60.894 54.419 29.785 18.000 7.404 61.054 54.558 30.528 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536 18.000 7.406 61.961 55.468 55.902 33.536					,	•	•	
100								Infinite
4400 4.999 44.713 43.445 0.507 500 5.106 45.838 43.815 1.012 600 5.328 46.787 44.233 1.552 700 5.660 47.632 44.659 2.081 800 6.060 46.413 45.080 2.667 900 6.477 49.151 45.492 3.294 900 6.863 49.854 45.893 3.294 900 7.184 50.524 46.284 4.664 900 7.184 50.524 46.284 4.664 900 7.184 50.524 46.284 4.664 900 7.185 50.751 51.761 47.033 6.146 900 7.561 51.761 47.033 6.146 900 7.563 52.326 47.391 6.500 900 7.663 52.326 47.391 6.500 900 7.663 52.326 47.391 6.500 900 7.663 52.326 47.391 9.207 900 7.424 51.160 46.664 5.395 900 7.657 53.351 48.074 8.444 900 7.657 53.351 48.074 8.444 900 7.466 46.604 49.711 9.963 900 7.426 46.604 49.711 9.963 900 7.426 46.60 49.013 10.710 900 7.332 55.028 49.304 11.448 900 7.426 54.650 49.013 10.710 900 7.780 56.035 50.118 13.608 900 7.080 56.035 50.118 13.608 900 7.080 56.035 50.118 13.608 900 6.886 57.403 51.302 17.083 900 6.886 57.403 51.302 17.083 900 6.886 57.403 51.302 17.083 900 6.886 57.403 51.302 17.083 900 6.886 57.403 51.302 17.083 900 6.886 57.403 51.302 17.083 900 6.886 57.403 51.302 17.083 900 6.886 57.403 51.302 17.083 900 7.021 59.326 53.351 18.431 900 6.894 58.532 52.135 19.427 900 7.144 9.883 19.225 19.969 900 7.188 60.055 53.680 21.899 900 7.188 60.055 53.680 22.123 19.227 900 7.186 60.055 53.680 22.123 19.227 900 7.186 60.055 53.680 22.123 19.227 900 7.186 60.055 53.680 22.123 19.227 900 7.186 60.055 53.680 22.123 19.227 900 7.186 60.055 53.680 22.125 19.000 7.125 99.326 53.894 22.256 900 7.186 60.055 53.680 22.1296 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 22.1299 900 7.186 60.055 53.680 23.1299 900 7.186 62.266 53.990 33.900 32.264 900 7.186 62.26								
500 5.106 45.838 43.815 1.012 600 5.328 46.787 44.233 1.532 700 5.660 47.7 49.151 45.080 2.667 800 6.060 48.413 45.080 2.667 900 6.477 49.151 45.492 3.294 900 6.865 49.854 45.893 3.961 100 7.184 50.524 46.284 4.664 100 7.424 51.160 46.664 5.395 100 7.581 51.761 47.033 6.146 100 7.663 52.266 47.391 6.999 100 7.687 53.351 48.074 8.444 100 7.657 53.351 48.074 8.444 100 7.657 53.351 48.074 8.444 100 7.597 53.814 46.398 9.207 100 7.375 55.028 49.304 11.448 100 7.057 59.305 49.304 11.448 100 7.057 59.305 50.205 49.304 11.448 100 7.050 55.718 49.595 11.2.896 100 7.050 55.718 49.595 11.2.896 100 7.015 56.335 50.311 14.313 100 7.016 56.892 50.615 11.5011 100 7.018 56.892 50.615 11.5011 100 6.887 57.153 51.080 16.395 100 6.887 57.153 51.080 16.395 100 6.887 57.153 51.080 16.395 100 6.884 57.43 51.516 17.769 100 6.894 59.134 52.257 22.596 100 6.894 59.134 52.257 22.596 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.021 59.326 53.030 23.296 100 7.022 59.697 53.362 24.708 100 7.403 60.894 54.419 29.785 100 7.404 61.668 55.002 33.834 22.004 100 7.660 61.961 55.46 35.000 33.274 100 7.660 61.961 55.46 35.000 33.274 100 7.660 61.961 55.46 35.000 33.297 100 7.681 61.961 55.360 35.000 33.297 100 7.682 61.518 55.000 33.297 100 7.683 61.518 55.000 33.297 100 7.684 61.668 55.000 33.589 100 7.660 61.961 55.062 33.739 100 7.768 62.266 55.977 33.928 100 7.768 62.266 55.977 33.928 100 7.768 62.266 55.977 33.928								
1.00								
700	300	3. 100	45.656	43.613	1.012			
700	600	5. 328	46 787	44. 233	1.532			
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1700   7. 597   53.814   48.398   9. 207     3800   7. 517   54.246   48.711   9.963     3900   7. 426   54.650   49.013   10.710     3900   7. 322   55.028   49.304   11.448     3100   7. 241   55.384   49.585   12.176     3200   7. 156   55.718   49.857   12.896     3300   7. 080   56.035   50.118   13.608     4000   7. 015   56.335   50.371   14.313     5500   6.961   56.635   50.371   14.313     5500   6.961   56.892   50.852   15.705     5700   6.887   57.153   51.080   16.395     800   6.866   57.403   51.302   17.083     800   6.866   57.403   51.302   17.083     900   6.856   57.443   51.516   17.769     900   6.854   57.876   51.724   18.454     100   6.860   58.101   51.926   19.140     200   6.874   58.319   52.123   19.827     300   6.894   58.319   52.123   19.827     300   6.894   58.310   52.314   20.515     500   6.950   58.737   52.500   21.206     500   6.950   58.738   52.681   21.899     600   6.984   59.114   52.857   22.596     7. 021   59.326   53.030   23.296     800   7. 061   59.513   53.198   24.000     7. 188   60.055   53.680   26.137     7. 000   7. 188   60.055   53.680   26.137     7. 000   7. 188   60.055   53.680   26.137     7. 000   7. 144   59.878   53.523   25.420     100   7. 188   60.055   53.680   26.137     7. 000   7. 144   61.054   54.558   30.528     100   7. 186   60.567   54.132   28.313     100   7. 594   61.668   55.092   33.536     100   7. 594   61.668   55.092   33.536     100   7. 759   61.518   54.952   32.778     100   7. 786   62.266   55.947   38.928     100   7. 786   62.265   55.470   35.829     100   7. 786   62.265   55.947   38.928     100   7. 786   62.268   55.947   38.928     100   7. 786   62.268   55.947   38.928     100   7. 786   62.268   55.947   38.928     100   7. 786   62.268   55.947   38.928     100   7. 786   62.268   55.947   38.928     100   7. 786   62.268   55.947   38.928     100   7. 786   62.268   55.947   38.928     100   7. 786   62.265   55.947   38.928     100   7. 786   62.265   55.947   38.928     100   7. 786   62.265	1900	1.005	52. 650	47.730	7.077			
700	600	7,657	53.351	48.074	8.444			
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1400								
6500         6.961         56.620         50.615         15.011           6600         6.918         56.892         50.852         15.705           700         6.887         57.153         51.080         16.395           800         6.866         57.403         51.302         17.083           9900         6.856         57.643         51.516         17.769           000         6.854         57.876         51.724         18.454           100         6.860         58.101         51.926         19.140           200         6.874         58.319         52.123         19.827           300         6.894         58.530         52.314         20.515           400         6.920         58.737         52.500         21.206           500         6.950         58.938         52.681         21.899           600         6.984         59.134         52.857         22.596           700         7.021         59.533         53.198         24.000           800         7.061         59.513         53.198         24.000           900         7.102         59.967         53.362         24.708								
600 6.918 56.892 50.852 15.705 7700 6.887 57.153 51.080 16.395 800 6.866 57,403 51.302 17.083 900 6.854 57.876 51.724 18.454  100 6.860 58.101 51.926 19.140 200 6.874 58.319 52.123 19.827 300 6.894 58.530 52.314 20.515 400 6.920 58.737 52.500 21.206 500 6.550 58.938 52.681 21.899  600 6.984 59.134 52.857 22.596 800 7.061 59.513 53.198 24.000 7.021 59.697 53.362 24.708 900 7.102 59.697 53.362 24.708 900 7.102 59.697 53.362 24.708 100 7.188 60.055 53.680 26.137 200 7.231 60.228 53.834 26.858 100 7.361 60.732 54.277 29.047  600 7.403 60.894 54.419 29.785 800 7.361 60.732 54.277 29.047  600 7.403 60.894 54.419 29.785 800 7.361 60.732 54.277 29.047  600 7.559 61.518 54.962 32.778  100 7.559 61.518 54.962 32.778  100 7.594 61.668 55.092 33.556 100 7.594 61.668 55.092 33.556 100 7.594 61.668 55.092 33.556 100 7.594 61.668 55.092 33.556 100 7.594 61.616 55.220 34.297 100 7.660 61.961 55.346 35.061 100 7.594 61.668 55.092 33.556 100 7.660 61.961 55.346 35.061 100 7.594 61.668 55.092 33.556 100 7.660 61.961 55.346 35.061 100 7.594 61.668 55.092 33.556 100 7.660 61.961 55.346 35.061 100 7.594 61.668 55.092 33.556 100 7.774 62.246 55.592 36.600 17.774 62.523 55.810 38.149 100 7.774 62.523 55.810 38.149 100 7.774 62.553 55.810 38.149 100 7.798 62.658 55.947 38.928 100 7.798 62.658 55.947 38.928								
1.00	.500	0. 701	50.020	50.013	13.011			
1800   6.866   57.403   51.302   17.083   17.0			56.892	50.852	15.705			
900 6.856 57.643 51.516 17.769 000 6.854 57.876 51.724 18.454  100 6.860 58.101 51.926 19.140 200 6.874 58.319 52.123 19.827 300 6.894 58.530 52.314 20.515 400 6.920 58.737 52.500 21.206 500 6.950 58.938 52.681 21.899  600 6.984 59.134 52.857 22.596 700 7.021 59.326 53.030 23.296 800 7.061 59.513 53.198 24.000 900 7.102 59.697 53.362 24.708 900 7.104 59.878 53.523 25.420  100 7.188 60.055 53.680 26.137 200 7.231 60.228 53.834 27.583 300 7.275 60.399 53.984 27.583 300 7.318 60.567 54.132 28.313 500 7.361 60.732 54.277 29.047  600 7.403 60.894 54.419 29.785 800 7.484 61.211 54.695 31.274 900 7.522 61.366 54.830 32.024 900 7.594 61.668 55.92 33.536 100 7.594 61.668 55.220 34.297 100 7.594 61.668 55.92 33.536 200 7.628 61.816 55.220 34.297 100 7.594 61.668 55.92 33.536 200 7.628 61.816 55.220 34.297 100 7.606 61.961 55.346 35.061 400 7.594 61.668 55.92 33.536 200 7.628 61.816 55.220 34.297 100 7.628 61.816 55.220 34.297 100 7.594 61.668 55.92 33.536 200 7.628 61.816 55.220 34.297 100 7.594 61.668 55.92 33.536 200 7.628 61.816 55.220 34.297 100 7.691 62.105 55.406 35.061 100 7.774 62.523 55.830 38.149 100 7.774 62.523 55.830 38.149 100 7.798 62.658 55.947 38.928 100 7.782 62.266 55.592 36.600	700	6.887	57. 153	51.080	16.395			
000     6.854     57.876     51.724     18.454       100     6.860     58.101     51.926     19.140       200     6.874     58.319     52.123     19.827       300     6.894     58.530     52.314     20.515       400     6.920     58.737     52.500     21.206       500     6.950     58.938     52.681     21.899       600     6.984     59.134     52.857     22.596       700     7.021     59.326     53.030     23.296       800     7.061     59.513     53.198     24.000       900     7.102     59.697     53.362     24.708       900     7.144     59.878     53.523     25.420       100     7.188     60.055     53.680     26.137       200     7.231     60.228     53.834     26.858       300     7.275     60.399     53.984     27.583       400     7.318     60.567     54.132     28.313       500     7.404     61.054     54.558     30.528       800     7.484     61.211     54.695     31.274       900     7.522     61.366     54.830     32.024       900     7.524	800	6.866	57,403	51.302	17.083			
100 6.860 58.101 51.926 19.140 200 6.874 58.319 52.123 19.827 300 6.894 58.530 52.314 20.515 400 6.920 58.737 52.500 21.206 500 6.950 58.938 52.681 21.899 600 6.984 59.134 52.857 22.596 700 7.021 59.326 53.030 23.296 800 7.061 59.513 53.198 24.000 900 7.102 59.697 53.362 24.708 900 7.102 59.6878 53.523 25.420 100 7.188 60.055 53.680 26.137 200 7.231 60.228 53.834 26.858 300 7.275 60.399 53.984 27.583 400 7.318 60.567 54.132 28.313 500 7.361 60.732 54.277 29.047 600 7.403 60.894 54.419 29.785 800 7.522 61.366 54.830 32.024 900 7.559 61.518 54.962 32.778 100 7.594 61.668 55.020 34.297 100 7.594 61.668 55.020 34.297 100 7.594 61.668 55.020 34.297 100 7.626 61.816 55.220 34.297 100 7.626 61.816 55.220 34.297 100 7.626 61.816 55.220 34.297 100 7.626 61.816 55.220 34.297 100 7.660 7.770 62.246 55.592 36.600	900	6.856	57.643	51.516	17.769			
200       6.874       58.319       52.123       19.827         300       6.894       58.530       52.314       20.515         400       6.920       58.737       52.500       21.206         500       6.950       58.938       52.681       21.899         600       6.984       59.134       52.857       22.596         700       7.021       59.326       53.030       23.296         800       7.061       59.513       53.198       24.000         900       7.102       59.697       53.362       24.708         900       7.144       59.878       53.523       25.420         100       7.188       60.055       53.680       26.137         200       7.231       60.228       53.834       26.858         300       7.275       60.399       53.984       27.583         400       7.318       60.567       54.132       28.313         500       7.361       60.732       54.277       29.047         600       7.444       61.054       54.558       30.528         800       7.484       61.211       54.695       31.274         900	000	6.854	57.876	51,724	18.454			
200       6.874       58,319       52,123       19.827         300       6.894       58,530       52,314       20,515         400       6.920       58,737       52,500       21,206         500       6.950       58,938       52,681       21,899         600       6.984       59,134       52,857       22,596         700       7.021       59,326       53,030       23,296         800       7.061       59,513       53,198       24,000         900       7.102       59,697       53,362       24,708         900       7.144       59,878       53,523       25,420         100       7.188       60.055       53,680       26,137         200       7.231       60,228       53,834       26,858         300       7.275       60,399       53,984       27,583         400       7,318       60,567       54,132       28,313         500       7,361       60,732       54,277       29,047         600       7,403       60,894       54,419       29,785         700       7,444       61,054       54,558       30,528         800	100	6 840	58 101	51 026	19 140			
300 6.894 58.530 52.314 20.515 400 6.920 58.737 52.500 21.206 500 6.950 58.938 52.681 21.899 600 6.984 59.134 52.857 22.596 7.00 7.021 59.326 53.030 23.296 800 7.061 59.513 53.198 24.000 900 7.102 59.697 53.362 24.708 000 7.144 59.878 53.523 25.420 100 7.188 60.055 53.680 26.137 200 7.231 60.228 53.834 26.858 300 7.275 60.399 53.984 27.583 400 7.318 60.567 54.132 28.313 500 7.361 60.732 54.277 29.047 600 7.403 60.894 54.419 29.785 700 7.444 61.054 54.558 30.528 800 7.484 61.211 54.695 31.274 900 7.522 61.366 54.830 32.024 000 7.559 61.518 54.962 32.778 100 7.594 61.668 55.092 33.536 100 7.594 61.668 55.092 33.536 100 7.660 61.961 55.346 35.061 400 7.691 62.105 55.470 35.829 100 7.720 62.246 55.592 36.600								
400       6. 920       58. 737       52. 500       21. 206         500       6. 950       58. 938       52. 681       21. 899         600       6. 984       59. 134       52. 857       22. 596         700       7. 021       59. 326       53. 030       23. 296         800       7. 061       59. 513       53. 198       24. 000         900       7. 102       59. 697       53. 362       24. 708         000       7. 144       59. 878       53. 523       25. 420         100       7. 188       60. 055       53. 680       26. 137         200       7. 231       60. 228       53. 834       26. 858         300       7. 275       60. 399       53. 984       27. 583         400       7. 318       60. 567       54. 132       28. 313         500       7. 361       60. 732       54. 277       29. 047         600       7. 403       60. 894       54. 419       29. 785         700       7. 444       61. 054       54. 558       30. 528         800       7. 484       61. 211       54. 695       31. 274         900       7. 522       61. 366       54. 962								
500       6.950       58.938       52.681       21.899         600       6.984       59.134       52.857       22.596         700       7.021       59.326       53.030       23.296         800       7.061       59.513       53.198       24.000         900       7.102       59.697       53.362       24.708         000       7.144       59.878       53.523       25.420         100       7.188       60.055       53.680       26.137         200       7.231       60.228       53.834       26.858         300       7.275       60.399       53.984       27.583         400       7.318       60.567       54.132       28.313         500       7.361       60.732       54.277       29.047         600       7.403       60.894       54.419       29.785         700       7.444       61.054       54.558       30.528         800       7.484       61.211       54.695       31.274         900       7.522       61.518       54.962       32.778         100       7.594       61.668       55.092       33.536         200								
600 6. 984 59. 134 52. 857 22. 596 700 7. 021 59. 326 53. 030 23. 296 800 7. 061 59. 513 53. 198 24. 000 900 7. 102 59. 697 53. 362 24. 708 000 7. 144 59. 878 53. 523 25. 420  100 7. 188 60. 055 53. 680 26. 137 200 7. 231 60. 228 53. 834 26. 858 300 7. 275 60. 399 53. 984 27. 583 400 7. 318 60. 567 54. 132 28. 313 500 7. 361 60. 732 54. 277 29. 047  600 7. 403 60. 894 54. 419 29. 785 700 7. 444 61. 054 54. 558 30. 528 800 7. 484 61. 211 54. 695 31. 274 900 7. 522 61. 366 54. 830 32. 024 000 7. 559 61. 518 54. 962 32. 778  100 7. 594 61. 668 55. 092 33. 536 200 7. 626 61. 816 55. 220 34. 297 300 7. 660 61. 961 55. 346 35. 061 400 7. 691 62. 105 55. 470 35. 829 500 7. 720 62. 246 55. 592 36. 600 600 7. 748 62. 386 55. 712 37. 373 700 7. 748 62. 523 55. 830 38. 149 800 7. 782 62. 668 55. 947 38. 928 900 7. 821 62. 792 56. 062 39. 709								
1700       7,021       59,326       53,030       23,296         1800       7,061       59,513       53,198       24,000         1900       7,102       59,697       53,362       24,708         1000       7,144       59,878       53,523       25,420         11100       7,188       60,055       53,680       26,137         1200       7,211       60,228       53,834       26,858         1300       7,275       60,399       53,984       27,583         1400       7,318       60,567       54,132       28,313         1500       7,361       60,732       54,277       29,047         1600       7,403       60,894       54,419       29,785         1700       7,444       61,054       54,558       30,528         1800       7,484       61,211       54,695       31,274         1900       7,522       61,366       54,830       32,024         1900       7,594       61,668       55,092       33,536         1900       7,628       61,816       55,220       34,297         1900       7,691       62,105       55,470       35,829 <t< td=""><td></td><td>0.,,,,</td><td>001,700</td><td></td><td></td><td></td><td></td><td></td></t<>		0.,,,,	001,700					
1800       7. 061       59. 513       53. 198       24. 000         1900       7. 102       59. 697       53. 362       24. 708         1900       7. 144       59. 878       53. 523       25. 420         1100       7. 188       60. 055       53. 680       26. 137         1200       7. 211       60. 228       53. 834       26. 858         1300       7. 275       60. 399       53. 984       27. 783         1400       7. 318       60. 567       54. 132       28. 313         1500       7. 361       60. 732       54. 277       29. 047         1600       7. 403       60. 894       54. 419       29. 785         1700       7. 444       61. 054       54. 558       30. 528         1800       7. 522       61. 366       54. 830       32. 024         1900       7. 522       61. 366       54. 830       32. 778         1100       7. 594       61. 668       55. 092       33. 536         1200       7. 626       61. 816       55. 202       34. 297         1300       7. 660       61. 961       55. 346       35. 061         1400       7. 748       62. 246	600	6.984	59.134	52.857	22.596			
1900	700	7.021	59.326	53.030	23. 296			
1000       7, 144       59, 878       53,523       25,420         1100       7, 188       60,055       53,680       26,137         1200       7,211       60,228       53,834       26,858         1300       7,275       60,399       53,984       27,583         1400       7,318       60,567       54,132       28,313         1500       7,361       60,732       54,277       29,047         1600       7,403       60,894       54,419       29,785         1700       7,444       61,054       54,558       30,528         1800       7,484       61,211       54,695       31,274         1900       7,552       61,366       54,830       32,024         1900       7,594       61,668       55,092       33,536         1300       7,626       61,816       55,220       34,297         1300       7,660       61,961       55,470       35,829         1500       7,748       62,105       55,470       35,829         1500       7,748       62,286       55,592       36,600         1600       7,748       62,658       55,947       38,149	800	7.061	59.513	53.198	24.000			
7. 188 60. 055 53. 680 26. 137 2200 7. 231 60. 228 53. 834 26. 858 2300 7. 275 60. 399 53. 984 27. 583 2400 7. 318 60. 567 54. 132 28. 313 2500 7. 361 60. 732 54. 277 29. 047 27. 361 60. 732 54. 277 29. 047 28. 313 7. 361 60. 732 54. 277 29. 047	3900		59.697					
12200       7, 231       60, 228       53,834       26,858         1300       7, 275       60,399       53,984       27,583         1400       7, 318       60,567       54,132       28,313         1500       7, 361       60,732       54,277       29,047         1600       7, 403       60,894       54,419       29,785         1700       7,444       61,054       54,558       30,528         1800       7,484       61,211       54,695       31,274         1900       7,559       61,366       54,830       32,024         1900       7,559       61,518       54,962       32,778         1000       7,594       61,668       55,092       33,536         1200       7,628       61,816       55,220       34,297         1300       7,660       61,961       55,346       35,061         1400       7,691       62,105       55,470       35,829         1500       7,720       62,246       55,592       36,600         1600       7,748       62,386       55,712       37,373         1600       7,778       62,658       55,947       38,149	1000	7. 144	59.878	53. 523	25.420			
1200       7, 231       60, 228       53, 834       26, 858         1300       7, 275       60, 399       53, 984       27, 583         1400       7, 318       60, 567       54, 132       28, 313         1500       7, 361       60, 732       54, 277       29, 047         1600       7, 403       60, 894       54, 419       29, 785         1700       7, 444       61, 054       54, 558       30, 528         1800       7, 484       61, 211       54, 695       31, 274         900       7, 522       61, 366       54, 830       32, 024         1000       7, 559       61, 518       54, 962       32, 778         1100       7, 594       61, 668       55, 092       33, 536         2200       7, 628       61, 816       55, 220       34, 297         3300       7, 660       61, 961       55, 346       35, 061         400       7, 691       62, 105       55, 470       35, 829         500       7, 720       62, 246       55, 592       36, 600         600       7, 748       62, 523       55, 810       38, 149         800       7, 798       62, 658       55, 9	100	7 100	40 055	E2 400	26 137			
3300       7, 275       60, 399       53, 984       27, 583         1400       7, 318       60, 567       54, 132       28, 313         1500       7, 361       60, 732       54, 277       29, 047         6600       7, 403       60, 894       54, 419       29, 785         700       7, 444       61, 054       54, 558       30, 528         8800       7, 484       61, 211       54, 695       31, 274         990       7, 522       61, 366       54, 830       32, 024         900       7, 559       61, 518       54, 962       32, 778         1100       7, 594       61, 668       55, 092       33, 536         200       7, 628       61, 816       55, 220       34, 297         300       7, 660       61, 961       55, 346       35, 061         400       7, 691       62, 105       55, 470       35, 829         5500       7, 720       62, 246       55, 592       36, 600         600       7, 748       62, 658       55, 712       37, 373         700       7, 774       62, 658       55, 947       38, 928         900       7, 821       62, 658       55, 947 </td <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td>								
1400								
500     7, 361     60, 732     54, 277     29, 047       600     7, 403     60, 894     54, 419     29, 785       700     7, 444     61, 054     54, 558     30, 528       800     7, 484     61, 211     54, 695     31, 274       900     7, 522     61, 366     54, 830     32, 024       000     7, 559     61, 518     54, 962     32, 778       100     7, 594     61, 668     55, 092     33, 536       200     7, 628     61, 816     55, 220     34, 297       300     7, 660     61, 961     55, 346     35, 061       400     7, 691     62, 105     55, 470     35, 829       500     7, 720     62, 246     55, 592     36, 600       600     7, 748     62, 386     55, 712     37, 373       700     7, 774     62, 523     55, 810     38, 149       800     7, 798     62, 658     55, 947     38, 928       900     7, 821     62, 792     56, 062     39, 709								
600 7. 403 60.894 54.419 29.785 700 7. 444 61.054 54.558 30.528 800 7. 484 61.211 54.695 31.274 900 7. 522 61.366 54.830 32.024 000 7. 559 61.518 54.962 32.778  100 7. 594 61.668 55.092 33.536 200 7.628 61.816 55.220 34.297 300 7.660 61.961 55.346 35.061 400 7.691 62.105 55.470 35.829 560 7. 720 62.246 55.592 36.600  600 7. 748 62.386 55.712 37.373 700 7. 7774 62.523 55.830 38.149 800 7.798 62.658 55.947 38.928 900 7.821 62.792 56.062 39.709								
700 7.444 61.054 54.558 30.528 800 7.484 61.211 54.695 31.274 900 7.522 61.366 54.830 32.024 000 7.559 61.518 54.962 32.778  100 7.594 61.668 55.092 33.536 200 7.626 61.816 55.220 34.297 300 7.660 61.961 55.346 35.061 400 7.691 62.105 55.470 35.829 500 7.720 62.246 55.592 36.600  600 7.748 62.386 55.712 37.373 700 7.774 62.523 55.830 38.149 800 7.798 62.668 55.947 38.928 900 7.821 62.792 56.062 39.709								
800 7, 484 61, 211 54, 695 31, 274 900 7, 522 61, 366 54, 830 32, 024 000 7, 559 61, 518 54, 962 32, 778  100 7, 594 61, 668 55, 092 33, 536 200 7, 628 61, 816 55, 220 34, 297 300 7, 660 61, 961 55, 346 35, 061 400 7, 691 62, 105 55, 470 35, 829 500 7, 720 62, 246 55, 592 36, 600  600 7, 748 62, 386 55, 712 37, 373 700 7, 774 62, 523 55, 830 38, 149 800 7, 798 62, 668 55, 947 38, 928 900 7, 821 62, 792 56, 062 39, 709								
900 7.522 61.366 54.830 32.024 000 7.559 61.518 54.962 32.778 100 7.594 61.668 55.092 33.536 200 7.628 61.816 55.220 34.297 300 7.660 61.961 55.346 35.061 400 7.691 62.105 55.470 35.829 560 7.720 62.246 55.592 36.600 600 7.748 62.386 55.712 37.373 700 7.774 62.523 55.830 38.149 800 7.798 62.658 55.947 38.928 900 7.821 62.792 56.062 39.709								
000     7.559     61.518     54.962     32.778       100     7.594     61.668     55.092     33.536       200     7.626     61.816     55.220     34.297       300     7.660     61.961     55.346     35.061       400     7.691     62.105     55.470     35.829       500     7.720     62.246     55.592     36.600       600     7.748     62.386     55.712     37.373       700     7.774     62.523     55.810     38.149       800     7.798     62.658     55.947     38.928       900     7.821     62.792     56.062     39.709								
100 7.594 61.668 55.092 33.536 200 7.626 61.816 55.220 34.297 300 7.660 61.961 55.346 35.061 400 7.691 62.105 55.470 35.829 500 7.720 62.246 55.592 36.600 600 7.748 62.386 55.712 37.373 700 7.774 62.523 55.830 38.149 800 7.798 62.658 55.947 38.928 900 7.821 62.792 56.062 39.709								
200     7. 628     61. 816     55. 220     34. 297       300     7. 660     61. 961     55. 346     35. 061       400     7. 691     62. 105     55. 470     35. 829       500     7. 720     62. 246     55. 592     36. 600       600     7. 748     62. 386     55. 712     37. 373       700     7. 774     62. 523     55. 830     38. 149       800     7. 798     62. 658     55. 947     38. 928       900     7. 821     62. 792     56. 062     39. 709	υ00	7. 559	61.518	54.962	32.778			
200     7.628     61.816     55.220     34.297       300     7.660     61.961     55.346     35.061       400     7.691     62.105     55.470     35.829       500     7.720     62.246     55.592     36.600       600     7.748     62.386     55.712     37.373       700     7.774     62.523     55.830     38.149       800     7.798     62.658     55.947     38.928       900     7.821     62.792     56.062     39.709	100	7.594	61.66R	55, 092	33, 516			
300     7. 660     61. 961     55. 346     35. 061       400     7. 691     62. 105     55. 470     35. 829       500     7. 720     62. 246     55. 592     36. 600       600     7. 748     62. 386     55. 712     37. 373       700     7. 774     62. 523     55. 810     38. 149       800     7. 798     62. 658     55. 947     38. 928       900     7. 821     62. 792     56. 062     39. 709								
400     7.691     62.105     55.470     35.829       500     7.720     62.246     55.592     36.600       600     7.748     62.386     55.712     37.373       700     7.774     62.523     55.830     38.149       800     7.798     62.658     55.947     38.928       900     7.821     62.792     56.062     39.709								
500     7.720     62.246     55.592     36.600       600     7.748     62.386     55.712     37.373       700     7.774     62.523     55.810     38.149       800     7.798     62.658     55.947     38.928       900     7.821     62.792     56.062     39.709								
700     7.774     62.523     55.830     38.149       800     7.798     62.658     55.947     38.928       900     7.821     62.792     56.062     39.709								
700 7.774 62.523 55.830 38.149 800 7.798 62.658 55.947 38.928 900 7.821 62.792 56.062 39.709				_				
800 7.798 62.658 55.947 38.928 900 7.821 62.792 56.062 39.709								
900 7.821 62.792 56.062 39.709								
70.172								
		1.074	04.763	30.173	10. 176			
•								
•								
					1			

TECHNETIUM IDEAL MONATOMIC GAS

		I/ok Ma	• • •	<b>′</b>	Kcal/	•	`
T,°K	ح.	s <sub>T</sub>	$-(F_{T}^{\circ} - H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	AH?	ΔF	Log I
298.15	±.000	±.002	<b>*.</b> 002	±.000			
1000	±.001	±.002	±.002	±.000			
2000	±.001	±.003	±.003	±.001			
3000	±.001	±.003	±.003	±.001			
4000	<b>±.</b> 001	±.003	±.003	±.002			
5000	±.001	±.003	±.003	±.002			
6000	±.001	±.003	±.003	±.003			

# 23. Titanium

Prior to the publication of the JANAF Thermochemical Panel Interim Tables, <sup>75</sup> an analysis of the available basic data on titanium had been made on the present project. Since the results of the two analyses were in very close agreement, the values of the former analysis were accepted for the sake of compatibility and consistency with the addition of uncertainty limits from the new analysis. The following summary shows the extent of agreement of important quantities:

Quantity	Units	JANAF Table Value <sup>75</sup>	Avco RAD Analysis
T <sub>t</sub>	° K	1155	1154
ΔH <sub>t</sub>	Kcal/gfw	0.950	0.943
Melting Point	° K	1950	1945 ± 10
ΔH <sub>m</sub>	Kcal/gfw	3.7	4.0 ± 0.5
S°298	e.u.	7.33	7.334
ΔH <sub>v</sub>	Kcal/gfw	102.5*	
Boiling Point	° K	3550	
ΔH° <sub>s298</sub>	Kcal/gfw	112.49	112, 794

<sup>\*</sup>Taken from monatomic gas table and rounded off.

# a. Selection of Condensed-Phase Data

# 1) Crystal structure and solid-state transition

Titanium exists in two crystalline modifications. <sup>57</sup> The form stable at ordinary temperatures is close-packed hexagonal. This undergoes a transition <sup>325</sup>, <sup>326</sup> to the body-centered cubic form at about 1155° K. Hansen and Anderko <sup>213</sup> have reported a transition point value of 1158° K and Kothen <sup>266</sup> has reported a value of 1154° K for it.

The 1155°K value used in the JANAF tables for this transition point was adopted for the present work.

<sup>325</sup> Edwards, J. W., H. L. Johnston, and W. E. Ditmars, J. Am. Chem. Soc. 73, 4729 (1951).

<sup>326</sup> McQuillan, A. D. Proc. Roy. Soc. (London) A204, 309 (1950).

<sup>\*</sup>Taken from monatomic gas table and rounded off.

# Melting point

There were many reported melting points for titanium. The recent compilation of Goldsmith et al  $^{277}$  listed five references with an average recommended value of  $1944^{\circ}$  K. Stull and  $^{50}$  chose  $^{1950^{\circ}}$  ±  $20^{\circ}$  K. Kelley  $^{56}$  chose  $1940^{\circ}$  K which is based on the work of Deardorff and Hayes.  $^{327}$  A recent determination by Savitskii and Burkhanov  $^{328}$  yielded a value of  $1953^{\circ}$  K.

The JANAF table value of 1950° K was accepted for the present work with an estimated uncertainty of  $\pm$  10° K.

# 3) Heat of transition

Golutvin<sup>329</sup> reported a solid-state heat of transition of 820  $\pm$  20 cal/g atom while Schofield's value<sup>330</sup> of 830  $\pm$  100 cal/g atom was quoted by Kubaschewski and Evans. <sup>182</sup> Stull and Sinke<sup>77</sup> chose a value of 950 cal/g atom, and Kothen's<sup>266</sup> measurements yielded a value of 943 cal/g atom. The agreement between the last two values is good. The JANAF table value of 950 cal/g atom was chosen for the present work.

## 4) Heat of fusion

There were no experimental data available for the heat of fusion of titanium. Values have been estimated on the assumption that the entropy of fusion has a value characteristic of the change from a body-centered cubic structure to the liquid. The following estimates have been reported.

ΔH <sub>fusion</sub> (cal/g atom)	Reference
3700	Stull and Sinke <sup>77</sup>
4500 ± 500	Kubaschewski and Evans 182
4460	Kelley <sup>56</sup>

<sup>327</sup> Deardorff, D. K. and E. T. Hayes, J. Metals 8, 509 (1956).

<sup>328</sup> Savitskii, E. M. and G. S. Burkhanov, Zhur. Neorg. Khim. 2, 2609 (1957).

<sup>329</sup>Golutvin, Y., Zhur. Fiz. Khim. 33, 1798 (1959); C. A. 54, 9479i (1960).

<sup>330</sup> Schoffeld, T. H., J. Inst. Metals 85, 68 (1956).

Some intermediate value like  $4400 \pm 600$  cal/g atom would appear to be called for in a conservative evaluation. However, Kelley's value of 3700 cal/g atom was chosen to maintain agreement with the JANAF tables.

# 5) Low-temperature heat capacity and S<sub>298</sub>

Several sets of low-temperature heat capacity data, needed for the calculation of the entropy at 298.15° K, were summarized by Beckett et al. <sup>331</sup>

S <sub>298</sub> (e. u.)	Reference
7.32	Beckett et al 331
7.33 ± 0.02	Stull and Sinke <sup>77</sup> and Kothen and Johnston <sup>333</sup>
7.334	Kothen 266
7.37 ± 0.02	Clusius and Franzosini <sup>332</sup>

The recent work of Clusius and Franzosini compared well with the earlier determinations of Kothen,  $^{266}$  and Kothen and Johnston.  $^{333}$  The value for  $^{9}_{298}$  chosen in the present work was 7.330, and the value for  $^{9}_{198}$  - $^{10}_{198}$  was 1150 cal/mole, in agreement with those of the JANAF tables.

#### 6) High-temperature heat capacity

Heat capacity measurements above room temperature have been made by several investigators. 266, 334, 335, 337, 338 From Goldsmith's 277 plot of these data, it could be seen that the results of Kothen 266 and Scott 336 agree near the transition point, whereas those of Loewen 335 and Rea 334 appeared to be high. Kothen's 333 data also agree in this range with those of Jaeger et al. 337, 338

Bur. Stds, Rept. 6645 (1 January 1960); Amended (1 April 1960).

<sup>332</sup> Clusius, K. and P. Franzosini, Z. Physik, Chem. neue Folge 16, 194 (1958).

<sup>133</sup> Kothen, C. W. and H. L. Johnston, J. Am. Chem. Soc. 75, 3101 (1953).

<sup>334</sup>Rea, J. A., The Construction of a Furnace Calorimeter and the Evaluation of a Method of Thermal Analysis for Obtaining the Specific Heat of Solids at High Temperatures, M. S. Thesis, Oklahoma A and M, Stillwater (1953).

<sup>335</sup> Loewen, E. G., Trans. Am. Soc. Mech. Engrs. <u>78</u>, 667 (1956).

<sup>336</sup> Scott, J. L., A Calorimeter Investigation of Zirconium. Titanium, and Zirconium Alloys from 60° to 960°C, Oak Ridge, Rept. ORNL-2328, AD-138-838. (1957)

<sup>337</sup> Jaeger, F. M., F. Rosenbohm, and R. Fonteyne, Proc. Acad. Sci. (Amsterdam 39, 442 (1936).

<sup>338</sup> Jaeger, F. M., E. Rosenbohm, and R. Fonteyne, Rec. trav. chim. 55, 615 (1936).

The heat capacities beyond 1476° K used in the JANAF tables were accepted for the present work with some reservations since Kothen's 333 value of 10.47 cal/g atom at 1900° K was somewhat higher and his data at lower temperatures appeared to be good. Additional measurements on titanium at high temperatures therefore appeared to be desirable, and this was included in the work in Phase III of the project.

## 7) Heat of sublimation

Vapor pressure measurements have been reported by Edwards, Johnston, and Ditmars,  $^{339}$  Blocker and Campbell,  $^{340}$  Carpenter and Mair,  $^{341}$  and Carpenter and Reavell.  $^{342}$  Edwards et al  $^{339}$  reported a heat of sublimation at 0° K of  $\Delta \rm H_{sO}^{\circ} = 112,763 \pm 83$  cal/mole. The last authors have corrected the work of the other investigators to obtain values of  $\Delta \rm H_{sO}^{\circ}$  equal to 112,167 and 111,497 cal/mole. The JANAF table value of  $\Delta \rm H_{s298}^{\circ} = 112,490$  cal/mole was adopted.

# 8) The liquid heat capacity

The value of  $C_p^o$  (liquid) = 8.000 cal/  $^o$ K mole used in the JANAF tables for liquid titanium was adopted.

#### b. Calculations for Reference-State Tables

Thermodynamic function values from the JANAF tables for the reference state of titanium were adopted for Table XLVI with the addition of uncertainty estimates and extra entries to define discontinuities at transformations. Interpolations required for the extra entries were made by means of the Lagrangian interpolation formula 343 to assure accuracy in the third decimal place. The uncertainty calculations, summarized on the back of the table, were made by the methods described in section III-G.

<sup>339</sup> Edwards, J. W., H. L. Johnston, and W. E. Ditmars, J. Am. Chem. Soc. 75, 2467 (1953).

<sup>340</sup> Blocker, J. M. and I. E. Campbell, J. Am. Chem. Soc. 71, 4040 (1949).

<sup>341</sup> Carpenter, L. G. and W. N. Mair, Proc. Phys. Soc. (London) 64B, 57 (1951).

<sup>342</sup> Carpenter, L. G. and F. R. Reavell, Nature 163, 527 (1949).

<sup>343</sup> Sokolnikoff, I. S. and E. S. Sokolnikoff, Higher Mathematics for Engineers and Physicists, McGraw-Hill, N. Y. (1941).

Reference State for Calculating ΔH°, ΔF°, and Log Kp : Solid from 298.15° to 1950°K, Liquid from 1950° to 3550°K, Gas from 3550° to 6000°K.

fw = 47.90		$T_{\epsilon}(t) = 1$	133 K	m.p. = 1950°	- 10 10		3550° ± 15
T,°K	C <sub>p</sub> c	st	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	Meal/gf ΔH;	ΔF	Log K
		-		-1.150		•	- 1
0	0.000	6.000	Dufinite 2, 330	0.000			
298.15	5.970	7. 330	7.330				
300	5.980	7.367	7.330	0.011			
400	6.360	9.147	7.570	0.631		•	
500	6.620	10.595	8.035	1.280			
600	6.840	11.822	8.566	1.953			
700	7.020	12.890	9.109	2,647			
	7.180	13.838	9.642	3.357			
800							
900	7.330	14.693	10.157	4.082 4.822			
1000	7.470	15.472	10.650	4.622			
1100	7.600	16.190	11.121	5.576			
1155	7.667	16.563	11.372	5.996			
1155	7.667	17.385	11.372	6.946	_		
1200	7.720	17.679	11.603	7.292	-		
1300	7.840	18.302	12.094	8.070			
1 <b>4</b> 00 1500	7.950 8.060	18.887 19.439	12.559 12.999	8.860 9.660			
1500	0,000	.,,	1-1777	,,,,,,			
1600	8.160	19.963	13.418	10.471			
1700	B. 260	20.460	13.818	11.292			
1800	8.360	20.935	14.200	12.123			
1900	8.460	21.390	14.567	12.964			
1950	8.510	21.610	14.745	13.388			
1950	8.000	23,507	14.745	17.088			
2000	8.000	23.710	14.966	17. 489			
2100	B. 000	24.101	15.392	18. 289			
2200	8.000	24.473	15.796	19.089			
2300	8.000	24.829	16.181	19.889			
2400	8.000	25.169	16.549	20.689			
2500	8.000	25.496	16.900	21.489			
2600	8.000	25.809	17.237	22. 289			
2700	8.000	26. 111		23. 089			
			17.560				
2800	8.000	26.402	17.871	23.889			
2900	8.000	26.683	18.170	24.689			
3000	8.000	26.954	18.458	25.489			
3100	8.000	27.217	18.736	26. 289			
3200	8.000	27.470	19.005	27. 089			
3300	8.000	27.717	19.266	27.889			
3400	8.000	27.955	19.518	28.689			
3500	8.000	28.187	19.762	29. <del>4</del> 89			
3550	8.000	28.303	19.881	29.889			
3550	8.068	57.162	19.881	132.346			
3600	8.137	57. 275	20.400	132.751			
3700	8, 274	57.500	21.400	133. 571			
3800	8.408	57.723	22.353	134.405			
3900	8.539	57.943	23. 262	135. 253			
1000	8.666	58. 160	24. 132	136.113			
1100	8.790	58.376	24.965	136.986			
1200	8.910	58. 589	25.763	137.871			
1300							
	9.026	58.800	26.529	138.768			
1400 1500	9.137 9.244	59.009 59.216	27. 265 27. 972	139.676 140.595			
,,,,,	7. 6.11	77.210	.,.,,,	1 40. 373			,
000	9.346	59.420	28.654	141.524			
700	9.443	59.622	29.310	142.464			
800	9.535	59.822	29.944	143.413			
900	9.623	60.019	30.556	144.371			
000	9.706	60. 214	31.147	145, 337			
100	9.784	60.407	31.719 - '	146.312			
200	9.857	60.598	32. 272	147. 294			
100	9.926	60.787	32.809	148.283			
400	9.990	60.973	33.328	149. 279			
500	10.050	61.157	33.833	150. 281			
600	10.105	61.338	34. 322	151. 289			
700	10.155	61.517	34. 798	152.302			
800	10. 202	61.694	35. 260	153.320			
900	10. 245	61.869	35.710	154. 342			
000	10. 284	62.042	36.147	155. 368			

TITANIUM REFERENCE STATE
SUMMARY OF UNCERTAINTY ESTIMATES

		I/°K gfu		Kcal/glv			
T, °K	C.	ST	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	AH ?	ΔF į	Log Kp
298.15	± .050	± .020	±.020	± .000			
1000	± .500	± .346	±.157	± .189			
1155	± .500	± .418	±.188	± .266			
1155	± .500	± .504	±.188	± .366			
1350	±1.000	± .896	±.403	± .962			
1950	±1.000	±1.152	±.403	±1.462			
2000	±1.000	±1.177	±.421	±1.512			
3000	± 2.000	±1.785	±.781	±3.012			
3550	± 2,000	± 2. 121	±.963	±4.112			
3550	± 2.000	± .003	±,284	±1,002			
4000	± .002	± .003	±.253 -	±1.002			
5000	± .005	± .003	±.203	±1.003			
6000	± .010	± .003	±.170	±1.004			

# 1) Uncertainties in $C_{p}^{\circ}$

Uncertainties in  $C_p^{\circ}$  values were estimated from an examination of the following available data and derived points:

		<sup>C</sup> p in cal/g atom °K								
Source	298° K	(a)	1155° K (a)	1155° K (β)	1950° K ( <i>β</i> )	1950° K ( <b>1</b> )				
JANAF Tables	5.970	7.47	7.67	7.67	8.51	8.00				
Coldsmith et al <sup>277</sup>	5.987	7.66	8.14	7.18	10.77					
Kelley56	6.00	7.77	8.16	7.50	7.50	8.00				
Kothen 266	5.976	7.96	8,40	7.14	(10.77)*					
Golutvin <sup>329</sup>	4.783	8.435		7.968	( 7.968)**					
Clusius and Franzosini332	5.998									

<sup>\*</sup> Kothen 266 reported a value of 10.47 at 1900° K. This was extrapolated for the value at 1950° K. Goldsmith's 277 data were based on Kothen's 266 determinations.

The following are the values adopted for the uncertainties in cal/  $^{\circ}K$  mole:

Temp(°K)	δCp°	Temp(° K)	δCp°
298	± 0.05	2000	± 1.0
1000	± 0.5	3000	± 2.0
1155 (a)	± 0.5	3550	± 2.0
1155 (β)	± 0.5	4000(v)	± 0.002
1950 (β)	± 1.0	5000(v)	± 0.005
1950 (1)	± 1.0	6000(v)	± 0.010

<sup>\*\*</sup>Golutvin<sup>329</sup> reported a value of 7.968 for the range from 1155° to 1400° K.

# 2) Uncertainties in ( $H_T^{\circ} - H_{298}^{\circ}$ )

As explained in section III-G, average values of  $\delta C_p^o$  over the appropriate temperature ranges were calculated from the  $\delta C_p^o$  data as described just above, multiplied by the temperature interval, and summed cumulatively to obtain the uncertainties in (  $H_T^o - H_{298}^o$ ) in Table XLVI up to the boiling point.

Above the boiling point, the equation used for calculating uncertainties was

$$\delta(H_T^{\circ} - H_{298}^{\circ})_{(1)} = \delta \Delta H_{298}^{\circ} + \delta(H_T^{\circ} - H_{298}^{\circ})_{(2)} , \qquad (158)$$

where subscript (1) = gas referred to solid at 298.15° K, and subscript (2) = gas referred to gas at 298.15° K.

It is evident from this equation that the uncertainty in  $\Delta H_{298}^{\circ}$  contributes nearly all the total uncertainty in the gas enthalpy function of titanium because the last term on the right is very small.

## 3) Uncertainty in entropy

The equations used in calculating the uncertainty in  $S_T^\circ$  for condensed phases were discussed in section III-G. The mean errors in specific heat values for titanium presented in section IV-A23b(1) above were used for the numerical computations. For the gas phase above the boiling point, the errors in  $S_T^\circ$  were taken from the machine calculation for the ideal monatomic gas described in section IV-A23c below.

#### 4) Uncertainty in free-energy function

The method used for the calculation of the uncertainty in the free-energy function of the condensed phases was also discussed earlier in section III-G of this report. The uncertainties in the free-energy function of the gas phase were also taken from the machine computation for the ideal monatomic gas described in section IV-A23c below.

The uncertainty estimates for the free-energy function of the condensed phases obtained in this work were larger than those reported by Hultgren et al: <sup>76</sup>

Ti

Reference State for Calculating  $\Delta H_F^2$ ,  $\Delta F_F^2$ , and  $\log K_p$ : Solid from 298.15° to 1950°K, Liquid from 1945° to 3500°K, Gas from 3500° to 6000°K.

gfw = 47.90 m.p. = 1950° ± 10°K b.p. = 3550° ± 150°K  $T_{\rm t}(I)=1155\,{}^{\rm s}{\rm K}$ -cel/°K gfw -Kcal/gfw C<sub>P</sub> ST  $-(F_{T}^{o} - H_{298}^{o})/T$ T. °E HT - H296 AH ; ΔF Log Kp 0.000 -1.802 0.000 Infinite 111.838 111.838 Infinite 298.15 5.838 5.831 43.068 43.068 0.000 112.490 112.490 101.835 -74-643 -74-135 43.104 43.068 0.011 101.769 300 400 5.522 44.735 43.293 0.577 112.416 98.201 -53.652 5.344 500 45.946 -41.371 43.707 1.120 112.330 94.654 5.237 600 46.911 1.648 112.185 -33.193 44.164 91.132 700 5.170 47.712 44.615 2.168 112.011 87.636 -27.360 800 5.128 2.683 48, 400 45.046 111.816 84.167 -22.992 5.104 49.002 45.453 3.194 1000 5.095 49.539 45.835 3.704 111.372 77.305 -16.894 1100 5.106 50.025 46, 194 4.214 111.128 73.909 -14.684 1155 5.118 50.275 46.383 4.496 110.990 72.052 -13.633 4. 496 1155 5.118 20, 275 46. 383 110.040 72.052 -13.633 4.726 50.471 46.532 109.924 1200 70.574 5.132 -12.853 5. 241 5. 762 1300 5.176 50.883 46.851 109.661 67.306 -11.315 51.269 5.237 1400 47.153 109.392 64.057 -9.999 1500 5.313 51.633 47.440 6.289 109.119 60.829 -8.862 1600 5.403 51.978 47.713 6.825 108.844 57.619 -7.870 7.370 1700 5.506 52.309 47.974 108.568 54.425 -6.996 1800 5.616 52.627 48.223 7.926 108.293 51.248 1900 5.736 52.934 48.463 8.494 108.020 48.087 -5.531 53.084 48.580 107.884 -5.213 8.782 1950 5.799 53.084 48.580 104.184 46.512 -5,213 5.863 53.231 48.694 9.074 104.075 45.033 -4.921 53.520 103.868 2100 48.917 9.667 -4.380 2200 6.131 53.802 49.133 49.342 10.273 103.674 39.150 -3.889 6.269 54.078 36.222 2300 10.893 103.494 -3.442 6.411 2400 54.348 49.545 11.527 103.328 33. 299 -3.032 49.742 30.386 2500 54.612 12.175 103.176 -2.656 54.872 27.475 2600 6.698 12.837 103.038 2.309 49.934 6.843 24.571 21.672 -1.989 -1.691 2700 55.127 50.122 13.514 102.915 2800 55.379 50.305 14, 206 102.807 102.713 18.776 3000 7.281 55.871 50.660 15.633 102,634 15.883 -1.157 56.112 3100 7.427 50.832 16, 368 102.569 12.994 -0.916 17.118 3200 7.571 56.350 51.001 10.102 7.715 7.857 51.166 51.329 7.218 4.328 3300 56.585 17.882 102.483 -0.478 56.818 18.661 102.462 -0.278 3400 3500 7.998 57.048 51.489 19.454 102.455 1.443 -0.090 3550 8.068 57.162 51.569 19.856 102.458 0.009 0.001 3550 8.068 57.162 51.569 19.856 51.647 51.802 3600 8.137 57.275 20.261 3700 8.274 57.500 21.081 3800 8.408 57.722 51-955 21.915 8.539 57.942 22.763 3900 52.106 4000 58.160 52.254 23.623 4100 8.790 58.376 52.401 24.496 25. 381 4200 8.910 58.589 52.546 4300 9.026 -2.689 26. 277 4400 9.137 59.009 52.830 27.186 28, 105 9. 244 52.970 4600 9.346 59.419 53.108 29.034 9.443 9.535 53.244 53.379 4700 59.621 29.974 59.821 30.923 4900 9.623 60.019 53, 513 31.881 9.706 60.214 53.645 32.847 5000 5100 9.784 60.407 53.775 60.598 60.786 5200 9.857 53.905 34.804 9.926 35.793 5300 54.033 9.990 54.160 54.285 5400 60.972 36. 789 37.791 5500 61.156 38.798 5600 10.105 61.338 54.509 10.156 61.517 54.533 54.654 39.812 40.829 5700 5800 5900 10.245 10.284 54.775 54.895 41.852 42.878 6000 62.041

TITANIUM IDEAL MONATOMIC GAS

	cal/°K gfu				Kcal/gfw		`
T, °K	c*	s <sub>T</sub>	$-(F_{T}^{\circ} - H_{298}^{\circ})/T$	$H_T^o - H_{298}^o$	ΔH°	ΔF	Log Kp
198.15	±.000	±.002	±.003	±.000	±1.000	±1.007	±.738
1000	±.001	±.002	±.003	±.001	±1.190	±1.160	± . 253
1155	±.001	±.002	±.003	±.001	±1.267	±1.220	±.230
1155	±.001	±.002	± · 003	±.001	±1.367	±1.220	±.230
1950	±.001	±.002	±.003	±.001	±1.963	±1.791	± . 200
1950	±.001	±.002	±.003	±.001	± 2.463	±1.791	±.200
2000	±.001	±.002	±.003	± - 001	±2.513	±1.848	±.201
3000	±.001	±.003	±.003	± . 002	±4.014	± 3.352	±.244
3550	± - 002	±.003	±.003	±.002	±5.114	±4.429	±.272
3550	±.002	±.003	±.003	±.002			
4000	±.002	±.003	±.002	±.002			
5000	±.005	±.003	±.003	±.003			
6000	±.010	±.003	±.004	±.004			

Source	298° K	1155° K	1950° K	3000° K
Hultgren76	± 0.02	± 0.11	± 0.13	± 0.23
This work	± 0.02	± 0.19	± 0.40	± 0,78

The difference between the estimates is attributable to the larger uncertainties assigned in this work to the heat capacity values of the solid and liquid at high temperatures because of the discrepancies discussed in section IV-A23b(1) above.

# c. Ideal Monatomic Gas Calculations

The ideal monatomic gas functions in Table XLVII were calculated by the methods described in section III-D using the energy levels of Moore.  $^{52}$  The results agreed well with those in the JANAF tables. For the sake of consistency between tabulations, values of the thermodynamic functions in the latter tables were adopted with the uncertainty limits from the present computation summarized on the back of the table. The JANAF table value of  $H_{298}^{\circ} - H_{0}^{\circ} = 1,802$  cal/mole for the gas was accepted herein.

# 24. Tungsten

#### a. Crystal Structure and Transition Temperatures

The stable form of solid tungsten at 25°C is the body-centered cubic crystal. 344-347 A face-centered cubic form has been reported to be produced by electrolysis of fused tungstates, but it reverts irreversibly to the body-centered form if heated above  $700^{\circ}\text{C}$ . 346 No true allotropes of tungsten have been observed. 348 The body-centered cubic form was therefore taken as the stable form from room temperature to the melting point in this work. The melting point adopted for tungsten is  $3650^{\circ}$   $\pm$  30°K and the estimated standard boiling point is  $5891^{\circ}$   $\pm$  275°K

## b. Melting Point

The "best" value of the melting point of tungsten has been taken to be 3650°K in recent compilations. 76, 77, 349 Other reported values ranged from 3370° to 3660°K. These older values were reviewed by Smithells 345 and by Richert, Beckett, and Johnston. 283

The heat of fusion had not been experimentally determined. Estimated values ranged from 3000 to about 8400 cal/gfw. 76, 77, 256 In the absence of conclusive experimental data, an estimated heat of fusion of 8395 cal/gfw was chosen for this compilation. This value is based on an assumed entropy of fusion of 2.3 e.u. An uncertainty of  $\pm 1000$  cal/gfw was arbitrarily assigned to the heat of fusion at the melting point.

c. Standard Heat of Sublimation at 298.15°K,  $\Lambda H_{5298}^{\circ}$ 

Vapor pressure measurements for solid tungsten have been reported by Jones, Langmuir and MacKay,  $^{261}$  and by Zwikker.  $^{350}$  A  $_{5298}$  value of 202, 770 cal/gfw was calculated with the vapor pressure values

<sup>&</sup>lt;sup>344</sup>Jette, E.R. and F. Foote, J. Chem. Phys. 3, 605 (1935).

<sup>345</sup> Smithells, C.J., Tungsten, Chemical Publ., N.Y. (1953).

<sup>346</sup>Kirk, R.E. and D.F. Othmer, Encyclopedia of Chemical Technology, Interscience Publ., N.Y. (1955).

<sup>347</sup> Pugh, J.W., Metals 10, 335 (1958).

<sup>348</sup> Charlton, M.G. and G.L. Davis, Nature 175, 131 (1955).

<sup>349</sup> Brewer, L., National Nuclear Energy Ser. IV-19B (L.L. Quill, ed.), Mc-Graw-Hill, N.Y. (1950), paper 3.

<sup>350</sup> Zwikker, C., Physica 5, 249 (1925).

of Jones and co-workers,  $^{261}$  and the free-energy functions from the present compilation. A similar calculation with the vapor pressure data of Zwikker $^{350}$  over the same temperature range yielded a  $\Delta \rm H_{s298}^{\circ}$  value of 203, 380 cal/gfw. On the basis of these two calculated values, the one chosen in the present work was 203, 100  $\pm$  1800 cal/gfw.

#### d. Boiling Point

The boiling point of tungsten had not been experimentally determined.

Estimated and/or quoted values ranged from 5100° to 6970°K; e.g.,

5100 - 5200°K<sup>256</sup>

5400°K182

5800°K<sup>77</sup>

5808°K<sup>76</sup>

6970°K. 261

The chosen  $\Delta H_{s298}^{\circ}$  value of 203, 100  $\pm$  1800 cal/gfw and free-energy functions for the gas and condensed phases from the present compilation were used to calculate a standard boiling point of 5891°  $\pm$  275°K in the present work.

The heat of vaporization at the standard boiling point was then estimated from the value of  $\Delta H_{s298}^{\circ}$  and the enthalpy functions for the gaseous and condensed phases at the standard boiling temperature. The value thus calculated was 192, 265  $\pm$  11, 400 cal/gfw.

In Table XLVIII are summarized the heats of transformation for the various phase changes of tungsten.

TABLE XLVIII
TRANSITION DATA FOR TUNGSTEN

Transition	Temperature (°K)	ΛΗ,(cal/gfw)
solid — → liquid	3650 ± 3∪	8395 ± 1000
inquid gas	5891 ± 275	192, 265 ± 11, 400
solid <u> </u>	298.15	203, 100 ± 1800

#### e. Thermodynamic Functions for Condensed Phases

Recent compilations of thermodynamic functions for tungsten include those of Stull and Sinke, 77 Hultgren, 76 and Kelley. 56 The compilations of Stull and Sinke 77 and Kelley 56 extend to only 3000°K, thereby only including data for the solid phase. None of these compilations takes into account the recent low-temperature heat capacity data of Clusius and Franzosini, 265 or the heat capacity values at high temperatures very recently reported by workers at the Union Carbide Corporation. 351

# f. Entropy and Enthalpy at 298.15°K

Kelley<sup>56</sup>has reported an  $S_{298}^{\circ}$  value of 8.04 ± 0.10 e.u. based on the heat capacity measurements of Lange<sup>352</sup> (26° to 92°K), and of Zwikker and Schmidt<sup>353</sup> (92° to 290°K). This value was used by Stull and Sinke:<sup>77</sup> It should be noted that the heat capacity values of Zwikker and Schmidt<sup>353</sup> scatter over a range of ± 10 percent. Hultgren<sup>76</sup> reported an  $S_{298}^{\circ}$  value of 7.95 ± 0.10 e.u. based on the  $C_p^{\circ}$  values of Waite, Graig, and Wallace, <sup>354</sup> and of Horowitz and Daunt<sup>280</sup> for temperatures ranging up to 20°K; the  $C_p^{\circ}$  data of Lange<sup>352</sup> and DeSorbo<sup>355</sup> up to 90°K; and the data of Zwikker and Schmidt<sup>353</sup> up to room temperature. DeSorbo<sup>355</sup> reported an  $S_{298}^{\circ}$  value of 8.2 ± 0.2 e.u. from his measured  $C_p^{\circ}$  values combined with the data of Waite, Graig, and Wallace, <sup>354</sup> and of Zwikker and Schmidt. <sup>353</sup> Clusius and Franzosini <sup>263</sup> had recently measured the heat capacity very accurately over the temperature range from 10° to 273°K and reported  $S_{298}^{\circ}$  to be 7.83 c.u. The latter value has been accepted in the present work and assigned an uncertainty of ± 0.05 e.u. Integration of the heat capacity data of Clusius and Franzosini leads to a value of  $H_{298}^{\circ}$  –  $H_0^{\circ}$  of 1195 ± 5 cal/gfw.

<sup>381</sup> Schomaker, V., R.H. Crist and R. Lowrie, Union Carbide Corporation for Advanced Research Projects Agency, Contract DA-30-069-ORD-2787, Progress Report 31 December 1960.

<sup>3521</sup> ange, F., Z. Physik Chem. 110, 343 (1924).

<sup>353.7</sup> wikker, C. and G. Schmidt, Z. Physik 52, 668 (1028).

<sup>\*\*\*4</sup> Waite, I.R., R.S. Craig and W.F. Wallace, Phys. Rev. 104, 1240 (1086).

Desorbo, W., I. Phys. Chem. 62, 965 (1958).

#### g. Thermodynamic Functions above 298.15°K

Several investigators have reported C<sub>p</sub>° values for the range of room temperature and above. 87, 194, 269, 353, 356-359 Previous 56, 76, 77 compilers had given most weight to the work of Jaeger and Rosenbohm 357 and of Magnus and Hotzmann 87, and then, used an extrapolation of these data up to high temperatures. However, comparison of the C<sub>p</sub>° values thus obtained with low-temperature measurements of Clusius and Franzosini, 265 and the high-temperature measurements of Schomaker, Crist, and Lowrie 351 (1300°K - 2500°K), leads to the conclusion that values of previous compilers 56, 76, 77 are too high near room temperature and too low at temperatures above 1300°K.

Accordingly, the values of Clusius and Franzosini<sup>265</sup> were extended so as to join smoothly with the values of Schomaker, Crist, and Lowrie<sup>351</sup> at  $1300\,^{\circ}\text{K}$ . These  $C_p^{\circ}$  values were included in the present tables. Above  $1300\,^{\circ}\text{K}$ , the  $C_p^{\circ}$  values fit equation (159),

$$C_p^o = 4.70 + 1.5 \times 10^{-3} \,\mathrm{T}$$
, (159)

which was used for extrapolation up to the melting point of 3650°K.

From 298.15° to 1300°K, values of  $\rm H_T^\circ\text{--}H_{298}^\circ$  and  $S_T^\circ$  were evaluated by

graphical integration. Values of  $-\left(\frac{F_T^c - H_{208}^c}{T}\right)$  were obtained from equation (108).

Above 1300°K to the melting point,  $S_T^{\circ}$  and  $H_T^{\circ}$ -  $H_{298}^{\circ}$  values were calculated from equations (160) and 161).

$$H_{\rm T}^{\circ} - H_{298}^{\circ} = 4.707 + 75 \cdot 10^{-5} T^2 - 1130$$
, (160)

$$S_T^0 = 4.70 \ln T + 1.5 \times 10^{-3} T - 18.762$$
 (161)

The values of the constants of integration in the above equations were evaluated from the tabular values of  $S_T^o$  and  $H_T^ H_{208}^o$  at 1300°K. The free-energy function was then calculated as indicated above.

<sup>[18]</sup> Jacket, F.M. and F. Rosenbohm, Proc. Acad. Sci. (Amsterdam) 30, 1069 (1927).

Saeger, F.M. and J. Rosenbohm, Proc. Acad. Sci. (Amsterdam) 33, 457 (1930).

Shagnus, A. and H. Danz, Ann. Phys. 8, 408 (1970).

Foresthe W.F. and A.S. Wortbing, Astrophys. J. 1 140 1025).

No experimental value of  $C_p^\circ$  for liquid tungsten had been published. The heat capacity of liquid tungsten was taken to be constant at 10.00 cal/°K gfw. This value was chosen from a comparison of the values used for chromium (9.4 cal/° K gfw), molybdenum (10.00 cal/° K gfw), and solid tungsten at the melting point (10.175 cal/°K gfw). Previous compilations have used an estimated value of 8.5 cal/°K gfw. 76, 77

Entropy and enthalpy values for liquid tungsten were therefore calculated with equations (162) and (163), respectively.

$$S_{\rm T}^{\circ} = 10 \ln T - 54.460 , \qquad (162)$$

$$H_{\rm T}^{\circ} - H_{\rm 298}^{\circ} = 10 \, {\rm T} - 2088 \, .$$
 (163)

The values of the constants of integration in the above equations were evaluated from the tabular values of  $S_T^o$  and  $H_T^o$ -  $H_{298}^o$  for liquid tungsten at the melting point. The free-energy function for liquid tungsten was calculated from these values of  $S_T^o$  and  $H_T^o$ -  $H_{298}^o$  in the manner described in section III-G.

The reference state thermodynamic functions of tungsten are given in Table XLIX. Uncertainty estimates are summarized on the back of the table.

h. Thermodynamic Functions for the Gaseous Phase

Thermodynamic properties for the ideal monatomic gas were calculated using the spectroscopic energy levels listed by Moore. <sup>221</sup> Energy levels and J values not definitely established in these tables were estimated. The equations employed in these calculations have been discussed in two recent publications, <sup>51</sup>, <sup>75</sup> and are summarized in section III-D.  $H_{208}^{\bullet}$  -  $H_{0}^{\bullet}$  was calculated to be 1486 cal/mole.

The  $\Delta H_f^o$ ,  $\Delta F_f^o$ , and  $log_{10}K_p$  functions of gaseous tungsten were calculated by means of equations (42), (43), and (44).

The ideal monatomic gas thermodynamic functions of tungsten are given in Table L. Uncertainty estimates are summarized on the back of the table.

i. Uncertainty in Condensed Phase Functions

Uncertainties in the condensed phase functions of tungsten were calculated by the methods described in section III-G.

#### REFERENCE STATE

Reference State for Calculating ΔH<sup>2</sup><sub>f</sub>, ΔF<sup>2</sup><sub>f</sub>, and Log K<sub>p</sub>: Solid from 298.15° to 3650°K, Liquid from 3650° to 5891°K, Gas from 5891° to 6000°K.

gfw = 183.86

m.p. = 3650° ± 30°K

b.p. = 5891° ± 275°K

		-cel/°K gfv			Kcal/gfw -		<b>`</b>
T, °K	C.	ST	$-(F_T^o - H_{298}^o)/T$	н <mark>т</mark> – н <sub>298</sub>	∆H °	ΔF	Log
0	0.000	0.000	Infinite	-1.195			
298.15	5.800	7.830	7.830	0.000			
300	5.810	7.866	7.830	0.011			
400	5.960	9.580	8.082	0.599			
500	6.040	10.901	8.501	1.200			
600	6.110	12. 027	9.015	1.807			
700	6.180	12.955	9.496	2. 421			
800	6. 240	13.803	9.999	3.043			
900	6.300	14.523	10.444	3.671			
1000	6.360	15. 209	10.906	4.303			
1100	6.430	15.799	11.305	4.943			
1200	6.520	16.382	11.724	5.589			
1300	6.650	16.888	12.082	6. 248			
1400	6.800	17.386	12.442	6.921			
1500	6.950	17.860	12.788	7.608			
1600	7.100	18.313	13.119	8.311			
1700	7.250	18.748	13.437	9.028			
1800	7.400	19.167	13.744	9.761			
1900	7.550	19.571	14.040	10.508			
2000	7.700	19.962	14. 326	11. 271			
2100	7.850	20.342	14.605	12.048			
2200	8.000	20.710	14.873	12.841			
2300	8.150	21.069	15.135	13.648			
2400	8.300	21.419	15.389	14.471			
2500	8.450	21.761	15.638	15.308			
2600	8.600	22.095	15.879	16. 161			
2700	8.750	22. 423	16. 116	17.028			
28 OC	8.900	22.744	16.347	17.911			
2900	9.050	23.059	16.573	18.808			
3000	9.200	23.368	16.794	19.721			
3100	9.350	23.672	17.011	20.648			
3200 3300	9.500 9.650	23.971 24.266	17. 224 17. 433	21.591 22.548			
3400	9.800	24. 556	17.638	23. 521			
3500	9.950	24.842	17.840	24. 508			
3600	10 100	25 125	18 030	25.511			
3650	10.100 10.175	25. 125 25. 265	18.039 18.137	26.017			
3650	10.000	27.565	18. 137	34.412			
700	10.000	27.701	18. 265	34.912			
800	10.000	27.968	18.517	35.912			
1900	10.000	28. 227	18.762	36.912			
1000	10.000	28.481	19.003	37.912			
100	10.000	28.727	19. 236	38.912			
200	10.000	28.968	19.465	39.912			
300	10.000	29.204	19.690	40.912			
400	10.000	49.434	19.909	41.912			
500	10.000	29.658	20.122	42.912			
400	10.000	20 070	20 132	43 012			
1600 1700	10.000	29.878 30.093	20. 332 20. 537	43.912 44.912			
800	10.000	30.304	20.739	45.912			
900	10.000	30.510	20.936	46.912			
000	10.000	30.712	21.130	47.912			
100	10.000	30.910	21.319	48.912			
200	10.000	31, 104	21.506	49.912			
300	10.000	31. 295	21.689	50.912			
400	10.000	31.482	21.869	51.912			
500	10.000	31.665	22.045	52.912			
600	10.000	31.845	22. 218	53.912			
700	10.000	32. 022	22. 388	54.912			
800	10.000	32. 196	22.556	55.912			
891	10.000	32, 352	22.706	56.822			
891	9.682	64.988	22.706	249.087			
900	9.668	65.003	22.770	249, 174			
	9.753	65. 166	23. 475	250.146			
000							
000							
000							
000							
000							
000							

TUNGSTEN REFERENCE STATE

		I/°K gfu			Kcal/	`	
T.°K	C.	s <sub>T</sub>	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	746	$\Delta F_{f}$	Log Ep
0				± .005			
298.15	± .100	± .050	± .050	± .000			
1000	± .500	± .410	± .200	± .210			
2000	± .500	± .760	± .410	± .710			
3000	±1.000	±1.060	± .570	±1.460			
3650	±1.500	±1.300	± .680	± 2. 270			
3650	± 2.000	±1.580	± .680	±3.270			
4000	± 2.000	±1.760	± .770	±3.970			
5000	±3,000	± 2.320	±1.030	±6.470			
5891	±4.000	± 2.890	±1.260	±9.590			
5891	± .007	± .005					
6000	± .007	± .005					

Reference State for Calculating AH<sup>a</sup>, AF<sup>a</sup>, and Log K<sub>p</sub>: Solid from 298.15° to 3650° K.
Liquid from 3650° to 5891° K, Gas from 5891° to 6000° K.

gfw = 183.86 m.p. = 3650° ± 30° K b.p. = 5891° ± 275° K

τ, <b>°</b> κ 0	C.	5α .	$-(F_{T}^{0} - H_{298}^{0})/T$	HT - H298	ΔHγ̈́	ΔF	Lo
0		•	1 298"	··T - ··298	1	1	Lo
	0.000	0.000	Infinite	-1,486	202.809	202.809	Infi
298.15	5.092	41.551	41.551	0.000	203.100	193.046	- 14
300	5.097	41.583	41,551	0.009	203.098	192.983	- 14
400	5.536	43, 101	41.755	0.538	203.039	189.631	-10
500	6.297	44,413	42, 158	1,128	203, 028	186, 272	-8
600	7. 251	45,643	42.637	1.804	203.097	182, 927	-6
700	7, 218	46.835	43, 152	2.578	203, 257	179.541	- 5
800	9,026	47.987	43,685	3.442	203.499	176.151	-4
900	9.577	49.085	44, 224	4.375	203.804	172,697	- 4
000	9.856	50,111	44.762	5, 348	204,145	169, 244	- 3
100	9.904	51.054	45.292	6.338	204.495	165.714	- 3
200	9.788	51, 912	45.809	7.324	204.835	162, 197	- 2
300	9.569	52, 687	46.308	8.292	205.144	158.607	- Z
400 500	9.298 9.008	53.387 54.018	46.789 47.251	9.236 10.151	205.415 205.643	155.015 151.407	- 2 - 2
600	8,721	54.590	47.692	11.038	205.827	147, 784	- 2
700	8.451	55.111	48.113	11.896	205.968	144.153	-1
800	8, 206	55.587	48.515 48.899	12,729	206.068	140.513	- 1
900	7.987 7.797	56.025 56.429	49.266	13,538 14,327	206. 130 206. 156	136,870 133,220	-1 -1
100	7.635	56.806 57.158	49.616 49.951	15.098	206, 150 206, 114	129.576	- 1 - 1
200	7.500	57. 158	50.271	15.855 16.599	206, 051	125, 930 122, 286	-1
300 400	7.391 7.306	57.489 57.801	50.579	17.334	205. 963	118.646	-1
500	7. 243	58.098	50.874	18.061	205.853	115.010	-1
					205 723		
700	7.201 7.179	58.381 58.653	51.157 51.430	18.783 19.502	205.722 205.574	111.379 107.752	-
800	7.179	58.913	51.692	20.220	205, 409	104, 132	
900	7, 184	59.165	51.946	20.937	205, 229	100.520	-
000	7.209	59.409	52, 190	21.657	205.036	96. 909	-
		50 (1)	52 437	22 200	204 022	03.310	
100	7.247	59,646	52.427 52.656	22.380 23.107	204.832	93.310 89.718	-
300	7.297 7.357	59, 877 60, 103	52.878	23.839	204. 391	86.130	
400	7.426	60, 323	53.094	24.578	204, 157	82.552	
500	7,503	60,540	53.304	25, 325	203, 917	78.974	
600	7.586	60,752	53.508	26.079	203.668	75.413	
650	7,630	60,857	53,608	26,460	203, 543	73, 631	
650	7.630	60,857	53,608	26.460	195.148	73.631	
700	7.675	60.961	53.706	26.842	195.030	71.969	-
800	7.769	61.167	53.900	27.615	194.803	68,647	-
900	7.866 7.965	61.370 61.570	54.089 54.274	28, 396 29, 188	194.584 194.376	65.325 62.016	:
•••	1, 703		31.4.1				
100	8.067	61.768	54,454	29.989	194, 177	58,704	
200	8.169	61, 964	54.630	30.801	193, 989	55, 401 52, 116	
300	8. 273	62, 157	54,803	31.623 32.456	193, 813 193, 644	48,818	
400 500	8.376 8.478	62.349 62.538	54.973 55.139	33, 298	193.486	45,522	
600	8.580	62 726	44 301 44 461	34, 151	193, 339	43.242	- 1
700 800	8.680 8.778	62, 911 63, 095	55.461 55.619	35.014 35.887	193, 202 193, 075	38. <b>963</b> 35, 674	
900	5.874	63, 277	55.773	36, 770	192.958	32, 399	
000	8.968	63.457	55. 925	37.662	192.850	29.125	
100	9.059	63,636	56.074	38, 563	192.751	25,852	
200	9. 059	63.812	56, 221	39.473	192,661	22,584	
300	9, 234	63.988	56. 366	40.393	192.581	18. 312	- (
400	9. 317	64, 161	56, 509	41.320	192,508	16.043	- (
500	9. 397	64.333	56.650	42.256	192.444	12,771	- (
600	9.474	64.503	56.788	43.199	192, 387	9.509	- (
700	9.548	64.671	56. 925	44.150	192. 338	6,242	. (
800	9.619	64,838	57,060	45.109	192.297	2.975	- (
671	9.682	64, 988	57.181	45.987	192.265	0.000	(
891	9.682	64, 988	57.181	45, 987			
9( 0	9.688	65.003	57, 193 57, 325	46.074 47.046			
000	9.753	65, 166	57, 325	11,010			
				,			
	•			•			

TUNGSTEN IDEAL MONATOMIC GAS

,	cal/°K afe				Kcal/#		$\overline{}$
T, °K	c,	s <sub>T</sub>	-(F <sub>T</sub> - H <sub>290</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH °	AF (	Log Ky
298.15	±.000	±.002	±,002	±.000	±1.800	±1.820	±1.330
1000	<b>±</b> ,001	±.003	±.003	±.001	±2.010	±2.000	± .440
2000	±,001	±.003	<b>±.003</b>	±.001	± 2.510	±2.630	4.,290
3000	±.001	±.003	±.003	±.002	±3,260	±3.520	± .260
3650	±,002	£.003	±.003	±.002	±4.070	±4.290	± .260
3650	±.002	±.003	±,003	±.002	±5.070	±4.290	± ,260
4000	±.003	±.003	±.003	±.003	±5.770	±4.890	± .270
5000	±.006	±.004	±.003	±.007	±8. 280	±6.970	★ ,300
5891	±.007	±.005	±.003	±.012	±1.140	±9.240	★ .340
5891	±.007	±.005	±.003	±.012			
6000	±.007	±.005	±.003	±.013			

# Heat capacity

Graphical intercomparison of reported  $C_p^o$  values for solid tungsten led to the following choices of uncertainties:

- ± 0.1 cal/°K gfw at 298.15°K
- ± 0.5 cal/°K gfw at 1000°K
- ± 0.5 cal/°K gfw at 2000°K
- $\pm$  1.0 cal/°K gfw at 3000°K
- $\pm$  1.5 cal/°K gfw at m.p. (3650°K).

The heat capacity of liquid tungsten had apparently never been experimentally measured; therefore, a rather large overall uncertainty was arbitrarily assigned to the estimated value. Particular uncertainties assigned were as follows:

- $\pm$  2.0 cal/°K gfw at m.p. (3650°K)
- ± 2.0 cal/°K gfw at 4000°K
- $\pm$  3.0 cal/°K gfw at 5000°K
- $\pm$  4.0 cal/°K gfw at b.p. (5891°K).

# 2) Entropy

Uncertainties in entropy values were calculated from assigned uncertainties in  $C_p^o$  values, and assigned uncertainties for heats of transitions by the method described in section III-G. Equation (149) was used at transitions.

# 3) Free energy

The uncertainties in free-energy function were calculated from uncertainties in  $S_T^\circ$  and  $H_T^\circ$ -  $H_{298}^\circ$  by means of equation (120).

#### j. Uncertainties in Gas-Phase Functions

Uncertainties in the ideal gas thermodynamic functions at the specified temperatures were computed as explained in section III-D2. The uncertainties in  $\Delta H_{l}^{o}$ ,  $\Delta F_{l}^{o}$ , and  $\log_{10}K_{p}$  were calculated by means of equations (46) (47), and (48).

k. Other Reference Pertaining to the Thermodynamics of Tungsten

Heat capacity measurements at low temperatures have also been reported and discussed by Boosz, 278 Wolcott, 204 and Rayne. 279 Heat capacities at high temperatures have also been reported by Southern Research Institute 29 workers.

The vapor pressure data of Jones, Langmuir, and MacKay  $^{261}$  were re-calculated from the original data of Langmuir.  $^{360}$  The vapor pressure values reported by van Liempt  $^{282}$  are smoothed values from Langmuir's original work.  $^{360}$ 

Useful annotated bibliographies on tungsten were those of Goodwin and Ayton,  $^{209}$  and of Richert, Beckett, and Johnston.  $^{283}$ 

<sup>300</sup> Langmuir, I., Phys. Rev. 2, 450 (1913).

afw = 50.95

-		al/"K gfw			Keal/	Bia .	
T, °K	c.	ST	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	∆H <sub>t</sub> °	ΔF	Log !
0	0.000	0.000	Infinite	-			Infinit
298.15	6. 217	43.546	43.546	0.000 .			1111111
300	6.209	43.584	43-546	0.011			
400	5.891	45.321	43.785	0.615			
500	5.783	46.621	44.227	1.197			
	31,03	10.02.	••••	,.			
600	5.804	47.676	44.717	1.775			
700	5.875	48.576	45.205	2.359	•		
800	5.949	49.365	45.677	2.951			
900	6.003	50.069	46.127	3.548			
000	6.032	50.704	46.553	4. 150			
100	6.038	51. 279	46.957	4.754		4	
200	6.026	51.804	47.339	5.357			
300	6.003	52. 285	47.702	5. 959			
400	5.974	52.729	48.045	6.558			
500	5.943	53.140	48.371	7.154			
600	5.913	53.523	48.681	7.746			
700	5.887	53.881	48.977	8.336			
800	5.867	54. 216	49.259	8.924			
900 000	5.853 5.846	54. 533	49.528	9.510			
300	5.840	54.833	49.786	10.095			
100	5.848	55.119	50.033	10.680			
200	5.858	55.391	50.270	11.265			
300	5.877	55.652	50.499	11.851			
400	5.904	55.902	50.719	12.440			
500	5.940	56.144	50.931	13.033			
			11 .57				
500	5.985	56. 378	51.136	13.629			
700	6.038	56.605	51.334	14. 230			
300	6.099	56.825	51.526	14.837			
900	6.168	57.040	51.713	15.450			
000	6. 245	57. 251	51.894	16.070			
00	6.328	57.457	52.070	16.699			
200	6.418	57.659	52.242	17.336			
300	6.515	57.858	52.409	17.983			
400	6.617	58.054	52.572	18.639			
500	6.723	58. 248	52.731	19.306			
				-,			
600	6.835	58.438	52.887	19.984			
700	6.950	58.627	53.040	20.673			
300	7.068	58.814	53.189	21.374			
900	7.188	58.999	53.336	22.087			
000	7.311	59.183	53.480	22.812			
100	7 415	50 145	61 (1)	22 540			
00.	7.435	59.365	53.621	23.549			
00	7.560	59.546	53.760	24. 299			
00	7.685	59.725	53.897	25.061			
00	7.810	59.903	54.031	25.836			
00	7.935	60.080	54.164	26.623			
00	8.058	60.256	54.294	27.423			
00	8.180	60.430	54.423	28.235			
00	В. 300	60.604	54.550	29.059			
00	8.419	60.776	54.675	29.895			
00	8.534	60.947	54.799	30.743			
00	0 440	(1)	54.033	21 (0:			
00 00	8.648 8.758	61.118	54.921	31.602			
		61.287	55.042	32.472			
00 00	8.866	61.454	55.161	33. 353 34. 245			
00	8.970 9.071	61.621 61.787	55.279 55.396	34. 245 35. 1 <b>4</b> 7			
00	9.169	61-951	55-512	36.059			
00	9. 264	62.114	55.626	36.981			
00	9.354	62.276	55.739	37.912			
00	9.442	62.437	55.852	38.852			
00	7.526	62 596	55.963	39.800			
		~					

#### VANADIUM IDEAL MONATOMIC GAS

					Ccel/gfv			
T, °E	c <b>,</b>	S <sup>*</sup> T	$-(F_{T}^{o} - H_{290}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	VH.	AF ;	Loging	
298.15	±.000	±.002	±.003	±.000				
1000	±.000	±.002	±.003	±.000				
2000	±.000	±.003	±.003	±.001				
3000	±.001	±.003	2.003	±.001				
4000	±.001	±.003	±.003	±.002				
5000	±.002	±.003	±.003	±.003				
6000	±.003	±.004	±.003	±.005				

# 25. Vanadium

The ideal monatomic gas thermodynamic functions of vanadium in Table LI were calculated from the energy levels listed by Moore <sup>52</sup> with the computer program discussed in section III-D. Uncertainty estimates are summarized on the back of the table.

#### 26. Zirconium

The reference state thermodynamic functions of zirconium are given in Table LII. Uncertainty estimates are summarized on the back of the table.

#### a. Condensed Phase Data

### 1) Crystalline forms and range of stability

Elemental zirconium is known to exist in two different crystalline modifications. <sup>361</sup> At room temperature, the stable modification has a hexagonal, close-packed structure which persists up to 1135°K. Above this temperature, the body-centered cubic structure is the stable one.

## 2) Transition temperatures

#### a) Solid state transition

Miller  $^{361}$  accepted 1135°K (862°C) as the solid-state transition temperature, Hansen and Anderko  $^{213}$  have used a value of 1138°K (865°C), Skinner  $^{362}$  found a value of 1143°K, and Kelley  $^{56}$  adopted a value of 1135°K. The last value is the one used in the present tabulation with an uncertainty of  $\pm$  10°K to include all the above values.

#### b) Melting point

For pure, hafnium-free zirconium, Miller <sup>361</sup> tabulated melting points of 2118°K (1845°C), based on the work of Adenstedt <sup>219</sup> and 2128°± 15°K (1855°± 15°C), from the work of Deardorff and Hayes. <sup>327</sup> Oriani and Jones <sup>363</sup> obtained a melting point of 2141°K. Hultgren et al <sup>76</sup> interpreted the last results to obtain a melting point of 2125°K. The Hultgren et al value was accepted for the present compilation.

## c) Boiling point

Accurate experimental determinations of the boiling point of zirconium appeared not to be available. Hultgren et al<sup>76</sup> have calculated a boiling point of 4688°K. Miller<sup>361</sup> reported a value of 3850°K (3577°C) based on the older work of Quill. <sup>364</sup>

<sup>361</sup> Miller, G., Zirconium, Academic Press, N.Y. (1957).

<sup>362</sup> Skinner, G.B., Ph.D. Thesis, Ohio State University (1951).

<sup>363</sup> Oriani, R.A. and T.S. Jones, Rev. Sci. Instr. 25, 248 (1954).

<sup>364</sup> Quill, L.L., The Chemistry and Metallurgy of Miscellaneous Materials, McGraw-Hill, N.Y. (1950).

Reference State for Calculating AH<sub>p</sub><sup>o</sup>, AF<sub>p</sub><sup>o</sup>, and Log K<sub>p</sub>: Solid from 298.15° to 2125°K, Liquid from 2125° to 4743°K, Gas from 4743° to 6000°K.

fw = 91.22		T <sub>t</sub> = 113:			± 10°K		4743° ± 16
T, *K	C <sub>p</sub>	ST	-(F <sub>T</sub> - H <sub>299</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>o</sup> <sub>f</sub> Kcal/gfv	ΔF	Log K
0	0.000	0.000	Infinite	-1.313	,	•	
298.15	6. 001	9. 290	9. 290	0.000			
300	6. 015	9.327	9. 290	0.011			
400	6.556	11.141	9.533	0.643			
500	6.882	12.642	10.011	1.316			
600	7.125	13.920	10.559	2. 016			
700	7.327	15.034	11.121	2.739			
800	7.508	16.025	11.674	3.481			
900	7.677	16.920	12.208	4, 240			
1000	7.838	17.737	12.721	5.016			
1100	7.995	18.493	13.211	5.810			
1135	8.049	18.745	13.378	6.091			
1135	7.900	19.551	13,378	7.006			
1200	7.900	19.991	13.725	7.519			
1300	7.900	20.623	14.231	8.309			
1400	7.900	21.209	14.709	9.099			
1500	7.900	21.754	15. 161	9.889			
1600	7.900	22. 264	15.589	10.679			
1700	7.900	22.743	15.996	11.469			
1800	7.900	23. 194	16.383	12. 259			
1900	7.900	23,621	16.753	13.049			
2000	7.900	24. 027	17. 107	13.839			
2100	7.900	24. 412	17.446	14.629			
2125	7.900	24.505	17. 528	14.826			
2125	9.000	26.811	17. 528	19.726			
2200	a. 000	27.088	17.849	20.326			
2300	8.000	27.444	18. 259	21.126			
2400	8.000	27. 785	18.649	21.9:6			
2500	8.000	28. 111	19.021	22.726			
2600	8.000	28. 425	19.376	23.526			
2700	8.000	28.727	19.717	24.326			
2800	8.000	29.018	29.044	25. 126			
2900	8.000	29. 299	20.359	25.926			
3000	8.000	29. 570	20.661	26.726			
0018	8.000	29.832	20.953	27.526			
3200	8.000	30.086	21. 234	28.326			
3300	8.000	30.332	21,506	29.126			
1400	8.000	30.571	21.769	29.926			
3500	8.000	30.803	22.024	30.726			
1600	8.000	31.028	22. 271	31.526			
3700	8.000	31.248	22.511	32. 326			
1600	8.000	31.461	22.743	33.126			
900	8.000	31.669	22.970	33.926			
000	8.000	31.871	23.190	34.726			
100	8.000	32.069	23.404	35. 526			
200	8.000	32, 262	23.612	36. 326			
300	8.000	32, 450	23.816	37. 126			
400	8.000	32, 634	24.014	37.926			
500	8.000	32,814	24. 208	38.726			
600	8.000	32.989	24, 397	39. 526			
700	8.000	33. 161	24.581	40. 326			
743.340	8.000	33. 234	24.659	40. 673			
743, 34	9.008	62.416	24.659	179.096			
800	9.039	62.524	25.106	179.607			
900	9.091	62.711	25.872	180.514			
000	9.139	62.895	26.610	181.425			
100	9.185	63.076	27. 323	182.341			
200	9.226	63.255	28.012	183. 262			
300	9. 265	63.431	28.679	184. 187			
400	9. 300	63.605	29. 324	185. 115			
500	9. 332	63.775	29.948	186. 046			
600	9.361	63.944	30, 554	186.981			
700	9. 387	64.110	31.142	187. 919			
800	9.409	64. 273	31.711	188.858			
900	9.429	64. 434	32. 264	189.800			
000	9. 446	64. 593	32.802	190.744			

ZIRCONIUM REFERENCE STATE

### SUMMARY OF UNCERTAINTY ESTIMATES

		/°K gfw			Kcal/	gf v	_
T, °K	c <b>"</b>	s <sub>T</sub>	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	VH 0	ΔF	Log K
298.15	± .050	± .040	± .040	± .000			
1000	± .500	± .123	± .065	± .058			
1135	± .500	± .185	± .077	± .123			
1135	± .500	± .273	± .077	± .223			
2000	±1.000	± .569	± .229	± .680			
2125	±1.000	± .625	± .251	± .796			
2125	±2.000	± .860	± .251	±1.296			
3000	± 2.000	±1.550	± .535	±3.046			
4000	± 2.000	± 2.125	± .864	±5,046		•	
4743.34	± 2.000	± 2.465	±1.088	±6,532			
4743.34	± .002	± .004					
5000	± .002	± .004					
6000	± .001	± .004					

Kubaschewski and Evans<sup>182</sup> reported an approximate value of 5023°K (4750°C), and Stull and Sinke<sup>77</sup> obtained a value of 4650°K. From the data in the present compilation, a boiling point of 4743° ± 165°K was calculated and adopted.

### 3) Heats of transformation

#### a) Heat of transition

The following values had been reported for the solid-state heat of transition at 1135 °K:

Heat of Transition (cal/mole)	Source
1040	Stull and Sinke <sup>77</sup>
920	Miller, 361 p. 151, based on Coughlin and King's work 365
915	Kelley, <sup>56</sup> p. 209

In the present tabulation, Kelley's value of 915 cal/mole was accepted.

### b) Heat of fusion

There were several estimates available for the heat of fusion of zirconium.

Heat of Fusion (cal/mole)	Source		
5500	Miller, <sup>361</sup> p. 151, based on Quill <sup>364</sup>		
4000	Stull and Sinke <sup>77</sup>		
4890	Hultgren <sup>76</sup>		

A value of 4900 cal/mole as recommended by Kelley was used for the heat of fusion of zirconium in the present tabulation.

<sup>365</sup> Coughlin, J.P. and E.G. King, J. Am. Chem. Soc. 73, 2032 (1951).

### c) Heat of sublimation

The only vapor pressure measurements reported for zirconium were those of Skinner, Edwards, and Johnston.  $^{366}$  Stull and Sinke  $^{77}$  used these data to determine that  $\Delta H_{1298}^{\circ} = 146,000$  cal/mole for the temperature range from 1949° to 2054°K assuming the condensation coefficient to be equal to unity. Hultgren et al  $^{76}$  obtained a value of 145,760 cal/mole from the same data. Lewis et al  $^{220}$  have tabulated a value of 146,000 ± 1000 cal/mole. The latter was accepted in the present compilation.

## 4) Heat capacity

## a) Low-temperature data

Low-temperature heat capacity data have been reported by Skinner and Johnston  $^{367}$  for the range from  $14^\circ$  to  $300^\circ$ K. Their data yield a standard state entropy of  $S_{298}^\circ = 9.29 \pm 0.04$  e.u. Additional data have been reported by  $Todd^{368}$  for the range from  $51^\circ$  to  $298^\circ$ K and by Burk, Estermann, and Friedberg  $^{218}$  for the range from  $15^\circ$  to  $200^\circ$ K. The latter data agree within 1 percent with those of Skinner and Johnston,  $^{367}$  which were accepted here since they cover a wider temperature range. The above value of the standard state entropy was also accepted.  $H_{298}^\circ - H_0^\circ$  was taken to be 1313 cal/gfw.

### b) High-temperature data

High-temperature heat capacity data for zirconium from various sources have been reviewed by Kelley. <sup>56</sup> His review included the recent work of Douglas and Victor. <sup>369</sup> Other sources of data were as follows:

<sup>366</sup>Skinner, G.B., J.W. Edwards, and H.L. Johnston, J. Am. Chem. Soc. <u>73</u>, 174 (1951).

<sup>367</sup> Skinner, G.B. and H.L. Johnston, J. Am. Chem. Soc. 73, 4549 (1951).

<sup>368</sup> Todd, S.S., J. Am. Chem. Soc. 72, 2914 (1950).

<sup>369</sup> Douglas, T.B. and A.C. Victor, J. Research Nat. Bur. Stds. 61, 13 (1958).

Zг

T<sub>t</sub> = 1135° <u>+</u> 10° K m. p. = 2125 \* + 10 \* K b.p. = 4743°+ 165° K gfw = 91.22 cal/oK gfw Kcal/gfw H<sub>T</sub> - H<sub>298</sub> ΔF C<sub>p</sub> s<sub>T</sub>  $-(F_{T}^{\circ} - H_{298}^{\circ})/T$  $\Delta H_I^\circ$ T, °E Los Kp -1.629 0.000 0.000 Infinite Infinite 6.368 6.375 43, 317 43, 356 43.317 43.317 0.000 298.15 146.000 300 6.612 400 45, 231 43.571 0.664 500 46.707 1.326 44.056 1.979 600 6.464 47.899 44.601 6.316 48.884 49.719 45.144 45.665 2.618 3.243 700 800 900 6.133 50,445 46 157 3.859 6, 121 51,090 4.472 1000 46.619 5,085 51.912 51.912 47, 230 47, 230 5.350 5.350 1135 6.182 1200 6,226 52, 213 47,460 5.704 6.320 52,715 47.845 6, 331 1400 6.428 53, 188 48.210 6.969 1500 6.542 7,617 53.635 48.557 1600 54.061 48.888 8,277 1700 6.764 54.468 49, 204 8.948 1800 6.866 54.857 9.629 6,960 55, 231 10.321 1900 49.799 2000 7,047 55,590 50.080 11.021 55, 936 56, 020 11.730 11.909 2100 7,128 50.350 50.416 2125 7.148 7,148 7,204 56.020 56.269 50.416 50.612 11.909 12.447 2125 2200 56.591 56.902 50.865 51.110 13, 171 13, 902 2 300 7.276 2400 7.345 2500 7.413 57.203 51.348 14.640 7.481 7.549 57.496 57.779 51.578 15, 384 2600 2700 7,618 7,688 2800 58.055 52,021 16.894 3000 7.760 58.585 52,441 18.432 52.644 19,212 3100 58,841 7.833 3200 3300 7.908 7.984 59.091 59.335 52, 841 53, 034 19.999 3400 8.061 59.575 53, 223 21.595 22.405 3500 8.139 59.810 53,408 3600 8.217 60.040 53,589 23.223 8.294 8.371 60.266 60.448 53.767 53.941 3700 24,049 3800 24.882 1900 8.447 60.707 54, 111 25.723 4000 8,522 60. 922 26.571 4100 8.595 61.133 54.443 27,427 28, 290 4200 8.666 61.341 54.605 6.735 8.802 61.546 54.764 54.921 29.160 30.037 4300 4400 4500 8.865 61.946 55.075 30,921 62, 141 62, 334 31.810 4500 8.926 55, 226 4700 8.984 55.375 32.706 4800 9.039 62.524 55. 522 33.607 34.514 4900 5000 9, 139 62.895 55.810 35.425 9.185 63.076 55.950 36.341 5100 5200 5300 9. 226 9. 265 63.255 63.431 56.089 56.226 37. 262 38. 187 9, 300 5400 63.605 56.361 39. 15 63.775 56.494 40. 346 5500 5600 56.626 40.981 9. 387 64.110 64.273 5700 56.756 41.919 5800 56.884 42.858 5900 9.429 64.434 57.011 43,800 64.593 44.744

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ZIRCONIUM IDEAL MONATOMIC GAS

#### SUMMARY OF UNCERTAINTY ESTIMATES

,	a	d/°K gf+		Kcal/gfv			`
T, ° <b>K</b>	c,	s <sub>T</sub>	$-(F_{T}^{0}-H_{290}^{0})/T$	H <sub>T</sub> - H <sub>298</sub>	AR?	AF !	Log Eq
298. 15	±.001	±.002	±.003	±.000	±1,000		
1000	±.001	±,002	±.003	±.000			
1135	±.001	±.002	±.003	±.000			
1135	±.001	±,002	±.003	±.000			
2000	±.001	±.003	±.003	±,001			
2125	±.001	±,003	±.003	±.001			
2125	<b>±.001</b>	±.003	±.003	±.001			
3000	±.002	±.003	±.003	±.002			
4000	±.002	±.003	±.003	±.003			
5000	±.002	±.004	±.003	±.005			
6000	±.001	±.004	±.003	±.006			

Temperature Range	Reference
298-1371	Coughlin and King <sup>370</sup>
423-1273	Redmond and Lones 371
363-1223	Scott <sup>336</sup>
294-1074	Jaeger and Veenstra <sup>372</sup>

The values chosen by Kelley were accepted herein, including his estimated value of  $C_p^\circ$  = 8.000 cal/gfw for the liquid.

### c) Monatomic gas table

The ideal monatomic gas thermodynamic functions of zirconium in Table LIII were calculated from the energy levels listed by Moore  $^{52}$  with the computer program described in section III-D Uncertainty estimates are summarized on the back of the table. H  $^{\circ}_{298}$  - H  $^{\circ}_{0}$  was found to be 1,629 cal/mole for the ideal gas.

<sup>3&</sup>quot;0Coughlin, J.P. and E.G. King, J. Am. Chem. Soc. 72, 2262 (1950).

<sup>371</sup> Redmond, R.F. and J. Lones, AEC, ORNL-1342 (1952).

<sup>&</sup>lt;sup>372</sup>Jaeger, F.M. and W.A. Veenstra, Rec. trav. chim. <u>53</u>, 917 (1934).

#### B. COMPOUNDS

# 1. Beryllium Oxide (BeO)

#### a. Crystal Structure and Melting Point

Beryllium oxide has a hexagonal (wurtzite-type) structure at room temperature. <sup>231</sup> Jeffrey, Parry, and Mozzi<sup>373</sup> determined some of the structural details by X-ray analysis. The hexagonal structure appears to be thermally stable. Klein<sup>374</sup> found the thermal expansion of BeO to be isotropic up to at least 2025°K. The heat content measurements of Kandyba et al<sup>375</sup> from 1200°K to the melting point gave no indication of any solid-state transformation.

Recent reported values for the melting point of BeO have ranged from 2723° to 2843°K.  $^{375-380}$  A melting point of 2820°  $\pm$  15°K $^{375}$  was selected for this compilation.

#### b. Thermodynamic Properties of Condensed Phases

## 1) Heat of fusion

Kandyba et al<sup>375</sup> made heat content measurements on solid and liquid BeO. From one heat content measurement on liquid BeO at 2840 °K, the heat of fusion was calculated to be 15.440 Kcal/gfw. An uncertainty of  $\pm$  0.500 Kcal/gfw was assigned. The entropy of fusion was thus  $5.475 \pm .180 \text{ cal/}^{O}\text{K}$  gfw. The heat of fusion had been estimated to be 14 Kcal/gfw in the JANAF compilation,  $^{75}$  and to be 17 Kcal/gfw (from an estimated entropy of fusion of 6.0 cal/° K gfw) by Erway and Seifert.  $^{381}$ 

<sup>373</sup> Jeffrey, G., G. Parry, and R. Mozzi, J. Chem. Phys. 25, 1024 (1956).

<sup>374</sup>Klein, D., North American Aviation Co. Rept. NAA-SR-2542 (1958).

<sup>375</sup> Kandyba, V.V., P.B. Kantor, R.M. Krasovitskaya, and E.N. Fomichev, Doklady Akad. Nauk SSSR 131, 566 (1960).

<sup>376</sup>Ol'shanskii, Y., Doklady Akad. Nauk SSSR 59, 1105 (1948).

<sup>377</sup> Wartenberg, H. von and H. Werth, Z. anorg, u. allgem. Chem. 190, 178 (1930).

<sup>&</sup>lt;sup>378</sup>Engberg, C. and E. Zehms, J. Am. Ceram. Soc. 42, 300 (1959).

<sup>379</sup> Wartenberg, H. von and H.J. Reusch, Z. anorg. Chem. 207, 1 (1932).

<sup>380</sup> Wartenberg, H. von, H.J. Reusch, and E. Saran, Z. anorg. Chem 230, 267 (1937).

<sup>381</sup> Erway, N.D. aud R.L. Seifert, J. Electrochem. Soc. 98, 83 (1957).

## 2) Entropy and heat content at 298.15°K

Low-temperature heat capacity measurements of BeO made by Gunther  $^{143}$  (76° to 85°K) and by Kelley  $^{382}$  (55° to 292°K) were not in agreement. Kelley  $^{139}$  gave  $\rm S_{298}^{\circ}$  as 3.37  $\pm$  0.02 cal/°K gfw from his measurements. The National Bureau of Standards  $^{78}$  joined the low-temperature data of Kelley  $^{382}$  smoothly at 400°K with the unpublished high-temperature heat content measurements of Victor and Douglas and calculated  $\rm S_{298}^{\circ}$  to be 3.376  $\pm$  0.050 cal/°K gfw. This value was adopted here. Cp at 298.15°K was thereby changed from 6.07 cal/°K gfw as given by Kelley  $^{139}$  to 6.105 cal/°K gfw.  $\rm H_{298}^{\circ}$ -Ho was taken as 686.6 cal/gfw from the National Bureau of Standards.78

## 3) High-temperature heat content

High-temperature heat content measurements on BeO have been made by Magnus and Danz<sup>358</sup> (293° to 1175°K), Nilson and Pettersson<sup>383</sup> (273° to 293°K), Victor and Douglas<sup>78</sup> (273° to 1200°K), and Kandyba et al<sup>375</sup> (1200° to 2840°K). The results of Magnus and Danz<sup>358</sup> were 0 to 1.5 percent higher than those of Victor and Douglas<sup>78</sup> over the temperature range of measurement. At 1200°K, Magnus and Danz<sup>358</sup> and Kandyba et al<sup>375</sup> were one percent higher and lower, respectively, than Victor and Douglas.<sup>78</sup> Equations representing heat content data from these three sources were:

- a) Magnus and Danz<sup>358</sup> (298° to 1200°K in cal/gfw)  $H_{\rm T}^{\circ} H_{298}^{\circ} = 8.45 \, \text{T} + 2.00 \times 10^{-3} \, \text{T}^2 + 3.17 \times 10^5 \, \text{T}^{-1} 3700 \, . \quad (164)$
- b) Victor and Douglas  $^{78}$  (298° to 1200°K in cal/gfw)  $H_{T}^{\circ} H_{298}^{\circ} = 14.088T + 4.878 \times 10^{-5} T^{2}$   $5548.7 \log T + 9522.88 . \tag{165}$

A small correction term, negligible above 500°K, is omitted.

<sup>382</sup> Kelley, K.K., J. Am. Chem. Soc. 61, 1217 (1939).

<sup>383</sup> Nilson, L.F. and O. Pettersson, Ber. Chem. Gesell. 13, 1459 (1880).

c) Kandyba et al<sup>375</sup> (1200° to 2820°K in cal/gfw) 
$$H_T^o - H_{298}^o = 9.471 T + 1.045 \times 10^{-3} T^2 - 3540.$$
 (166)

For the present compilation, the extrapolated heat capacity data of Victor and Douglas 78 were joined at 1500°K with the heat capacity data of Kandyba et al. 375 The result of this procedure was a heat content at 2800°K,3.5 percent greater than that tabulated by the National Bureau of Standards 78 from an extrapolation of the data of Victor and Douglas. 78

The uncertainty assigned to the heat content was one percent up to 1500°K, and was increased to two percent at the melting point.

The heat capacity of liquid BeO was assumed to be 17 cal/°K gfw. Thermodynamic functions of the condensed phases of BeO are given in Table LIV. Analyses of heat-of-formation data had not been completed at the time of report writing.

## c. Thermodynamic Properties of Ideal Molecular Gas

The thermodynamic functions of BeO gas were calculated with the computer program based on the treatment of the diatomic molecule outlined in section III-E of this report. The spectroscopic constants used we those given by Herzberg. <sup>54</sup> All the electronic states listed in that reference were included in the calculation. The constants were converted to those for a naturally occurring isotopic mixture by the procedure discussed in section IV-Al2 from data for the isotopic masses and abundances from the same sources. Values of De for some of the states were estimated from Dunham's <sup>53</sup> equations. The constants (in units of cm<sup>-1</sup>) used were as follows:

Constant	$x^1\Sigma^+$	л¹П	Β1Σ+	$C(^{1}\Sigma)$	D <sup>1</sup> II
E	0	9234.93	211196.7	38917.9	41130
ω <sub>e</sub>	1487. 256	1144.187	1370.755	1081.4	1016
ω <sub>e</sub> x <sub>e</sub>	11.8286	8.4137	7.7448	9.1	10
ω <sub>e</sub> y <sub>e</sub>	0.02335	0.03389	-0.00027	0	0
B <sub>e</sub>	1.6509	1.3660	1.5757	1.308	()
ac	0.0190	0.01628	0.0154	0.01	0
$D_e(x10^6)$	8 198	7.78	8.3	7 6	0
),	0	0	0		0
g	1	2	ì		,

(w = 25.01			m.p. = 28	4 1/4			
T, °K	C <sub>p</sub> *	cal/°K gfw S <sub>T</sub>	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>296</sub>	- Keal/ ΔH°	ΔF,	Log K
				1112	,	u.,	
0	0.000	0.000	Infinite	-0.687			Infinit
298.15	6.105	3.376	3.376	0.000			
300	6.148	3.414	3.376	0.011			
400	8.083	5.467	3.643	0.730 1.604			
500	9.310	7.412	4. 204	1.004			
600	10.128	9.186	4.889	2.578			
700	10.714	10.793	5.619	3.622			
800	11.154	12.254	6.359	4.716			
900	11.498	13.588	7.089	5.849			
000	11.776	14.815	7.801	7.014			
100	13.005	15 049	8.491	8.203			
100	12.005	15.948	9.157	9.413			
200	12.197	17.001		10.641			
300 400	12.361 12.503	17.984 18.905	9.798 10.416	11.885			
500	12.628	19.772	11.011	13.142			
556	12.723	20.235	11.333	13.851			
556	12.723	20. 235	11.333	13.851			
600	12.815	20.592	11.584	14,412			
700	13.024	21.375	12.137	15.704			
800	13. 233	22.125	12.671	17.017			
900	13.442	22.846	13.188	18.351			
000	13.651	23.541	13.688	19.706			
100	13.860	24. 212	14.174	21.081			
200	14.069	24.862	14.645	22.478			
300	14. 278	25.492	15.103	23.895			
400	14.487	26.104	15.549	25.333			
500	14.696	26.699	15.982	26.792			
	14.006	37 300	17 404	28.272			
600	14.905	27. 280	16.406				
700	15.114	27.846	16.819	29.774			
75 <b>4</b> 754	15. 227	28.146	17.037	30.593 30.593			
754	15. 227	28.146	17.037				
800 820	15.323	28.400	17.223	31.295			
820	_ 15.365	28.509	17.303	- 31.602 47.042			
820	17.000	33.984	17.303				
900	17.000 17.000	34.459 35.036	17.769 18.335	48.402 50.102			
100	17.000	35.593	18.883	51.802			
200	17.000	36.133	19.414	53.502			
300	17.000	36.656	19.928	55.202			
400	17.000	37.164	20.428	56.90Z			
500	17.000	37.656	20.913	58.602			
600	17.000	38.135	21.384	60.302			
700	17.000	38.601	21.844	62.002			
800	17.000	39.054	22.290	63.702			
900	17.000	39.496	22.726	65.402			
000	17.000	39.926	23.150	67.102			
100	17.000	40 146	21 645	68 803			
100 200	17.000	40.346	23.565 23.970	68.802 70.502			
			,,,,				
						•	

BERYLLIUM OXIDE CONDENSED PHASES
SUMMARY OF UNCERTAINTY ESTIMATES

,		ıl∕°K gfə ──			Kcal/gfv		$\overline{}$
T,°€	c,	$s_{T}^{\bullet}$	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH °	ΔF	Log Kp
298.15	± .100	± -050	± .050	± .000			
1000	± .300	± .150	± .080	± .070			
2000	± .700	± .290	± .150	± .270			
2820	±1.580	± .444	± .220	± .630			
2820	±1.000	± .620	± .220	±1.130			
4000	± 2.000	±1.140	± .420	±2.900			

 $H_{298}^{\circ}$  -  $H_{0}^{\circ}$  was calculated to be 2076.6 cal/gfw.

The results of all the calculations are given in Table LV. The National Bureau of Standards 78 has reported thermodynamic functions of gaseous BeO calculated from spectroscopic constants for the ground state alone.

No attempt has been made to give uncertainties for the above calculations at this time. The real uncertainty results from the effect of neglecting triplet states, which doubtless exist, but which have not been reported. Because BeO is isoelectronic with  $C_2$ , a similar sequence of states might be expected in the two gaseous molecules. Among other states,  $C_2$  has a  ${}^1\Sigma^+_g$  ground state, a  ${}^3\Pi_u$  state only 610 cm<sup>-1</sup> above the ground state, and a  ${}^3\Sigma^-_g$  state 6243.5 cm<sup>-1</sup> above the ground state.  ${}^{162}$  It is intended that additional calculations for gaseous BeO will be made after reasonable estimates of additional states are obtained.

The analysis of the heat-of-formation data had not been completed at time of report writing, and  $\Delta H_f^{\circ}$ ,  $\Delta F_f^{\circ}$  and  $\log_{10} K_p$  could not be included.

gfw = 25.013

0 298.15 300 400 500 600 700 800	CP 0.000 7.046 7.049	5T 0.000	$-(F_{T}^{o}-H_{290}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>o</sup> <sub>f</sub>	$\Delta F_{I}$	Log K
298.15 300 400 500 600 700	0.000 7.046	0.000					
298.15 300 400 500 600 700	7.046		Infinite	-2.077			Infini
300 400 500 600 700		47.209	47.209	0.000			
400 500 600 700		47 - 252	47.209	0.013			
500 600 700	7.254	49.306	47.488	0.727			
700	7.510	50.952	48.021	1.465			
700							
	7.757	52.344	48.628	2. 229			
800	7.970	53.556	49. 248	3.016			
	8.146	54.632	49.855	3.822			
900	8.289	55.600	50.440	4.644		•	
000	8.406	56.480	51.001	5.479			
				7			
100	8.504	57.285	51.536	6.324			
200	8.588	58.029	52.046	7.179			
30u	8.665	58.720	52. 534	8.042			
400 500	8.737 8.810	59.364 59.970	52.999 53.443	8.912 9.789			
300	0.010	37.770	33.443	7.107			
556	8.852	60.290	53.681	10.284			
556	8.852	60.290	53.681	10.284			
500	8.885	60.541	53.869	10.674			
700	8.966	61.082	54. 278	11.567			
800	9.052	61.597	54.670	12.467			
900	9.146	62.088	55.048	13.377			
000	9.246	62.560	55.412	14.297			
	0.355			10.00			
100	9.353	63.014	55.763	15.227			
200	9.465	63.451	56.103	16. 167			
100 100	9.582	63.875	56.431	17.120			
	9.703	64. 285	56.750 57.060	18.084 19.061			
500	9.827	64.684	51.000	19.001			
000	9.951	65.072	57.360	20.049			
00	10.076	65.450	57.653	21.051			
154	10.142	65.649	57.807	21.598			
54	10.142	65.649	57.807	21.598			
300	10.199	65.818	57.938	22.065			
20	10.223	65.890	57.994	22. 270			
320	10.223	65.890	57.994	22.270			
900	10.320	66.179	58.216	23.091			
000	10.437	66.530	58.488	24.128			
100	10.551	66.875	58.753	25.178			
200	10.659	67.212	59, 012	26. 239			
100	10.763	67.541	59. 266	27.310			
100	10.861	67.864	59. 514	28.391			
00	10.953	68.181	59.757	29.482			
			,				
00	11.038	68.491	59.996	30.582			
00	11.118	68.794	60. 229	31.690			
00	11.191	69.092	60.459	32.806			
00	11.258	69.384	60.684	33.929			
00	11.319	69.670	60.906	35.058			
00	11.374	69.950	61.123	36. 193			
	11.423	70.226	61. 337	37.333			
	11. 467	70.495	61.547	38.478			
	11.506	70.760	61.754	39.628			
	11.540	71.019	61.957	40.780			
		·					
	11.570	71.274	62.157	41.937			
	11.595	71.523	62.354	43.096			
	11.617	71.768	62.548	44.257			
	11.635	72.008	62.739	45.421			
00	11.649	72.244	62.927	46.586			
00	11.661	72.476	63.113	47.752			
00	11.669	72.703	63.295	48.920			
00	11.676	72.926	63.475	50.088			
	11.680	73.145	63.653	51.257			
00	11.682	73.360	63.828	52.427			
20	11 40.	21. (21.	44.001	63 602			
	11.682	73.572	64.001	53. 597			
	11.681	73.779	64.171	54.766			
	11.678	73.983	64. 339	55.936			
	11.674 11.670	74.184	64.505	57.105 58.274			
		74.381	64.669	58.274			

## 2. Calcium Oxide (CaO)

### a. Crystal Structure and Melting Point

Calcium oxide has a face-centered cubic (NaCl type) structure at room temperature<sup>57</sup> which presumably persists up to the melting point. Beals and Cook<sup>384</sup> measured the lattice parameters up to 1500°K by X-ray methods.

Ol'shanskii  $^{376}$  gave the melting point of CaO as 2893°K. Schumacher  $^{385}$  reported it to be 2849°K, and Kanolt  $^{386}$  gave a value of 2843°K. The average for these values of 2860°  $\pm$  30°K was adopted here.

## b. Thermodynamic Properties of the Condensed Phases

### 1) Heat of fusion

The entropy of fusion of CaO was assumed to be 6.0  $\pm$  0.5 cal/°K gfw, which corresponded to a heat of fusion of 17.2  $\pm$  1.4 Kcal/°K gfw. Kubaschewski and Evans <sup>182</sup> estimated the latter quantity to be 19 Kcal/gfw. Kelley <sup>137</sup> used a heat-of-fusion value of 12.24 Kcal/°K gfw from melting points in the CaO-ZrO<sub>2</sub> system.

## 2) Entropy and heat content at 298.15°K

The low-temperature heat capacity of CaO was measured by Nernst and Schwers  $^{233}$  (28° to 90°K) and by Parks and Kelley  $^{387}$  (87° to 293°K). From these data,  $S^{\circ}_{298}$  was calculated to be 9.561  $\pm$  0.15 cal/°K gfw, and  $H^{\circ}_{298}$  - $H^{\circ}_{0}$  was calculated to be 1668 cal/gfw.

### 3) High-temperature heat content

The heat content equation given by Kelley<sup>56</sup> in cal/gfw for use up to 2000°K was adopted here and extrapolated to the melting point.

$$H_{T}^{e} - H_{298}^{e} = 11.67T + 0.54 \times 10^{-3}T^{2} + 1.56 \times 10^{5}T^{-1} - 4051$$
 . (167)

<sup>384</sup> Beals, R. and R. Cook, J. Am. Ceram. Soc. 40, 279 (1957).

<sup>385</sup> Schumacher, Z. E., J. Am. Chem. Soc. 48, 396 (1926).

<sup>386</sup> Kanolt, L., J. Vash. Acad. Sci. 3, 315 (1931).

<sup>387</sup> Parks, G. S. and K. K. Kelley, J. Phys. Chem. 30, 47 (1926).

The uncertainty assigned to the heat content up to 1000°K was 1 percent and this was increased to 2 percent at the melting point. Kelley's <sup>56</sup> equation was based primarily on the data of Lander <sup>388</sup> (298° to 1177°K).

The heat capacity of liquid CaO was assumed to be 16.5 cal/°K gfw. The calculated thermodynamic functions for the condensed phases of CaO are given in Table LVI. The analysis of the heat-of-formation data in the literature was not completed at the time of report writing. Uncertainty estimates are summarized on the back of the Table.

#### c. Thermodynamic Properties of the Gaseous Phase

The thermodynamic functions of gaseous, molecular calcium oxide were calculated with the computer program based on the treatment of the diatomic molecule outlined in section III-E of this report. The spectroscopic constants used (in units of cm<sup>-1</sup>) were taken from Hultin and Lagerquist, <sup>389</sup> and Lagerquist. <sup>390</sup>

Constant	χ'¹Σ	Α'1Σ	в -1П	C '1Σ
E	0	11584.84	25913.0	28772.4
ω <sub>e</sub>	732.11	716.0	580.0	560.9
ω <sub>e</sub> x <sub>e</sub>	4.81	1.60	2. 80	4.0
ω <sub>e</sub> y <sub>e</sub>		<b></b> -		
B <sub>e</sub>	0.44447	0.4063	0.3882	0.3731
a <sub>e</sub>	0.00335	0.00141	0.0055	0.0032
γ <sub>e</sub>	# T F			
D <sub>e</sub> (× 10 <sup>6</sup> )	0.656	0.54	0.70	0.70
8	1	1	2	1

No corrections were made for the naturally occurring isotopic mixture.

<sup>388</sup> Lander, J. J., J. Am. Chem. Soc. 73, 5794 (1951).

<sup>389</sup> Hultin, M. and A. Lagerqvist, Ark. Fys. 2, 471 (1950).

<sup>390</sup> Lagerqvist, A., Ark. Fys. 8, 83 (1954).

	cal/oK gre			m.p. = 2860° ± 30°K		Kcai/gfu		
T, *K	c <sub>p</sub>	S <sub>T</sub>	-(FT -H298)/T	H <sub>T</sub> H <sub>298</sub>	∆H °	$\Delta F_f$	Log K	
0	0.000	0.000	Infinite	-1.668			Infin	
298.15	10.230	9.561	9.561	0.000			*****	
300	10.254	9.624	9.561	0.019				
400	11.120	12.708	9.976	1.093				
500	11.579	15.243	10.783	2. 230				
600	11.878	17.382	11.709	3.404				
700	12.101	19.231	12.655	4.603				
737	12.172	19.856	13.001	5.052				
737	12.172	19.856	13.001	5.052				
800	12.283	20.859	13.581	5.827				
900	12.442	22.315	14.472	7.059				
1000	12.587	23.634	15.324	8.310				
1100	12.722	24.840	16. 135	9.576				
1123	12.752	25. 103	16.315	9.869				
1123	12.752	25.103	16.315	9.869				
1200	12.851	25.952	16.906	10.855				
1300	12.975	26.986	17.643	12.146				
1400	13.095	27.952	18.345	13.450				
1500	13.214	28.859	19.016	14.765				
600	13.330	29.716	19.658	16.092				
700	13.445	30.527	20. 273	17.431				
765	13.519	31.033	20.661	18.307				
765	13.519	31.033	20.661	18.307				
800	13.559	31.299	20.865	18.781				
900	13.672	32.035	21.433	20.143				
000	13.784	32,739	21,981	21.516				
100	12 00/	33.414	22 500	22 000				
100	13.896		22.509	22.900				
200	14.007	34.063	23.020	24. 295				
300	14.117	34.688	23.514	25.701				
400	14.228	35.292	23.993	27.118				
500	14.338	35.875	24. 457	28.546				
600	14.448	36.439	24. 906	29.986				
700	14. 365	36.986	25, 343	31.436				
800	14.667	37.518	25. 769	32.897				
860	_ 14.733	37.830	26.019	33.779				
860	16.500	- 43.844	26.019	50.979				
900	16.500	44.073	26. 266	51.639				
000	16.500	44.632	26.869	53. 289				
•••			20.00,	55. 20 /				
100	16.500	45.173	27.451	54.939				
200	16.500	45.697	28.013	56.589				
300	16.500	46.205	28.557	58.239				
400	16.500	46.698	29.084	59.889				
500	16.500	47.176	29.593	61.539				
600	16.500	47.640	30.088	63.189				
70¢	16.500	48.093	30.569	64.839				
900	16.500	48.533	31.036	66.489				
900	16.500	48.961	31.489	68,139				
000	16.500	49.379	31.932	69.789				
	Ama-3							

#### CALCIUM OXIDE CONDENSED PHASES

#### SUMMARY OF UNCERTAINTY ESTIMATES

	a	L/°K gtv			Kcal/glv		
T, °K	c <b>\$</b>	s <sub>T</sub>	$-(P_{\rm T}^{\bullet}-H_{290}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	AH f	ΔF į	Log K
298.15	± .200	± .150	± .150	± .000			
1000	± .430	± .290	± .210	± .080			
2000	± .930	± .460	± .300	± .330			
2860	±1.740	± .610	± .370	± .680			
860	±1.000	±1.100	± .370	± 2.080			
4000	± 2.000	±1.600	± .650	±3.790			

The thermodynamic functions of molecular CaO (gas) calculated with the above spectroscopic constants are given in Table LVII. It is not certain  $^{391-393}$  that the ground state of CaO (g) is a singlet state. Therefore, uncertainties have not been determined for the present calculation pending further analysis of the effect of assuming other possible energy level schemes. Thermodynamic functions based on the assumption of the singlet ground state were also given by Kelley,  $^{56}$  and Veits and Gurvich.  $^{394}$  H $^{2}_{298}$  - H $^{8}_{0}$  was found to be 2,140 cal/mole.

The review of data for the heat of formation of CaO(g) was not completed at the time of report writing, and  $\Delta H_f^\circ$ ,  $\Delta F_f^\circ$ , and  $\log_{10} K_p$  could not be included.

 $<sup>^{391}</sup>$ Brewer, L. and R. F. Porter, J. Chem. Phys.  $\underline{22}$ , 1867 (1954).

<sup>392</sup> Lagerqvist, A. and L. Huldt, Ark. Fys. 8, 427 (1954).

<sup>&</sup>lt;sup>393</sup>Huldt, L. and A. Lagerqvist, Ark. Fys. <u>9</u>, 227 (1955).

<sup>394</sup> Veite, I. and L. Gurvich, Zhur. Fiz. Khim. 32, 2532 (1958).

g(w = 56.08

	- ca	I/°K gfw			Kcal/gfv		$\overline{}$
T, °K	c <sub>p</sub>	ST	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>296</sub>	AH °	ΔF	Log I
0	0.000	0.000	Infinite	-2.140			Infini
298.15	7.758	52.489	52.489	0.000			21111111
300	7.766	52.537	52.489	0.014			
400	8.148	54.827	52.799	0.811			
500	8.399	56.674	53.395	1.640			
600	8.565	58.221	54.074	2. 488			
700	8.679	59.551	54.764	3.351			
737	8.712	59.998	55.013	3.674			
737	8.712	59.998	55.013	3.674			
800	8.762	60.715	55.437	4. 223			
900	8.825 8.874	61.75l 62.684	56.082 56.696	5.103 5.988			
	0.01.	02.00.	30.070	3. 700			
100	8.914	63.531	57.280	6.877			
123	8.922	63.713	57.407	7.082			
200	8.922	63.713	57.407	7.082			
300	8.948 8.978	64.309 65.026	57.833 58.359	7.770 8.666			
400	9.005	65.692	58.860	9.566			
500	9.030	66.315	59. 336	10.467			
600	9.055	66.898	59.791	11.372			
700 765	9.079 9.096	67.448 67.787	60. 226 60. 496	12.278 12.869			
765	9.096	67.787	60.496	12.869			
800	9.105	67.968	60.642	13.187			
900	9.131	68.461	61.040	14.099			
000	9.159	68,930	61.423	15.014			
100	9. 189	69.378	61.792	15.931			
200	9. 220	69.807	62.147	16.851			
300	9. 254	70.217	62.489	17.775			
400	9. 289	70.612	62.820	18.702			
500	9.326	70.993	63.139	19.633			
400	0.265	71 260	42.440	20 547			
700	9.365 9.406	71.360 71.714	63.449 63.749	20.567 21.506			
800	9.449	72.058	64.040	22.449			
860	9.475	72.258	64. 210	23.017			
860	9.475	72.258	64. 210	23.017			
900	9.492	72.391	64.323	23.396			
000	9.537	72.714	64.598	24. 347			
100	9.583	73.028	64.866	25.303			
200	9.630	73.334	65.126	26. 264			
300	9.678	73.631	65.380	27.229			
400	9.726	73.922	65.628	28.199			
500	9.775	74.205	65.870	29.174			
600	9.825	74.482	66.106	30.154			
700	9.874	74.753	66. 337	31.139			
800	9.925	75.018	66.563	32.129			
1900	9.976	75.278	66.785	33.123			
000	10.027	75.532	67-001	34.123			
100					•		
200	10.078	75.782 76.026	67.214 67.422	35.128 36.138			
300	10.130	76.267	67.626	37.154			
400	10.235	76.503	67.827	38.174			
500	10.289	76.735	68.024	39. 200			
600	10 147	7/ 0/-	10.010	40 333			
600 700	10.343 10.397	76.963 77 188	68.218	40.231			
800	10.397	77.188 77.409	68.408 68.595	41.268 42.309			
960	10.507	77.627	68.779	43.357			
000	10.564	77.842	68.960	44.410			
100	10 ( )0	70 62		45.446			
100 200	10.620	78.054 78.263	69.138 69.314	45.468 46.532			
300	10.736	78.469	69.487	47.602			
400	10.795	78.672	69.658	48.678			
500	10.854	78.873	69.826	49.760			
600	10.915	70 071	60.00	50 040			
700	10.915	79.072 79.268	69.992 70.156	50.848 51.941			
800	11.037	79.462	70. 156	53.041			
900	11.100	79.654	70.477	54.147			
000	11.163	79.844	70.634	55. 260			

## 3. Chromium Oxides

The compilation of thermodynamic data for both condensed and gaseous phases of the chromium oxides was in progress at the time of report writing. The thermodynamic functions for gaseous chromium dioxide (CrO<sub>2</sub>) and gaseous chromium trioxide (CrO<sub>3</sub>) were included in this report; the remainder will be reported later.

## a. Chromium Dioxide (CrO2)

No experimental spectroscopic data had been reported for gaseous chromium dioxide. All of the molecular constants required in the calculation of the thermodynamic functions of  $\text{CrO}_2$  were therefore estimated. The thermodynamic functions for gaseous  $\text{CrO}_2$  given in Table LVIII were calculated by means of the computer program described in section III-F with the following molecular data:

## Molecular configuration

Symmetric nonlinear molecule with

$$\angle O - Cr - O = 107 \text{ deg.}$$

Product of moments of inertia

$$I_A I_B I_C = 340637 \times 10^{-120} g^3 cm^6$$

Symmetry number

 $\theta = 2$  .

## Fundamental frequencies

$$\omega_1 = 870 \text{ cm}^{-1}$$

$$\omega_2 = 388 \text{ cm}^{-1}$$

$$\omega_3 = 926 \text{ cm}^{-1}$$

## Ground electronic state

 $^{1}\Sigma$  .

gfw = 84.01

	cal/°K gfv				Kcal/gf		$\overline{}$
T, *K	C <sub>p</sub>	s <sup>e</sup> T	-(F <sub>T</sub> - H <sub>298</sub> )/T	н <mark>т</mark> – н <sub>298</sub>	ΔH°	ΔF	Log E
0	0.000	0.000	Infinite	-2.640			Infini
298.15	10.453	61.856	61.856	0.000			1111111
300	10.473	61.921	61.856	0.019			
600	11.422	65.071	62.279	1.117			
500	12.085	67.696	63.107	2.294			
500	12.537	69.942	64.064	2 627			
700	12.849	71.899	65.046	3.527			
300	13.070	73.630	66.013	4.797			
900	13.070	75.179	66.947	6.093 7.409			
000	13.350	76.580	67.842	8.738			
100 200	13.441 13.512	77.857 79.029	68.695 69.508	10.07B 11.426			
300	13.569	80.113	70.282	12.780			
100	13.614	81.120	71.021	14:139			
500	13.651	82.061	71.726	15.502			
	12 (0)	03.043	73.400	1/ 0/0			
500	13.681	82.943	72.400	16.869			
700	13.707	83.773	73.045	18. 239			
300	13.728	84.557	73.663	19.610			
900 000	13.747 13.762	85.300 86.006	74. 256 74. 826	20.984 22.360			
00	13.776	66.677	75.374	23.737			
200	13.788	87.319	75.903	25.115			
100	13.798	87.932	76. 413	26.494			
100 300	13.807 13.815	88.519 89.083	76.905 77.381	27 - 874 29 - 256			
,,,,		07.003	111,301	27.230			
000	13.822	89.625	77.841	30.637			
00	13.829	90.147	78.288	32.020			
300	13,834	90.650	78.720	33.403			
000	13.840	91.135	79.140	34.787			
100	13,844	91.605	79.548	36.171			
00	13.848	92.059	79.944	37.556			
200	13.852	92.498	80.329	38.941			
300	13.856	92.925	80.705	40.326			
100	13.859	93.338	81.070	41.712			
500	13.862	93.740	81.426	43.098			
500	13.864	94.131	81.774	44.484			
00	13.867	94.511	82.113	45.871			
100	13.869	94.880	82.444	47.258			
000	13.871	95: 241	82.768	48.645			
100	13.873	95.592	83.084	50.032			
100	13.875	95.934	83.393	51,419			
.00	13.877	96.269	83.696	52.807			
00	13.878	96.595	83.992	54.195			
100	13.880	96.914	84.282	55.582			
00	13.881	97.226	84.566	56.970			
00	13.882	97.532	84.845	58.359			
00	13.884	97.830	85.118	59.747			
00	13.885	98.122	85.386	61.135			
00	13.886	98.409	85.649	62.524			
00	13.867	98.689	85.907	63.912			
00	13.888	98.964	86.160	65.301			
00	13.889	99.234	86.409	66.690			
00	13.889	99.498	. 86 . 653	68.079			
00	13.890	99.758	86.894	69.468			
00	13.891	100.013	87.130	70.857			
00	13.892	100.263	87.362	72.246			
00	13.892	100.509	87.591	73.635			
00	13.893	100.751	87.816	75.024			
00	13.893	100.988	88.037	76.414			
00	13.894	101.222	88.255	77.803			

## l) Molecular configuration

The molecular configuration of CrO2 was unknown. Consideration of the periodic group to which chromium belongs and the work of Walsh<sup>395</sup> on bonding and structural relations led to the conclusion that CrO2 was a symmetric, nonlinear molecule. Therefore, it was so considered in the present work. In the absence of experimental evidence, it is to be expected that some other workers would accept the alternative conclusion that it is linear symmetric. For example, the free-energy function of CrO, at several selected temperatures was recently calculated by Grimley, Burns, and Inghram<sup>396</sup> on the assumption of Chandrasekharaiah and Brewer<sup>397</sup> that the Group IV, V, and VI transition metal dioxides all form linear symmetric molecules. Ano-Ct-0 angle of 107 degrees was chosen in the present work as representing a reasonable value in comparison to known compounds of similar bonding. The Cr - O bond distance was assumed to be identical with the known corresponding distance for the chromium monoxide (CrO) molecule; i. e., 1.627Å.  $^{398}\,$ 

### 2) Moments of inertia

The moments of inertia of  $\text{CrO}_2$  were calculated from the above bond angles and bond distances by means of equations <sup>399</sup> (168), (169), (170), and (171).

$$I_{x} = \left(\frac{2M_{o}M_{Cr}}{2M_{o} + M_{Cr}}\right) r_{o}^{2} \cos^{2}\left(\frac{\zeta}{2}\right)$$
 (168)

$$I_y = 2M_0 r_0^2 \sin^2\left(\frac{\zeta}{2}\right) \tag{169}$$

$$I_z = I_x + I_y \tag{170}$$

$$I_{A}I_{B}I_{C} = I_{x}I_{y}I_{z} , \qquad (171)$$

<sup>395</sup> Walsh, A. D., J. Chem. Soc. 2266 (1953).

<sup>396</sup>Grimley, R. T., R. P. Burns and N. G. Inghram, J. Chem. Phys. 34, 664 (1961).

<sup>397</sup> Chandrasekharaiah, M. S. and L. Brewer, U.S. AEC Rept UCRL-8736 (April 1959).

<sup>398</sup> Ninomiya, M., J. Phys. Soc. (Japan) 10, 829 (1955).

<sup>399</sup> Moelwyn-Hughes, E. A., Physical Chemistry, Pergamon Press, London (1957).

Mo = mass of oxygen atom

M<sub>Cr</sub> = mass of chromium atom

 $r_0 = Cr - 0$  bond distance and

 $\zeta = 0 - Cr - 0$  bond angle.

## 3) Fundamental frequencies

The estimation of the fundamental frequencies of  $\text{CrO}_2$  was based on the following three assumptions:

- a) The fundamental vibrations may be described by a valence force-field method.  $^{400}$
- b) The stretching force constant  $(k_1)$  for  $\text{CrO}_2$  is the same as that for CrO. This assumption has been employed by previous workers. The stretching force constant for CrO was calculated from experimental spectroscopic data  $^{398}$ ,  $^{401}$  by means of equation (172).

$$k_1 = 4\pi^2 c^2 \mu \omega^2 \quad , \tag{172}$$

where

 $k_1$  = stretching force constant

c = velocity of light

 $\mu$  = reduced mass of CrO molecule

and

 $\omega$  = vibrational frequency.

c) The ratio of the bond-bending and bond-stretching force constants is 0.0940, the average of those observed for several nonlinear molecules.  $^{400}$ 

$$k_8/k_1 k^2 = 0.0940.$$
 (173)

<sup>400</sup> Herzberg, G., Molecular Spectra and Molecular Structure, II. Infrared and Raman Spectra of Polyatomic Molecules, Van Nostrand, N.Y. (1945).

<sup>401</sup> Brewer, L. and M. S. Chandrasekharaiah, U.S. AEC Rept. UCRL-8717 Rev. (June 1960).

The values of the fundamental frequencies  $(\omega_1, \omega_2, \text{ and } \omega_3)$  were therefore calculated from equations (174), (175), and (176).

$$\omega_3^2 = \frac{\left[1 + \frac{2M_o}{M_{Cr}} \sin^2 \alpha\right] \frac{k_1}{M_o}}{0.3548 \times 10^{23}}$$
 (174)

$$\omega_1^2 + \omega_2^2 = \frac{\left[1 + \frac{2M_o}{M_{Cr}}\cos^2\alpha\right] \frac{k_1}{M_o} + \frac{2}{M_o} \left[1 + \frac{2M_o}{M_{Cr}}\sin^2\alpha\right] \frac{k_b}{k_2}}{0.3548 \times 10^{23}}$$
(175)

$$\omega_1^2 \omega_2^2 = \frac{2\left[1 + \frac{2M_0}{M_{Cr}}\right] \frac{k_1}{M_0^2} \frac{k_\delta}{6^2}}{0.1259 \times 10^{46}},$$
(176)

 $\alpha = \frac{\zeta}{2} \tag{177}$ 

### 4) Electronic states

The electronic states of  $\text{CrO}_2$  were unknown. The general practice, when no data are available, of considering only the ground state and assuming it to be a  $^{1\Sigma}$  state has been followed in this work. This procedure is simpler and is believed to be as correct as that used by other workers  $^{397}$ ,  $^{401}$  who have estimated electronic levels from a crude ionic central atom model.

It should be emphasized that the thermodynamic functions of gaseous  $\text{CrO}_2$  in Table LVIII represent "reasonable" estimates only; the numerical values could be appreciably altered should experimentally determined molecular constants become available for  $\text{CrO}_2$ .  $\text{H}^\circ_{298}$  –  $\text{H}^\circ_0$  was found to be 2,640 cal/mole.

#### b. Chromium Trioxide (CrO<sub>3</sub>)

Experimental spectroscopic data also had not been reported for gaseous chromium trioxide. All of the molecular constants required in the calculation of the thermodynamic functions of CrO<sub>3</sub> were again estimated. The thermodynamic functions for gaseous CrO<sub>3</sub> given in Table LIX were also calculated by means of the machine program described in section III-F with the following molecular data:

Molecular configuration

Planar, symmetrical, cart-wheel molecule with

$$\angle O - Cr - O = 120 \text{ deg.}$$

$$r_0 = 1.627 \text{ A}$$

wfw = 100.01

	cal/°K g/v			\	ΔH <sup>o</sup> <sub>1</sub> ΔF <sup>o</sup> <sub>1</sub>		las F
T, °E	C <sub>p</sub>	ST	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	AH i	ΔF	Log
0	0.000	0.000	Infinite	-3.108			Infin
298.15	13.881	64.500	64.500	0.000			
300	13.916	64.586	64.500	0.026			
400	15.533	68.824	65.067	1.503			
500	16.663	72.419	66.187	3.116			
	*******	,					
500	17.441	75.530	67.491	4.824			
700	17.984	78.262	68.839	6.596			
300	18.371	80.690	70.171	8.415			
900	18.654	82.871	71.463	10. 267			
000	18.867	84.848	72.704	12.144			
,,,,		71.535					
100	19.029	86.654	73.892	14.039			
:00	19.156	88.316	75.025	15.948			
00	19.257	89.853	76.108	17.869			
00	19.338	91.283	77.141	19.799			
00	19-404	92.620	78.129	21.736			
00	19.459	93.874	79.074	23.679			
00	19.505	95.055	79.980	25.628			
00	19.543	96.171	80.849	27.580			
00	19.576	97.229	81.683	29.536			
00	19.605	98.233	82.486	31.495			
0.0	10 (30	00.101	03.350	22 457			
00	19.629	99.191	83.259	33.457			
00	19.650	100.104	84.004	35. 421			
00	19.669	100.978	84.723	37.387			
00	19.685	101.816	85.418	39.355			
00	19.700	102.619	86.090	41.324			
00	10 712	102 202	86.741	43 205			
00	19.713	103.392		43. 295			
00	19.724	104.137	87.371	45.266			
00	19.734	104.854	87.983	47.239			
00	19.744	105.547	88.577	49.213			
00	19.752	106. 216	89.154	51.188			
00	19.760	106.864	89.714	53.164			
00	19.766	107.491	90.260	55.140			
00	19.773	108.100	90.792	57.117			
00	19.779	108.690	91.309	59.094			
00	19.784	109.264	91.814	61.073			
00	19.789	109.821	92.307	63.051			
00	19.793	110.363		65.030			
00	19.797	110.363	92.787	67.010			
00	19.801	111.405	93. 257 93. 716	68.990			
00	19.804	111.907	94. 164	70.970			
			,	,			
00	19.808	112.396	94.603	72.951			
00	19.811	112.873	95.032	74.931			
00	19.814	113.339	95, 453	76.913			
00	19.816	113.795	95.864	78.894			
00	19.819	114.240	96. 268	80.876			
00	19.821	114.676	96.663	82.858			
00	19.823	115.102	97.051	84.840			
00	19.825	115.520	97.431	86.823			
00	19.827	115.928	97.805	88.805			
00	19.829	116.329	98.171	90.788			
			27 .13	C.77			
00	19.831	116.722	98.531	92.771			
0	19.832	117.107	98.885	94.754			
0	19.834	117.484	99.232	96.737			
0	19.835	117.855	99.574	98.721			
10	19.836	118.219	99.909	100.704			
00	19.838	118.577	100-239	102.688			
0	19.839	118.928	100.564	104.672			
0	19.840	119. 273	100.884	106.656			
10	19.841	119.612	101.198	108.640			
0	19.842	119.945	101.508	110.624			
-	177076	1.7.7.7.3	,00				

### Product of moments of inertia

$$I_A I_B I_C = 2346881 \times 10^{-120} g^3 cm^6$$

## Symmetry number

$$\theta = 6$$
.

## Fundamental frequencies

$$\omega_1 = 840 \text{ cm}^{-1}$$

$$\omega_2 = 397 \text{ cm}^{-1}$$

$$\omega_3 = 1023 \text{ cm}^{-1}(2)$$

$$\omega_4 = 347 \, \text{cm}^{-1}(2)$$

## Ground electronic state

 $1_{\Sigma}$ 

### Molecular configuration

The molecular configuration of CrO<sub>3</sub> was unknown. The molecule was assumed to be of the symmetrical, planar, cart-wheel type. The only resonable alternative structure was pyramidal, but the pyramidal structure was considered to be unlikely in view of the known planar structure of other molecules having central atoms in the same periodic group as chromium; e.g., so<sub>3</sub>. The Cr - 0 bond distance was also assumed in this case to be identical with the known distance for the chromium monoxide (CrO) molecule; i.e., 1.627Å. <sup>398</sup>

## 2) Moments of inertia

The moments of inertia of  $CrO_3$  were calculated for the assumed structure by means of equations  $^{399}$  (170), (171), and (178).

$$I_{xx} = I_{y} = \frac{3M_{o}r_{o}^{2}}{2} , \qquad (178)$$

where the symbols are as defined in section IV-B3a above.

### 3) Fundamental frequencies

The estimation of the fundamental frequencies of CrO<sub>3</sub> was based on the following assumptions:

- a) Assumption (a) in paragraph a(3) above for CrO2.
- b) The stretching force constant  $(k_1)$  for  $CrO_3$  may be calculated from an estimated value for the corresponding frequency  $\omega_1$  according to equation (179).

$$k_1 = 0.3548 \times 10^{23} M_0 \omega_1^2$$
 (179)

The value of  $\omega_1$  was estimated on the assumption that the  $\text{CrO}_3$  molecule could be considered approximately a  $\text{CrO}_2$  molecule ( $^2\text{O}-\text{Cr}-\text{O}=120^\circ$ ) with an additional O atom attached. A value of  $\omega_1^\bullet$  corresponding to this pseudo-molecule was then calculated by the procedure described in the preceding section on the  $^{\text{CrO}_2}$  molecule.

The value 847 cm<sup>-1</sup> was thus obtained for  $\omega_1^{\bullet}$ . It was then arbitrarily lowered to take into account the additional mass of the third oxygen atom. The final value for  $\omega_1$  was 840 cm<sup>-1</sup>.

c) The other force constants ( $^k\Delta$  and  $^k\delta$ ) may be evaluated by averaging the ratios of force constants calculated from observed frequencies for several planar, symmetrical, cartwheel molecules.  $^{400}$  These averages for  $^{\text{CrO}_3}$  were

$$k_8/k_1$$
  $k_2 = 0.0440$  , (180)

$$k_{\Lambda}/k_{1}$$
  $\lambda^{2} = 0.1160.$  (181)

The values of the fundamental frequencies were then calculated from equations (182), (183), (184), and (185).

$$\omega_1^2 = \frac{k_1}{0.3548 \times 10^{23} \,\mathrm{M}_0} \tag{182}$$

$$\omega_2^2 = \frac{\left[1 + \frac{3M_o}{M_{Cr}}\right] \left(\frac{1}{M_o}\right) \left(\frac{k_\Delta}{\lambda^2}\right)}{0.3548 \times 10^{23}}$$
(183)

$$\omega_3^2 + \omega_4^2 = \frac{\left[1 + \frac{3M_0}{2N_{Cr}}\right] \left[\frac{k_1}{M_0} + \frac{3k_{\mathcal{E}}}{M_0 R^2}\right]}{0.3548 \times 10^{23}}$$
(184)

$$\omega_3^2 \omega_4^2 = \frac{3\left[1 + \frac{3M_o}{M_{Cr}}\right] \left(\frac{k_1}{M_o}\right) \left(\frac{k_\delta}{2}\right)}{0.1259 \times 10^{46}}$$
(185)

# 4) Electronic states

The electronic states of  $CrO_3$  were unknown. The general practice, when no data are available, of considering only the ground state and assuming it to be a  $^1\Sigma$  state was also followed herein.

It should be emphasized here also that the thermodynamic functions for  $\text{CrO}_3$  in Table LIX represent "reasonable" estimates only, and that the numerical values may be appreciably altered should experimental molecular constants become available for  $\text{CrO}_3$ .  $\text{H}^9_{298}$  -  $\text{H}^9_0$ was found to be 3, 108 cal/mole.

## 4. Magnesium Oxide (MgO)

### a. Crystal Structure and Melting Point

Crystalline magnesium oxide has a face-centered cubic (NaCl type) structure at room temperature, <sup>57</sup> which was assumed to persist up to the melting point. Engberg and Zehms <sup>378</sup> found the coefficient of expansion to be practically constant from 1300°-to 2300°K. The melting point of MgO has been given as 2913°K by Ebert and Cohn from phase studies in the MgO-ZrO<sub>2</sub> system. However, it has been almost universally accepted as 3075°K. This latter value was given by Kanolt, <sup>386</sup> Ruff and Schmidt, <sup>403</sup> and Wartenberg, Reusch, and Saran, <sup>380</sup> and was adopted here. An uncertainty of ± 50°K was assigned to it.

### b. Thermodynamic Properties of Condensed Phases

### 1) Heat of fusion

The heat of fusion of MgO was calculated by Kelley <sup>137</sup> to be 18.5 Kcal/gfwfrommelting-point measurements in the MgO-ZrO<sub>2</sub> system. This value, which gave a reasonable value of 6.0 cal/<sup>o</sup>K gfw for the entropy of fusion, was adopted and assigned an uncertainty of 1.5 Kcal/gfw.

# 2) Entropy and heat content at 298. 15°K

The low-temperature heat capacity of MgO has been measured by Gunther \$^{143}\$ (21° to \$4°K), Parks and Kelley \$^{387}\$ (94° to 291°K), Giauque and Archibald \$^{404}\$ (20° to 301°K), Barron, Berg, and Morrison \$^{405}\$ (10° to 270°K), and Lien and Philips \$^{406}\$ (1.5 to 4°K). The data of Giauque and Archibald, \$^{404}\$ and Lien and Philips, \$^{406}\$ were from microcrystalline samples, and those of the other authors were from macrocrystalline samples. Results for these two crystalline states of MgO differed appreciably. For purposes of this compilation, the macrocrystalline state was taken as the standard state and data for it alone were tabulated.

<sup>402</sup>Ebert, F. and E. Cohn, Z. anorg. Chem. 213, 321 (1933).

<sup>403</sup>Ruff, O. and P. Schmidt, Z. anorg. Chem. 117, 172 (1921).

<sup>404</sup>Giauque, W.F. and R.C. Archibald, J. Am. Chem. Soc. 59, 561 (1937).

<sup>405</sup> Barron, T.H.K., W.T. Berg, and J.A. Morrison, Proc. Roy. Soc. (London) 250A, 70 (1959).

<sup>406</sup>Lien, ♥. and N. Phillips, J. Chem. Phys. 29, 1415 (1958).

-6-- - 40 1

m.p. = 3075 + 50'1

fw = 40.32	m.p. = 3075' + 50' K							
T,*K		۱/°K واح	-(FT -H298)/T		AH; Keal/	ΔF,	`r	
	c <b>;</b>	sf,		H <sub>T</sub> - H <sub>298</sub>	OH !	AF (	Log Kp	
0 298, 15	0.000 8.906	0.00Q 6.439	Infinite 6.439	-1.235 0.000			Infinite	
300	8.939	6.495	6, 440	0.000				
400	10.148	9. 252	6.807	0.978				
500	10.854	11.599	7.538	2.031				
600	11.323	13.622	8.367	3, 141				
700	11.656	15. 393	9.263	4.291				
300	11.905	16. 967	10.130	5.469				
900	12.098 12.135	18.381 18.683	10.970 11.154	6.670 6.949				
923 923	12.135	18.683	11, 154	6.949				
000	12.251	19.663	11.775	7.888				
100	12.375	20.837	12.547	9.119				
200	12.478	21.918	13,283	10.362				
100	12.565	22, 921	13.987	11,614				
77	12.622	23, 644	14.505	12.584				
377 100	12,622 12,638	23, 644 23, 855	14.505 14.659	12.584 12.874				
500	12.701	24.729	15, 301	14.141				
00	12 764	25 550	15 016	15 414				
500 700	12.756 12.804	25.550 26.325	15.916 16.506	15.414 16.692				
300	12.845	27.058	17.072	17.975				
000	12.882	27.754	17.616	19.261				
00	12.915	28.415	18,139	20,551			ĺ	
100	12,945	29.046	18.644	21.844				
200	12.971	29.649	19.131	23,140				
100	12.994	30.226	19.601	24.438				
600 500	13.016 13.035	30.780 31.311	20,055 20,494	25.739 27.042				
00	13.052	31.823	20.921	28, 346				
100	13.068 13.082	32, 316 32, 791	21,334 21,734	29.652 30.959				
00	13.095	33. 251	22.124	32.268				
000	13.107	33.695	22,502	33.578				
75	13.115	34.019	22.779	34.562				
75	14.600	40.035	22.779	53,062				
00	14.600	40.153	22,918	53,427				
00	14.600	40.617	23,465	54.887				
00	14.600	41.066 41.502	23.991 24.500	56,347 57,807				
00	14.600	41.925	24.992	59.267				
00	14.600	42, 336	25, 467	60,727				
100	14.600	42.736	25, 929	62, 167			i	
100	14,600	43, 125	26.376	63.647				
00	14,600	43,505	26.811	65.107				
00	14.600	43, 875	27.233	66.567				
							Ì	
							j	
							1	

## MAGNESIUM OXIDE CONDENSED PHASES

### SUMMARY OF UNCERTAINTY ESTIMATES

cal/°K gfw-					Kcal/gfv		`	
T,°K	S.	s <sub>T</sub>	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH o	ΔF <sub>1</sub>	Log Kp	
298.15	± .050	± .020	±,020	± .000				
1000	± .280	± .160	±,080	± .080				
2000	± .940	± .390	±.180	± .410				
3075	±1.780	± .570	±.290	± .860				
3075	±1.000	±1.060	±.290	± 2.360				
4000	± 2,000	±1.450	±.510	±3,750				

The National Bureau of Standards <sup>78</sup> joined the low-temperature data for the macroscopic solid phase with the unpublished data of Victor and Douglas (273° to 1173°K). The results of this analysis, which were accepted here, yielded a value for S°298 of 6.439 + 0.020 cal/°K gfw and for H°298 - H°0 of 1234.6 cal/gfw. Kelley <sup>139</sup> reported S°298 to be 6.4 + 0.1 cal/°K gfw for macrocrystalline MgO.

## 3) High-temperature heat content

Results of the analysis of the unpublished data of Victor and Douglas by the National Bureau of Standards<sup>78</sup> was adopted for the high-temperature heat content of MgO. According to this analysis, the heat capacity of MgO from 450° to 1200°K in cal/°K gfw was given by equation (186).

$$C_p^{\circ} = 13.7146 - 4.494 \times 10^{-5} T - 1418/T$$
 (186)

The NBS report also stated that the enthalpies derived from this equation could be extrapolated from  $1200^{\circ}$  to  $2100^{\circ}$ K with an uncertainty of  $\pm$  2 percent. This uncertainty was presumably arrived at by comparison with Kelley's <sup>56</sup> tabulation. Kelley <sup>56</sup> derived equation (187) for the enthalpy in cal/gfw,

$$H_{\rm T}^{\circ} - H_{298}^{\circ} = 10.18T + 0.87 \times 10^{-3}T^{2} + 1.48 \times 10^{5}/T - 3609$$
 (187)

from the data of Magnus 407 (288° to 1040°K) and Wilkes 408 (303° to 2073°K). The enthalpies tabulated by the NBS are from 1 to 5 percent higher than those given by Kelley, with the maximum difference in the range from 700° to 800°K.

The heat capacity of liquid MgO was assumed to be 14.6 cal/°K gfw.

Thermodynamic functions of the condensed phases of MgO are given in Table LX. Analyses of heat-of-formation data had not been completed at the time of report writing. Uncertainly estimates are summarized on the back of the table.

<sup>407</sup> Magnus, A., Phys. Z. 14, 5 (1913).

<sup>408</sup> wilkes, G.B., J. Am. Ceram. Soc. 15, 72 (1932).

## c. Thermodynamic Properties of the Ideal Molecular Gas

The thermodynamic functions of MgO gas were calculated with the computer program based on the treatment of the diatomic molecule outlined in section III-E of this report. The spectroscopic constants

for the assumed  $^{1}\Sigma$  ground state given by the National Bureau of Standards  $^{78}$  were used. These constants had been corrected to those appropriate for the naturally occurring isotopic mixture. Spectro-

scopic constants for the A  $^{1}\Pi$  and B  $^{1}\Sigma$  states were taken from

Herzberg.  $^{54}$  Values of D<sub>e5</sub> for the excited states were estimated from Dunham's equations. Other electronic states of higher energy were listed by Herzberg,  $^{54}$  but their positions with respect to the assumed ground state were not known. The constants used (in units of cm<sup>-1</sup>) were as follows:

Constant	χ'1Σ	" A <sup>1</sup> П	B <sup>1</sup> Σ
E	0	3494. 4	20004.7
$\omega_{\mathbf{e}}$	782.84	664.4	824.1
<sup>ω</sup> e <sup>x</sup> e	5.15	3, 91	4.76
ω <sub>e</sub> y <sub>e</sub>			****
B <sub>e</sub>	0.5711	0.5056	0.5822
a <sub>e</sub>	0.005	0.0046	0.0045
γ <sub>e</sub>			
D <sub>e</sub> (x10 <sup>6</sup> )	1.22	1.2	1,2
g	1	2	1

'H $_{298}^{\circ}$  -  $H_{0}^{\circ}$  was calculated to be 2129. 2 cal/gfw.

The results of all the computations are given in Table LXI. The National Bureau of Standards has reported thermodynamic functions for gaseous MgO from spectroscopic constants for the ground state alone. Veits and Gurvich 394 used essentially the same constants as those adopted here to calculate thermodynamic functions up to 3500°K.

The calculations leading to Table LXI are subject to the same uncertainties as encountered with similar calculations discussed previously for BeO and CaO in sections IV - B1 and IV - B2, respectively, of this report. It is not certain that the lowest state of the observed singlet systems is the ground state. If one were to adopt the energy level diagram of MgO(g) given by Brewer and Porter 391

in which the ground state was postulated to be the  $^3\Sigma$  state (with an

adjacent <sup>3</sup> II state) and to make reasonable estimates of spectroscopic constants of the triplet states, the free-energy functions at 298.15° and 6000°K would change from 50.960 and 70.453 cal/°K gfw, respectively (as tabulated in Table LXI), to 55.143 and 73.060 cal/°K gfw, respectively. However, the interpretation of the ultraviolet bands on which Brewer and Porter's <sup>391</sup> energy-level diagram was based is itself not certain as those bands may have been due to MgOH or a polyatomic oxide. <sup>409</sup> Analysis of the above uncertainties will therefore be a continuing activity.

The analysis of the heat-of-formation data of MgO(g) had not been completed at the time of report writing.

<sup>409</sup> Pesic, D. and A. Gaydon, Proc. Phys. Soc. (London) 73A, 244 (1959).

w = 40.32	m.p. = 3075	+ 50

- 0-		-cai/°K gfw	,,, ,,, ,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		Kcal/gfw '	AF:	
T, °E	c <mark>,</mark>	s <sup>e</sup> t	$-(F_{T}^{o} - H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH	ΔF <sub>f</sub>	Log I
0	0.000	0.000	Infinite	-2.129			Infini
298.15	7.668	50.960	50,960	0.000			
300	7.676	51.007	50.960	0.014			
400	8,069	53, 272	51.266	0.803			
500	8.354	55.105	51.856	1.624			
400	0 601	54 440	62 520	2 472			
600	8.591	56, 649	52,530	2,472			
700	8.831	57.991	53,216	3, 343			
800	9.093	59.187	53.889	4, 239			
900	9.376	60.274	54.539	5.162			
923	9.445	60.513	54.683	5.381			
923	,9.445	60.513	54.683	5.381			
000	9.665	61,27	55.163	6.114			
1100	9.945	62.212	55.762	7.095			
1200	10,201	63.088	56.336	8.102			
300	10,423	63.914	56.888	9.134			
1377	10.565	64.517	57.296	9.944			
377	10.565	64,517	57.296	9.944			
400	10.606	64.693	57.418	10.186			
500	10.749	65.430	57.928	11.254			
1600	10.854	66.128	58,419	12,334			
700	10.925	66.788	58.892	13,423			
1800	10.968	67.414	59.348	14.518			
900	10.986	68.008	59.789	15,616			
000	10.984	68.572	60,214	16.715			
2100	10.968	69.108	60.625	17.813			
2200	10.941	69.618	61.023	18.909			
300	10.906	70.104	61.407	20.001			
400	10.865	70.567	61,780	21.090			
500	10.821	71,010	62.141	22.174			
600	10.776	71.435	62.490	23, 255			
700	10.770	71.841	62.830	24, 330			
800	10.685	72.231	63, 159	25.401			
900	10.642	72,606	63.479	26.468			
000	10.601	72.967	63.790	27.530			
075	10.572	73, 228	64.017	28.324			
1075	10.572	73.228	64.017	28.324			
100	10.562	73, 315	64.093	28.589			
200	10.525	73.651	64.387	29.644			
300	10.492	73.975	64.673	30.695			
400	10.461	74.289	64.953	31.743			
500	10.433	74.593	65.225	32.789			
			45.400				
600	10.407	74.888	65.490	33.831			
700	10.385	75.174	65.749	34.872			
800	10,365	75.452	66.002	35,910			
900	10.348	75.723	66.249	36.946			
000	10.333	75.986	66.491	37.981			
			// ===				
100	10,320	76. 243	66.727	39.015			
200	10.310	76.493	66.958	40.047			
300	10.302	76.738	67.185	41.079			
400	10.295	76.977	67.406	42,110			
500	10.291	77.210	67.624	43,140			
600	10.288	77.439	67.837	44, 170			
700	10,287	77.662	68.045	45,200			
800	10.288	77.882	68.250	46, 230			
	10.288	78.096	68.451	47.261			
900 000	10.290	78.307	68, 649	48.291			
100	10.298	78,514	68,843	49.322			
200	10.304	78,717	69.034	50.354			
300	10.311	78.917	69.221	51.386			
600	10, 319	79,113	69.405	52.419			
500	10.328	79.306	69.587	53,453			
600	10,338	79.495	69.765	54, 488			
700	10.349	79.682	69.941	55.525			
800		79.866	70,114	56.562			
	10.360						
900	10.372	80.047	70, 285				
	10.385	80,226	70,453	58,640			
300							
000							
500							
,,,,							

# 5. Molybdenum Oxides

The important oxides of molybdenum for which thermodynamic properties were available are molybdenum monoxide (MoO), molybdenum dioxide (MoO<sub>2</sub>) and molybdenum trioxide (MoO<sub>3</sub>). Although polymeric species of MoO<sub>3</sub>; i.e.,  $(MoO_3)_2$ ,  $(MoO_3)_3$ , etc., are known to exist, there were insufficient basic data to permit the calculation of thermodynamic tables for them.

#### a. Molybdenum Monoxide (MoO)

Molybdenum monoxide does not appear to exist in the condensed phase, <sup>264</sup> but its existence in the vapor phase at high temperatures has been verified by mass spectrographic work. <sup>410</sup> Consequently, only the thermodynamic functions for gaseous MoO in Table LXII were prepared for the present compilation.

These thermodynamic functions were calculated by means of the computer program described in section III-F with the following estimated molecular data:

#### Bond distance

 $r_o = 1.73 \stackrel{\circ}{A}$ .

### Moment of inertia

 $I = 68.139 \times 10^{-40} g \text{ cm}^2$ .

# Symmetry number

 $\theta = 1$ .

#### Fundamental frequency

 $\omega = 840 \text{ cm}^{-1}$ .

# Ground electronic state

 $^{1}\Sigma$ 

#### 1) Bond distance

The Mo-O bond distance had not been experimentally determined. A value of 1.66 Å has been calculated  $^{410}$  by means of the

<sup>410</sup> DeMaria, G., R. Burns, J. Drowart, and M. Inghram, J. Chem. Phys. 32, 1373 (1960).

Reference State for Calculating ΔH°, ΔF°, and Log K, : Solid Mo from 298, 15° to 2890°K, Liquid Mo from 2890° to 4965° K, Gaseous Mo from 4965° to 6000° K; Gaseous O<sub>2</sub>; Gaseous MoO.

gfw = 111.95

T, *K	C <sub>p</sub>	−cal/°K gfo −−−− S <sub>T</sub>	-(FT -H0298)/T	H <sub>T</sub> - H <sub>298</sub>	—————Kcal/gfw ΔH°	ΔF	Log
-, -	P	٠٦	-(FT - 1298// I		r	J. 1	,
0	0.000	0.000	Infinite	-2.116	87.413	87.413	Infin
298,15	7.542	54.587	54.587	0.000	87.400	80.467	-58.
300	7.550	54.634	54.587	0.014	87.396	80.424	-58.
400	7.932	56.861	54.888	0.789	87.232	78.124	-42,
500	8,203	58.662	55.469	1.597	87.067	75.869	- 33.
600	8,388	60.175	56.130	2.427	86.897	73.643	-26.
700	8.515	61.478	56.803	3. 272	86.718	71,448	-22.
800			57,461	4. 129	86.537		
	8.604	62,621				69.278	-18.
900 1000	8.669 8.717	63.639 64.555	58.092 58.693	4.992 5.862	86, 342 86, 138	67.133 65.010	-16. -14.
1100 - 1200	8.754	65.387 66.150	59.264 59.807	6.735 7.612	85.912 85.665	62.906 60.827	-12. -11.
1300	8.806	66,854	60.322	8.492	85.396	58.767	-9.
1400 1500	8,824	67.508 68.117	60.812 61.279	9.373 10.256	85.105 84.804	56,729 54,714	-8. -7.
	0,007	) 79	******		• • • • • • • • • • • • • • • • • • • •	J	
1600	8.851	68.689	61.725	11,141	84.470	52,717	-7.
1700	8.861	69. 225	62.150	12.027	84.108	50.743	-6.
0081	8.870	69.731	62,557	12.913	83,715	48.794	-5.
900	8.877	70.211	62.948	13,800	83, 291	46.862	-5.
2000	8.883	70.667	63.322	14.688	82.834	44.958	-4.
2100	8.889	71,100	63.683	15.577	82, 342	43.073	-4.
2200	8.893	71.514	64.029	16.466	81,813	41.219	-4.
2300	8.898	71.909	64.363	17.356	81, 246	39. 385	-3.
		72, 288	64,686			37.579	
2400 2500	8.901 8.904	72, 651	64.997	18.246 19.136	80.637 79.985	35.800	-3, -3.
600	8.907	73.001	65.298	20.027	79.290	34.047	-2.1
700	8.910	73.337	65.590	20.917	78.549	32, 314	-2.
800	8.912	73,661	65.872	21.809	77.761	30,621	-2.
2890	8,914	73.943	66.119	22.611	77.009	29.117	-2.
890	8.914	73.943	66.119	22.611	70.359	29,117	-2.
900	8.914	73,974	66.146	22,700	70.300	28.980	-2.
000	8.916	74,276	66,412	23.591	69.715	27,564	-2.
100	8.918	74,568	66,671	24.483	69,129	26.167	-1.
200	8.919	74.852	66.922	25.375	68.540	24.790	-1.
300	8.921	75, 126	67.166	26.267	67.949	23,433	-1.
400	8.922	75. 392	67.404	27.159	67.357	22.093	-1.
500	8,923	75.651	67.636	28,051	66.761	20.766	-1.
600	8.924	75.902 76.147	67.862	28.944 29.836	66.165 65.567	19.465 18.178	-1.1
1700	8.925		68.083				-1.0
800	8.926	76. 385	68.298	30.729	64.967	16.906	-0.9
900	8.927 8.928	76, 617 76, 843	68.509 68.714	31,621 32,514	64.365 63.762	15.639 14.408	-0.8 -0.1
000	0. 720	10,013	00,111	30, 311	03,702	11,100	-0.
100	8.928	77.063	68.915	33, 407	63.157	13.177	-0.
200	8.929	77.278	69.112	34.300	62.550	11.966	-0.6
300	8.930	77.489	69.304	35.193	61.941	10,776	-0.5
400	8.930	77.694	69.493	36.086	61.330	9.583	-0.4
500	8.931	77,895	69.677	36.979	60.718	8.415	-0.4
600	8.931	78.091	69.858	37.872	60,103	7.263	-0.
700	8.932	78.283	70.035	38.765	59.485	6,124	-0.2
800	8.932	78.471	70.209	39, 658	58.865	4.992	-0.2
900	8.933	78.655		40,551	58, 241	3.886	-0.1
			70.379				
965	8.933	78.773	70,488	41.132	57.834	3, 168	-0.1
965 000	8.933 8.933	78.773 78.836	70.488 70.547	41.132 41.445	-83.463 -83.767	3, 168 3, 775	-0.1 -0.1
100	8.933	79.012	70.711	42.338	-84.663	5,534	-0.2
200	8.934	79, 186	70.872	43, 231	-85.591	7.311	-0.3
300	8,934	79.356	71.031	44, 125	-86,549	9.111	-0.3
400 500	8,934	79,523	71.186	45.018	-87.539 -88.557	10.930 12.760	-0.4 -0.5
500	8.935	79.687	71,340	45.912	-80.557	14.100	-0.5
600	8.935	79.848	71.490	46,805	-89.608	14.610	-0,5
700	8.935	80.006	71.638	47.699	-90.688	16.484	-0.6
800	8.935	80.162	71.784	48.592	-91.800	18.380	-0.6
900	8.936	80.314	71.927	49.486	-92.943	20.278	-0.7
000	8,936	80,465	72,068	50.379	-94.122	22,218	-0.8
		•					

Guggenheimer relation 411 and the estimated fundamental frequency of Swaminathan and Krishnamurty. 412 A value of 1.73 Å has also been estimated by Brewer and Chandrasekharaiah 413 who interpolated between values for the monoxides of transition metals. The 1.73 Å value was chosen for the present work.

# 2) Moment of inertia

The moment of inertia, I, was calculated from the above assumed value for the Mo-O bond distance by means of equation (188),

$$I = \mu r_o^2 = \left(\frac{M_{Mo}M_o}{M_{Mo} + M_o}\right) r_o^2 , \qquad (188)$$

wherein

 $\mu$  = reduced mass

M<sub>Mo</sub> = mass of molydbenum atom

M<sub>o</sub> = mass of oxygen atom

and

r = Mo-O bond distance.

#### Fundamental frequency

The fundamental frequency,  $\omega$ , of MoO had not been accurately determined. An approximate bond analysis by Swaminathan and Kristnamurty 412 yielded a value of 950 cm<sup>-1</sup>. However, Brewer and Chandrasekharaiah 413 estimated this value to be 840 cm<sup>-1</sup>. The value of 840 cm<sup>-1</sup> was chosen for the present work as being more in accord with the postulate that the bonding in CrO is similar to that in MoO. Mass effects alone (M<sub>Mo</sub>>M<sub>Cr</sub>) would therefore indicate the choice of a lower fundamental frequency for MoO than for CrO. In view of the large uncertainty associated with the value of  $\omega$ , no attempt was made to take into account anharmonicity effects and interaction terms. The thermodynamic functions given in Table LXII therefore apply to a rigid rotator-harmonic oscillator model.

<sup>411</sup> Guggenheimer, K.M., Proc. Phys. Soc. (London) 58, 456 (1946).

<sup>412</sup> Swaminathan, T.M. and S.G. Krishnamurty, Current Sci. 23, 258 (1954).

<sup>413</sup> Brewer, L. and M.S. Chandrasekharlaiah, U.S. AEC Rept. UCRL-8713 Rev. (June 1960).

#### 4) Electronic states

The electronic states of MoO were unknown. The general practice, when no data are available, of considering only the ground state and assuming it to be a  $^{1}\Sigma$  state was followed in this work. This procedure is simpler and is believed to be as correct as that used by other workers  $^{410}$ ,  $^{413}$  who have estimated electronic levels from a crude ionic central atom model.

The standard heat of formation of gaseous MoO at 298.15°K,  $\Delta H_{298}^{9}$ , had not been directly determined. It was therefore determined by indirect methods. DeMaria and co-workers,  $^{410}$  in a mass spectrographic study of Al<sub>2</sub>O<sub>3</sub> using Mo crucibles, measured the partial pressures of MoO and monatomic oxygen in equilibrium with solid Mo at several temperatures in the range from  $^{2200}$  to  $^{2500}$  K. These measured pressures were used to obtain values for the equilibrium constant (K) of reaction (189).

$$Mo_{(s)} + O_{(g)} \rightarrow MoO_{(g)}$$
 (189)

$$K = \frac{P_{\text{MoO}(g)}}{P_{\text{O}(g)}} \quad . \tag{190}$$

The standard free-energy change,  $\Delta F^{\circ}$ , for this reaction at the several temperatures was evaluated by means of equation (191).

$$\Delta F^{\circ} = -RT \ln K_{p}. \tag{191}$$

The value of  $\Delta H_{298}^{\circ}$  for reaction (189) was then obtained by means of equation (192).

$$\frac{\Delta H_{298}^{\circ}}{T} = \frac{\Delta F^{\circ}}{T} - \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{MoO_{(g)}} + \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{Mo_{(s)}} + \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{O_{(g)}}. (192)$$

The values of the free-energy functions for  $\text{MoO}_{(g)}$ ,  $\text{Mo}_{(s)}$ , and  $\text{O}_{(g)}$  were taken from Tables I XII, XXVIII, and XXV of this report. A value for  $\Delta \text{H}^2_{298}$  was calculated at each temperature for which DeMaria and coworkers  $^{410}$  reported measured pressures. The average of all the  $\Delta \text{H}^2_{298}$  values was combined with the  $\Delta \text{H}^2_{298}$  of dissociation of oxygen gas  $(\text{O}_2)$  to yield the heat—of formation of gaseous MoO in accordance with the reaction scheme

$$Mo_{(g)} + O_{(g)} \rightarrow MoO_{(g)}$$
 (193)

$$\frac{1}{2}O_{2(g)} + O_{(g)}$$
 (194)

$$Mo_{(8)} + \frac{1}{2}O_{2(g)} + MoO_{(g)}$$
 (195)

The value of the heat of formation so obtained was  $87400 \pm 5000$  cal/gfw. The value of H<sub>298</sub> - H<sub>0</sub> for MoO was found to be 2116 cal/gfw.

The values of  $\Delta H_f^o$ ,  $\Delta F_f^o$ , and  $\log_{10} K_p$  were than evaluated from the value of  $\Delta H_{f208}^o$  and equations (44), (196) and (197).

$$\Delta H_{f}^{\circ} = \Delta H_{f298}^{\circ} + (H_{T}^{\circ} - H_{298}^{\circ})_{MoO(g)} - (H_{T}^{\circ} - H_{298}^{\circ})_{Mo(g)} - \frac{1}{2}(H_{T}^{\circ} - H_{298}^{\circ})_{O_{2}(g)}$$
(196)

$$\Delta F_{t}^{o} = \Delta H_{f298}^{o} + (F_{T}^{o} - H_{298}^{o})_{MoO(g)} - (F_{T}^{o} - H_{298}^{o})_{Mo(u)} - \frac{1}{2} (F_{T}^{o} - H_{298}^{o})_{O_{2(g)}}.(197)$$

The statement concerning the approximate nature of the functions for  $CrO_2$  and  $CrO_3$  in Tables LVIII and LIX also applies to those for MoO in Table LXII.

b. Molydbenum Dioxide (MoO2)

#### 1) Solid state

Thermodynamic properties of solid MoO<sub>2</sub>, based on the low-temperature heat capacity measurements of King, <sup>414</sup> the high-temperature enthalpy data of King, Weller, and Christensen, <sup>415</sup> and the heat-of-formation data of Mah<sup>416</sup> have been reported.

<sup>414</sup>King, E.G., J. Am. Chem. Soc. 80, 1799 (1959).

<sup>415</sup> King, E.G., W.W. Weller, and A.V. Christensen, U.S. Bur. Mines Rept. Inv. 5664 (1960).

<sup>416</sup> Mah, A.D., J. Phys. Chem. 61, 1572 (1957).

The only experimental investigation of the low-temperature heat capacity of  $M_0O_2$  was that of King  $^{414}$  which extended from  $53^{\circ}$  to  $296^{\circ}$ K. The value of  $S_{298.15}^{\circ}$  obtained from these experimental data was  $11.06 \pm 0.05$  e. u. /gfw.

King, Weller, and Christensen<sup>415</sup> had reported the only experimental enthalpy values for MoO<sub>2</sub> at high temperatures (400° to 1800°K). The enthalpy functions for solid MoO<sub>2</sub> in Table LXIII are accordingly the smoothed values reported by King and coworkers<sup>415</sup> after extrapolation to 2000°K and to room temperature.

The tabular entropy values for solid MoO<sub>2</sub> were calculated from the enthalpy functions by the method of Kelley. <sup>56</sup>

Values for the free-energy function were calculated from equation (108). Tabular values of  $C_p^o$  (in cal/ $^O$ K gfw) were calculated from equation (198) due to King and co-workers.  $^{4.15}$ 

$$C_p^o = 14.11 + 5.82 \times 10^{-3} T - 2.18 \times 10^{+5} T^{-2}$$
 (198)

 $MoO_2$  does not exhibit a true melting point since disproportionation occurs to yield solid Mo and MoO<sub>3</sub> vapor (including MoO<sub>3</sub> polymeric species) before melting occurs. 417,418

The standard heat of formation,  $\Delta H_{f298}^{\circ}$  of solid MoO<sub>2</sub> was recently determined by Mah<sup>416</sup> from experimental measurements of the heat of combustion of Mo(s) to MoO<sub>3(s)</sub> and of MoO<sub>2(s)</sub> to MoO<sub>3(s)</sub>. These measurements led directly to the heat of formation of MoO<sub>2(s)</sub>. Mah obtained a value for  $\Delta H_{f298}^{\circ}$  of-140640 ± 130 cal/gfw, and after critical comparison of this value with earlier values,  $^{419-423}$  recommended a value of -140800 ± 200 cal/gfw. This recommended value was accepted in the present compilation.

Values of  $\Delta H_f^o$  ,  $\Delta F_f^o$  and  $\log_{10} K_p$  were calculated from equations (44), (199), and (200).

<sup>417</sup> Blackburn, P.E., M. Hoch, and H.L. Johnston, J. Phys. Chem. <u>62</u>, 769 (1958).

<sup>418</sup> Burns, R.P., G. DeMaria, J. Drowart, and R.T. Grimley, J. Chem. Phys. 32, 1363 (1960).

<sup>419</sup> Staskiewicz, B.A., J.R. Tucker, and P.E. Snyder, J. Am. Chem. Soc. 77, 2987 (1955).

<sup>420</sup> Mixter, W.G., Am. J. Sci. 29, 488 (1910).

<sup>421</sup> Chaudron, G., Ann. Chim. 16, 221 (1921).

<sup>422</sup> Tonosaki, K., Bull. Inst. Phys. Chem. Research (Tokyo) 19, 126 (1940).

<sup>423</sup>Gokcen, N.A., J. Metals 5, 1019 (1953).

Reference State for Calculating  $\Delta H_1^p$  ,  $\Delta F_1^o$  , and Log  $\kappa_p$  : Solid Mo; Gaseous O2; Solid MoO2.

gfw = 127.95

	cı	ıl/°K g(▼ ———			Kcal/g	·	
T, °K	C <sub>p</sub> *	ST	$-(F_{T}^{\circ} - H_{298}^{\circ})/T$	H <sub>T</sub> - H <sub>298</sub>	AH °	ΔF	Log Kp
0	0.000	0.000	Infinite	-1,995	-139.628	-139,628	Infinite
298.15	13,380	11.060	11.060	0.000	-140.800	-127.450	93.419
300	13,421	11.143	11.060	0.025	-140.799	-127.367	92.782
400	15.075	15, 232	11.607	1.450	-140.668	-122.906	67.150
500	16,148	18.730	12.690	3.020	-140.437	-118.489	51.789
600	16.996	21.774	13.957	4.690	-140.145	-114.128	41.569
700	17.739	24.468	15.268	6.440	-139.807	-109.817	34.285
800	18,425	26.898	16.573	8.260	-139, 425	-105.559	28.836
900	19.079	29.112	17.845	10.140	-139.009	-101.350	24.610
1000	19.712	31.145	19.075	12.070	-138.567	-97.189	21.240
1100	20.332	33.022	20,258	14,040	-138,116	-93.073	18,491
1200	20.943	34.781	21.398	16.060	-137.644	-89.000	16.208
1300	21.547	36.429	22.491	18.120	-137.161	-84,968	14.284
1400	22,147	37.992	23.542	20.230	-136.655	-80.972	12,640
1500	22.743	39.503	24.555	22.420	-136.085	-77.013	11.220
1600	22.337	41.007	25.538	24.750	-135.412	-73.096	9.984
1700	23.929	42.565	26.494	27.320	-134.532	-69.231	8.900
1800	24.519	44.256	27,434	30.280	-133.295	-65.425	7.943
1900	25,108	46.180	28.369	33,840	131.493	-61.701	7.097
2000	25.695	48.457	29.317	38.280	-128.848	-58.094	6.348

$$\Delta F_{f}^{\circ} = \Delta H_{f298}^{\circ} + (F_{T}^{\circ} - H_{298}^{\circ})_{MoO_{2(s)}} - (F_{T}^{\circ} - H_{298}^{\circ})_{Mo_{(s)}}$$

$$- (F_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}} ,$$
(199)

$$\Delta H_{f}^{\circ} = \Delta H_{f298}^{\circ} + (H_{T}^{\circ} - H_{298}^{\circ})_{MoO_{2(s)}} - (H_{T}^{\circ} - H_{298}^{\circ})_{Mo(s)}$$

$$- (H_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}} .$$
(200)

### 2) Gaseous Phase

No experimental spectroscopic data had been reported for gaseous MoO<sub>2</sub>. All of the molecular constants required in the calculation of its thermodynamic functions were therefore estimated. The thermodynamic functions for gaseous MoO<sub>2</sub> given in Table LXIV were calculated by means of the machine program described in section III-F with the following molecular data:

Molecular configuration

Symmetric, nonlinear molecule with

$$\angle$$
 O-Mo-O = 107 deg

$$r_0 = 1.73 \, \mathring{\Lambda}$$
.

Product of moments of inertia

$$I_A I_B I_C = 628260 \times 10^{-120} \, \text{g}^3 \, \text{cm}^6$$
.

Symmetry number

$$\theta = 2$$
.

Fundamental frequencies

$$\omega_1 = 824 \text{ cm}^{-1}$$

$$\omega_2 = 367 \text{ cm}^{-1}$$

$$\omega_3 = 857 \text{ cm}^{-1}$$
.

Ground electronic state

 $^{1}\Sigma$  .

Reference State for Calculating ΔH<sup>o</sup><sub>r</sub>, ΔF<sup>o</sup><sub>r</sub>, and LogK<sub>p</sub>: Solid Mo from 298.15° to 2890°K, Liquid Mo from 2890° to 4965°K, Gaseous Mo from 4965° to 6000°K; Gaseous O<sub>2</sub>; Gaseous MoO<sub>2</sub>

gfw = 127.95

		cal/°K gfw		\		ıl/gf=	
T, °K	¢°	sf	$-(F_{T}^{o} - H_{298}^{o})/T$	HT - H298	ΔH°	ΔF	Log
0	0.000	5.000	Infinite	-2.670	0.297	0,297	Infi
298.15	10,663	63.874	63.874	0.000	-0.200	-2,596	1.90
300	10.683	63.940	63.874	0.020	-0.204	-2.611	1.90
400	11.624	67.151	64.306	1.138	-0.380	-3.386	1.8
500	12, 256	69.817	65.149	2.334	-0.523	-4.118	1.80
600	12.677	72,091	66,121	3,582	-0.653	-4.826	1.79
700	12.962	74.068	67.118	4.865	-0.782	-5.513	1.7
800	13, 162	75,813	68.098	6.172	-0.913	-6.179	1.6
900	13.307	77, 372	69.044	7.496	-1.053	-6.829	1.6
1000	13.414	78.780	69.948	8.832	-1.205	-7.462	1.6
1100	11 404	BO 043	70.010	10 170	1 170	0.001	
1100 1200	13.496 13.559	80.062 81.240	70,810 71,631	10.178 11.531	-1.378 -1.573	-8.081 -8.681	1,60
300	13.609	82, 327	72.412	12.889	-1.792	-9.265	1.5
400	13.649	83.337	73, 157	14.252	-2.033	-9.832	1.5
500	13,682	84.280	73.867	15,619	-2.286	-10.379	1.51
600	13.709	85, 164	74.546	16.988	-2,574	-10.909	1.46
700	13.731	85.995	75, 195	18.360			1.49
800	13.750	86.781			-2.892	-11.422	1.46
900	13.767		75,817	19.734	-3, 241 -3, 623	-11.912	1.44
000	13.780	87.525 88.231	76,414 76,987	21,110 22,488	-3.623 -4.040	-12,384 -12,834	1.42
100 200	13,792 13,803	88,904 89,546	77.539 78.070	23.866 25.246	-4.496 -4.990	-13,264 -13,669	1, 38
300	13,803	90.160	78.583	26.627	-4.990 -5.524		1.35
400						-14,053	1, 33
500	13,820	90.748 91.312	79.077 79.556	28.008 29.391	-6.102 -6.725	-14.410 -14.745	1,31
600 700	13,833	91.854 92.376	80.018 80.466	30.774 32,157	-7.394 -8.112	-15.051 -15.333	1.26
800	13,844	92.880	80.901	33.541	-8.878	-15.585	1.21
890	13.848	93. 317	81.271	34.788	-9.612	-15.762	1.19
890	13.848	93.317	81.271	34.788	-16,262	-15.762	1.19
900	13.848	93, 366	81, 322	34.926	-16,319	-15.785	1.19
000	13.852	93.835	81.732	36, 311	-16.886	-15.759	1.14
100	13.054	24 300	0.1.1.10	20 /0/			
200	13.856	94.290 94.729	82.129 82.516	37.696 39.082	-17,458 -18,034	-15,708 -15,648	1.10
300	13,862	95, 156	82.893	40,468	-18.613	-15.563	1.03
100	13.865	95.570	83,260	41,855	-19.196	-15.463	0.99
500	13.868	95.972	83,617	43.241	-19.784	-15, 341	0.95
600	13,870	96. 363	83.966	44.628	-20,375	-15.206	0.92
700	13.872	96, 743	84.306	46.015	-20,969	-15.052	0.88
300	13,874	97.113	84.638	47.403	-21,566	-14,885	0.856
900	13,876	97.473	84.963	48.790	-22.168	-14.703	
000	13.878	97.824	85.280	50.178	-22,722	-14.703	0.824
00	13.879	98.167	05 500	£) £()	33 300	14.300	
200	13.881	98,501	85,590 85,893	51,566 52,954	-23,380 -23,992	-14.289 -14.057	0.76
00	13.882	98.828	86.190	54.342	-24.607	-13.807	0,702
00	13.884	99.147	86.481	55.730	-25,227	-13,548	0.67
00	13.885	99.459	86.756	57.119	- 25.849	-13,280	0,649
00	13.004	00.7/4	07.044	50 503			
00 00	13.886	99.764 100,063	87,046 87,319	58.507 59.896	-26.477 -27.109	-12,990 -12,690	0.617
00	13.888	100,355	87,588	61,284	-27.748	-12,374	0,563
00	13.889	100.642	87.851	62.673	-28.392	-12.044	0,537
65	13,890	100.824	88.019	63.576	-28.816	-11.817	0.540
65	13,890	100,824	88.019	63,576	-170,113	-11,817	0.540
00	13,890	100.922	88.110	64.062	-170,426	-10.705	0.468
00	13.890	101.198	88.364	65.451	-171, 351	-7.502	0, 321
00	13.891	101.467	88.613	66.840	-172.313	-4,280	0, 121
00	13.892	101.732	88.858	68.229	-173, 312	-1.019	0.043
00	11.891	101.992	89.099	69.617	-174.349	2.225	-0.090
00	13.893	102, 246	89.316	71,008	-175,425	5,511	-0.219
00	13.894	102.497	89.569	72.397	-176.543	8,803	-0.344
00	13.895	102,743	89.798	73.787	-177.703	12, 135	-0.465
00	13.895	102.984	90.023	75.176	-178,911	15,480	-0,496
00	13.896	103, 222	90.245	76.566	-180,169	18,839	-0.698
00	13.896	103, 455	90.463	77.955	-181,484	22, 236	-0.810

#### a) Molecular configuration

The molecular configuration of MoO<sub>2</sub> was unknown. Consideration of the periodic group to which molybdenum belongs and the work of Walsh<sup>395</sup> on bonding and structural relations led to the conclusion that MoO<sub>2</sub> is a symmetric, nonlinear molecule. It therefore was so considered in the present work. DeMaria and co-workers<sup>410</sup> also assumed it to have a nonlinear structure, whereas Chandrasekharaiah and Brewer<sup>397</sup> assumed it to have the linear structure of all of the Group IV, V, and VI transition metal dioxides.

An O-Mo-O angle of 107 degrees was chosen in the present work as representing a reasonable value in comparison with known compounds of similar bonding.

The Mo-O bond distance was assumed to be identical to the estimated corresponding distance for the molybdenum monoxide (MoO) molecule; i.e., 1.73Å.

#### b) Moments of inertia

The moments of inertia of MoO<sub>2</sub> were calculated in a manner analogous to that used for the corresponding CrO<sub>2</sub> molecule.

#### c) Fundamental frequencies

The fundamental frequencies of MoO<sub>2</sub> were estimated by the same method used for the corresponding CrO<sub>2</sub> molecule (see section IV-B3a above), except that the stretching force constant for MoO was calculated from estimated spectroscopic data. 413 The frequencies so obtained are somewhat lower than those estimated by DeMaria and co-workers. 410

#### d) Electronic states

The electronic states for  $MoO_2$  were treated in the same manner as those of the  $CrO_2$  molecule.

The standard enthalpy of formation,  $\Delta H_{1298}^{o}$ , of gaseous  $M_{002}$  had not been directly determined but could be indirectly evaluated by two different calculations. The first calculation was based on results of the mass spectrographic study of  $Al_{203}$  reported by De-Maria and co-workers using molybdenum crucibles. These workers measured the partial pressures of  $M_{002}$  and monatomic oxygen in equilibrium with solid molybdenum at several temperatures

in the range from  $2200^{\circ}$  to  $2500^{\circ}$ K. From these pressures, the equilibrium constant, K, in equation (202) and the standard free energy change,  $\Delta F^{\circ}$ , for reaction (201) could be calculated

$$Mo_{(g)} + 2O_{(g)} \longrightarrow MoO_{2(g)}$$
 (201)

$$K = \frac{P_{MoO_{2(g)}}}{P_{O_{(g)}}^2} , \qquad (202)$$

as explained in the preceding section of the report concerning MoO.

A value of  $\Delta H_{298}^2$  for the above reaction at each temperature for which measured pressures were reported was then calculated by the Third Law Method, which assumes the form of equation (203).

$$\frac{\Delta H_{298}^{\circ}}{T} = \frac{\Delta F^{\circ}}{T} - \left(\frac{F_{T}^{\bullet} - H_{298}^{\circ}}{T}\right)_{MoO_{2(g)}} + \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{Mo_{(g)}} + 2\left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{O_{(g)}}$$
(203)

The values of the free-energy functions for  $MoO_{2(g)}$ ,  $Mo_{(g)}$ , and  $O_{(g)}$  were taken from Tables LXIV, XXVIII, and XXV of this report. The average of all the  $\Delta H^{\circ}_{298}$  values for reaction (201) was then combined with the  $\Delta H^{\circ}_{298}$  of dissociation of oxygen gas (O2) to yield the heat of formation of gaseous  $MoO_2$  in accordance with the reaction scheme

$$Mo_{(g)} + 2O_{(g)} \longrightarrow MoO_{2(g)}$$
 (204)

$$O_{2(g)} \longrightarrow {}^{2O_{(g)}}$$
 (205)

$$Mo(s) + O_{2(s)} \longrightarrow MoO_{2(s)}$$
 (206)

The first value of the heat of formation of  $MoO_2$  gas so obtained was 5380  $\pm$  4500 cal/gfw at 298.15°K.

The second calculation was based on results of the mass spectrographic study of the gaseous species in equilibrium with solid  $MoO_2$  reported by Burns and co-workers. <sup>418</sup> Partial pressures of  $MoO_{2(g)}$  in equilibrium with  $MoO_{2(s)}$  were reported at several temperatures in the range from  $1560^{\circ}$  to  $1780^{\circ}$  K. From these measured pressures, the standard free-energy change,  $\Delta F^{\circ}$ , for the sublimation of  $MoO_2$  as in reaction (207) could be calculated at each temperature.

$$MoO_{2(s)} \longrightarrow MoO_{2(g)}$$
, (207)

by means of equation (208),

$$\Delta F^{\circ} = -RT \ln P_{MoO_{2(g)}}$$
 (208)

values of  $\Delta H_{298}^{\circ}$  corresponding to each calculated  $\Delta F^{\circ}$  value were then calculated from equation (129).

The values of the free-energy function used for  $MoO_{2(s)}$  and  $MoO_{2(g)}$  were taken from Tables LXIII and LXIV of this report. The average of all values of  $\Delta H^\circ_{298}$  for reaction (207) was combined with the heat of formation of solid  $MoO_2$  to yield the heat of formation of gaseous  $MoO_2$  in accordance with the reaction scheme at 298.15°K.

$$MoO_{2(s)} \longrightarrow MoO_{2(g)}$$
 (209)

$$Mo_{(s)} + O_{2(g)} \longrightarrow MoO_{2(s)}$$
 (210)

$$Mo_{(s)} + O_{2(g)} \longrightarrow MoO_{2(g)}$$
 (211)

The second value of the heat of formation of  $MoO_2$  gas so obtained was  $-5700 \pm 2000$  cal/gfw. The average of the two values, after rounding off to the nearest hundred calories, was  $-200 \pm 6000$  cal/gfw. The value of  $H_{298}^{\circ} - H_{0}^{\circ}$  for  $MoO_{2(g)}$  was found to be 2670 cal/gfw.

Values of  $\Delta {\rm H_f^o}$  ,  $\Delta {\rm F_f^o}$  , and  ${\rm log_{10}K_p}$  —were calculated by methods already described.

# c. Molybdenum Trioxide (MoO3)

#### 1) Condensed phase

#### a) Melting point and heat of fusion

The melting point of MoO<sub>3</sub> had been determined by Hoermann 424 (1068°K), Cosgrove and Snyder 425 (1068°K), Babadzhan 426 (1070°K), and King, Weller, and Christensen 415 (1074°K). The average value of 1070° ± 5°K was adopted for the present compilation.

The heat of fusion, as determined from enthalpy values of the solid and liquid at the melting point, was 11,683 cal/gfw. An uncertainty of 500 cal/gfw was arbitrarily assigned to this heat of fusion. The  $\Delta H$  value is almost identical to that reported by King, Weller, and Christensen<sup>415</sup> (11,690 cal/gfw), but appreciably lower than the value reported by Cosgrove and Snyder <sup>425</sup> (12,540 cal/gfw).

#### b) Boiling point

The equilibrium vapor above MoO<sub>3</sub> consists primarily of (MoO<sub>3</sub>)<sub>3</sub>, (MoO<sub>3</sub>)<sub>4</sub>, and (MoO<sub>3</sub>)<sub>5</sub> according to Berkowitz, Inghram, and Chupka. <sup>427</sup> Evidence for the existence of polymeric MoO<sub>3</sub> vapor species is also furnished by the work of Blackburn, Hoch, and Johnston, <sup>417</sup> Babadzhan, <sup>426</sup> and of Zelikman, Gorovits, and Prosenkova. <sup>428</sup> No attempt has been made in the present work to define a boiling point for MoO<sub>3</sub>. A temperature of about 1450°K had been quoted <sup>204</sup> as the temperature at which the total pressure above MoO<sub>3</sub> becomes one atmosphere. No attempt was made to estimate thermodynamic functions for these polymeric vapor species because of the lack of basic data.

<sup>424</sup>Hoermann, F., Z. anorg. u. allgem. Chem. 177, 145 (1928).

<sup>425</sup> Congrove, L. A. and P. E. Snyder, J. Am. Chem. Soc. 75, 1227 (1953).

<sup>426</sup> Babadahan, A. A., Trudy Inst. Met., Akad. Nauk SSSR Ural. Filiai, Sbomik Rabot 1, 74 (1957).

<sup>427</sup> Berkowitz, J., M. G. Inghram, and W. A. Chupka, J. Chem. Phys. 26, 842 (1957).

<sup>428</sup> Zelikman, A. N., N. N. Gorovite, and T. E. Prosenkova, Zhur. Neorg. Khim. 1, 632 (1956).

# c) Entropy at 298.15° K (S<sub>298</sub>)

Kelley and King  $^{318}$  recommended 18.58  $\pm$  0.10 e.u./gfw as the value of S  $^{\rm O}_{298}$  for MoO<sub>3</sub>. This value was based on the low-temperature heat capacity measurements of Seltz, Dunkerley, and DeWitt,  $^{429}$  and of Smith, Brown, Dworkin, Sasmor, and Van Artsdalen.

#### d) Thermodynamic functions for the condensed state

Enthalpy measurements by dropping methods have been reported by Cosgrove and Snyder \$^{425}\$ (300° to 1300°K) and by King, Weller, and Christensen \$^{415}\$ (400° to 1400°K). The results of the latter workers were arbitrarily chosen for this compilation. The results reported by Cosgrove and Snyder \$^{425}\$ were about 2 percent higher than the former results.

The  $C_p^o$  values (in cal/ $^O$ K gfw) for solid  $MoO_3$  from 298.15 $^O$ K to the melting point (1070 $^O$ K) given in Table LXV were calculated by means of equation (212) given by King, Weller and Christensen.  $^{415}$ 

$$C_p^{\circ} = 17.97 + 7.80 \times 10^{-3} \text{T} - 2.10 \times 10^5 \text{T}^{-2}.$$
 (212)

The derived equations used to calculate the enthalpy and entropy functions for solid  $MoO_3$  were

$$H_T^{\circ} - H_{298}^{\circ} = 17.97T + 390.0 \times 10^{-5}T^2 + 2.10 \times 10^5T^{-1} - 6409$$
 (213)

$$S_T^{\circ} = 17.97 \text{ ln T} + 7.80 \times 10^{-3} \text{T} + 1.05 \times 10^{5} \text{T}^{-2} - 87.313$$
. (214)

Values for the free-energy function were calculated by means of equation (108).

The heat capacity of liquid  $MoO_3$  was reported to be constant at 30.20 cal/ $^{\rm O}$ K gfw by King and co-workers. This value was chosen in the present work in preference to the rather

<sup>429</sup> Seltz, H., F. J. Dunkerley, and B. J. DeWitt, J. Am. Chem. Soc. 65, 600 (1943).

<sup>430</sup> Smith, D. F., D. Brown, A. S. Dworkin, D. J. Sasmor, and E. R. Van Artsdalen, J. Am. Chem. Soc. 78, 1533 (1956).

Reference State for Calculating ΔH<sup>o</sup><sub>I</sub>, ΔF<sup>o</sup><sub>I</sub>, and Log K<sub>p</sub> : Solid Mo; Gaseous O<sub>2</sub>; Solid MoO<sub>3</sub> from 298.15 ct 1070 K, Liquid MoO<sub>3</sub> from 1070 to 1500 K.

Cal	/°K e/=	m.p. = 101	<u> </u>	Koal/efa		
c <sub>p</sub>	ST	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>o</sup>	AF (	Log Kp
G.000	0.000	Infinite	-3.009	-176.905	-176.905	Infinite
17.934	18,580	18.580	0.000	-178.100	-159.686	117.04
19,777	24.130	19. 310	1.928	-177.851	-159, 572	116, 24 83, 82
21.030	28.684	20.742	3 971	-177.513	-147.361	64,40
22.067	32,612	22.400	6.127	-177, 113	-141, 369	51,49
						42, 28 35, 40
24.731	42.076	27, 457	13, 157	-175.591	-123.807	30.06
25.560	44.724	29.053	15.671	-174.979	-118.084	25.80
26.133	46.473	30.136	17.481	-174, 526	114, 123	23, 30
						23, 39 22, 40
30,200	60.855	33, 280	33.090	-161.471	-108,277	19.71
						17, 46- 15, 54-
30.200	67.594	39.494	42, 150	-158.508	-95.331	13.88
		*			***	
			•			
	C°, G.000 17.934 17.977 19.777 21.030  22.067 23.001 23.882 24.731 25.560  26.133 30.200 30.200 30.200 30.200 30.200 30.200 30.200	G.000 0.000 17, 934 18, 580 17, 977 18, 691 19, 777 24, 130 21, 030 28, 684  22, 067 32, 612 23, 001 36, 084 23, 882 39, 213 24, 731 42, 076 25, 560 44, 724  26, 133 46, 473 30, 200 57, 392 30, 200 58, 227 30, 200 63, 272 30, 200 63, 272 30, 200 65, 511	C° <sub>p</sub> S° <sub>T</sub> -(F° <sub>T</sub> - H° <sub>298</sub> )/T  G.000 0.000 Infinite  17.934 18.580 18.580  17.977 18.691 18.581  19.777 24.130 19.310  21.030 28.684 20.742  22.067 32.612 22.400  23.001 36.084 24.111  23.882 39.213 25.805  24.731 42.076 27.457  25.560 44.724 29.053  26.133 46.473 30.136  30.200 57.392 30.136  30.200 58.227 30.891  30.200 63.272 35.495  30.200 65.511 37.561	$ \begin{array}{cccccccccccccccccccccccccccccccccccc$	$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	Cell ** Kel/gf*

unexpected values reported by Cosgrove and Snyder.  $^{425}$   $H_T^{\circ} - H_{298}^{\circ}$ ,  $S_T^{\circ}$ , and  $-\left(\frac{F_T^{\circ} - H_{298}^{\circ}}{T}\right)$  for liquid MoO<sub>3</sub> were then calculated by means of equations (215), (216), and (108).

$$H_T^{\circ} - H_{298}^{\circ} = 30.20T - 3150$$
 (215)

$$S_T^o = 30.20 \text{ ln T} - 153.265$$
. (216)

e) Standard heat of formation at 298.15°K (  $\Delta H_{f298}^{O}$ )

The standard heat of formation,  $\Delta\,H_{f298}^{\,\,\rm O}$ , of solid MoO3 was recently determined by Mah,  $^{416}$  from experimental measurements of the heat of combustion of Mo(s) to MoO3(s) , to be -178, 160  $\pm$  110 cal/gfw. From a comparison of this value with that of earlier workers,  $^{419}$ ,  $^{420}$ ,  $^{431}$ - $^{433}$  Mah  $^{416}$  chose a "recommended" value of -178, 100  $\pm$  100 cal/gfw. This "recommended" value was adopted in the present compilation.

The values of  $\Delta H_f^o$  ,  $\Delta F_f^o$  , and  $log_{10} K_p$  were than calculated according to equations (217), (218), and (44).

$$\Delta F_{1}^{\circ} = \Delta H_{1298}^{\circ} + (F_{T}^{\circ} - H_{298}^{\circ})_{MoO_{3(c)}} - (F_{T}^{\circ} - H_{298}^{\circ})_{Mo_{(s)}}$$
$$- 3/2 (F_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}}$$
(217)

$$\Delta H_{1}^{\circ} = \Delta H_{1298}^{\circ} + (H_{T}^{\circ} - H_{298}^{\circ})_{MoO_{3(c)}} - (H_{T}^{\circ} - H_{298}^{\circ})_{Mo_{(s)}}$$
$$- 3/2 (H_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}}. \tag{218}$$

#### 2) Gaseous phase

No experimental spectroscopic data had been reported for gaseous  $MoO_3$ . All of the molecular constants required in the calculation of the thermodynamic functions were therefore estimated. The thermodynamic functions for gaseous  $MoO_3$  given in Table LXVI were calculated by means of the machine program described in section III-F with the following molecular data:

<sup>431</sup> Delepine, M., Bull. Soc. Chim. 29, 1166 (1903).

<sup>432</sup> Moose, J. E. and S. W. Paar, J. Am. Chem. Soc. 46, 2656 (1924).

<sup>433</sup> Newmann, B., C. Kroger, and H. Kunz, A. anorg. u. allgem. Chem. 218, 379 (1934).

Reference State for Calculating  $\Delta H_i^o$ ,  $\Delta F_i^o$ , and  $Log K_p$ : Solid Mo from 298.15' to 2890 'K, Liquid Mo from 2890' to 4965' K, Gaseous Mo from 4955' to 6000' K; Gaseous O2; Gaseous MoO3.

gfw = 143.95

m.p. = 1070° + 5° K

0 0,000 0,000 0,000 Infinite			-cal/°K gfw			Kcal	/gf w	$\overline{}$
299, 15   14,498   66,653   66,653   0.000   -81,000   -76,919   56,   300   14,533   66,742   66,653   0.027   -81,004   -76,694   56,   500   17,147   74,867   68,407   3.20   -81,156   -75,504   41,   500   17,147   74,867   68,407   3.20   -81,156   -72,682   26,   500   17,838   78,059   69,756   4,982   -81,158   -72,682   26,   500   13,308   80,846   71,145   6,790   -81,150   -71,271   22,   500   18,087   83,313   72,515   8,659   -81,159   -71,271   22,   500   18,677   83,313   72,515   8,659   -81,159   -65,661   19,   18,082   85,752   73,840   19,312   -81,138   -65,461   16,   1900   19,456   89,344   76,322   14,324   -81,138   -65,461   16,   19100   19,186   89,344   76,322   14,324   -81,165   -65,629   13,   1100   19,186   89,344   76,322   14,324   -81,165   -65,629   13,   1100   19,186   89,344   76,322   14,324   -81,165   -65,629   13,   1100   19,491   91,018   77,478   16,248   -81,213   -64,216   11,   1100   19,490   94,004   79,631   20,122   -81,380   -61,373   9,   1100   19,440   94,004   79,631   20,122   -81,380   -61,373   9,   1100   19,579   95,666   81,593   24,021   -81,632   -58,496   7,   1700   19,579   95,666   81,593   24,021   -81,632   -58,496   7,   1700   19,677   101,940   85,811   33,829   -82,560   -51,16   5,   1800   19,677   101,940   85,811   33,829   -82,560   -51,16   5,   1800   19,677   101,940   85,811   33,829   -82,560   -51,16   5,   1800   19,677   101,940   85,811   37,768   -83,644   -48,099   4,5   1900   19,677   101,940   85,811   37,768   -83,644   -48,099   4,5   1900   19,677   101,940   85,811   37,768   -83,644   -48,099   4,5   1900   19,677   101,940   85,811   37,768   -83,644   -48,099   4,5   1900   19,784   105,198   103,198   11,100   49,415   -86,651   -44,900   3,9   19,774   101,959   103,732   87,311   37,768   -83,649   -44,900   3,9   19,774   101,959   103,732   87,311   37,768   -83,649   -44,900   3,9   19,784   105,198   106,499   103,499   103,491   103,499   103,499   103,499   103,499   103,499   103,499   103,499	T, °K	c <sub>p</sub>	$S_{\mathbf{T}}^{\mathbf{c}}$	$-(F_T^0 - H_{298}^0)/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF	Log
14.533		0.000	0.000	Infinite			-80,023	Infin
16.05								56.3
17.147								56.0
17.838   78.059   69.756   4.982   -81.158   -72.682   26.								41.2
700 18,308 80,846 71,145 6.790 -31,150 -71,271 22, 28, 800 18,677 83,313 72,515 8.699 -41,139 -69,661 19, 990 18,876 85,523 73,840 10.515 -81,133 -68,651 16, 14, 14, 1100 19,186 89,344 76,322 14,324 -81,135 -65,629 13, 1100 19,186 89,344 76,322 14,324 -81,165 -65,629 13, 1100 19,186 89,344 76,322 14,324 -81,165 -65,629 13, 1100 19,186 89,344 76,322 14,324 -81,165 -65,629 13, 1100 19,291 91,018 77,478 16,248 -81,213 -64,216 11, 1100 19,174 92,565 78,580 18,18 -81,285 -62,798 10, 19,494 93,347 80,634 22,069 -81,489 -53,940 8, 1500 19,494 93,347 80,634 22,069 -81,489 -53,940 8, 1500 19,494 95,347 80,634 22,069 -81,489 -53,940 8, 1500 19,494 95,347 80,634 22,069 -81,489 -53,940 8, 1500 19,576 97,792 82,512 25,977 -81,808 -55,949 7, 1700 19,576 97,792 82,512 25,977 -81,808 -55,949 7, 1700 19,576 97,792 82,512 25,977 -81,808 -55,949 7, 1700 19,576 97,792 82,512 25,977 -81,808 -55,949 7, 1700 19,576 97,792 82,512 25,977 -81,808 -55,949 7, 1700 19,576 97,792 82,512 25,977 -81,808 -55,949 7, 1700 19,576 97,792 82,512 25,977 -81,808 -55,949 7, 1700 19,576 97,792 82,513 33,829 82,860 -51,116 5, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3, 3,	500	17.147	74.867	. 68.407,	3, 230	-81, 154	-74.094	32.3
18,637   33,313   72,515   8,639   -81,139   -69,861   19,900   18,876   85,523   73,840   10.515   -81,138   -67,041   14,1000   19,052   87,521   75,110   12,412   -81,138   -67,041   14,1000   19,052   87,521   75,110   12,412   -81,138   -67,041   14,1000   19,052   87,521   75,110   12,412   -81,138   -67,041   14,1000   19,400   19,291   91,018   77,478   16,248   -81,213   -64,216   11,1000   19,440   94,004   79,511   20,122   -81,380   -61,373   91,500   19,440   94,004   79,511   20,122   -81,380   -61,373   91,500   19,599   96,606   81,593   24,021   -81,632   -58,496   7,7000   19,576   97,792   82,512   25,977   -81,808   -57,049   7,7000   19,576   97,792   82,512   25,977   -81,808   -57,049   7,7000   19,576   97,972   82,512   25,977   -81,808   -57,049   7,7000   19,657   100,981   85,841   31,829   -82,259   -54,110   61,800   19,657   100,981   85,841   31,829   -82,259   -54,110   61,800   19,657   100,981   85,831   31,829   -82,500   -51,116   51,200   19,657   100,981   85,831   31,829   -82,500   -51,116   51,200   19,772   100,576   88,891   41,772   -84,569   -44,930   3,980   19,774   105,376   88,891   41,772   -84,569   -44,930   3,980   19,774   105,376   88,891   41,772   -84,569   -44,930   3,980   19,762   107,614   90,601   47,637   86,593   -94,175   30,839   19,768   106,239   91,140   49,415   -66,693   -36,576   -47,756   108,978   91,781   51,590   -94,128   -36,560   -34,531   -48,009   19,768   106,239   91,140   49,415   -66,693   -36,576   -44,930   19,769   103,089   19,762   107,614   90,601   47,637   -86,593   -30,577   -38,184   -48,009   -48,000   19,776   108,978   91,781   51,590   -94,128   -36,468   2,600   19,776   108,978   91,781   51,590   -94,128   -36,468   2,600   19,776   108,978   91,781   51,590   -94,128   -36,468   2,600   19,776   108,978   91,781   51,590   -94,128   -36,468   2,600   19,787   108,978   91,781   51,590   -94,128   -36,468   2,600   19,815   114,172   95,441   65,466   -97,453   -99,888   11,384   -67,040   19,845   116,569								26.4
19.00								22,2
19,052		18,637	33, 313	72,515	8.639	-81.139	-69.861	19.0
1100 19, 186 89, 344 76, 322 14, 324 -81, 165 -65, 629 13, 1200 19, 291 91, 018 77, 478 16, 248 -81, 213 -64, 216 11, 1300 19, 374 92, 565 78, 580 18, 18 -81, 285 -62, 798 10, 1400 19, 440 94, 004 79, 631 20, 122 -81, 380 -61, 373 91, 1500 19, 494 95, 347 80, 634 22, 069 -81, 489 -59, 940 8, 1500 19, 494 95, 347 80, 634 22, 069 -81, 489 -59, 940 8, 1500 19, 576 97, 792 82, 512 25, 977 -81, 808 -77, 049 77, 100, 19, 576 97, 792 82, 512 25, 977 -81, 808 -77, 049 79, 191 83, 392 27, 936 -82, 106 -55, 566 6, 190 19, 657 100, 981 85, 049 31, 862 -82, 259 -34, 110 6, 100 19, 657 100, 981 85, 049 31, 862 -82, 259 -34, 110 6, 100 19, 657 100, 981 85, 049 31, 862 -82, 560 -51, 166 52, 100 19, 677 101, 400 85, 831 33, 829 -82, 860 -51, 116 53, 300 19, 677 101, 570 88, 891 31, 37, 768 -83, 221 -49, 597 4, 500 19, 677 100, 571 88, 801 33, 77, 68 -83, 221 -49, 597 4, 500 19, 677 100, 571 88, 801 33, 77, 788 -83, 221 -49, 597 4, 500 19, 677 100, 571 88, 801 33, 77, 788 -83, 221 -49, 597 4, 500 19, 774 105, 378 88, 691 41, 772 -84, 559 -44, 390 3, 980 19, 774 105, 378 88, 691 41, 772 -84, 559 -44, 390 3, 980 19, 774 105, 378 88, 691 41, 772 -84, 559 -44, 390 3, 980 19, 774 105, 378 88, 691 41, 772 -84, 559 -44, 390 3, 980 19, 776 105, 898 89, 984 45, 661 -85, 709 -44, 390 3, 980 19, 776 105, 898 91, 894 45, 661 -85, 709 -44, 390 3, 980 19, 776 105, 898 91, 180 49, 415 -86, 583 -18, 580 19, 776 108, 978 91, 180 49, 415 -86, 583 -18, 580 19, 776 108, 978 91, 180 19, 787 100, 844 91, 845 91, 846		18.876	85, 523			-81,133	-68,451	16.6
1200   19, 291   91, 018   77, 478   16, 248   -81, 213   -64, 216   11, 1300   19, 374   92, 565   78, 580   18, 18   -81, 285   -62, 788   10, 1400   19, 440   94, 004   79, 611   20, 122   -81, 1380   -61, 1373   91, 1500   19, 494   95, 347   80, 634   22, 069   -81, 489   -59, 940   8, 1500   19, 576   97, 792   82, 512   25, 977   -81, 808   -57, 049   7, 792   82, 512   25, 977   -81, 808   57, 049   7, 798   70, 799   70,	1000	19.052	87.521	75.110	12,412	-81,138	-67.041	14.6
1200   19,291   91,018   77,478   16,248   -81,213   -64,216   11,000   19,374   92,565   78,580   18,18   -81,285   -62,788   10,000   19,440   94,004   79,631   20,122   -81,380   -61,373   9,000   19,440   95,347   80,634   22,069   -81,489   -59,940   8,000   19,576   97,792   82,512   25,977   -81,808   -57,049   7,700   19,576   97,792   82,512   25,977   -81,808   -57,049   7,700   19,576   97,792   82,512   25,977   -81,808   -57,049   7,700   19,677   100,981   85,049   31,862   -82,559   -54,110   61,555   66,60   61,600   19,634   99,973   84,237   29,898   -82,259   -54,110   61,500   61,000   19,657   100,981   85,831   33,829   -82,580   -52,620   51,100   19,677   101,940   85,831   33,829   -82,540   -52,620   51,100   19,677   101,940   85,831   33,829   -83,221   -49,597   4.5,100   19,799   103,732   87,311   37,768   -83,624   -80,599   4.5,100   19,799   103,732   87,311   37,768   -88,624   -80,599   4.5,100   19,793   103,732   87,311   37,768   -88,624   -80,599   4.5,100   19,733   106,896   89,884   45,661   -85,709   -44,730   3.9,800   19,768   108,239   91,140   49,415   -86,353   -40,071   3.1,800   19,768   108,239   91,140   49,415   -86,353   -40,071   3.1,800   19,768   108,239   91,140   49,415   -35,633   -36,576   2.9,800   19,768   108,239   91,140   49,415   -35,633   -36,576   2.9,800   19,768   108,239   91,140   49,415   -35,633   -36,576   2.9,800   19,769   108,878   91,280   49,415   -35,633   -36,576   2.9,800   19,769   108,878   91,280   49,415   -35,633   -36,576   2.9,800   19,769   108,878   91,280   49,415   -36,635   -40,071   3.1,800   19,769   108,878   91,280   49,415   -35,633   -36,576   2.9,800   19,769   108,878   91,280   49,415   -35,633   -36,576   2.9,800   19,769   108,878   91,280   91,48	1100	19 186	RQ 344	76 322	14 324	-81 165	-65 629	13.0
1300   19, 374   92, 565   78, 580   18, 18   81, 1285   62, 788   10, 100   19, 400   49, 400   49, 400   47, 631   20, 122   81, 380   61, 373   39, 100   19, 494   95, 347   80, 634   22, 069   81, 489   59, 940   8.								
19,440   94,004   79,611   20,122   -81,180   -61,173   39,500   19,494   95,347   80,634   22,069   -81,489   -59,940   8.								
19, 494   95, 347   80,634   22,069   -81,489   -59,940   8.								
19, 576   97, 792   82, 512   25, 977   81, 808   57, 049   71, 709   71,								8.7
19, 576   97, 792   82, 512   25, 977   81, 808   57, 049   71, 709   71,	600	19,539	96, 606	81.593	24.021	-81.632	-58.496	7.0
19,607   98,912   83,992   27,936   82,016   .55,586   6,000   19,634   99,973   84,237   29,899   82,2259   .54,110   61,600   19,657   100,981   85,049   31,862   .82,540   .52,620   51,7   100,981   85,049   31,862   .82,540   .52,620   51,7   100   19,677   101,940   85,831   33,829   .82,2540   .52,620   51,7   100   19,694   102,856   86,584   35,798   .83,221   .49,597   .49,597   .49,590   19,709   103,732   87,911   37,768   .83,624   .48,659   .45,800   19,722   104,571   88,813   39,739   .84,072   .46,507   .42,900   .99,000   19,734   105,176   88,934   41,712   .84,559   .44,930   3,9   .90   .99,733   106,896   89,984   45,661   .85,709   .41,715   33,800   19,763   101,586   89,984   45,661   .85,709   .41,715   33,800   19,762   107,614   90,601   47,637   .86,535   .40,071   31,1890   19,768   108,239   91,140   49,415   .86,833   .36,576   2,9   .990   19,769   103,308   91,200   49,415   .93,633   .38,576   2,9   .990   19,769   103,308   91,200   49,415   .93,633   .38,576   2,9   .990   19,769   103,978   91,781   51,590   .94,128   .36,488   2,8   .28								
900 19,634 99,973 84,237 29,898 82,259 -54,110 6.7 100 19,657 100,981 85,049 31,862 -82,540 -52,620 5.7 100 19,677 101,940 85,831 33,829 -82,860 -52,620 5.7 200 19,694 102,856 86,584 35,798 -83,221 -49,597 4.5 200 19,709 103,732 87,311 37,768 -83,624 -48,059 4.5 200 19,722 104,571 88,013 39,739 -84,072 -46,507 4.2 200 19,734 105,376 88,691 41,712 -84,569 -44,930 3.9 200 19,744 106,150 89,348 43,686 -85,113 -43,334 3.6 200 19,762 107,614 90,601 47,637 -86,535 -40,071 3.1 200 19,762 107,614 90,601 47,637 -86,535 -40,071 3.1 200 19,768 108,239 91,140 49,415 -86,033 -38,576 2.9 200 19,768 108,239 91,140 49,415 -93,633 -38,576 2.9 200 19,769 108,308 91,200 49,613 -93,577 -38,384 2.8 200 19,769 108,308 91,200 49,613 -93,577 -38,384 2.8 200 19,776 108,978 91,781 51,590 -94,128 -16,468 2.6 200 19,787 110,255 92,896 55,547 -95,050 -32,598 2.2 200 19,787 110,255 92,896 55,547 -95,050 -32,598 2.2 200 19,787 110,255 92,896 55,547 -95,050 -32,598 2.2 200 19,787 110,255 93,953 59,505 -95,995 28,665 1.8 200 19,787 110,255 93,953 59,505 -95,995 28,665 1.8 200 19,803 113,129 94,461 61,485 -96,475 -26,670 1.4 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,803 113,129 95,441 65,466 -97,453 -22,655 1.3 200 19,804 117,609 98,901 99,808 113,130 0.18 200 19,805 113,130 99,809 110,100 99,809 110,100 99,809 110,100 99,809 110,100 99,809 110,100 99,809 110,100 99,809 110,100 99,809 110,100 99,809 110								
19,657   100,981   85,049   31,862   -82,540   -52,620   5.7								
200								5.75
200	100	19,677	101.940	85.831	33, 829	-82,860	-51.116	5. 31
19, 709								
19,722   104,571   88,013   39,739   -84,072   -46,507   4,2								
19,734								
19.753								3.92
19.753	600	19,744	106, 150	89.348	43,686	-85.113	-43, 334	3.64
880         19.762         107.614         90.601         47.637         -86.353         -40.071         3.1           880         19.768         108.239         91.140         49.415         -86.983         -38.576         2.9           890         19.769         108.308         91.200         49.615         -93.637         -38.384         2.8           900         19.769         108.308         91.200         49.613         -93.677         -38.384         2.8           100         19.776         108.978         91.781         51.590         -94.128         -36.468         2.6           100         19.782         109.626         92.346         53.568         -94.586         -34.531         2.4           100         19.782         110.864         93.432         57.526         -95.518         -30.634         2.0           100         19.797         111.455         93.953         59.505         -95.995         -28.665         1.8           100         19.797         111.455         93.953         59.505         -95.995         -28.665         1.8           100         19.801         112.586         94.957         63.466         -96.962         -24.667<	700	19.753	106.896	89.984				3. 37
890         19.768         108.239         91.140         49.415         -86.983         -36.576         2.9           890         19.768         108.239         91.140         49.415         -93.633         -38.576         2.9           8900         19.769         108.308         91.200         49.613         -93.577         -38.384         2.8           8000         19.776         108.978         91.781         51.590         -94.128         -36.468         2.6           8100         19.782         109.626         92.346         53.568         -94.586         -34.531         2.4           8100         19.787         110.255         92.896         55.547         -95.050         -32.598         2.2           8100         19.797         111.455         93.953         59.505         -95.915         -22.665         1.8           8100         19.805         112.028         94.461         61.485         -96.475         -26.670         1.6           8100         19.805         112.586         94.957         63.466         -96.962         -24.667         1.4           8100         19.805         113.329         95.441         65.446         -97.453	800	19.762						3.12
19.768	890	19.768	108, 239					2.91
900 19.769 108.308 91.200 49.613 -93.577 .38.384 2.8 000 19.776 108.978 91.781 51.590 -94.128 -36.468 2.6 100 19.782 109.626 92.346 53.568 -94.586 .34.531 2.4 100 19.787 110.255 92.886 55.547 -95.050 .32.598 2.2.2 100 19.792 110.864 93.432 57.526 -95.518 .30.634 2.0 100 19.797 111.455 93.953 59.505 -95.995 .28.665 1.6 100 19.801 112.028 94.461 61.485 -96.475 .26.670 11.66 100 19.805 112.586 94.957 63.466 -96.962 -24.667 1.49 100 19.809 113.129 95.441 65.446 -97.455 .22.655 1.3 100 19.812 113.657 95.913 67.427 -97.949 .20.626 11.16 100 19.815 114.172 96.375 69.409 -98.451 -18.584 1.04 100 19.815 114.674 96.826 71.390 -98.985 .16.528 0.99 100 19.821 115.163 97.267 73.372 -99.470 .14.461 0.77 100 19.823 115.641 97.699 75.354 -99.988 .12.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .12.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .12.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .12.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .12.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .10.0.881 0.52 100 19.823 115.641 97.699 75.354 -99.988 .10.0.881 0.52 100 19.823 115.641 97.699 75.354 -99.988 .10.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .10.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .10.382 0.64 100 19.823 115.641 97.699 75.354 -99.988 .10.382 0.64 100 19.825 116.107 98.122 77.337 -100.509 -10.281 0.52 100 19.827 116.563 98.536 99.325 -104.161 3.933 0.88 100 19.831 117.444 99.339 83.285 -102.114 -3.933 0.88 100 19.831 117.671 99.729 85.260 -102.662 -1.791 0.08 100 19.835 118.289 100.111 87.252 -103.219 0.370 -0.01 100 19.836 118.698 100.486 99.235 -104.161 3.957 0.071 100 19.841 120.234 101.371 95.187 -247.497 15.798 -0.66 100 19.843 120.623 102.261 99.155 -104.481 20.087 10.086 100 19.844 120.989 100.854 91.219 -245.488 3.957 0.071 100 19.845 121.347 102.932 103.124 -251.544 36.210 -1.41 100 19.845 121.347 102.932 103.124 -251.544 36.210 -1.41 100 19.847 122.383 103.893 109.078 -255.163 51.737 1.90 100 19.847 122.383 103.893 109.078 -255.163 51.737 1.90	890	19.768	108, 239		49,415	- 93, 633		2.91
100         19,776         108,978         91,781         51,590         -94,128         -36,468         2,6           100         19,782         109,626         92,346         53,568         -94,586         -34,531         2,4           100         19,787         110,255         92,886         55,547         -95,050         -32,598         2,2           100         19,792         110,864         93,432         57,526         -95,518         -30,634         2,07           100         19,797         111,455         93,953         59,505         -95,995         -28,665         1,8           100         19,801         112,028         94,461         61,485         -96,475         -26,670         1,61           100         19,805         12,586         94,957         63,466         -96,962         -24,667         1,49           100         19,809         113,129         95,441         65,446         -97,433         -22,655         1,31           100         19,812         131,674         96,375         69,409         -98,451         18,584         1,02           100         19,813         114,674         96,826         71,390         -98,958         -16,5	900	19.769						2.89
19, 787	000	19.776						2.65
19, 787	100	19.782	109, 626	92, 346	53, 568	-94,586	-34,531	2,43
100 19,792 110,864 93,432 57,526 -95,518 -30,634 2,01 19,801 19,801 112,028 94,461 61,485 -96,475 -26,670 1.6 1.6 1.6 1.6 1.6 1.6 1.6 1.6 1.6 1.6	200	19.787	110,255	92.896				2.22
19, 197	300	19.792	110.864	93.432	57.526	-95.518		2.02
19.801 112.028 94.461 61.485 -96.475 -26.670 1.66 19.805 112.586 94.957 63.466 -96.962 -24.667 1.47 100 19.809 113.129 95.441 65.446 -97.453 -22.655 1.31 100 19.812 113.657 95.913 67.427 -97.949 -20.626 1.16 100 19.815 114.172 96.375 69.409 -98.451 -18.584 1.00 100 19.818 114.674 96.826 71.390 -98.958 -16.528 0.90 100 19.821 115.163 97.267 73.372 -99.470 -14.461 0.77 100 19.823 115.641 97.699 75.354 -99.988 -12.382 0.64 100 19.825 116.107 98.122 77.337 -100.509 -10.281 0.52 100 19.827 116.563 98.536 79.319 -101.040 -8.180 0.40 100 19.829 117.009 98.941 81.302 -101.573 -6.066 0.29 100 19.831 117.444 99.339 83.285 -102.114 -3.933 0.18 100 19.831 117.444 99.339 83.285 -102.114 -3.933 0.18 100 19.835 118.289 100.111 87.252 -103.219 0.370 -0.01 19.835 118.289 100.111 87.252 -103.219 0.370 -0.01 19.835 118.988 100.725 90.525 -104.161 3.957 -0.17 100 19.837 118.938 100.725 90.525 -104.161 3.957 -0.17 100 19.841 120.234 101.573 93.167 -247.497 15.798 -0.66 19.843 120.625 102.263 99.155 -245.458 3.957 -0.17 100 19.844 120.234 101.320 97.171 -248.438 20.871 -0.85 100 19.843 120.625 102.263 99.155 -245.458 3.957 -0.17 100 19.844 120.234 101.320 97.171 -248.438 20.871 -0.85 100 19.845 12.347 102.932 103.124 -251.544 36.210 -1.417 100 19.846 12.0989 102.600 101.139 -250.458 31.086 -1.239 100 19.847 122.043 103.579 107.093 -253.800 46.551 -1.759 100 19.847 122.043 103.579 107.093 -255.163 51.737 -1.916	100	19.797	111.455					1.84
19,809	500	19.801	112,028	94.461	61.485	- 96, 475		1.66
19.809	500	19,805	112,586	94.957	63.466	- 96, 962	-24,667	1.49
19.812	700	19.809	113, 129	95.441	65.446	-97,453		1, 338
19.815	300	19.812	113.657	95.913	67.427	-97.949	-20,626	1.186
19.818 114.674 96.826 71.390 -98.958 -16.528 0.90  19.821 115.163 97.267 73.372 -99.470 -14.461 0.77  100 19.823 115.641 97.699 75.354 -99.988 -12.382 0.64  100 19.825 116.107 98.122 77.337 -100.509 -10.281 0.52  100 19.827 116.563 98.536 79.319 -101.040 -8.180 0.40  19.829 117.009 98.941 81.302 -101.373 -6.066 0.29  100 19.831 117.444 99.339 83.285 -102.114 -3.933 0.18  100 19.833 117.671 99.729 85.269 -102.662 -1.791 0.08  100 19.835 118.289 100.111 87.252 -103.219 0.370 -0.01  19.836 118.698 100.486 99.235 -103.786 2.533 -0.11  65 19.837 118.958 100.725 90.525 -104.161 3.957 -0.17  65 19.837 118.958 100.725 90.525 -104.161 3.957 -0.17  65 19.837 118.958 100.725 90.525 -245.458 3.957 -0.17  19.838 119.098 100.854 91.219 -245.745 5.710 -0.25  19.839 119.491 101.216 93.203 -246.600 10.746 -0.46  19.841 120.234 101.370 97.171 -248.438 20.871 -0.86  19.843 120.625 102.283 99.155 -249.245 25.969 -1.05  19.845 121.347 102.932 103.124 -251.544 36.210 -1.39  100 19.845 121.347 102.932 103.124 -251.544 36.210 -1.39  100 19.847 122.043 103.589 109.078 -255.163 51.737 -1.596	000	19.815	114, 172	96.375	69.409	- 98. 451		1.041
19.823 115.641 97.699 75.354 -99.988 -12.382 0.64 19.825 116.107 98.122 77.337 -100.509 -10.281 0.52 116.563 98.536 79.319 -101.040 -8.180 0.40 19.827 116.563 98.536 79.319 -101.573 -6.066 0.29 17.829 117.009 98.941 81.302 -101.573 -6.066 0.29 18.831 117.444 99.339 83.285 -102.114 -3.933 0.18 18.00 19.833 117.671 99.729 85.269 -102.662 -1.791 0.08 19.835 118.289 100.111 87.252 -103.219 0.370 -0.01 19.835 118.289 100.111 87.252 -103.219 0.370 -0.01 19.836 118.698 100.486 99.235 -103.786 2.553 -0.11 65 19.837 118.958 100.725 90.525 -104.161 3.957 -0.17 65 19.837 118.958 100.725 90.525 -104.161 3.957 -0.17 65 19.837 118.958 100.725 90.525 -245.458 3.757 -0.17 65 19.838 119.098 100.854 91.219 -245.745 5.710 -0.25 19.838 119.098 100.854 91.219 -245.745 5.710 -0.25 19.838 12.284 101.371 95.187 -247.497 15.798 -0.66 19.841 120.254 101.370 97.171 -248.438 20.871 -0.86 19.843 120.625 102.263 99.155 -249.245 25.969 -1.05 19.844 120.989 102.600 101.139 -250.958 31.086 -1.239 100 19.845 121.347 102.932 103.124 -251.544 36.210 -1.419 100 19.846 121.698 103.256 105.108 -255.686 41.371 -1.586 100 19.847 122.043 103.579 107.093 -255.163 51.737 -1.916	000	19.818	114.674	96.826	71.390	-98,958	-16.528	0,90
19.825								0.771
00         19.827         116.563         98.536         79.319         -101.040         -8.180         0.40           00         19.829         117.009         98.941         81.302         -101.573         -6.066         0.29           00         19.831         117.444         99.339         83.285         -102.114         -3,933         0.18           00         19.833         117.871         99.729         85.269         -102.662         -1.791         0.08           00         19.835         118.289         100.111         87.252         -103.219         0.370         -0.01           00         19.836         118.698         100.486         89.235         -103.786         2.533         -0.11           65         19.837         118.958         100.725         90.525         -104.161         3.957         -0.17           65         19.837         118.958         100.725         90.525         -104.161         3.957         -0.17           00         19.838         119.098         100.854         91.219         -245.458         3.757         -0.17           00         19.839         119.491         101.216         93.203         -246.600         10								0.644
00         19.829         117.009         98,941         81,302         -101,573         -6,066         0,29           00         19.831         117.444         99,339         83,285         -102,114         -3,933         0,18           00         19.833         117.671         99,729         85,269         -102,662         -1.791         0,08           00         19.835         118.289         100,111         87.252         -103,219         0,370         -0.01           00         19.835         118.698         100,486         89,235         -103,786         2,533         -0.11           65         19.837         118.958         100,725         90.525         -104.161         3,957         -0.17           65         19.837         118.958         100,725         90.525         -104.161         3,957         -0.17           65         19.837         118.958         100,725         90.525         -245.458         3,957         -0.17           65         19.837         118.958         100,725         90.525         -245.458         3,957         -0.17           60         19.838         119.098         100.854         91.219         -245.745         5								0,523
00								0,406
00         19.833         117.671         99.729         85.269         -102.662         -1.791         0.08           00         19.835         118.289         100.111         87.252         -103.219         0.370         -0.01           00         19.836         118.698         100.486         89.235         -103.786         2.533         -0.11           65         19.837         118.958         100.725         90.525         -104.161         3.957         -0.17           65         19.837         118.958         100.725         90.525         -104.161         3.957         -0.17           00         19.838         119.098         100.854         91.219         -245.458         3.957         -0.17           00         19.839         119.491         101.216         93.203         -246.600         10.746         -0.46           00         19.840         119.876         101.571         95.187         -247.497         15.798         -0.66           00         19.841         120.254         101.920         97.171         -248.438         20.871         -0.86           00         19.843         120.625         102.263         99.155         -249.245	00	19.829	117.009	98,941	81,302	-101,573	-6.066	0.295
000         19.835         118.289         100.111         87.252         -103.219         0.770         -0.01           000         19.836         118.698         100.486         89.235         -103.786         2.533         -0.11           65         19.837         118.958         100.725         90.525         -104.161         3.957         -0.17           65         19.837         118.958         100.725         90.525         -245.458         3.957         -0.17           000         19.838         119.098         100.854         91.219         -245.745         5.710         -0.25           000         19.839         119.491         101.216         93.203         -246.600         10.746         -0.46           000         19.840         119.876         101.571         95.187         -247.497         15.798         -0.66           000         19.841         120.254         101.320         97.171         -248.438         20.871         -0.86           000         19.843         120.625         102.263         99.155         -249.245         25.969         -1.05           000         19.844         120.989         102.600         101.139         -250.458 <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td></td> <td>0.187</td>								0.187
19,836 118,698 100,486 89,235 -103,786 2,533 -0.11 18,958 100,725 90.525 -104,161 3,957 -0.17 65 19,837 118,958 100,725 90.525 -245,458 3,957 -0.17 700 19,838 119,098 100,854 91,219 -245,745 5,710 -0.25 19,839 119,098 100,854 91,219 -245,745 5,710 -0.25 19,839 119,491 101,216 93,203 -246,600 10,746 -0.46 100 19,840 119,876 101,571 95,187 -247,497 15,798 -0.66 100 19,841 120,254 101,920 97,171 -248,438 20,871 -0.86 100 19,843 120,625 102,263 99,155 -249,245 25,969 -1.05 19,843 120,625 102,263 99,155 -249,245 25,969 -1.05 19,844 120,989 102,600 101,139 -250,958 31,086 -1,231 100 19,845 121,347 102,932 103,124 -251,544 36,210 -1,411 100 19,846 121,698 103,256 105,108 -255,686 41,371 -1,586 106 19,847 122,043 103,579 107,093 -255,163 51,737 -1,916								0.083
65 19.837 118.958 100.725 90.525 -104.161 3.957 -0.17 65 19.837 118.958 100.725 90.525 -245.458 3.957 -0.17 60 19.838 119.098 100.854 91.219 -245.745 5.710 -0.25  00 19.839 119.491 101.216 93.203 -246.600 10.746 -0.46  00 19.840 119.876 101.571 95.187 -247.497 15.798 -0.66  00 19.841 120.254 101.920 97.171 -248.438 20.871 -0.86  00 19.843 120.625 102.263 99.155 -249.245 25.969 -1.05  19.844 120.989 102.600 101.139 -250.458 31.086 -1.25  00 19.845 121.347 102.932 103.124 -251.544 36.210 -1.41  00 19.845 121.347 102.932 103.124 -251.544 36.210 -1.41  00 19.845 121.347 102.932 103.124 -251.544 36.210 -1.41  00 19.845 121.347 102.932 103.124 -251.544 36.210 -1.41  00 19.845 122.343 103.256 105.108 -252.686 41.371 -1.586								-0.017
65								-0.113
19.838 119.098 100.854 91.219 -245.745 5.710 -0.25  19.839 119.491 101.216 93.203 -246.600 10.746 -0.46  19.840 119.876 101.371 95.187 -247.497 15.798 -0.66  19.841 120.254 101.320 97.171 -248.438 20.871 -0.86  100 19.843 120.625 102.263 99.155 -249.245 25.969 -1.05  100 19.844 120.989 102.600 101.139 -250.458 31.086 -1.239  100 19.845 121.347 102.932 103.124 -251.544 36.210 -1.419  100 19.845 121.347 103.256 105.108 -252.686 41.371 -1.586  101 19.846 121.698 103.256 105.108 -252.686 41.371 -1.586  101 19.847 122.043 103.579 107.093 -253.890 46.551 -1.759								-0.174
19,839 119,491 101,216 93,203 -246,600 10,746 -0,46 19,840 119,876 101,571 95,187 -247,497 15,798 -0,66 19,841 120,254 101,920 97,171 -248,438 20,871 -0,86 19,843 120,625 102,263 99,155 -249,245 25,969 -1,05 19,844 120,989 102,600 101,139 -250,958 31,086 -1,239 19,845 121,347 102,932 103,124 -251,544 36,210 -1,419 100 19,845 121,698 103,256 105,108 -255,686 41,371 -1,589 100 19,847 122,043 103,579 107,093 -255,163 51,737 -1,916								-0.174
00     19,840     119,876     101,571     95,187     -247,497     15,798     -0.66       00     19,841     120,254     101,320     97,171     -248,438     20,871     -0.86       00     19,843     120,625     102,263     99,155     -249,245     25,969     -1.05       00     19,844     120,989     102,600     101,139     -250,458     31,086     -1,23       00     19,845     121,347     102,932     103,124     -251,544     36,210     -1,41       100     19,846     121,698     103,256     105,108     -252,686     41,371     -1,39       100     19,847     122,045     103,579     107,093     -253,890     46,551     -1,75       100     19,847     122,383     103,895     109,078     -255,163     51,737     -1,916	0.0							
00								
00 19.843 120.625 102.263 99.155 -249.245 25.969 -1.05 00 19.844 120.989 102.600 101.139 -250.458 31.086 -1.239 00 19.845 121.347 102.932 103.124 -251.544 36.210 -1.419 00 19.846 121.696 103.256 105.108 -252.686 41.371 -1.586 00 19.847 122.043 103.579 107.093 -253.890 46.551 -1.759 00 19.847 122.383 103.895 109.078 -255.163 51.737 -1.916								
19.844 120.989 102.600 101.139 -250.958 31.086 -1.239 100 19.845 121.347 102.932 103.124 -251.544 36.210 -1.419 100 19.846 121.698 103.256 105.108 -252.686 41.371 -1.586 100 19.847 122.043 103.579 107.093 -253.890 46.551 -1.759 100 19.847 122.383 103.895 109.078 -255.163 51.737 -1.916								
00' 19.846 121,696 103.256 105.108 -252,686 41,371 -1.586 00 19.847 122.043 103.579 107.093 -253,890 46,551 -1.754 00 19.847 122.383 103.895 109.076 -255,163 51,737 -1.916								-1.235
00" 19.846 121,696 103,256 105,108 -252,686 41,371 -1.586 10 19.847 122,043 103,579 107,093 -253,890 46,551 -1.756 10 19.847 122,383 103,895 109,078 -255,163 51,737 -1.916	00	19,845	121, 347	102, 932	103.124	-251, 544	36, 210	-1,413
0C 19.847 122.043 103.579 107.093 -253.890 46.551 -1.754 0D 19.847 122.383 103.895 109.078 -255.163 51.737 -1.916					105.108	- 252, 686	41.371	-1.586
00 19.847 122,383 103.895 109.078 -255,163 51,737 -1,916		19.847	122.043	103,579		-253,890		-1.754
								-1.916
	00	19.848	122,716	104.206				-2.075
-								
·								

Molecular configuration

Planar, symmetrical, cart-wheel molecule with

$$\angle$$
 O - Mo - O = 120 deg.  
 $r_0 = 1.73\text{Å}$ .

Product of moments of inertia

$$I_A I_B I_C = 3392032 \times 10^{-120} g^3 cm^6$$
.

Symmetry number

 $\theta = 6$ .

Fundamental frequencies

$$\omega_1 = 800 \text{ cm}^{-1}$$
 $\omega_2 = 344 \text{ cm}^{-1}$ 
 $\omega_3 = 897 \text{ cm}^{-1}$  (2)
 $\omega_4 = 317 \text{ cm}^{-1}$  (2).

Ground electronic state

1

These molecular constants were estimated by the procedures employed in the case of the corresponding  $\text{CrO}_3$  molecule (see section IV-B3b). The Mo-Obond distance was assumed to be the same as the estimated distance for the corresponding bond in MoO  $^{413}$ ; i.e., 1.73Å.

The standard enthalpy of formation,  $\Delta H_{f298}^{O}$ , of gaseous  $M_{OO_3}$  had not been directly determined but could be indirectly evaluated by two calculations similar to those described in connection with  $M_{OO_2}$ ; see section IV-B5c(2).

The first calculation was based on the mass spectrographic study of  ${\rm Al_2O_3}$  reported by DeMaria and co-workers  $^{410}$  using molybdenum crucibles. These workers measured the partial pressures of  ${\rm MoO_3}$  and monatomic oxygen in equilibrium with solid molybdenum at

several temperatures in the range from  $2200^{\circ}$  to  $2500^{\circ}$ K. From the partial pressures of these workers, the equilibrium constant, K, and the standard free-energy change,  $\Delta F^{\circ}$ , for reaction (219) could be evaluated

$$Mo_{(s)} + 3O_{(g)} \longrightarrow MoO_{3(g)}$$
 (219)

$$K = \frac{P_{MoO_{3(g)}}}{P_{O_{(g)}}^3}$$
 (220)

as explained in section IV-B5a for the case of MoO.

A value of  $\Delta H^0$  for the above reaction was calculated at each temperature for which a measured pressure was reported by the Third Law Method as explained in section IV-B5a which takes the form of equation (221).

$$\frac{\Delta H_{298}^{\circ}}{T} = \frac{\Delta F^{\bullet}}{T} - \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{MoO_{3(g)}} + \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{Mo_{(g)}} + 3\left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{O_{(g)}}$$
(221)

The values of the free-energy functions for  $MoO_{3(g)}$ ,  $Mo_{(s)}$  and  $O_{(g)}$  were taken from Tables LXVI, XXVIII, and XXV of this report. The average value of  $\Delta$   $H^{O}_{298}$  was then combined with the heat of dissociation of oxygen gas ( $O_2$ ) to yield the heat of formation of gaseous  $MoO_3$ , in accordance with the reaction scheme at 298.15°K

$$Mo(s) + 3O(g) \longrightarrow MoO_{3(g)}$$
 (222)

$$(3/2) O_{2(g)} \longrightarrow 3O_{(g)}$$
 (223)

$$Mo_{(g)} + (3/2) O_{2(g)} \longrightarrow MoO_{3(g)}$$
 (224)

The first value of the heat of formation so obtained was  $-77,100 \pm 3000 \text{ cal/gfw at } 298.15^{\circ}\text{K}$ .

Likewise the second calculation was based on the mass spectrographic study of the gaseous species above solid  $MoO_2$  reported by

Burns and co-workers.  $^{418}$  Partial pressures of  $_{3(g)}$  in equilibrium with  $_{602(s)}$  and  $_{6(s)}$  were reported at several temperatures in the range from  $1560^{\circ}$  to  $1780^{\circ}$ K. From these measured pressures, the standard free-energy change,  $_{\Delta F^{\circ}}$ , at each temperature was calculated for reaction (225)

$$(3/2) \text{MoO}_{2(s)} \longrightarrow \text{MoO}_{3(g)} + (1/2) \text{Mo}_{(s)}$$
 (225)

by methods already described in connection with MoO and  $\,\text{MoO}_2\,$  . Values of  $\,\Delta\,H^O_{298}\,$  corresponding to each calculated  $\Delta F^o$  value calculated by means of equation (226).

$$\frac{\Delta H_{298}^{\circ}}{T} = \frac{\Delta F^{\circ}}{T} - \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{MoO_{3(g)}} - (1/2) \left(\frac{F_{T}^{\circ} - H_{298}^{\circ}}{T}\right)_{Mo(s)}$$

+ 
$$(3/2) \left( \frac{F_T^{\circ} - H_{298}^{\circ}}{T} \right)_{MoO_{2(s)}}$$
 (226)

The values of the free-energy functions used for  $MoO_{3(g)}$ ,  $Mo_{(s)}$  and  $MoO_{2(s)}$  are given in Tables LXVI, XXVII, and LXIII of this report. The average of all the values of  $\Delta H^o_{298}$  for equation (225) was then combined with the heat of formation of solid  $MoO_2$  to yield the heat of formation of gaseous  $MoO_3$ , in accordance with the reaction scheme at 298.15°K,

$$(3/2) MoO_{2(8)} \longrightarrow MoO_{3(g)} + (1/2) Mo_{(8)}$$
 (227)

$$(3/2) Mo_{(a)} + (3/2) O_{2(g)} \longrightarrow (3/2) MoO_{2(g)}$$
 (228)

$$Mo_{(g)} + (3/2)O_{2(g)} \longrightarrow MoO_{3(g)}$$
 (229)

The second value of the heat of formation so obtained was -84, 900 + 1000 cal/gfw.

The average of the values obtained by two different methods for the heat of formation of gaseous  $MoO_3$  was -81,000  $\pm$  6000 cal/gfw. The value of  $H^0_{298}$  -  $H^0_{0}$  for  $MoO_{3(g)}$  was found to be 3227 cal/gfw.

Values of  $\Delta H_1^p$  ,  $\Delta F_2^p$  , and  $\log_{10} K_p$  were calculated by methods previously described.

# 6. Strontium Oxide (StO)

# a. Crystal Structure and Melting Point

Strontium oxide has a face-centered cubic (NaCl type) structure<sup>57</sup> at room temperature which was assumed to persist to the melting point. The thermal expansion was measured by Beals and Cook<sup>384</sup> up to 1500°K. The melting point of SrO was taken as 2690° ± 50°K from the results of Schumacher<sup>385</sup> (corrected to the International Temperature Scale of 1948).

# b. Thermodynamic Properties of the Condensed Phases

# l) Heat of fusion

The heat of fusion of SrO was assumed to be  $16.1 \pm 1.4$  Kcal/gfw from an estimated entropy of fusion of  $5.985 \pm 0.5$  Kcal/°K gfw. Kubaschewski and Evans <sup>182</sup> estimated the entropy of fusion to be 6.1 Kcal/°K gfw.

# 2) Entropy and heat content at 298. 15°K

The low-temperature heat capacity of SrO was measured by Anderson. He from these data,  $S^{O}_{298}$  was calculated to be 13.060  $\pm$  0.200 cal/ $^{O}$ K gfw.  $H^{O}_{298}$ - $H^{O}$  was found to be 2037.7 cal/gfw.

# 3) High-temperature heat content

The high-temperature heat content of SrO was measured by Lander<sup>388</sup> (298° to 1266°K). Kelley<sup>56</sup> fitted Lander's data in cal/gfw to equation (230).

$$H_T^{\circ} - H_{298}^{\circ} = 12.13T + 0.63 \times 10^{-3}T^2 + 1.55 \times 10^{5}/T - 4192$$
 . (230)

Equation (230) was adopted here and extrapolated to the melting point. An uncertainty of  $\pm$  3 percent was assigned to the enthalpy.

The heat capacity of liquid SrO was estimated to be 17.0 cal/°K gfw.

Thermodynamic functions of the condensed phases of SrO are given in Table LXVII. Analyses of the heat-of-formation data had not been completed at the time of report writing. Uncertainty estimates are summarized on the back of the table.

<sup>434</sup> Anderson, C. T., J. Am. Chem. Soc. 57, 429 (1935).

#### c. Thermodynamic Properties of the Ideal Molecular Gas

The thermodynamic functions of SrO gas were calculated with the computer program based on the treatment of the diatomic molecule outlined in section III-E of this report. The spectroscopic constants used for the electronic states (in units of cm<sup>-1</sup>) were:

Constant	χ'1Σ	Α'1Σ	в₁п	C'1Σ
E	. 0	10885.0	24004.0	28546. 4
ω <sub>e</sub>	653.47	619.6	520.0	480.2
ω <sub>e</sub> z <sub>e</sub>	3. 95	0.9	3.5	2.6
ω <sub>e</sub> y <sub>e</sub>	en en en			
B <sub>e</sub>	0.3379	0.3047	0.2936	0.2742
a <sub>e</sub>	0.0021	0.0011	0.0020	0.0021
γ <sub>e</sub>				
D <sub>e</sub> (×10 <sup>6</sup> )	0.42	3. 2	0.37	0.35
8	1	1	2	1

The above spectroscopic constants were not corrected to those appropriate for a naturally occurring isotopic mixture. Constants for the assumed ground state were from Kovacs and Budo, 435 and were practically identical to those given by Lagerquist and Selin. Constants for the A' state were from Almkvist and Lagerquist. The data of Mahanti and Lagerquist 390 were used for the B'state, and those of Lagerquist and Almkvist were used for the C'state. The results of the computation are given in Table LXVIII. H 298-H was calculated to be 2160.9 cal/gfw. Veits and Gurvich tabulated thermodynamic functions of SO(g) up to 3500°K using the first two electronic states

<sup>435</sup> Kovacs, I. and A. Budo, Ann. Physik 12, 17 (1953).

<sup>436</sup> Lagerquist, A. and L.E. Selin, Ark. Fys. 11, 323 (1956).

<sup>437</sup> Almkwist, G. and A. Lagerqvist, Ark. Fys. 1, 477 (1949).

<sup>438</sup> Mahanti, P.C., Phys. Rev. 42, 609 (1932).

<sup>439</sup> Lagerquist, A. and G. Almkvist, Ark. Fys. 8, 481 (1954).

CONDENSED PHASES

gfw = 103.63

m.p. = 2690° ± 50°K

fw = 103.6	53		m.p. = 26	90° ± 50°K			
	-	cel/°K gfv			Kcel/g	ΔF	`
T, *K	c <mark>p</mark>	54	$-(F_T^0 - H_{296}^0)/T$	$H_{\mathrm{T}}^{o} - H_{290}^{o}$	AH °	ΔF	Log
0	0.000	0.000	Infinite	-2.038			Infin
298.15	10.760	13.060	13.060	0.000			
300	10.784	13.126	13.060	0.020			
400	11.663	16.365	13.495	1.148			
500	12.138	19.024	14. 344	2.340			
600	12. 453	21. 267	15.316	3.571			
700	12. 694	23.205	16. 307	4.829			
800	12.894	24.914	17. 278	6.108			
862	13.006	25.881	17.863	6.912			
862	13.006	25.881	17.863	6.912			
900	13.071	26. 443	18. 213	7.407			
1000	13.233	27.829	19.107	8.723			
1045	13.303	28.413	19.495	9.320			
1045	13,303	28.413	19.495	9.320			
1100	13.386	29.098	19.958	10.054			
200	13.532	30.269	20.769	11.400			
300	13.674	31.358	21.542	12.760			
400	13.813	32.376	22. 280	14.135			
500	13.949	33,334	22.985	15.523			
600	14. 083	34. 239	23.661	16.925			
641	14. 138	34.596	23.929	17.504			
641	14. 138	34.596	23.929	17.504			
700	14. 216	35.097	24.309	18.340			
800	14.348	35.913	24.930	19.769			
900	14.479	36.693	25.530	21.210			
000	14.609	37. 439	26.107	22.665			
100	14. 739	38.155	26.663	24.133			
200	14.868	38.844	27, 202	25.613			
300	14.997	39.507	27.721	27.107			
400	15.125	40.148	28.226	28.613			
500	15. 253	40.769	28.716	30.132			
500	15.381	41.369	29. 191	31.664			
590	15.496	41.895	29.607	33.054			
590	17.000	47.880	29.607	49.154			
700	17.000	47.943	29.675	49.324			
300	17.000	48.561	30.338	51.024			
00	17.000	49.158	30.977	52.724			
000	17.000	49.734	31.593	54. 424			
100	17.000	50, 292	32.187	56.124			
200	17.000	50.832	32.762	57.824			
300	17.000	51.354	33.316	59.524			
100	17.000	51.862	33.855	61.224			
500	17.000	52. 355	34. 377	62.924			
500	17.000	52.834	34.883	64.624			
700	17.000	53.299	35.374	66.324			
00	17.000	53.753	35.852	68.024			
00	17.000	54. 194	36.316	69.724			
00	17.000	54.625	36.769	71.424			
			50				
		· ·					
•							

#### STRONTIUM OXIDE CONDENSED PHASES

#### SUMMARY OF UNCERTAINTY ESTIMATES

		ul/°K gfv —			Kcal/gfw-		_	
T, <b>°</b> K	,	s <sub>T</sub>	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH?	$\Delta F_f$	`	Log Kp
298.15	± .200	± .200·	± .200	± .000				•
1000	± .940	± .650	± .390	± .260	A settlement		,	
2000	±1.780	± .940	± .600	± .680				
2690	±2.680	±1.070	± .700	± .990				
2690	±1.000	±1.590	± .700	±2.390				
4000	±2.000	±2.190	±1.100	±4.350				

only. As in the case of the other alkaline earth oxides discussed in this report, the true ground state of SrO is in question. Further analysis of the effect of this uncertainty on the thermodynamic functions is required.

The review of the heat-of-formation data in the literature was not completed at the time of report writing.

gfw = 103.63

m.p. = 2690° ± 50°K

T, °A	c <sub>p</sub> *	cal/°K gfv	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	——Keal/giw — ΔΗ <sup>°</sup>	ΔΕ΄	Log K
0	0.000	0,000	Infinite	-2.161		•	Infini
298.15	7.910	54.961	54.961	0.000			mim
300	7.919		54-962	0.015			
400	8.309	57.342	55. 277	0.826			
500	8.501	59, 215	55.883	1.666			
600	8.644	60.778	56.572	2.523			
700	8.742	62, 118	57. 271	3.393			
800	8.813	63.291	57.952	4.271			
862	* S. 845.	63.946	58.356	4.819			
862	8.846	63.946	58.356	4.819			
900	8.866	64.332	58.604	5. 155	•		
000	8.909	65.268	59.224	6.044			
.045	8.925	65.657	59.489	6.446			
045	8.925	65.657	59.489	6. 446			
100	8.944	66. 119	59.813	6.937			
200	8.974	66.899	60. 372	7.832			
300	9.001	67.618	60.902	8.731			
400	9.027	68. 286	61.406	9.633			
500	9.052	68.910	61.886	10.537			
600	9.077	69.495	62. 343	11.443			
641	9.088	69.722	62.522	11.816			
541 700	9.088	69.722	62.522	11.816			
700	9.103	70.046	62.780	12.352			
900	9.131	70.568	63. 199	13.264			
900 000	9.162 9.195	71.062 71.533	63.600 63.985	14.178 15.096			
000	7. 173	71.555	03.705	15.070			
100	9.231	71.983	64.356	16.017			
200	9.270	72.414	6 <b>4.</b> 713	16.942			
300	9.312	72.827	65.057	17.871			
100	9.357	73.225	65.389	18.805			
00	9.405	73.608	65.711	19.743			
00	9.455	73.978	66.022	20.686			
90	9.503	74. 301	66.294	21.539			
590	9.503	74.301	66. 294	21.539			
700	9.508	74.337	66.324	21.634			
00	9.564	74.684	66.617	22.588			
00	9.621	75.021	66.902	23.547			
000	9.681	75.349	67.179	24.512			
00	9.742	75.668	67.448	25. 483			
00	9.804	75.979	67.711	26.460			
00	9.868	76. 283	67.967	27.443			
00	9.933	76.579	68.216	28.433			
00	9.999	76.869	68.461	29.430			
00	10.066	77.153	68.699	30. 433			
00				31, 442			
	10.134	77.430	68.932				
00	10. 202	77.703 77.970	69.161 69.385	32. 459 33 <b>. 48</b> 2			
<b>00</b> 00	10. 272 10. 341	78. 232	69.604	34.513			
00	10. 341	16. 232	67.004	34. 313			
00	10.412	78.490	69.819	35.550			
00	10.483	78.743	70.030	36.594			
00	10.554	78.992	70. 237	37.645			
00	1C.626	79. 237	70.440	38.704			
00	10.699	79.478	70.640	39.769			
00	10.771	79.715	70.837	40.842			
00	10.844	79.950	71.030	41.92.			
00	10.918	80.180	71. 220	43.009			
00	10.991	80.408	71.408	44, 103			
00	11.065	80.633	71.592	45.205			
0.0	11 120	00.07		46 314			
00 00	11.139 11.214	80.855 81.074	71.774	46.314 47.430			
Çυ	11. 288	81.291	72.129	48.554			
00	11. 363	81.505	72. 304	49.685			
00	11. 437	81.716	72. 475	50, 824			
				£1 070			
00	11.512	81.925	72.645	51.970			
00	11.586	82.132	7.2. 813	51. 123			
00	11.661	82.337	72.978	54. 284			
00	11.736	82.540	73.142	55. 452 56. 627			
, ,	11.610	82.741	73, 303	30.021			

#### 7. Titanium Borides

#### Titanium Diboride

The available data on the thermodynamics of titanium diboride have been reviewed, and work was started on the preparation of tables of thermodynamic functions.

The value of the heat of formation of TiB2 has been subject to considerable uncertainty. The following values which range from -72 to -32 Kcal/mole have been reported:

Reference	ΛH° <sub>f298</sub> (Kcal/mole)
Brewer and Haraldsen 440	-72
Samsonov 441, 442	-70
Schissel and Williams 120	-32
Williams 443	<b>~</b> -50

Studies of the heat capacity had also been made, and reports containing  $C_p^o$  data in the temperature range from 300° to 1200° K were available. However, additional data were necessary at high temperatures, and determinations were instituted in Phase III of this project. The latter work is discussed in section V-B.

Investigators	Temperature Range (°K) for Available C° Data			
Margrave, et al 444 Krestovnikov and Vendrikh 445 Walker, Ewing, and Miller 446 Ihnat (section V-B of this report) Pears, et al 447	420-1180 300-1000 303-977 Up to 2400 Up to destruction temper- ature			

<sup>440</sup> Brewer, L. and H. Haraldsen, J. Electrochem. Soc. <u>102</u>, 399 (1955).

<sup>441&</sup>lt;sub>Samsonov</sub>, G.V., Zhur. Fiz. Khim. <u>30</u>, 2059 (1956). 442<sub>Samsonov</sub>, G.V., Zhur. Prik. Khim. <u>28</u>, 1018 (1955).

<sup>443</sup> Williams, W.S., Private Communication from P. Schissel.

<sup>444</sup> Margrave, J., D. Barnes, R. Mezaki, and R. Rutherford, Private Communication from J. Margrave.

<sup>445</sup> Krestovníkov, A.N. and M.S. Vendrikh, Thermodynamics of Titanium Diboride, Isv. Tevet. Metall. 2, 54 (1959); Henry Brutcher Transl. No. 4673.

<sup>446</sup> Walker, B., C. Ewing, and R. Miller, J. Phys. Chem. 61, 1682 (1957).

<sup>447</sup> Pears, C.D. and S. Oglesby, The Thermophysical Properties of Refractory Materials from 2000°F to Their Destruction Temperatures, Southern Research Inst. Quart. Rept. 2, for WADD AF33(616)-7319 (November 1960).

Final calculations of thermodynamic functions were postponed temporarily until more high-temperature heat capacity data become available because of uncertainties encountered in extrapolating existing data to high temperatures. It was also considered worthwhile to review carefully the literature that has been uncovered for other thermochemical data that might be used in obtaining a better estimate of the heat of formation.

# b. Other Borides $(Ti_2B, TiB, and Ti_2B_5)$

#### 1) Physical property and structural data

In the Ti-B system there are several phases of somewhat lower stability than  $\text{TiB}_2$  which are known. Hansen and Anderko have given much of the basic physical property and structural data on these compounds.

# a) Ti<sub>2</sub>B

The compound  $Ti_2B$  was reported to have a tetragonal structure. Its temperature range of stability was in some doubt but was considered to be in the range from 1800° to 2200°C.

#### b) TiB

Conflicting data existed for the crystal structure of TiB. The reported structures were a cubic structure of the zinc blende type, a cubic structure of the NaCl type, and an orthorhombic structure of the FeB type. The compound has been considered to be stable from room temperature up to  $\sim 2060^{\circ}$  C.

# c) $Ti_2B_5$

 $Ti_2B_5$  is reported to be hexagonal with a structure isotypic with that of  $\Psi_2B_5$ . No actual melting point data have been presented for this compound, but the melting point appears to be lower than that of  $TiB_2$ .

# 2) Thermodynamic data

Brewer and Haraldsen<sup>440</sup> have discussed the titanium boride compounds and set limits for their heats of formation. However, there were insufficient data available in general for thermodynamic function calculations to be undertaken.

# 8. Titanium Carbide (TiC)

Titanium carbide has long been used as a tool material because of its characteristic hardness. Its high-temperature stability and its low density have made it very useful for many high-temperature applications. Typical uses have been discussed by Schwarzkopf and Kieffer. 448

There have been several recent thermodynamic property compilations which included tables of data  $^{75}$ , 449, 450 for titanium carbide. However, experimental data have been reported since then which could affect these tables markedly. For example, Fujishiro and Gokcen  $^{451}$  have reported vaporization experiments yielding a heat of formation for TiC of  $\Delta H_{f298}^{\circ} = -31$ , 333 cal/gfw, whereas the earlier combustion experiments of Humphrey  $^{452}$  (used in the aforementioned tabulations) yielded a value of  $\Delta H_{f298}^{\circ} = -43$ , 800 cal/gfw.

The heat of formation of TiC is of considerable interest because of its usefulness in checking the heat of sublimation of Ti, which is uncertain, and because it can be used to evaluate the data of other refractories such as the titanium borides. It was therefore felt that a particularly careful evaluation of the heat of formation of TiC should be made. This evaluation was not complete at the time of report writing. Therefore, it was only possible to include the partial summary presented below.

#### a. Heat of Formation

#### 1) Direct determinations

Fujishiro and Gokcen's <sup>451</sup> and Humphrey's <sup>452</sup> heats of formation of TiC given above appeared to be the only directly measured values reported.

# 2) Equilibrium data based on the reduction of TiO2

The older work of Brantley and Beckman<sup>453</sup> has been often referred to as a source of thermochemical data for TiC. Those authors

<sup>448</sup> Schwarzkopf, P. and R. Kieffer, Refractory Hard Metals, Macmillan, N.Y. (1953).

Heckett, C.W. et al., Preliminary Report on the Thermodynamic Properties of Selected Light Element Compounds, Nat. Bur. Stds. Rept. 6928 (1 July 1960).

<sup>450</sup> Elliott, J.F. and M. Gleiser, Thermochemistry for Steel-making, vol. I., Addison-Wesley, Reading, Mass. (1960).

<sup>451</sup> Fujishiro, S. and N. Gokcen, J. Phys. Chem. 65, 161 (1961).

<sup>452</sup> Humphrey, G.L., J. Am. Chem. Soc. 73, 2261 (1951).

<sup>453</sup> Brantley, L.R. and A.O. Beckman, J. Am. Chem. Soc. 52, 3956 (1930).

determined the equilibrium pressure of CO in a system which initially contained TiO<sub>2</sub> and C at temperatures from 1278° to 1428°K. They felt that reaction (231) was the one occurring.

$$TiO_2 + 3C \iff TiC + 2CO$$
. (231)

Richardson<sup>454</sup> attempted to interpret their data but found it to yield free energies of formation equal to -64, 500 cal/gfw at 1200° K and -54, 480 cal/gfw at 1400° K. He concluded that their data must be in error or needed to be interpreted differently.

A more specific criticism of the Brantley and Beckman<sup>453</sup> work was made by Meerson and Krein <sup>455</sup> who stated that reaction (232) should be the final step.

$$TiO + 2C \Longrightarrow TiC + CO$$
 . (232)

Furthermore, they pointed out that TiO and TiC form a continuous series of solid solutions.

Kutsev and Ormont  $^{456}$  also conclude from high-temperature reduction studies in the range from 1880° to 2600°K that TiC and TiO form solid solutions. They stated that only three phases exist at equilibrium (i.e.,  $\text{TiC}_{\mathbf{x}}O_{\mathbf{y}}$ , C, and CO) at the temperatures and pressures of their experiments although they suggested that the existence of a fourth-phase  $\left(\text{Ti}_2\text{O}_3\right)$  might be possible at lower temperatures.

Because Brantley and Beckman 453 claimed to have identified TiO<sub>2</sub> in their equilibrium mixture, their paper was carefully reviewed. X-ray diagrams were reproduced in their figure 5. From an examination of this figure, it appeared that the observed lines could be ascribed to TiC and graphite and the existence of TiO<sub>2</sub> in their mixture seemed to be seriously in doubt. Brantley and Beckman's 453 results were therefore interpreted here as pertaining to the TiC<sub>x</sub>O<sub>y</sub>-C-CO system for which the equilibrium is given by reaction (233).

$$TiO_{(soln)} + C_{(s)} \longrightarrow TiC_{(soln)} + CO_{(g)}$$
 (233)

<sup>454</sup>Richardson, F.D., J. Iron Steel Inst. 175, 33 (1953).

<sup>455</sup> Meerson, G.A. and O.E. Krein, Russian J. Appl. Chem. 25, 143 (1952).

<sup>456</sup> Kutsev, V.S. and B.F. Ormont, Zhur. Fiz. Khim. 31, 1866 (1957).

Further thermodynamic calculations were not possible because concentrations or activities of the TiO and TiC in solution were not reported.

The results of Meerson and Krein<sup>455</sup> and Kutsev and Ormont<sup>456</sup> for the Ti-C-O system were being studied in more detail at the time of report writing to determine whether they could be used as a source of thermodynamic data.

# 3) Equilibrium data in the Ti-Ta-C system

Since the TiC and TaC compounds have approximately the same thermodynamic stabilities, a search of the literature was made for more specific data on the Ti-Ta-C system. The work of McMullin and Norton  $^{457}$  yielded an isothermal section of the ternary diagram at 1820°C. They found that three phases ( $\beta$ -y- $\delta$ ) coexisted in equilibrium. These phases had the following compositions in atomic percent:

Phase	Atomic percent Ta	Atomic percent Ti	Atomic percent C
β	60	38	2
у	67	0	33
δ	22	50	28

The  $\beta$ -phase is essentially a solid solution of Ta and Ti; the  $\gamma$ -phase is essentially Ta<sub>2</sub>C; and the  $\delta$ -phase is a solid solution of TiC-TaC. The equilibrium involved can be represented by reaction (234).

$$2Ta_{(\beta)} + TiC_{(\delta)} \stackrel{\longleftarrow}{\longleftarrow} Ta_2C_{(\gamma)} + Ti_{(\beta)} . \tag{234}$$

The following activities were calculated from Raoult's law applied to the components in high concentration in the solid solutions:

<sup>457</sup> McMullin, J.G. and J.T. Norton, J. Netals 5, 1205 (1953).

Phase	Composition	<sup>a</sup> Ta	a <sub>Ti</sub>	aTa <sub>2</sub> C	*TiC
β	Ta <sub>0.60</sub> Ti <sub>0.38</sub> C <sub>0.02</sub>	0.60	0.38		
y	Ta <sub>0.67</sub> C <sub>0.33</sub>			1	
δ	(TiC) <sub>0.28</sub> Ti <sub>0.22</sub> Ta <sub>0.22</sub> (TiC) <sub>0.388</sub> Ti <sub>0.305</sub> Ta <sub>0.305</sub>				0.388

The equilibrium constant in equation (235),

$$K = \frac{{}^{a}Ta_{2}C {}^{a}Ti}{{}^{a}TiC {}^{a}Ta} , \qquad (235)$$

is therefore equal to 2.77, and the standard free-energy change for reaction (234) is -4232 cal/gfw when calculated from equation (191).

Since equation (236) holds for reaction (234),

$$\Delta F^{\circ} = \Delta F_{Ti}^{\circ} + \Delta F_{Ta_{2}C}^{\circ} - \Delta F_{TiC}^{\circ} - 2\Delta F_{Ta}^{\circ} , \qquad (236)$$

and the free energies in the standard state are zero for the elements, equation (237) obtains.

$$\Delta F^{\circ} = \Delta F^{\circ}_{Ta_{2}C} - \Delta F^{\circ}_{TiC} \qquad (237)$$

Since Elliott and Gleiser  $^{450}$  have reported that  $\Delta F_{Ta_2C}^{\circ}$ ,  $_{2093}^{\circ}$ K = -31, 200 cal/mole, it was possible to calculate that  $\Delta F_{TiC,2093}^{\circ}$ K = -26, 968 cal/mole from equation (237). With the free-energy functions from the JANAF tables,  $^{75}$  it was then found that  $\Delta H_{298, TiC}^{\circ}$  = -33, 768 cal/mole.

The above analysis therefore gave a  $\Delta H_{298}^{o}$  value in good agreement with that of Fujishiro and Gokcen<sup>451</sup> of  $\Delta H_{298}^{o}$  = -31, 333. This provides evidence in support of the validity of their data rather than the heat-of-combustion data of Humphrey. <sup>452</sup> (At this stage, too much emphasis should not be placed on this analysis since further work is planned.)

The principal source of uncertainty in the latter analysis is the application of Raoult's law to the solid solutions. An analysis of the work in the Ti-C-O system by Kutsev and Ormont<sup>456</sup> may make possible an independent check of these results.

# b. Condensed Phase Data

# 1) Crystalline forms

TiC has a face-centered cubic structure of the NaC1 type. <sup>213</sup> The lattice parameter for the stoichiometric composition is  $a = 4.329 \pm 0.001 \text{ Å}$ .

#### 2) Phase-transformation temperatures

# a) Melting Point

Several reported melting points have been reviewed by Hansen and Anderko.  $^{213}$ 

m.p. (°C)	Reference
3160	Friederich and Sittig $^{458}$
3140	Agte and Moers <sup>459</sup>
3030	Geach and Jones 460
3250	Schwartzkopf and Kieffer 448

The average of these determinations is 3145°C (3418°K), and is in good agreement with the value (3410°K) used by the Bureau of Standards<sup>449</sup> and the JANAF tables.<sup>75</sup> The latter value was adopted and an estimated uncertainty of ± 100°K was assigned to it.

#### b) Boiling point

There were few published data regarding the boiling point of TiC. The National Research Council tables 461 listed a value

<sup>458</sup> Friederich, E. and L. Sittig, Z. anorg. Chem. 144, 171 (1925).

<sup>459</sup> Agte, C. and K. Moers, Z. anorg. Chem. 198, 233 (1931).

<sup>460</sup> Geach, G.A. and F.O. Jones, Plansee Proc. p. 80 (1955).

<sup>461</sup> Silverman, A., Data on Chemicals for Ceramic Use, Nat. Research Council Bull. 118 (June 1949).

of 4300°C (4573°K) but did not give an original reference. On the basis of the work of Fujishiro and Gokcen<sup>451</sup> and of Chupka, Berkowitz, Giese, and Inghram, <sup>462</sup> who showed that the primary vaporization products are the elemental species, it should be possible to calculate the temperature at which the decomposition pressure reaches one atmosphere.

#### Heat changes

#### a) Heat of fusion

Reports of experimental determinations of the heat of fusion of TiC were not found. Experimental measurements would be rather difficult to make because of the very high melting point of this compound. An NBS report gave an estimate of this quantity obtained on the assumption of an entropy of fusion of 2.5 e.u./g atom or 5 e.u./mole of TiC. On this basis, the heat of fusion was thus calculated to be 17,050 cal/mole. The latter value has been used in both the NBS 449 and JANAF tables 75 and was accepted here.

#### b) Heat of vaporization

Calculations of the heat of sublimation or vaporization can be made if the heat of formation of the compound is known together with the heats of sublimation of the elemental species. On the assumption that TiC dissociates into atoms (e.g., species such as C<sub>2</sub>, C<sub>3</sub> are neglected) and that  $\Delta H_{f_1}^{\circ}$  TiC, 298 = -43.8 Kcal/mole, NBS workers found a value of  $\Delta H_{sublimation, 298\,^{\circ}K}^{\circ}$  = 328.51 Kcal/mole. It is expected that this value will be lowered somewhat by the acceptance of a more positive value of the heat of formation.

#### 4) Heat capacity

#### a) Low-temperature data

Experimental heat capacity data by Kelley  $^{463}$  for the temperature range from 55° to 295°K have been analyzed by the NBS  $^{331}$  who found that  $S_{298}^{\circ} = 5.80 \pm 0.10$  e.u. This value was adopted for the present tabulation.

<sup>462</sup> Chupka, W.A., J. Berkowitz, C.F. Giese, and M.G. Inghram, J. Phys. Chem. 62, 611 (1958).

<sup>463</sup>Kelley, K.K., Ind. Eng. Chem. 36, 865 (1944).

# b) High-temperature data

The heat capacity data of Naylor 464 in cal/\* K gfw over the temperature range from 298° to 1735°K have been reviewed and accepted by Kelley 56 who gave equation (238)

$$C_p^{\circ} = 11.83 + 0.80 \times 10^{-3} \text{T} - 3.58 \times 10^5 \text{T}^{-2}$$
 (238)

for the temperature range from 298° to 2000°K.  $C_p^o$  data obtained on the present project are discussed in section V-B below and compared with data from other sources.

# c) Liquid heat capacity

The heat capacity of liquid TiC was reported by the NBS<sup>331</sup> to be the estimated value of 7.8 cal/g atom °K (15.6 cal/mole °K) at the melting point. It was felt here that their further assumption of a negative temperature coefficient was not sufficiently justified, and that a better choice will be possible when better data on the solid become available.

<sup>- 464</sup> Naylor, B.F., J. Am. Chem. Soc. 68, 370 (1946).

# 9. Titanium Oxides (TiO, Ti<sub>2</sub>O<sub>3</sub>, Ti<sub>3</sub>O<sub>5</sub>, and TiO<sub>2</sub>)

The Ti-O system is relatively complicated as indicated by its phase diagram.  $^{213}$  The known oxides of titanium for which data were available are TiO,  $\text{Ti}_2\text{O}_3$ ,  $\text{Ti}_3\text{O}_5$ , and  $\text{TiO}_2$ . A  $\delta$ -phase of approximately  $\text{Ti}_4\text{O}_3$  composition in the system had been reported, but its existence had not been established with certainty. The literature on the first four above-listed compounds was reviewed, and the data were under analysis at the time of report writing. Complete tables of thermodynamic function were under preparation for all solid phases.

# 10. Tungsten Oxides

The important oxides of tungsten for which thermodynamic properties have been compiled are tungsten monoxide (WO), tungsten dioxide (WO<sub>2</sub>), and tungsten trioxide (WO<sub>3</sub>). Although polymeric species of WO<sub>3</sub>; i.e., (WO<sub>3</sub>)<sub>3</sub>, (WO<sub>3</sub>)<sub>4</sub>, etc., are known to exist, virtually no thermodynamic data were available on them. Estimation of the thermodynamic properties of these polymeric species was not attempted.

# a. Tungsten Monoxide (WO)

Tungsten monoxide does not appear to exist in a pure condensed phase, but may be part of the solid oxide layer formed during surface oxidation of tungsten metal. The existence of WO in the gas phase at high temperatures has been verified by mass spectrographic work. Only the thermodynamic functions for gaseous WO are given in the present compilation. The thermodynamic functions for gaseous WO given in Table LXIX were calculated by means of the computer program described in section III-F with the following estimated molecular data:

## Bond distance

 $r_0 = 1.78\mathring{\Lambda}$ .

Moment of inertia

 $I = 77.426 \times 10^{-40} \text{ g cm}^2$ .

Symmetry number

 $\theta = 1$ .

Fundamental frequency

 $\omega = 803 \, \mathrm{cm}^{-1} \, .$ 

Ground electronic state

 $^{1}\Sigma$ 

# l) Bond distance

The  $\Psi$ -0 bond distance had not been experimentally determined. A value of 1.70Å had been calculated  $^{410}$  by means of the Guggenheimer relation  $^{465}$  and the estimated fundamental frequency of Vittalachar

<sup>465</sup> Guggenheimer, K. M., Proc. Phys. Soc. (London) 58, 456 (1946).

IDEAL MOLECULAR GAS

Reference State for Calculating  $\Delta H_{i}^{o}$ ,  $\Delta F_{i}^{o}$ , and  $Log~K_{p}$ : Solid W from 298.15° to 3650°K, Liquid W from 3650° to 5891°K, Gaseous W from 5891° to 6000°K; Gaseous O<sub>2</sub>; Gaseous WO.

gfw = 199.86

T, °K	C°P	ST	-(F <sub>T</sub> -H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	AH ?	ΔF	Log I
٠, ١	C <sup>b</sup>	5Т	-(FT - H <sub>298</sub> )/I	HT - H298	anı	art	Log
0	0.000	0.000	Infinite	-2.122	97.510	97.510	Infinit
298.15	7.601	56.597	56.597	0.000	97.400	90.166	-66.0
300	7.609	56.643	56.597	0.014	97.396	90.121	-65.6
400	7.990	58.888	56.900	0.795	97. 234	87.730	-47.9
500	8.252	60.701	57.485	1.608	97.081	85.362	-37.3
		7	27		-,,		
600 700	8. 428	62. 222	58.151	2. 443	96.931	83.044	-30.2
	8.547	63.531	58.828	3. 292	96.777	80.728	-25.2
800	8.631	64. 678	59.489	4.151	96.616	78.461	-21.4
900 000	8.691 8.736	65.698 66.616	60.123 60.728	5.017 5.889	96. 446 96. 273	76. 184 73. 962	-18.49 -16.16
000	0.130	00.010	00.720	3,007	70. 273	13.702	-10.10
100	8.770	67.450	61.301	6.764	96.088	71.717	-14.24
200	8.796	68.215	61.846	7,642	95.896	69.535	-12.66
300	8.817	68.920	62.363	8.523	95.689	67.319	-11.31
400	8.834	69.574	62.855	9.405	95.466	65.145	-10.16
500	8.847	70. 183	63.324	10.290	95.230	62.988	-9.17
600	8.859	70.755	63.771	11.175	94.973	60,843	-8.31
700	8.868	71. 292	64.197	12.061	94.701	58.721	-7.54
800							
	8.876	71.799	64.606	12.948	94.410	56.614	-6.87
9 <b>00</b> 000	8.883 8.888	72. 279 72. 735	64.997 65.373	13.836 14.725	94.104 93.780	54. 521 52. 444	-6. 27 -5. 73
	0.000	, ( ) )	031313	43.143	, , , , , , ,	JE. 777	-3.73
100	8.893	73.169	65.734	15.614	93.439	50. 387	-5.24
200	8.898	73.583	66.081	16.503	93.080	48.345	-4.80
00	8.901	73.978	66.416	17.393	92.705	46.320	-4.40
100	8.905	74.357	66.739	18.284	92.311	44.314	-4.03
00	8.908	74.721	67.051	19.174	91.900	42, 323	- 3.70
00	8.910	75.070	67, 353	20.065	91.472	40.347	- 3. 39
00	8.910	75.407	67.645	20. 956	91.472	38. 386	-3.10
00	8.915	75. 731	67.928	21.848	90. 565	36.445	-2.84
00	8.917 8.918	76.044 76.346	68.202	22.739	90.085	34.525 32.613	- 2. 60 - 2. 37
	0.410	70.340	68.469	23.631	89.588	32.013	-4. 111
00	8.920	76.638	68.7.38	24.523	89.075	30.724	-2.16
00	8.921	76.922	68.979	25.415	88,543	28.854	-1.97
00	8.922	77.196	69.224	26.307	87.995	26.994	-1.788
00	8.924	77.463	69.463	27.200	87.431	25, 153	-1.617
00	8.925	77.721	69.695	28.092	86.848	23.328	-1.457
00	8.926	77 071	. 0 . 0 . 1	10.005	04 340	31 (10	-1.307
50		77.973	69.921	26.985	86. 249	21.528	
	8.927	78.095	70.032	29.431	85.944	20.633	-1, 235
50	8.927	78.095	70.032	29.431	77.549	20.633	-1, 235
00	8.927	78. 217	70.142	29.877	77.250	19.851	-1.172
00	8.927	78.455	70.358	30.770	76.650	18.312	-1.053
00	8.928	78.687	70.569	31.663	76.049	16.774	-0.940
00	8.929	78.913	70.774	32.555	75.445	15.276	-0.835
00	8.930	79.134	70.976	33.448	74.840	13,768	- 0. 734
00	8.910	79.349	71.172	34. 341	74. 233	12. 247	-0.637
00	8.931	74.559	71. 365				-0.550
00				35.234	73.624	10.827	-0.465
00	8.931 8.932	79. 76 <b>4</b> 79. <b>9</b> 65	71.554 71.738	36.128 37.021	73.014 72.402	9.372 7.929	-0.385
	0.772	,	,0	,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,,		,.,	
00	8.932	80.161	71.919	37.914	71.787	6.509	-0,309
00	8.911	80. 153	72.097	38.807	71.169	5. 095	-0.237
00	8.933	80.542	72, 271	39.700	70.549	3.691	- 0. 168
00	8.913	80.726	72.441	40.594	69.926	2. 313	-0.103
00	8,934	80.906	72,609	41.487	69. 299	0.940	-0.041
00	8.914	81.083	72.773	42.381	68.668	-0.423	0.018
10	8.935	81.257	72.935	43.274	68.031	-1.768	0.074
00 0.	8.934	81.427	73.093	44.167	67. 187	- 3. 101	0.128
00	8.915	81.594	73,249	45.061	66.737	-4.417	0.179
0	8.915	81.758	73.402	45,954	66.078	-5.731	0.228
0	8.936	81.919 82.077	73,553 73,701	46.848	65.408 64.726	-7.034 -8.322	0. 274
				47.742	64.726		
0	8.936	82. 232	73.847	48.635	64. 027	-9, 593	0.361
1	8.936	82. 371	73.977	49.449	63.376	-10.739	0. 198
1	8.916	82. 171	73.977	49.449	-128.889	-10.739	0.398
0	8.936	82.385	73.990	49.529	-128.951	-10.567	0. 191
0	8.937	82.535	74.132	50.422	-129,663	~8.550	0, 311

and Krishnamurty. 466 A value of 1.78Å had been estimated for this distance by Brewer and Chandrasekharaiah. 401 The value 1.78Å was chosen for the present work.

# 2) Moment of inertia

The moment of inertia, I, was calculated from the assumed value for the  $\Psi$ -0 bond distance by means of equation (239)

$$I = \frac{M_{\overline{W}}M_{O}}{M_{\overline{W}} + M_{O}} r_{o}^{2} , \qquad (239)$$

where

 $M_{\overline{W}}$  = mass of tungsten atom

Mo = mass of oxygen atom

 $t_0 = \nabla \cdot 0$  bond distance.

# 3) Fundamental frequency

The fundamental frequency  $\omega$ , of WO had not been experimentally determined. An approximate band analysis by Vittalachar and Krishnamurty \$^{466}\$ was the basis for a suggested value of 1060 cm \$^{-1}\$. This same value was also used in a paper by Gatterer and Krishnamurty. \$^{467}\$ However, the 1060 cm \$^{-1}\$ value was estimated from a comparison with other transition monoxides, and the value employed for a key item in the comparison (i. e.,  $\omega$  for TaO) was incorrect. \$^{468}\$ Brewer and Chandrasekharaiah \$^{401}\$ estimated the fundamental frequency to be 803 cm  $^{-1}$ . The 803 cm  $^{-1}$  value was chosen in the present work as being more in accord with the postulate that the bonding in CrO, MoO, and WO are very similar. Mass effects alone would therefore indicate a frequency order of  $\omega_{\rm Cr} > \omega_{\rm Mo} > \omega_{\rm W}$ . In view of the large uncertainty associated with the value of  $\omega$ , no attempt was made to include anharmonicity and interaction terms in the calculation of thermodynamic functions for the WO molecule.

### 4) Electronic states

The electronic states of WO were unknown. As in the similar case of MoO, only the ground state was included; and it was assumed to be a  $^1\Sigma$  state.

<sup>466</sup>Vittalachar, V. and S. G. Krishnamurty, Current Sci. 23, 357 (1954).

<sup>467</sup> Gatterer, A. and S. G. Krishnamurty, Nature 169, 543 (1952).

<sup>468</sup>Premaswarup, D. and R. F. Barrow, Nature 180, 602 (1957).

The standard enthalpy of formation,  $\Delta H_{f\,298}^{O}$ , had not been directly determined. The value of  $\Delta H_{f\,298}^{O}$  was, therefore, determined by an indirect method identical to that employed in the case of MoO described in section IV-B5a of this report. The required partial pressures of WO and monatomic oxygen in equilibrium with solid tungsten were those measured by DeMaria and co-workers  $^{4\,10}$  in their mass spectrographic study of  $Al_2O_3$  in tungsten containers. The value of the heat of formation so obtained was  $+\,97,\,400\,\pm\,4500$  cal/gfw.  $H_{2\,98}^{O}-H_{0}$  for gaseous WO was found to be 2122 cal/gfw.

Values of  $\Delta H_f^0$ ,  $\Delta F_f^0$ , and  $\log_{10} K_p$  were calculated in a fashion identical to that described in section IV-B5a for the corresponding MoO molecule.

# b. Tungsten Dioxide (VO2)

# Condensed phase

The thermodynamic properties of solid  $wo_2$  have been based on the low-temperature heat capacity data of King, Weller, and Christensen,  $^{415}$  the high-temperature enthalpy data of the same workers, and the heat-of-formation data of Mah.  $^{469}$ 

The only experimental investigation of the low-temperature heat capacity of  $wo_2$  has been that of King, Weller, and Christensen<sup>415</sup> who made measurements over the temperature range from 52° to 297°K. Their data yield an  $S^o_{298}$  value of 12.08  $\pm$  0.07 e. u./gfw.

The only experimental high-temperature enthalpy data were those of King, Weller, and Christensen<sup>415</sup> (400° to 1800°K). The smoothed values reported by these workers were employed in the present compilation, except that those near room temperature were altered slightly to join the low-temperature data smoothly at 298. 15°K. Tabular entropy values were calculated by the procedure of Kelley. <sup>56</sup> The free-energy functions in Table LXX were calculated from equation (108). Heat capacity values were calculated from equation (240)

$$C_p^o = 15.49 + 3.58 \times 10^{-3} \text{T} - 2.80 \times 10^5 \text{T}^{-2}$$
 (240)

except for the values calculated near room temperature which were altered slightly to join the low-temperature data smoothly at 298. 15 K.

<sup>469</sup> Mah, A. D., J. Am. Chem. Soc. 81, 1582 (1959).

O<sub>2</sub>w

# TABLE LXX CONDENSED PHASE

TUNGSTEN DIOXIDE

# Reference State for Calculating $\delta H_1^0$ , $\delta F_1^0$ , and $\log \kappa_{p}=0$ : Solid W; Gaseous O2; Solid WO2.

gfw = 215.86

	cal/°K afw				Kcal	giv -	$\overline{}$	
T,°E	C <sub>P</sub>	s <sub>T</sub>	-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>	ΔH°	ΔF	Log Kp	
0	0.000	0.000	Infinite	-2.077	-139.747	-139.747	Infinite	
298.15	13.320	12.080	12.080	0.000	-140.940	-127.596	93.526	
300	13.350	12.162	12.080	0.025	-140.939	-127.513	92.889	
400	15.172	16. 266	12.618	1.459	-140.803	-123.041	67. 223	
500	16.160	19.767	13.707	3.030	-140.564	-118.636	51.853	
600	16.860	22.827	14.994	4.700	-140.257	-114.277	41.623	
700	17.425	25. 493	16. 293	6.440	-139.908	-109.977	34.335	
800	17.916	27.884	17.596	8.230	-139.538	-105.713	28.878	
900	18.366	30.026	18.859	10.050	-139.160	-101.524	24.652	
1000	18.790	31.975	20.075	11.900	- 38.770	-97.342	21.273	
1100	19. 197	33.767	21. 240	13.780	-138.369	-93.242	18.524	
1200	19.592	35.419	22.352	15.680	-137.963	-89.130	16. 232	
1300	19.978	36.965	23.419	17.610	-137.549	-85.107	14.307	
1400	20.359	38.417	24. 438	19.570	-137.126	-81.091	12.658	
1500	20.736	39.804	25.417	21.580	-136.673	-77.103	11.233	
1600	21.109	41.147	26. 359	23.660	-136.173	-73.150	9.991	
1700	21.479	42.468	27. 268	25.840	-135.593	-69.231	8.900	
1900	21.847	43.771	28.149	28.120	-134.935	-65.345	7.934	
1900	22. 214	45.058	29.005	30,500	-134.196	-61.499	7.074	
2000	22.580	46.330	29.840	32.980	-133.379	-57.692	6.304	

WO<sub>2</sub> does not exhibit a true melting point since disproportionation occurs to yield solid W and WO<sub>3</sub> vapor (probably including WO<sub>3</sub> polymeric species) before melting occurs. 470, 346

The standard enthalpy of formation,  $\Delta\,H^{O}_{f\,298}$  . of solid  $\text{WO}_2$  was determined by Mah $^{469}$  from the heats of combustion of  $\text{W}_{(s)}$  to  $\text{WO}_{3(s)}$  and of  $\text{WO}_{2(s)}$  to  $\text{WO}_{3(s)}$  . Mah's  $^{469}$  value of -140, 940  $\pm$ 210 cal/gfw was accepted in the present compilation. Other less accurate values have been reported by Delepine and Hallopeau,  $^{471}$  by Coughlin,  $^{472}$  and by Griffis.

Values of  $\Delta H_f^0$ ,  $\Delta F_f^0$ , and  $\log_{10} K_P$  were calculated from equations (44), (241), and (242).

$$\Delta H_{1}^{\circ} \sim \Delta H_{1298}^{\circ} + (H_{T}^{\circ} - H_{298}^{\circ})_{WO_{2(s)}} - (H_{T}^{\circ} - H_{298}^{\circ})_{W(s)} - (H_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}}$$
(241)

$$\Delta F_{f}^{\circ} = \Delta H_{f298}^{\circ} + (F_{T}^{\circ} - H_{298}^{\circ})_{\Psi O_{2(s)}} - (F_{T}^{\circ} - H_{298}^{\circ})_{\Psi(s)} - (F_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}}.$$
 (242)

# 2) Ideal gas

All of the molecular constants required in the calculation of the thermodynamic functions for gaseous  $wo_2$  have been estimated since no experimental spectroscopic data have been reported. The thermodynamic functions for gaseous  $wo_2$  given in Table LXXI were calculated by means of the machine program described in section III-F with the following molecular data:

Molecular configuration

Symmetrical, nonlinear molecule with

Product of moments of inertia

$$I_A I_B I_C = 880082 \times 10^{-120} g^3 cm^6$$
.

<sup>470</sup>Brewer, L., Chem. Revs. <u>52</u>, 1 (1953).

<sup>471</sup> Delepine, N. and L.A. Hallopeau, Compt. rend. 131, 186 (1900).

<sup>472</sup> Coughlin, J.P., U.S. Bur. Mines Bull. 542 (1954).

<sup>473</sup>Griffia, R.C., J. Electrochem. Soc. 106, 418 (1959).

<sup>474</sup>Griffie, R.C., J. Electrochem. Soc. 105, 398 (1958).

# IDEAL MOLECULAR GAS

Reference State for Calculating ΔH<sup>\*</sup><sub>2</sub>, ΔF<sup>\*</sup><sub>2</sub>, and Log K<sub>p</sub>: Solid W from 298.15° to 3650°K, Liquid W from 3650° to 5891°K, Gaseous W from 5891° to 6000°K; Gaseous O<sub>2</sub>: Gaseous WO<sub>2</sub>.

gfw = 215.86

T, *E  0 298.15 300 400 500 600 700 800 900 100 200 300 600 700 800 900 600 700 800 900 600 700 800 900	C*P 0.000 10.814 10.835 11.762 12.370 12.767 13.035 13.222 13.356 13.455 13.598 13.671 13.701 13.701 13.726 13.747 13.764 13.779 13.792	0.000 65.893 65.960 69.213 71.908 74.201 76.190 77.944 79.509 80.922 82.208 83.388 84.477 85.489 86.433 87.318 88.151 88.151	- (F° - H° 298)/T  Infinite 65.893 65.893 66.330 67.184 68.167 69.174 70.163 71.116 72.027 72.895 73.721 74.507 75.256 75.970 76.652	H <sub>T</sub> - H <sub>298</sub> -2.693 0.000 0.020 1.153 2.362 3.620 4.911 6.224 7.554 8.894 10.244 11.600 12.961 14.326 15.695	ΔH <sup>o</sup> <sub>4</sub> 14. 477 13. 900 13. 896 13. 731 13. 608 13. 503 13. 403 13. 296 13. 184 13. 064 12. 935 12. 797 12. 642 12. 470	ΔF <sub>f</sub> 14, 477 11, 200 11, 183 10, 314 9, 466  8, 659 7, 846 7, 074 6, 285 5, 546  4, 777 4, 067 3, 318	Log Kp Infinit -8. 205 -8. 146 -5. 635 -4. 019 -3. 154 -2. 456 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741 -0. 558
298.15 300 400 500 600 700 800 900 100 200 400 500 600 700 800 900 100 200 100 200 100 200	10.814 10.835 11.762 12.370 12.767 13.035 13.222 13.356 13.455 13.530 13.588 13.634 13.671 13.701	65.893 65.960 69.213 71.908 74.201 76.190 77.944 79.509 80.922 82.208 83.388 84.477 85.489 86.433	65. 893 65. 893 66. 330 67. 184 68. 167 69. 174 70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	0.000 0.020 1.153 2.362 3.620 4.911 6.224 7.554 8.894 10.244 11.600 12.961 14.326	13.900 13.896 13.731 13.608 13.503 13.403 13.296 13.184 13.064 12.935 12.797	11. 200 11. 183 10. 314 9. 466 8. 659 7. 846 7. 074 6. 285 5. 546	-8. 209 -8. 146 -5. 635 -4. 019 -3. 154 -2. 450 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741
300 400 500 600 700 800 990 000 100 200 400 500 600 700 800 990 000	10.814 10.835 11.762 12.370 12.767 13.035 13.222 13.356 13.455 13.530 13.588 13.634 13.671 13.701	65.893 65.960 69.213 71.908 74.201 76.190 77.944 79.509 80.922 82.208 83.388 84.477 85.489 86.433	65. 893 65. 893 66. 330 67. 184 68. 167 69. 174 70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	0,020 1,153 2,362 3,620 4,911 6,224 7,554 8,894 10,244 11,600 12,961 14,326	13. 896 13. 731 13. 608 13. 503 13. 403 13. 296 13. 184 13. 064 12. 935 12. 797 12. 642	11. 183 10. 314 9. 466 8. 659 7. 846 7. 074 6. 285 5. 546	-8. 146 -5. 635 -4. 019 -3. 154 -2. 456 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741
300 400 500 600 700 800 990 000 100 200 400 500 600 700 800 990 000	10.835 11.762 12.370 12.767 13.035 13.222 13.356 13.455 13.530 13.588 13.634 13.671 13.701;	65.960 69.213 71.908 74.201 76.190 77.944 79.509 80.922 82.208 83.388 84.477 85.489 86.433	65. 893 66. 330 67. 184 68. 167 69. 174 70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	0,020 1,153 2,362 3,620 4,911 6,224 7,554 8,894 10,244 11,600 12,961 14,326	13. 896 13. 731 13. 608 13. 503 13. 403 13. 296 13. 184 13. 064 12. 935 12. 797 12. 642	10. 314 9. 466 8. 659 7. 846 7. 074 6. 285 5. 546	-5. 639 -4. 019 -3. 154 -2. 450 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741
400 500 600 700 800 990 000 100 200 300 400 500 600 700 800 900 000	11. 762 12. 370 12. 767 13. 035 13. 222 13. 356 13. 455 13. 530 13. 588 13. 634 13. 671 13. 701;	69. 213 71. 908 74. 201 76. 190 77. 944 79. 509 80. 922 82. 208 83. 388 84. 477 85. 489 86. 433 87. 318 88. 151	66. 330 67. 184 68. 167 69. 174 70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	1, 153 2, 362 3, 620 4, 911 6, 224 7, 554 8, 894 10, 244 11, 600 12, 961 14, 326	13. 731 13. 608 13. 503 13. 403 13. 296 13. 184 13. 064 12. 935 12. 797 12. 642	9.466  8.659 7.846 7.074 6.285 5.546  4.777 4.067	-5. 639 -4. 019 -3. 154 -2. 450 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741
500 600 700 800 900 000 100 200 300 400 500 600 700 800 900 000	12. 370  12. 767 13. 035 13. 222 13. 356 13. 455  13. 530 13. 634 13. 671 13. 701: 13. 726 13. 747 13. 764 13. 779	71.908  74.201 76.190 77.944 79.509 80.922  82.208 83.388 84.477 85.489 86.433  87.318 88.151	67. 184  68. 167 69. 174 70. 163 71. 116 72. 027  72. 895 73. 721 74. 507 75. 256 75. 970	2.362 3.620 4.911 6.224 7.554 8.894 10.244 11.600 12.961 14.326	13, 608  13, 503  13, 403  13, 296  13, 184  13, 064  12, 935  12, 797  12, 642	9.466  8.659 7.846 7.074 6.285 5.546  4.777 4.067	-4. 019 -3. 154 -2. 450 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741
600 700 800 990 000 100 200 300 400 500 600 700 800 900	12. 767 13. 035 13. 222 13. 356 13. 455 13. 530 13. 588 13. 634 13. 671 13. 701 13. 726 13. 726 13. 747 13. 764 13. 779	74. 201 76. 190 77. 944 79. 509 80. 922 82. 208 83. 388 84. 477 85. 489 86. 433 87. 318 88. 151	68. 167 69. 174 70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	3.620 4.911 6.224 7.554 8.894 10.244 11.600 12.961 14.326	13. 503 13. 403 13. 296 13. 184 13. 064 12. 935 12. 797 12. 642	8.659 7.846 7.074 6.285 5.546	-3. 154 -2. 456 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741
700 800 990 000 100 200 300 400 500 600 700 800 900 000	13. 035 13. 222 13. 356 13. 455 13. 530 13. 588 13. 634 13. 671 13. 701 13. 726 13. 747 13. 746 13. 779	76. 190 77. 944 79. 509 80. 922 82. 208 83. 388 84. 477 85. 489 86. 433 87. 318 88. 151	69. 174 70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	4.911 6.224 7.554 8.894 10.244 11.600 12.961 14.326	13. 403 13. 296 13. 184 13. 064 12. 935 12. 797 12. 642	7.846 7.074 6.285 5.546 	-2. 450 -1. 932 -1. 526 -1. 212 -0. 949 -0. 741
800 920 000 100 220 300 400 500 600 700 800 900 000	13. 222 13. 356 13. 455 13. 530 13. 588 13. 634 13. 671 13. 701 13. 726 13. 747 13. 764 13. 779	77.944 79.509 80.922 82.208 83.388 84.477 85.489 86.433	70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	6. 224 7. 554 8. 894 10. 244 11. 600 12. 961 14. 326	13. 296 13. 184 13. 064 12. 935 12. 797 12. 642	7. 074 6. 285 5. 546 4. 777 4. 067	-1.932 -1.526 -1.212 -0.949 -0.741
800 920 000 100 220 300 400 500 600 700 800 900 000	13. 222 13. 356 13. 455 13. 530 13. 588 13. 634 13. 671 13. 701 13. 726 13. 747 13. 764 13. 779	77.944 79.509 80.922 82.208 83.388 84.477 85.489 86.433	70. 163 71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	6. 224 7. 554 8. 894 10. 244 11. 600 12. 961 14. 326	13. 184 13. 064 12. 935 12. 797 12. 642	6. 285 5. 546	-1.526 -1.217 -0.949 -0.741
990 000 100 200 300 400 500 600 700 800 900 000	13. 356 13. 455 13. 530 13. 588 13. 634 13. 671 13. 701 13. 726 13. 726 13. 747 13. 764 13. 779	79.509 80.922 82.208 83.388 84.477 85.489 86.433 87.318 88.151	71. 116 72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	7.554 8.894 10.244 11.600 12.961 14.326	13. 184 13. 064 12. 935 12. 797 12. 642	6. 285 5. 546	-1.526 -1.217 -0.949 -0.741
000 100 200 300 400 500 600 700 800 900 000	13. 455  13. 530 13. 588 13. 634 13. 671 13. 701:  13. 726 13. 747 13. 764 13. 779	80.922 82.208 83.388 84.477 85.489 86.433 87.318 88.151	72. 027 72. 895 73. 721 74. 507 75. 256 75. 970	8.894 10.244 11.600 12.961 14.326	13.064 12.935 12.797 12.642	5. 546 4. 777 4. 067	-1.217 -0.949 -0.741
200 300 400 500 600 700 800 900 000	13.588 13.634 13.671 13.701 13.726 13.747 13.764 13.779	83.388 84.477 85.489 86.433 87.318 88.151	73.721 74.507 75.256 75.970	11.600 12.961 14.326	12.797 12.642	4.067	-0.741
200 300 400 500 600 700 800 900 000	13.588 13.634 13.671 13.701 13.726 13.747 13.764 13.779	83.388 84.477 85.489 86.433 87.318 88.151	73.721 74.507 75.256 75.970	11.600 12.961 14.326	12.797 12.642	4.067	-0.74
300 400 500 600 700 800 900 000	13.634 13.671 13.701 13.726 13.747 13.764 13.779	84.477 85.489 86.433 87.318 88.151	74.507 75.256 75.970	12.961 14.326	12.642		
400 500 600 700 800 900 000	13.701; 13.726 13.747 13.764 13.779	85.489 86.433 87.318 88.151	75.256 75.970	14.326		3.318	
500 600 700 800 900 000	13.701; 13.726 13.747 13.764 13.779	86.433 87.318 88.151	75.970		12.470		
600 700 800 900 000	13.726 13.747 13.764 13.779	87.318 88.151		15.695		2.605	-0.407
700 800 900 000 100 200	13.747 13.764 13.779	88.151	26 652		12.282	1.908	-0.278
700 800 900 000 100 200	13.747 13.764 13.779	88.151		17.066	12.073	1. 222	-0.167
800 900 000 100 200	13.764 13.779		77.304	18.440	11.847	0.551	-0.071
900 000 100 200	13.779	55. V1/				-0.108	0. 013
000 100 200			77.929	19.816	11.601		
1 <b>00</b> 200	13.792	89.682	78.528	21. 193	11.337	-0.751	0.086
200		90.389	79.103	22. 571	11.052	-1.378	0.151
200	13.803	91.062	79.657	23.951	10.749	-1.991	0.207
	13.812	91.704	80.190	25.332	10.426	- 2. 592	0. 257
	13.820	92.319	80.704	26.713	10.084	-3.176	0.302
400	13.828	92.907	81.200	28.096	9.722	-3.744	0.341
500	13.834	93.472	81.680	29.479	9.340	-4. 298	0.376
600	13.840	94.014	82.144	30.863	8.939	-4.836	0.406
700	13.845	94.537	82.593	32. 247	8.518	-5.357	0,434
800	13.850	95.040	83.029	33.632	8.078	-5.863	0.458
900	13.854	95.526	83.452	35.017	7.618	-6.354	0.479
000	13.857	95.996	83.862	36.402	7.138	-6.828	0. 497
100	13.861	96. <b>4</b> 50	84. 261	37.788	6.640	-7.282	0.513
200	13.864	96.891	84.649	39.175	6.122	-7.725	0.528
						-8.158	
300	13.867	97.317	85.029	40.561	5. 586		0.540
400 500	13.869 13.871	97.731 98.133	85. 394 85. 752	41.948 43.335	5.030 4.456	-8.558 -8.946	0.550 0.559
600	13.874	98.524	86.101	44.722	3.862	-9.317	0.566
550	13.875	98.714	86. 272	45.416	3.559	-9 <b>.4</b> 97	0.569
650	13.875	98.714	36.272	45.416	-4.836	-9.497	0.569
700	13.876	98.904	86.442	46.110	-5.132	-9.561	0.565
300	13.877	99,274	86.775	47.497	-5.730	-9.671	0.556
900	13.879	99.635	87.100	48.885	-6.331	-9.770	0.547
000	13.881	99.986	87.418	50.273	-6.935	-9.844	0,538
				** ***			
100	13.882	100.329	87.729	51.661	-7.543	-9.918	0.529
00	13.883	100.664	88.033	53.049	-8.155	-9.962	0.518
00	13.885	100.990	88.330	54.438	-8.769	-9.989	0.508
00	13.886	101.309	88.622	55.826	-9.389	-10.014	0.497
00	13.887	101.622	88.907	57.215	-10.011	-10.026	0.487
00	13.888	101.927	89.187	58.604	-10.638	-10.014	0.476
00	13.889	102. 225	89.461	59.993	-11.270	-9.992	0.465
300	13.890	102.518	89.730	61.382	-11.908	-9.955	0.453
00	13.891	102.804	89.994	62.771	-12.552	-9.908	0.442
000	13.891	103.085	90. 253	64.160	-13.204	-9.845	0.430
00	11 601		- 00 507	66 640	13 046	0 777	0.410
00	13.892	103.360	90.507	65.549	-13.865	-9.772	0.419
00	13.893	103.630	90.757	66.938	-14.536	-9.682	0.407
00	13.894	103.894	91.002	68.327	-15.220	-9.577	0. 395
00	11.894	104.154	91. 244	69,717	-15.918	-9.466	0.383
00	13.895	104.409	91.481	71.106	-16.634	-9.339	0.371
00	13.895	104.659	91.714	72.496	-17.371	-9.201	0. 359
00	13.896	104.905	91.941	73.885	-18, 134	-9.040	9. 347
100	13.876	105.147	72.169	75. 275	-18.928	-8.874	D. 334
91	13.397	105. 364	92.371	76.540	-19.684	-8.701	0.343
91	13.897		92. 371	76. 540	-211.949	-8.701	0. 323
		105.364		76.665			
00	13.897	105. 385	92.391		-212.021	-8.396	0.311
00	13.897	105.618	92.609	78.054	-212.869	-4. 926	0.179

Symmetry number

 $\theta = 2$ 

Fundamental frequencies

$$\omega_1 = 794 \text{ cm}^{-1}$$

$$\omega_2 = 351 \text{ cm}^{-1}$$

$$\omega_3 = 812 \text{ cm}^{-1}$$
.

Ground electronic state

 $^{1}\Sigma$ 

# a) Molecular configuration

The molecular configuration of the WO<sub>2</sub> molecule was unknown. Consideration of the periodic group to which tungsten belongs and the work of Walsh<sup>395</sup> on bonding and structural relations led to the conclusion that WO<sub>2</sub> is a symmetric, nonlinear molecule, and it was so considered in the present work. DeMaria and co-workers <sup>410</sup> also assumed it to have a nonlinear structure, whereas Chandrasekharaiah and Brewer<sup>397</sup> assumed it to have the linear structure which they assumed for all of the Group IV, V, and VI transition metal dioxides. An O-W-O angle of 107 degrees was chosen in the present work as representing a reasonable value in comparison with known compounds of similar bonding. The W-O bond distance was assumed to be identical to the estimated corresponding distance for the tungsten monoxide (WO) molecule; i.e., 1.78A.

# b) Moments of inertia

The moments of inertia of  $wo_2$  were calculated in a manner analogous to that used for the corresponding  $CrO_2$  molecule.

### c) Fundamental frequencies

The fundamental frequencies of  $WO_2$  were estimated by the same method used for the corresponding  $CrO_2$  molecule (see section IV-B3a), except that the stretching force constant for WO was calculated from estimated spectroscopic data.  $^{401}$  The frequencies so obtained are somewhat lower than those estimated by DeMaria and co-workers.  $^{410}$ 

### d) Electronic states

The electronic states for  $w_{0_2}$  were treated in the same manner as those of the  $c_{r_{0_2}}$  molecule (section IV-B3a).

The standard enthalpy of formation,  $\Delta H_{f298}^{\circ}$ , of gaseous wo\_2 had not been directly determined. The value of  $\Delta H_{298}^{\circ}$  was, therefore, determined by an indirect method identical to that employed in the case of MoO\_2 (see section IV-B5b) based on the mass spectrographic study of Al\_2O\_3 in tungsten containers by DeMaria and coworkers. The value of  $\Delta H_{f298}^{\circ}$  so obtained was + 13, 900  $\pm$  5000 cal/gfw.  $H_{298}^{\circ}$ - $H_{0}^{\circ}$  for gaseous wo\_2 was found to be 2693 cal/gfw.

Values of  $\Delta H_f^o$ ,  $\Delta F_f^o$ , and  $\log_{10} K_P$  were calculated in an identical fashion to that described in section  $I\hat{V}$ -B5b for the corresponding  $MoO_2$  molecule.

# c. Tungsten Trioxide (WO3)

# 1) Condensed phase

# a) The 1050°K transition

Tungsten trioxide is monoclinic at room temperature but undergoes a transition to the tetragonal form at  $1050^{\rm o}$ K. A value of about  $725^{\rm o}$ C for the transition temperature has been quoted,  $346^{\rm o}$  but the recent work of King, Weller, and Christensen  $415^{\rm o}$  has established  $1050^{\rm o} \pm 10^{\rm o}$ K as the best value. The heat of transition, from enthalpy measurements on the two forms,  $415^{\rm o}$  was found to be  $410^{\rm o}$  cal/gfw. An uncertainty of  $\pm 40^{\rm o}$  cal/gfw has been arbitrarily assigned to the heat of transition.

# b) Melting point and heat of fusion

The works of Jaeger and Germs  $^{475}$  and of King and co-workers  $^{415}$  are in excellent agreement on the melting point of  $1745^{\circ} \pm 10^{\circ}$ K for wo3. The heat of fusion, as determined from enthalpy measurements,  $^{415}$  is 17.550 cal/gfw. An uncertainty of  $\pm 1000$  cal/gfw has been arbitrarily assigned to the heat of fusion.

<sup>475</sup> Jaeger, F.M. and H.C. Germs, Z. morg. Chem. 119, 149 (1921).

# c) Boiling point

The equilibrium vapor above WO<sub>3</sub> consists primarily of (WO<sub>3</sub>)<sub>3</sub>, (WO<sub>3</sub>)<sub>4</sub>, and (WO<sub>3</sub>)<sub>5</sub> according to Berkowitz, Chupka, and Inghram. Other investigations concerning the vapor pressure of WO<sub>3</sub> are those of Blackburn, Hoch, and Johnston, 417 and of Meyer, Oosterom and deRoo. No attempt has been made in the present work to define a boiling point for WO<sub>3</sub>. A temperature of about 2100°K has been quoted 470 as the temperature at which the total pressure above WO<sub>3</sub> becomes one atmosphere. No attempt was made to estimate thermodynamic functions for the polymeric vapor species.

# d) Entropy at 298.15°K

Low-temperature heat capacity data for  $\mathtt{WO}_{3(s)}$  have been reported by King, Weller, and Christensen,  $^{415}$  and by Seltz, Dunkerley, and DeWitt.  $^{429}$  The results of Seltz and co-workers were appreciably higher than those of King and co-workers, and were believed to be subject to some systematic error.  $^{415}$  The data of King and co-workers yielded an  $S_{298}^{\circ}$  value of 18.15  $\pm$  0.12 e. u.

# e) Thermodynamic properties

The only experimental high-temperature enthalpy measurements on WO<sub>3</sub> are those of King, Weller, and Christensen 415 over the temperature range from 400° to 1840°K. Equation (243) for the heat capacity in cal/°K gfw, derived from their enthalpy data for the monoclinic form of WO<sub>3</sub>,

$$C_p^o = 21.26 + 3.38 \times 10^{-3} T - 4.42 \times 10^5 T^{-2}$$
, (243)

was used to calculate  $C^{\circ}$  values from  $400^{\circ}$ K to the transition point ( $1050^{\circ}$ K). These values were then extrapolated to join the low-temperature heat capacity data smoothly at 298.15°K. Enthalpy and entropy values in the range from 298.15° to  $400^{\circ}$ K were determined by graphical integration with these extrapolated heat capacity values. Enthalpy and entropy values in units of calories,  $^{\circ}$ K, and moles were calculated at other temperatures up to the transition point from equations ( $\mathbb{Z}44$ ) and ( $\mathbb{Z}45$ ).

<sup>476</sup>Berkowitz, J., W.A. Chupka, and M.G. Inghram, J. Chem. Phys. 27, 85 (1957).

<sup>477</sup> Meyer, G., J.F. Oosterom, and J.L. deRoo, Rec. trav. chim. 78, 412 (1959).

$$H_T^{\circ} - H_{208}^{\circ} = .21.26T + 1.69 \times 10^{-3}T^2 + 4.42 \times 10^5 T^{-1} - 7962$$
 (244)

$$S_T^o = 21.26 \ln T + 3.38 \times 10^{-3} T + 2.21 \times 10^5 T^{-2} - 106.448$$
 (245)

Free-energy functions for monoclinic WO<sub>3</sub> were calculated in the usual manner.

Heat capacities of tetragonal  $WO_3$  in cal/°K gfw were calculated from the transition point (1050°K) to the melting point (1745°K) by means of equation (246) derived from the enthalpy data of King and co-workers.

$$C_p^{\circ} = 20.79 + 2.75 \times 10^{-3} T$$
 (246)

Enthalpy and entropy values in units of calories, <sup>O</sup>K, and moles were calculated for tetragonal tungsten trioxide from equations (247) and (248).

$$H_T^{\circ} - H_{298}^{\circ} = 20.79T + 1.375 \times 10^{-3}T^2 - 6290$$
 (247)

$$S_T^{\circ} = 20.79 \ln T + 2.75 \times 10^{-3} T - 101.928$$
 (248)

Free-energy functions were calculated from the enthalpy and entropy values in the usual manner.

The heat capacity of liquid  $WO_3$  was found to be 31.50 cal/ $^{O}K$  gfw;  $^{415}$  hence, enthalpy and entropy values in units of calories,  $^{O}K$ , and moles were obtained from equations (249) and (250).

$$H_T^{\circ} - H_{298}^{\circ} = 31.50 \text{ T} - 3242$$
 (249)

$$S_T^{\circ} = 31.50 \ln T - 167.017$$
 (250)

The thermodynamic functions of the condensed phases of  $\mathtt{WO}_3$  are summarized in Table LXXII.

# f) Standard heat of formation at 298.15°K ( $\Delta H_{f298}^{\circ}$ )

The standard enthalpy of formation,  $\Delta H_{f298}^{\circ}$  of solid WO<sub>3</sub> was determined by Mah<sup>469</sup> from the heat of combustion of tungsten metal. Mah's value of -201, 460 + 200 cal/gfw was accepted

CONDENSED PHASES

0,1

Reference State for Calculating  $\Delta H_1^o$ ,  $\Delta F_1^o$ , and  $Log K_p$ : Solid W; Gaseous  $O_2$ , Solid  $WO_3$  from 298.15° to 1745°K, Liquid  $WO_3$  from 1745° to 2000°K.

iw = 231.86	5	$T_{t}(I) = 10$	050° ± 10° K	m, p, = 1745	* ± 10 K		
,		l °K gf⊎			Kenl	gf =	
T, *K	C <sub>p</sub> *	ST	$-(F_{T}^{o}-H_{298}^{o})/T$	H <sub>T</sub> - H <sub>298</sub>	ΔH <sup>c</sup>	ΔF	Log K
0	0.000	0.000	Infinite	-2.962	-200.115	-200.115	Infinite
298.15	17.600	18.150	18.150	0.000	-201.460	-182.620	133.85
300	17.650	18. 259	18.150	0.033	-201.458	-182.503	132.94
400	19.849	23.663	18.870	1.917	-201.226	-176.205	96.26
500	21.182	28. 249	20. 299	. 3.975	-200.866	-169.999	74.30
600	22.060	32, 193	21961	6. 139	-200.443	-163.852	59.68
700	22.724	35.645	23.674	8.380	-199.982	-157.803	49. 26
800	23.273	38.716	25. 366	10.680	-199.501	-151.797	41.46
900	23.756	41.486	27.005	13.033	-198.996	-145.130	35. 24
1000	24.198	44.012	28.582	15.430	-198.473	-139.986	30.59
1050	24.408	45. 197	29. 344	16.646	-198.207	-137.085	28.53
1050	23.678	45.587	29.344	17.056	-197.797	-137.085	28.53
1100	23.815	46.691	30.106	18.243	-197.559	-134.200	26.66
1200	24.090	48.775	31.577	20.638	-197.082	-128.438	23.39
1300	24.365	50.714	32.975	23.061	-196.603	-122.764	20.63
1409	24.640	52.530	34.308	25.511	-196.122	-117.107	18.28
500	24.915	54. 239	35.580	27.989	-195.637	-111.479	16. 24
600	25.190	55.856	36.797	30.494	-195.150	-105.883	14.46
700	25.465	57.391	37.963	33.027	-194.659	-100.320	12.89
745	25. 589	58.058	38.473	34.176	-194.440	-97.833	12.25
745	31.500	68.115	38.473	51.726	-176.890	-97.833	12.25
800	31.500	69.093	39.394	53.458	-176.294	-95.344	11.57
900	31.500	70.795	41.001	56.608	-175.232	-90.871	10.45
2000	31.500	72.411	42.532	59.758	-174.195	-86.458	9.447

in the present compilation in preference to other, older, and less accurate values.  $471,\,472,\,478-486$ 

Values of  $\Delta H_f^{\circ}$   $\Delta F_f^{\circ},$  and  $\log_{10} K_P$  were calculated from equations (44), (251), and (252).

$$\Delta H_{f}^{\circ} = \Delta H_{f298}^{\circ} + (H_{T}^{\circ} - H_{298}^{\circ})_{WO_{3(c)}} - (H_{T}^{\circ} - H_{298}^{\circ})_{W(s)} - (3/2)(H_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}}$$
(251)

$$\Delta F_{f}^{\circ} = \Delta H_{f298}^{\circ} + (F_{T}^{\circ} - H_{298}^{\circ})_{\Psi O_{3(c)}} - (F_{T}^{\circ} - H_{298}^{\circ})_{\Psi(s)} - (3/2)(F_{T}^{\circ} - H_{298}^{\circ})_{O_{2(g)}}.$$
(252)

# 2) Gas phase

All of the molecular constants required in the calculation of the thermodynamic functions for gaseous wo<sub>3</sub> have been estimated since no experimental spectroscopic data have been reported. The thermodynamic functions for gaseous wo<sub>3</sub> given in Table LXXIII were calculated by means of the machine program described in section III-F with the following molecular data:

Molecular configuration

Planar, symmetrical cart-wheel molecule with

$$\angle O-W-O = 120 \text{ deg}$$
 $r_O = 1.78 \text{ Å}$ .

Product of moments of inertia

$$I_A I_B I_C = 4024423 \times 10^{-120} g^3 cm^6$$
.

<sup>478</sup>Huff, G., E. Squitieri, and P.E. Snyder, J. Am. Chem. Soc. 70, 3380 (1948).

<sup>479</sup> Delepine, M. and L.A. Hallopeau, Compt. rend. 129, 600 (1899).

<sup>&</sup>lt;sup>480</sup>Mixter, W., Am. J. Sci. <u>26</u>, 125 (1908).

<sup>481</sup> Weiss, L., A. Martin, and A. Stimmelmayer, Z. Anorg. u. Allgem. Chem. 65, 279 (1910).

<sup>482</sup> van Liempt, J.A.M., Z. Anorg, u. Allgem. Chem. 129, 263 (1923).

<sup>483</sup> Shibata, Z., Tech. Repts. Tohoku Imp. Univ. <u>8</u>, 129 (1929).

<sup>&</sup>lt;sup>484</sup>Shibata, Z., Tech. Repts. Tohoku Imp. Univ. <u>8</u>, 145 (1929).

<sup>485</sup>Gerasimov, Ya. I. and I.A. Vasil'eva, J. Chem. Phys. 56, 636 (1959).

<sup>486</sup> Vasil'eva, I. A., Y. Gerasimov, Ya. I. Simonov, and T. Rezukhina, Zhur. Fiz. Khim. 31, 682 (1957).

 $o_3 w$ 

Reference State for Calculating  $\Delta H_f^o$ ,  $\Delta F_f^o$ , and  $Log\,K_p$ : Solid W from 298.15° to 3650°K, Liquid W from 3650° to 5891°K, Gaseous W from 5891° to 6000°K; Gaseous O<sub>2</sub>; Gaseous WO<sub>3</sub>.

$ \begin{array}{c ccccccccccccccccccccccccccccccccccc$	_		al/°K gfw			Kcal	/4=	$\overline{}$
298.15	T, ° <b>K</b>			-(F <sub>T</sub> - H <sub>298</sub> )/T	H <sub>T</sub> - H <sub>298</sub>			Logi
14.972	0	0.000	0.000	Infinite	-3.296	-64.089	-64.089	Infin
16,514   73,253   59,234   1,608   -65,175   -59,970   22,000   18,113   80,299   71,809   5.094   -65,128   -57,401   22,000   18,133   83,124   73,228   6.927   -65,075   -56,131   1,608	298.15	14.936	68.626	68.626	0.000	-65.100	-61.309	44. 9
17. 487   77. 051   70. 428   3.311   -65.170   -58.703   21.	300	14.972	68.718	68.626	0.028	-65.103	-61.286	44.6
17. 487   77. 051   70. 428   3.311   -65.128   -57. 401   26. 600   18. 133   80. 299   71. 809   5. 094   -65.128   -57. 401   26. 700   18. 530   83. 124   73. 228   6. 927   -65. 075   -56. 131   17. 800   18. 618   85. 618   74. 624   8. 795   -65. 075   -56. 131   17. 800   19. 107   89. 860   77. 262   12. 598   -64. 981   -53. 591   13. 1000   19. 177   89. 860   77. 262   12. 598   -64. 981   -53. 591   13. 1000   19. 177   89. 860   77. 262   12. 598   -64. 945   -52. 306   11. 1000   19. 192   91. 693   78. 492   14. 522   -44. 920   -51. 065   10. 1000   19. 452   94. 930   80. 778   18. 398   -64. 946   -49. 782   98. 11. 1000   19. 452   94. 930   80. 778   18. 398   -64. 946   -49. 782   98. 11. 1000   19. 554   97. 721   82. 855   22. 299   -64. 967   -46. 301   6. 1000   19. 592   98. 985   83. 824   24. 256   -65. 109   -41. 500   6. 1000   19. 592   98. 985   83. 824   24. 256   -65. 109   -41. 500   5. 1000   19. 672   102. 559   86. 492   30. 147   -65. 333   -40. 941   4. 1000   19. 672   102. 559   86. 492   30. 147   -65. 333   -40. 941   4. 1000   19. 672   102. 559   86. 492   30. 147   -65. 333   -40. 941   4. 1000   19. 765   105. 447   88. 857   36. 037   -55. 6122   -37. 055   3. 3100   19. 755   105. 447   88. 857   36. 037   -55. 6122   -37. 055   3. 3100   19. 755   105. 477   90. 979   41. 979   -66. 525   -31. 093   2. 1000   19. 752   109. 291   92. 279   45. 932   -61. 098   -30. 391   2. 1000   19. 755   105. 545   91. 639   91. 639   91. 66. 525   -31. 093   2. 1000   19. 755   105. 546   91. 639   91. 639   -66. 620   -31. 749   2. 6000   19. 755   105. 546   91. 639   91. 65. 525   -31. 093   2. 6000   19. 755   105. 546   91. 639   91. 65. 525   -31. 093   2. 6000   19. 756   107. 770   90. 979   41. 979   -66. 525   -31. 093   2. 6000   19. 756   107. 770   90. 979   41. 979   -66. 525   -31. 093   2. 6000   19. 756   107. 770   90. 979   41. 979   -66. 525   -31. 093   2. 6000   19. 772   109. 291   92. 790   47. 999   -66. 525   -31. 093   2. 6000   19. 816   110.	400					-65.175	-59.990	32.7
18								25.6
18, 130	600	10 112	BO 200	71 900	E 004	45 120	.57 401	20.9
18.0   18.0   18.0   18.0   18.0   19.0   19.0   19.0   19.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   18.0   19.177   18.0   19.177   18.0   18.0   19.177   18.0   19.177   19.181   19.3   17.2   19.181   19.3   17.0   18.0   19.3   19.3   18.0   17.8   18.3   18.0   19.4   18.5   19.5   1								17.5
19, 025								
1900								14.9
1000 19, 292 91, 693 78, 492 14, 522 -64, 920 -51, 065 10 19, 381 93, 376 79, 663 16, 456 -64, 904 -49, 782 81 1300 19, 452 94, 930 80, 778 18, 398 -64, 906 -48, 549 8 1400 19, 508 96, 374 81, 841 81, 841 20, 346 -64, 927 -46, 031 6 1500 19, 554 97, 721 82, 855 22, 299 -64, 967 -46, 031 6 19, 592 98, 985 83, 824 24, 256 -65, 028 -44, 766 6 19, 592 98, 985 83, 824 24, 256 -65, 102 8 -44, 766 6 19, 592 100, 173 84, 752 26, 217 -65, 109 -43, 500 19, 623 100, 173 84, 752 26, 217 -65, 109 -43, 500 19, 672 102, 359 86, 492 30, 147 -65, 333 -40, 943 4000 19, 672 102, 359 86, 492 30, 147 -65, 343 -40, 943 4000 19, 672 102, 359 86, 492 30, 147 -65, 488 -19, 656 400 19, 708 104, 329 88, 899 34, 085 -65, 644 -38, 359 38, 200 19, 722 105, 247 88, 857 316, 057 -65, 812 -37, 055 31 300 19, 735 106, 124 89, 889 38, 029 -66, 641 -35, 742 3, 340 19, 718 106, 964 90, 299 41, 979 -66, 525 -33, 093 2, 000 19, 772 109, 291 92, 279 41, 979 -66, 525 -33, 093 2, 000 19, 772 109, 291 92, 279 45, 912 -67, 098 -10, 11, 749 2, 200 19, 772 109, 291 92, 279 45, 912 -67, 098 -10, 11, 749 2, 200 19, 779 110, 010 92, 900 47, 909 -67, 416 -69, 10, 391 2, 200 19, 786 110, 705 93, 502 49, 887 -67, 757 -27, 652 2, 2000 19, 786 110, 705 93, 502 49, 887 -67, 757 -27, 652 2, 2000 19, 805 111, 834 96, 269 59, 787 -69, 780 -20, 577 1, 1000 19, 809 113, 854 96, 269 59, 787 -69, 780 -20, 577 1, 1000 19, 809 113, 854 96, 269 59, 787 -69, 780 -20, 577 1, 1000 19, 819 115, 529 97, 764 65, 731 -79, 626 16, 608 0, 19, 818 115, 528 97, 521 64, 740 -70, 987 -16, 907 1, 1000 19, 829 117, 564 99, 598 73, 561 -88, 908 -21, 450 1, 1000 19, 824 116, 573 98, 79, 764 65, 731 -79, 626 16, 608 0, 19, 818 115, 528 97, 521 64, 740 -70, 987 -16, 907 1, 1000 19, 824 116, 573 98, 700 69, 695 -80, 623 12, 589 0, 000 19, 816 114, 488 97, 521 64, 740 -70, 987 -16, 907 1, 1000 19, 819 115, 529 97, 764 65, 731 -79, 626 16, 608 0, 1000 19, 818 115, 528 97, 521 64, 740 -70, 987 -16, 907 1, 1000 19, 844 120, 604 100, 604 100, 604 100, 604 100, 604 100, 604 100, 604 100, 604 100, 604								13.0
19, 181	.000	19.177	89.860	77. 262	12.598	-64.945	-52.396	11.4
19, 181	100	10 202	01 601	79 40 2	14 522	64 070	51 045	10.1
19, 452								9. 0
19,508   96.374   81.841   20,346   -64.927   -47.292   7.500   19.554   97.721   82.855   22.299   -64.967   -46.031   7.500   19.592   98.985   83.824   24.256   -65.028   -44.766   6.600   19.592   98.985   83.824   24.256   -65.028   -44.766   6.600   19.623   100.173   84.752   26.217   -65.109   -43.500   5.500   19.623   100.173   84.752   26.217   -65.109   -43.500   5.500   19.622   102.359   86.492   30.147   -65.333   -40.943   4.000   19.691   103.368   87.311   32.115   -65.478   -39.656   4.000   19.691   103.368   87.311   32.115   -65.478   -39.656   4.000   19.722   105.247   88.857   36.057   -65.812   -37.055   3.000   19.722   105.247   88.857   36.057   -65.812   -37.055   3.000   19.735   106.124   89.589   38.029   -66.041   -35.742   3.000   19.746   106.964   90.296   40.004   -66.271   -34.426   3.000   19.746   106.964   90.296   40.004   -66.271   -34.426   3.000   19.772   109.291   92.279   41.979   -66.525   -33.093   2.2880   19.777   110.010   92.900   47.909   -67.416   -29.028   2.2900   47.909   -67.416   -29.028   2.2900   19.786   110.705   91.502   49.887   -67.808   -10.391   2.2880   19.786   110.705   91.502   49.887   -67.816   -29.028   2.2900   19.801   112.653   95.208   55.826   -68.908   -24.856   1.000   19.805   113.262   95.7545   97.806   -68.109   -24.856   1.000   19.805   113.262   95.7545   97.806   -68.908   -24.856   1.000   19.805   113.262   95.7545   97.806   -68.908   -24.856   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   63.749   -70.246   -19.117   1.000   19.818   115.258   97.278   -35.866   -36.879   -36.6								
19,554   97,721   82,855   22,299   -64,967   -46,031   6								8.1
19. 592   98. 985   83. 824   24. 256   -65. 028   -44. 766   6								7.3
19.623   100.173   84.752   26.217   -65.109   -43.500   5	500	19.554	97.721	82.855	22, 299	-64.967	- <b>46.</b> 031	6.7
800 19.649 101.296 85.640 28.181 -65.211 -42.226 5900 19.672 102.359 86.492 30.147 -65.333 -40.943 4 4 1000 19.691 103.368 87.311 32.115 -65.478 -39.656 4 1 100 19.708 104.329 88.099 34.085 -65.644 -38.359 3 101.772 105.247 88.857 36.057 -65.832 -37.055 3 100 19.735 106.124 89.589 88.029 -66.041 -35.742 3 100 19.746 105.964 90.296 40.004 -66.271 -34.426 3 100 19.765 107.770 90.979 41.979 -66.525 -33.093 2 100 19.755 107.770 90.979 41.979 -66.525 -33.093 2 100 19.756 107.770 90.979 41.979 -66.525 -33.093 2 100 19.775 107.770 90.979 45.932 -67.098 -30.3191 2 100 19.772 109.291 92.279 45.932 -67.098 -30.3191 2 100 19.775 107.000 19.775 107.000 19.775 107.000 19.775 107.000 19.775 107.000 19.700 19.800 1								6.1
900 19.672 102.359 86.492 30.147 -65.333 -40.943 4 100 19.691 103.368 87.311 32.115 -65.478 -39.656 4 1100 19.708 104.329 88.099 34.085 -65.644 -38.359 3 100 19.722 105.247 88.857 36.057 -65.812 -37.055 3 100 19.735 106.124 89.589 38.029 -66.041 -35.742 3 100 19.746 106.964 90.296 40.004 -66.271 -34.426 3 100 19.756 107.770 90.979 41.979 -66.525 -33.093 2 100 19.765 108.545 91.639 41.979 -66.525 -33.093 2 100 19.772 109.291 92.279 45.932 -67.098 -30.391 2 100 19.772 109.291 92.279 45.932 -67.098 -30.391 2 100 19.779 110.010 92.900 47.909 -67.416 -29.028 2 19.790 19.791 111.375 94.037 51.866 -68.119 -26.265 1 100 19.797 112.024 94.655 53.846 -68.502 -24.856 1 100 19.797 113.262 95.745 57.806 -69.332 -22.4550 1 100 19.801 112.653 95.208 55.826 -68.908 -22.44.55 1 100 19.809 113.854 96.269 59.787 -69.780 -20.777 1 19.813 114.428 96.780 61.768 -70.246 -19.177 1 100 19.809 113.854 96.269 59.787 -69.780 -20.777 1 100 19.813 114.428 96.780 61.768 -70.98 -10.917 1 100 19.809 113.854 96.269 59.787 -69.780 -20.577 1 100 19.813 114.428 96.780 61.768 -70.246 -19.177 1 100 19.813 114.628 97.521 64.740 -79.932 -16.907 1 100 19.813 115.528 97.521 64.740 -79.932 -16.907 1 100 19.814 115.529 97.764 65.731 -79.626 -16.058 0 19.816 114.986 97.278 63.749 -70.736 -17.647 1 100 19.82 116.058 98.239 67.713 -80.621 -12.589 0 19.831 116.509 106.456 77.678 -80.623 -12.589 0 19.841 115.529 97.764 65.731 -79.626 -16.058 0 19.851 118.042 106.058 98.239 67.713 -88.148 1.000 1 19.879 117.056 99.155 71.678 -81.128 -10.836 0 19.831 118.042 100.012 98.576 -80.623 -12.589 0 19.841 12.654 100.012 98.7564 -83.739 -18.89 0 19.844 121.604 101.279 81.594 -83.739 -18.89 0 19.845 119.410 101.279 81.594 -83.739 -18.89 0 19.846 119.410 101.279 81.594 -83.739 -18.89 0 19.847 122.629 104.477 105.917 95.481 -87.722 11.149 -0.00 19.847 122.4755 100.419 91.94.52 2.80.577 5.504 0 19.844 121.504 103.561 93.498 -87.117 9.241 -0.00 19.847 122.4755 100.419 101.477 -91.116 20.822 -0.00 19.847 122.4755 100.219 109.198 -24.64.01 -0.01 19.852 124.755 100.219 109.198 -	700	19.623	100.173	84.752	26. 217	-65.109	-43.500	5. 5
900 19.672 102.359 86.492 30.147 -65.333 -40.943 4 0000 19.691 103.368 87.311 32.115 -65.478 -39.656 4 100 19.708 104.329 88.099 34.085 -65.644 -38.359 3 200 19.722 105.247 88.857 36.057 -65.812 -37.055 3 300 19.755 106.124 89.589 38.029 -66.041 -35.742 3 300 19.756 106.964 90.296 40.004 -66.271 -34.426 3 300 19.756 107.770 90.979 41.979 -66.525 -33.093 2 200 19.765 108.545 91.639 41.979 -66.525 -33.093 2 200 19.775 109.291 92.279 45.932 -67.098 -30.391 2 200 19.779 100.010 92.900 47.909 -67.416 -29.028 2 2000 19.791 111.375 94.037 51.866 -68.119 -26.265 1. 2000 19.797 112.024 94.655 53.846 -68.519 -26.265 1. 2000 19.801 112.653 95.208 55.826 -68.908 -22.4456 1. 2001 19.809 133.854 96.269 95.787 -69.780 -22.4450 1. 2001 19.809 133.854 96.269 95.787 -69.780 -20.771 1. 2001 19.809 133.854 96.269 95.787 -69.780 -20.771 1. 2001 19.809 133.854 96.269 95.787 -69.780 -69.780 -10.577 1. 2001 19.809 133.854 96.269 95.787 -69.780 -69.780 -10.577 1. 2001 19.809 133.854 96.269 95.787 -80.780 -10.577 1. 2001 19.809 133.854 96.269 95.787 -80.800 -10.577 1. 2001 19.809 133.854 96.269 95.787 -80.800 -10.577 1. 2001 19.819 115.529 97.764 65.731 -79.626 -16.058 0. 2001 19.816 114.428 97.521 64.740 -79.932 -16.907 1. 2001 19.816 114.658 98.299 67.713 88.1014 -79.626 -16.058 0. 2001 19.819 115.529 97.764 65.731 -79.626 -16.058 0. 2001 19.821 114.628 98.529 67.521 64.740 -79.932 -16.907 1. 2001 19.821 116.058 98.299 67.713 88.16.19 -70.736 -17.647 1. 2001 19.821 116.058 98.299 67.713 88.16.19 -70.736 -75.504 0. 2001 19.831 118.509 100.456 77.627 88.148 3544 0. 2001 19.841 120.691 102.452 87.545 88.184 3544 0. 2001 19.842 121.100 102.279 88.5501 -84.828 1.772 0. 2001 19.844 121.694 103.561 93.498 87.717 92.41 -0. 2001 19.844 121.694 103.561 93.498 87.717 92.41 -0. 2001 19.844 121.694 103.561 93.498 87.717 92.41 -0. 2001 19.844 121.694 103.561 93.498 87.717 92.41 -0. 2001 19.844 121.694 103.561 93.498 87.717 92.41 -0. 2001 19.844 121.694 103.561 93.498 -87.117 92.41 -0. 2001 19.845 122.279 103.917 95.481 -89.550 1. 2001 19.846 12	800	19 640	101 204	85 640	28 191	-65 211	-47 276	5. 14
19.69  103.368	900							4.70
200	000	19.691					-39.656	4. 33
200	100	19.708	104.329	88.099	34.085	-65.644	-38.359	3.94
19,735								3.68
19.746								3. 39
19.756								3. 13
19, 772   109, 291   92, 279   45, 932   -67, 098   -30, 191   2, 290   19, 779   110, 010   92, 900   47, 909   -67, 416   -29, 028   2, 1900   19, 786   110, 705   93, 502   49, 887   -67, 757   -27, 652   2, 1900   19, 791   111, 375   94, 037   51, 866   -68, 119   -26, 265   1, 1900   19, 801   112, 053   95, 208   55, 826   -68, 902   -24, 856   1, 1900   19, 805   113, 262   95, 745   57, 806   -69, 312   -22, 014   1, 1900   19, 805   113, 262   95, 745   57, 806   -69, 312   -22, 014   1, 1900   19, 809   113, 854   96, 269   59, 787   -69, 780   -20, 577   1, 1900   19, 813   114, 428   96, 780   61, 768   -70, 246   -19, 117   1, 1900   19, 818   115, 258   97, 521   64, 740   -70, 987   -16, 907   1, 19, 819   115, 258   97, 521   64, 740   -70, 987   -16, 907   1, 19, 819   115, 259   97, 764   65, 731   -80, 121   -14, 334   0, 19, 822   116, 058   98, 239   67, 713   -80, 121   -14, 334   0, 19, 822   116, 058   98, 239   67, 713   -80, 121   -14, 334   0, 19, 827   117, 075   99, 155   71, 678   -81, 128   -10, 836   0, 19, 831   118, 042   100, 032   75, 644   -82, 155   -7, 300   0, 19, 831   118, 042   100, 032   75, 644   -82, 155   -7, 300   0, 19, 831   118, 042   100, 032   75, 644   -82, 155   -7, 300   0, 19, 831   118, 042   100, 032   75, 644   -82, 155   -7, 300   0, 19, 831   118, 042   100, 032   75, 644   -82, 155   -7, 300   0, 19, 831   118, 042   100, 032   75, 644   -82, 155   -7, 300   0, 19, 831   118, 042   100, 032   75, 644   -82, 155   -7, 300   0, 19, 831   118, 042   100, 032   75, 044   -83, 739   -1, 899   0, 100   19, 838   119, 846   101, 677   83, 578   -84, 828   1, 772   -0, 100   19, 838   119, 846   101, 677   83, 578   -84, 828   1, 772   -0, 100   19, 849   120, 273   100, 69   85, 561   -84, 828   1, 772   -0, 100   19, 844   121, 691   102, 829   87, 510   -85, 949   54, 83   -0, 100   19, 844   121, 691   102, 829   87, 510   -85, 949   54, 83   -0, 100   19, 844   121, 691   102, 829   87, 510   -86, 526   73, 666   -60, 937   -60, 930   100, 852   124								2.89
19, 772	. 00	10 745	100 545	01 410	43.055	44 800	21 740	2.66
19, 779								2.46
19, 786								
19.791   111.375   94.037   51.866   -68.119   -26.265   1.								2. 26
100								2.08
19,801   112,653   95,208   55,826   -68,908   -23,450   1,	000	19. 791	111.3/5	74.03/	31.866	-08.119	- 40. 465	1.91
19,805								1.75
19.809								1.60
19.813								1.45
19.816								1.32
19,818	300	19.813	114.428	96.780	01. 768	- 70. 246	-19.117	1. 19
650         19.816         115.258         97.521         64.740         -79.382         -16.907         1.           700         19.819         115.529         97.764         65.731         -79.626         -16.058         0.           800         19.822         116.058         98.239         67.713         -80.121         -14.334         0.           800         19.824         116.573         98.702         69.695         -80.623         -12.589         0.           800         19.827         117.075         99.155         71.678         -81.128         -10.836         0.           100         19.829         117.564         99.598         73.661         -81.639         -9.077         0.           100         19.831         118.042         100.032         75.644         -82.156         -7.300         0.           100         19.833         118.509         100.456         77.627         -82.677         -5.504         0.           100         19.835         118.965         100.871         79.610         -83.207         -3.696         0.           100         19.836         119.410         101.279         81.594         -83.739         -1.899								1.07
19.819								1.01
19.822								1.01
1900	700	19.819	115.529	97.764	65.731	-79.626		0.94
1900         19.827         117.075         99.155         71.678         -81.128         -10.836         0.           100         19.829         117.564         99.598         73.661         -81.639         -9.077         0.           100         19.831         118.042         100.032         75.644         -82.156         -7.300         0.           100         19.833         118.509         100.456         77.627         -82.677         -5.504         0.           100         19.835         118.965         100.871         79.610         -83.207         -3.696         0.           100         19.836         119.410         101.279         81.594         -83.739         -1.899         0.           100         19.838         119.846         101.677         83.578         -84.279         -0.600         0.           100         19.839         120.273         102.069         85.561         -84.828         1.772         -0.           100         19.841         120.691         102.452         87.545         -85.84         3.634         -0.           100         19.842         121.100         102.829         89.530         -85.949         5.483	300	19.822	116.058	98.239	67.713	-80.121	-14.334	0.82
100 19.829 117.564 99.598 73.661 -81.639 -9.077 0. 1200 19.831 118.042 100.032 75.644 -82.156 -7.300 0. 1200 19.833 118.509 100.456 77.627 -82.677 -5.504 0. 1200 19.835 118.965 100.871 79.610 -83.207 -3.696 0. 1200 19.836 119.410 101.279 81.594 -83.739 -1.899 0. 1200 19.838 119.846 101.677 83.578 -84.279 -Ω.060 0. 1200 19.838 119.846 101.677 83.578 -84.279 -Ω.060 0. 1200 19.841 120.691 102.452 87.545 -85.384 3.634 -0. 1200 19.841 120.691 102.452 87.545 -85.384 3.634 -0. 1200 19.842 121.100 102.829 89.530 -85.949 5.483 -0. 1200 19.843 121.501 103.198 91.514 -86.526 7.365 -0. 1200 19.844 121.894 103.561 93.498 -87.117 9.241 -0. 1200 19.845 122.279 103.917 95.483 -87.722 11.149 -0. 1200 19.846 122.657 104.267 37.467 -88.348 13.054 -0. 1200 19.847 123.028 104.611 99.452 -88.995 14.980 -0. 1200 19.848 123.392 104.949 101.437 -89.667 16.918 -0. 1200 19.849 123.750 105.282 103.422 -90.373 18.855 -0. 1200 19.841 123.028 104.611 99.452 -88.995 14.980 -0. 1200 19.842 124.755 106.219 109.198 -92.677 24.613 -0. 121.850 124.755 106.219 109.198 -92.677 24.613 -0. 121.852 124.755 106.219 109.198 -92.677 24.613 -0. 121.852 124.755 106.219 109.198 -92.677 24.613 -0. 121.852 124.755 106.219 109.198 -92.677 24.613 -0.	00	19,824	116.573	98.702	69.695	-80.623	-12.589	0.70
19.83!   118.042   100.032   75.644   -82.156   -7,300   0,	000	19.827	117.075	99.155	71.678	-81.128	-10.836	0.59
100	00	19.829	117.564	99.598	73.661		-9.077	0.48
19.6   19.835   118.965   100.871   79.610   -83.207   -3.696   0.     19.836   119.410   101.279   81.594   -83.739   -1.899   0.     19.838   119.846   101.677   83.578   -84.279   -0.060   0.     19.839   120.273   102.069   85.561   -84.828   1.772   -0.     100   19.841   120.691   102.452   87.545   -85.384   3.634   -0.     100   19.842   121.100   102.829   89.530   -85.949   5.483   -0.     100   19.843   121.501   103.198   91.514   -86.526   7.365   -0.     19.844   121.694   103.561   93.498   -87.117   9.241   -0.     100   19.845   122.279   103.917   95.483   -87.722   11.149   -0.     19.846   122.657   104.267   37.467   -88.348   13.054   -0.     19.847   123.028   104.611   99.452   -88.995   14.980   -0.     19.848   123.392   104.949   101.437   -89.667   16.918   -0.     19.849   123.750   105.282   103.422   -90.373   18.855   -0.     19.851   124.447   105.931   107.392   -91.907   22.800   -0.     19.852   124.755   106.219   109.198   -92.677   24.613   -0.     19.852   124.755   106.219   109.198   -92.677   24.613   -0.     19.852   124.756   106.247   109.377   -285.015   25.087   -0.	00	19.83!	118.042	100.032	75.644	-82.156		0.38
19. 835 118. 965 100. 871 79. 610 -83. 207 -3, 696 0. 19. 836 119. 410 101. 279 81. 594 -83. 739 -1. 899 0. 100 19. 838 119. 846 101. 677 83. 578 -84. 279 -0.060 0. 19. 839 120. 273 102. 069 85. 561 -84. 828 1. 772 -0. 100 19. 841 120. 691 102. 452 87. 545 -85. 384 3. 634 -0. 19. 842 121. 100 102. 829 89. 530 -85. 949 5. 483 -0. 19. 842 121. 501 103. 198 91. 514 -86. 526 7. 365 -0. 19. 844 121. 501 103. 198 91. 514 -86. 526 7. 365 -0. 19. 845 122. 279 103. 917 95. 483 -87. 722 11. 149 -0. 19. 845 122. 279 103. 917 95. 483 -87. 722 11. 149 -0. 19. 846 122. 657 104. 267 37. 467 -88. 348 13. 054 -0. 19. 846 122. 657 104. 267 37. 467 -88. 348 13. 054 -0. 19. 848 123. 392 104. 611 99. 452 -88. 995 14. 980 -0. 19. 848 123. 392 104. 949 101. 437 -89. 667 16. 918 -0. 19. 849 123. 750 105. 282 103. 422 -90. 373 18. 855 -0. 19. 849 123. 750 105. 282 103. 422 -90. 373 18. 855 -0. 19. 851 124. 447 105. 931 107. 392 -91. 907 22. 800 -0. 19. 851 124. 447 105. 931 107. 392 -91. 907 22. 800 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 852 124. 755 106. 219 109. 198 -92. 677 24. 613 -0. 19. 198. 198. 198. 198. 198. 198. 198.	00	19.833	118.509	100.456	77.627	-82.677	-5.504	0.28
19,838 119,846 101,677 83,578 -84,279 -0,060 0, 19,839 120,273 102,069 85,561 -84,828 1,772 -0, 100 19,841 120,691 102,452 87,545 -85,384 3,634 -0, 100 19,842 121,100 102,829 89,530 -85,949 5,483 -0, 100 19,843 121,501 103,198 91,514 -86,526 7,365 -0, 100 19,844 121,894 103,561 93,498 -87,117 9,241 -0, 100 19,845 122,279 103,917 95,483 -87,722 11,149 -0, 100 19,846 122,657 104,267 37,467 -88,348 13,054 -0, 19,847 123,028 104,611 99,452 -88,995 14,980 -0, 19,848 123,392 104,949 101,437 -89,667 16,918 -0, 19,849 123,750 105,282 103,422 -90,373 18,855 -0, 19,840 124,101 105,609 105,407 -91,116 20,822 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0, 19,852 124,755 106,219 109,198 -92,677 24,613 -0,		19.835	118.965	100.871		-83.207		0.18
100         19,839         120,273         102,069         85,561         -84,828         1,772         -0,00           100         19,841         120,691         102,452         87,545         -85,384         3,634         -0,00           100         19,842         121,100         102,829         89,530         -85,949         5,483         -0,00           100         19,843         121,501         103,198         91,514         -86,526         7,365         -0,00           00         19,844         121,894         103,561         93,498         -87,117         9,241         -0,00           10         19,845         122,279         103,917         95,483         -87,722         11,149         -0,00           19,846         122,657         104,267         37,467         -88,348         13,054         -0,00           19,847         123,028         104,611         99,452         -88,995         14,980         -0,00           19,848         123,750         105,282         103,422         -90,373         18,855         -0,00           19,850         124,101         105,609         105,407         -91,116         20,822         -0,00           19,851	00	19.836	119.410	101.279	81.594	-83.739	-1.899	0.09
00         19,841         120,691         102,452         87,545         -85,384         3,634         -0.           00         19,842         121,100         102,829         89,530         -85,949         5,483         -0.           100         19,843         121,501         103,198         91,514         -86,526         7,365         -0.           00         19,844         121,694         103,561         93,498         -87,117         9,241         -0.           00         19,845         122,279         103,917         95,483         -87,722         11,149         -0.           00         19,846         122,657         104,267         37,467         -88,348         13,054         -0.           00         19,847         123,028         104,611         99,452         -88,995         14,980         -0.           00         19,848         123,392         104,949         101,437         -89,667         16,918         -0.           00         19,849         123,750         105,282         103,422         -90,373         18,855         -0.           00         19,850         124,101         105,609         105,407         -91,116         20,822								0.00
00         19.842         121.100         102.829         89.530         -85.949         5.483         -0.           100         19.843         121.501         103.198         91.514         -86.526         7.365         -0.           00         19.844         121.894         103.561         93.498         -87.117         9.241         -0.           00         19.845         122.279         103.917         95.483         -87.722         11.149         -0.           00         19.846         122.657         104.267         37.467         -88.348         13.054         -0.           00         19.847         123.028         104.611         99.452         -88.995         14.980         -0.           00         19.848         123.392         104.949         101.437         -89.667         16.918         -0.           00         19.849         123.750         105.282         103.422         -90.373         18.855         -0.           00         19.850         124.101         105.609         105.407         -91.116         20.822         -0.           00         19.851         124.447         105.931         107.392         -91.907         22.800								-0.08
1900         19.843         121,501         103,198         91,514         -86,526         7,365         -0.           100         19.844         121,894         103,561         93,498         -87,117         9,241         -0.           100         19.845         122,279         103,917         95,483         -87,722         11,149         -0.           100         19.846         122,657         104,267         37,467         -88,348         13,054         -0.           100         19.847         123,028         104,611         99,452         -88,995         14,980         -0.           100         19.848         123,392         104,949         101,437         -89,667         16,918         -0.           00         19.849         123,750         105,282         103,422         -90,373         18,855         -0.           00         19.850         124,101         105,609         105,407         -91,116         20,822         -0.           00         19.851         124,447         105,931         107,392         -91,907         22,800         -0.           91         19.852         124,755         106,219         109,198         -92,677         24,613<	00	19.841	120.691	102.452	87.545	-85.384	3.634	-0.16
00	00	19.842	121.100	102.829	89.530	-85.949	5.483	-0.24
00         19.845         122,279         103,917         95.483         -87.722         11.149         -0.           00         19.846         122,657         104,267         37.467         -88.348         13.054         -0.           00         19.847         123.028         104.611         99.452         -88.95         14.980         -0.           00         19.848         123.392         104.949         101.437         -89.667         16.918         -0.           00         19.849         123.750         105.282         103.422         -90.373         18.855         -0.           00         19.850         124.101         105.609         105.407         -91.116         20.822         -0.           00         19.851         124.447         105.931         107.392         -91.907         22.800         -0.           91         19.852         124.755         106.219         109.198         -92.677         24.613         -0.           91         19.852         124.755         106.219         109.198         -284.012         24.613         -0.           00         19.852         124.786         106.247         109.377         -285.015         25.087 <td>00</td> <td>19.843</td> <td>121.501</td> <td>103.198</td> <td>91.514</td> <td>-86.526</td> <td>7. 365</td> <td>-0.32</td>	00	19.843	121.501	103.198	91.514	-86.526	7. 365	-0.32
00         19,846         122,657         104,267         97,467         -88,348         13,054         -0.           00         19,847         123,028         104,611         99,452         -88,995         14,980         -0.           00         19,848         123,392         104,949         101,437         -89,667         16,918         -0.           00         19,849         123,750         105,282         103,422         -90,373         18,855         -0.           00         19,850         124,101         105,609         105,407         -91,116         20,822         -0.           00         19,851         124,447         105,931         107,392         -91,907         22,800         -0.           91         19,852         124,755         106,219         109,198         -92,677         24,613         -0.           91         19,852         124,755         106,219         109,198         -284,942         24,613         -0.           00         19,852         124,786         106,247         109,377         -285,015         25,087         -0.								-0.39
00         19.847         123.028         104.611         99.452         -88.995         14.980         -0.           00         19.848         123.392         104.949         101.437         -89.667         16.918         -0.           00         19.849         123.750         105.282         103.422         -90.373         18.855         -0.           00         19.850         124.101         105.609         105.407         -91.116         20.822         -0.           00         19.851         124.447         105.931         107.392         -91.907         22.800         -0.           91         19.852         124.755         106.219         109.198         -92.677         24.613         -0.           91         19.852         124.755         106.219         109.198         -284.942         24.613         -0.           00         19.852         124.786         106.247         109.377         -285.015         25.087         -0.								-0.46
00     19.848     123.392     104.949     101.437     -89.667     16.918     -0.       00     19.849     123.750     105.282     103.422     -90.373     18.855     -0.       00     19.850     124.101     105.609     105.407     -91.116     20.822     -0.       00     19.851     124.447     105.931     107.192     -91.907     22.800     -0.       91     19.852     124.755     106.219     109.198     -92.677     24.613     -0.       91     19.852     124.755     106.219     109.198     -284.942     24.613     -0.       00     19.852     124.786     106.247     109.377     -285.015     25.087     -0.								-0.538
00 19.849 123.750 105.282 103.422 -90.373 18.855 -0. 00 19.850 124.101 105.609 105.407 -91.116 20.822 -0. 00 19.851 124.447 105.931 107.392 -91.907 22.800 -0. 91 19.852 124.755 106.219 109.198 -92.677 24.613 -0. 91 19.852 124.755 106.219 109.198 -284.942 24.613 -0. 00 19.852 124.756 106.247 109.377 -285.015 25.087 -0.								- 0. 606 - 0. 67
00     19.850     124.101     105.609     105.407     -91.116     20.822     -0.       00     19.851     124.447     105.931     107.392     -91.907     22.800     -0.       91     19.852     124.755     106.219     109.198     -92.677     24.613     -0.       91     19.852     124.755     106.219     109.198     -284.942     24.613     -0.       00     19.852     124.786     106.247     109.377     -285.015     25.087     -0.								
00     19.851     124.447     105.931     107.392     -91.907     22.800     -0.       91     19.852     124.755     106.219     109.198     -92.677     24.613     -0.       91     19.852     124.755     106.219     109.198     -284.942     24.613     -0.       00     19.852     124.786     106.247     109.377     -285.015     25.087     -0.								- 0. 736
91 19.852 124.755 106.219 109.198 -92.677 24.613 -0. 91 19.852 124.755 106.219 109.198 -284.942 24.613 -0. 00 19.852 124.786 106.247 109.377 -285.015 25.087 -0.								- 0. 798
91 19.852 124.755 106.219 109.198 -284.942 24.613 -0. 00 19.852 124.786 106.247 109.377 -285.015 25.087 -0.								-0.859
00 19.852 124.786 106.247 109.377 -285.015 25.087 -0.9	91	19.852	124.755	106.219	109.198	-92.677	24.613	-0.913
00 19.852 124.786 106.247 109.377 -285.015 25.087 -0.9		19.852	124.755	106.219	109.198	- 284. 942	24.613	-0.913
								- 0. 9 29
00 19.852 125.120 106,559 111.362 -285.900 30.360 -1.	91	19.852	144. 180	100.247				

Symmetry number

 $\theta = 6$ .

Fundamental frequencies

$$\omega_1 = 780 \text{ cm}^{-1}$$

$$\omega_2 = 298 \text{ cm}^{-1}$$

$$\omega_3 = 791 \text{ cm}^{-1} (2)$$

$$\omega_4 = 314 \text{ cm}^{-1} (2)$$

Ground electronic state

 $1_{\Sigma}$ 

The above molecular constants were estimated by the procedures employed in the case of the corresponding  $\text{CrO}_3$  molecule (see section IV-B3b). The W-O bond distance was assumed to be the same as the estimated distance for the corresponding bond in WO;  $^{401}$  i.e., 1.78Å. The estimated fundamental frequencies above are somewhat lower than those of DeMaria and co-workers  $^{410}$  and of Ackermann and Thorn.  $^{487}$ 

The standard enthalpy of formation,  $\Delta H_{f298}^{\circ}$ , of gaseous WO3 had not been directly determined, and was therefore determined by the indirect method employed in the case of MoO3 (see section IV-B5c) based on the mass spectrographic study of Al2O3 in tungsten containers by DeMaria and co-workers. 410 The value of the heat of formation so obtained was -65, 100  $\pm$  5000 cal/gfw.  $H_{298}^{\circ}$ -H0 for gaseous WO3 was found to be 3296 cal/gfw.

Values of  $\Delta H_f^{\circ},~\Delta F_f^{\circ},~$  and log  $_{10} K_p$  were calculated in an analogous fashion to that described in section IV-B5c for the corresponding MoO\_3 molecule.

<sup>487</sup> Ackermann, R.J. and R.J. Thorn, U.S. AEC Rept. ANL-5824 (January 1958).

# V. EXPERIMENTAL STUDIES

### A. PREPARATION AND ANALYSIS OF COMPOUNDS AND SPECIMENS

- 1. The three following methods were used to obtain specimens for heat capacity measurements:
  - a. Solid pieces of various refractory compounds were obtained from commerical sources and machined to specifications by the use of diamond tools and electric discharge (Elox) techniques. Materials obtained in this way were titanium diboride, zirconium diboride, tungsten boride, molybdenum boride, molybdenum carbide, titanium carbide, and zirconium carbide (all obtained from Carborundum Co.) and titanium metal (obtained from Foote Mineral Co.). X-ray diffraction analysis showed that the molybdenum boride and carbide specimens were multiphase systems, and further analyses were, therefore, discontinued. In the case of all the other specimens however, complete X-ray and chemical analyses were performed. The results are given with the heat capacity data for the respective specimens in section V-B, 4 below.
  - b. Materials were also obtained in the form of powders from commercial sources and fabricated into solid bodies which were subsequently machined to specifications. In most cases, the fabrication was accomplished by hot pressing the powders in graphite dies at temperatures above 1300°C and at pressures of from 2000 to 2500 psi. The details of the fabrication of each specimen are given in Table LXXIV.

Attempts to prepare elemental boron specimens by hot pressing in graphite dies with and without boron nitride liners and punches were unsuccessful. However, sound bodies were prepared by a cold-pressing and sintering technique. Boron powder was mixed with a small amount of stearic acid and compacted by cold pressing at 20,000 psi. The stearic acid was eliminated by heating at  $400\,^{\circ}$ F, and the boron body was then sintered at  $1300\,^{\circ}$ C for 2 hours in an argon atmosphere. Rods, 0.5 inch in diameter and 1-1/2 inches in length with a density between 1.30 and 1.38 g/cc, were fabricated by this method.  $\beta$ -rhombohedral boron was the only phase detected in these specimens, but there was an increase of 0.8 percent in carbon content over that detected in the original boron powder. This increase was probably due to incomplete elimination of the stearic acid binder.

c. Work was also started on the laboratory preparation of compounds. Silicon hexaboride, tantalum boride, and tantalum nitride were prepared in small quantities from the elements.

# 2. Chemical Analysis

# a. Oxygen Determination

The need for a rapid, accurate, and reliable method for the determination of oxygen in refractory compounds motivated the development and adaption of the inert-gas fusion method to this problem. Vacuum fusion and vacuum extraction have both been used in the past, but they did not lend themselves to rapid determinations. Often, in the past, the oxygen content was not determined but estimated as the difference between the major-constituents analysis and 100 percent.

Figure 5 is a schematic diagram of the apparatus fabricated for the inert-gas fusion method of determining oxygen in refractory materials. Argon was passed through a purifying train (containing "Ascarite", concentrated sulfuric acid, and heated titanium metal chips) and then, to a flow-regulating valve and meter. A pressure-relief valve was used to maintain a constant pressure throughout the system. The argon flowed to the main furnace chamber which contained a high-purity (spectrographically pure) graphite crucible packed in powdered graphite. The crucible contained a platinum bath and was maintained at 2100°C by means of induction heating. After outgassing of the system by heating until the blank run gave constant results, the platium bath was allowed to become saturated with carbon from the graphite crucible before the specimen was introduced.

A sample of 10 to 60 milligrams of finely ground refractory compound was weighed in a small, high-purity tin capsule which served as a vehicle. The sample was inserted in the furnace by means of a loading valve. The oxygen in the sample reacted with the carbon in the platinum bath to form carbon monoxide which was entrained by the flow of argon. The gases then passed through a tube containing copper oxide maintained at 750°C. The carbon monoxide was thus converted to carbon dioxide which was then carried to the conductimetric carbon determinator where the CO<sub>2</sub> was absorbed and measured.

The conductometric carbon determinator functioned on the principle of a Wheatstone bridge, measuring the conductivity of a barium hydroxide solution. The argon gas carrying the carbon dioxide was dispersed through the solution where the  $\text{CO}_2$  and  $\text{Ba}(\text{OH})_2$  reacted to form barium carbonate, thus changing the conductivity of the solution by an amount which was a measure of the  $\text{CO}_2$  absorbed.

Oxygen analyses were performed on five samples of unalloyed titanium, which were received from the Watertown Arsenal, to check the validity of the inert-gas fusion method of oxygen determination. These samples were previously analyzed for oxygen by a task force of 15 different laboratories. The results confirm the validity of the inert-gas fusion method used at Avco RAD.

TABLE LXXIV

CONDITIONS OF REFRACTORY POWDER HOT PRESSING

Material	Source	Lot No.	Temperature	Pressure psi	Time hours	Density of Piece g/cc	Theoretical Density g/cc
TaC	Starck	TAP-991 TaC	1350	2000	1	13. 2	14.5
TeC	Starck	Grade I	1500	2500	3	13.39	- 14,5
NЬC	Starck	931/c/3	1500	2500	2-1/2	6. 96	7.8
NbC	Starck	134/B	1300	2500	1	7 08	7.8
CrB <sub>2</sub>	Starck	ax-3159	1600	2500	1		5.6
₹2B5	Starck	TAP-151/B	1600	2500	2	8, 14	10.77
МоВ	Starck	151/D	1600	2500	2	7.05	8.8
ню	Wah Chang	R. D. 10603K	1800	2500	1	8. <b>4</b> 5	12.7
МоС	A.D. MacKay	NoC -100	1600	2500	2	7.3	8, 4

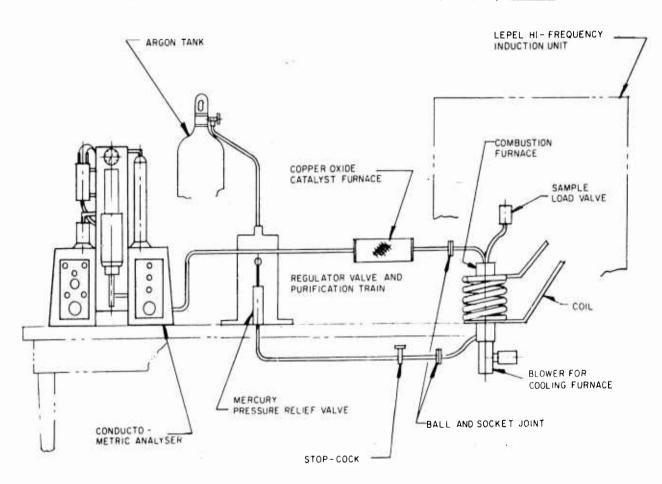


Figure 5 SCHEMATIC OF INERT-GAS FUSION APPARATUS

# 24 to .1 \* !=

b. After dissolution by one of the usual methods as required (i.e., acid, fusion and leaching, etc.), metal determinations were made as follows:

# 1) Titanium with Jones Reductor (zinc amalgam) and titration with potassium dichromate

A solution of the titanium (Ti<sup>+++</sup>) was passed through a standard Jones reductor where the titanium was reduced to Ti<sup>++</sup>. The resulting solution, containing the reduced titanium, was then titrated with an oxidizing agent (potassium dichromate). The titanium content was calculated from the standard value of titanium for the volume of the dichromate solution used.

# 2) Chromium by oxidation with perchloric acid and titration of the resulting dichromate

The chromium solution was oxidized to a dichromate solution by heating to fumes in perchloric acid. The oxidized solution was then cooled and titrated with a reducing solution (ferrous ammonium sulphate) for which a standard chromium value had been previously established.

# 3) Molybdenum by precipitation with alphabenzoinoxime

The sample containg molybdenum was dissolved and alphabenzoinoxime solution was added. The molybdenum was thus precipitated as the organic complex. The precipitate was then filtered and dried to constant weight. The molybdenum content was then computed from the weight of the precipitate in the usual way.

# 4) Tungsten by precipitation with cinchonine

The tungsten compound was dissolved by means of an alkali fusion. A solution of cinchonine was then added to the tungsten solution and the mixture heated gently to precipitate the tungsten complex. This precipitate was then filtered and dried to constant weight. The amount of tungsten was then computed in the usual way from the weight of the precipitate.

# 5) Niobium, tantalum, and hafnium by separation from other metals by ion exchange and gravimetric determination as the oxide

Niobium, tantalum and hafnium compounds were put into an acid solution, and passed through a resin column where the metals were absorbed. By means of varying acid strengths, the metals were selectively eluded from the resin. The individual solutions were brought to dryness, and the metals were converted to oxides by standard ashing techniques. The weight of the metal oxide was then computed and converted to the weight of the metal.

### c. Nonmetal determinations were made as follows:

# 1) Boron by conversion to acid with mannitol and titration

The boron compound was converted to soluble boric acid by means of alkali fusion. Mannitolorglycerine was added to the boric acid solution to form a readily titratable solution with sodium hydroxide. The boron content was computed from the amount and the standard value of the sodium hydroxide solution required for neutralization.

# 2) Nitrogen by Kjeldahl digestion and titration

The nitrogen compound was dissolved by means of acid digestion in a Kjeldahl flask. The flask was then transfered to a Kjeldahl distillation apparatus where the nitrogen-containing solution was made ammoniacal by addition of caustic solution. The ammonia thus formed was distilled and trapped in distilled water. The resultant solution was then titrated with a standard hydrochloric acid solution.

# 3) Carbon by combustion and volumetric measurement of liberated CO<sub>2</sub> with a Leco apparatus

The total carbon was determined volumetrically by means of a Leco combustion furnace and a Leco volumetric carbon determinator.

The free carbon was determined by means of combustion in air at a temperature below the decomposition temperature of the carbide. Thus, the loss in weight was a direct measure of the free carbon content. The combined-carbon content was obtained by difference from these two results.

# d. Trace-Impurity Determinations

Spectrographic analytical curves for known concentrations of trace impurities in refractory compounds had been established, and it was possible to determine quantitatively the concentrations of the trace impurities.

# 3. X-Ray Diffraction Analysis

Diffraction diagrams of the specimens were obtained with a 114.59 mm Debye-Scherrer camera with Ni-filtered Cu radiation. Lattice constants calculated from reflections above  $\theta$  = 50 degrees were plotted against  $\frac{\cos^2\theta}{\sin\theta} + \frac{\cos^2\theta}{\theta}$ , and the best straight-line fit (visual) was extrapolated to  $\theta$  = 90 degrees for the lattice constant. The precision of the measurements

was (± 0.0005Å). The results for the individual heat capacity measurement specimens are given with the heat capacity data in section V-B below.

Reaction between the specimens and the carbon vapor in the high-temperature heat capacity furnace was first noticed in the case of TiN. The outer surface of the specimen turned blue, and the lattice constant of this blue material was found to be larger than that of the starting TiN. Drillings were then taken (perpendicular to the rod axis) to a depth of approximately 1.60 mm and the X-ray measurement repeated to reveal the depth of carbon penetration. Results are summarized in Table LXXV.

# TABLE LXXV

# VARIATION OF LATTICE CONSTANT VERSUS DEPTH IN TIN SPECIMENS AFTER HIGH-TEMPERATURE HEAT CAPACITY DETERMINATION

Lattice Constant	Approximate Composition	Depth
4. 28	TiN <sub>0.5</sub> C <sub>0.5</sub>	0.40
4, 27	TiN <sub>0.65</sub> C <sub>0.35</sub>	0.80
4.24	TiN	1.20
4.24	TiN	1.60

Carbon concentrations were calculated on the basis of the following assumptions. (a) all the nonmetal sites were filled, and (b) the TiN – TiC solid solutions obey Vegard's straight-line relationship. Subsequent analyses on other specimens revealed carbide layers of 0.4 mm (TiC) in the case of TiB $_2$ , and 0.3 mm (WC) in the case of WB. The presence of ZrC was also found on the surface of the ZrB $_2$  specimen.

The presence of tungsten carbides at the contact areas of the TaC and NbC specimens with the tungsten electrodes and the absence of them in the TiN case indicated the possibility of some reaction between the tungsten and carbide specimens only.

The TiC, TaC, and NbC specimens were found in post-test analyses to be one-phase systems of the same lattice constants as the starting materials (except for a slight lattice-constant increase on the surface, probably due to increased carbonization). The ZrC specimen exhibited weak reflections of ZrO<sub>2</sub> similar to those of the starting material.

Since the first NbC specimen showed unusual behavior in the specific heat measurements, a second specimen (931C) was prepared and characterized. The lattice constant of the first NbC specimen was 4.4673Å. This corresponded to a C/Nb ratio of 0.93 according to the data of Kempter and Storms. 488 Since chemical analyses had also been made, it was possible to check the X-ray result. The analytical data on NbC are summarized in Table LXXVI. The C/Nb ratios obtained by chemical analysis were calculated directly from the total niobium (or niobium plus tantalum where tantalum is not reported). In most cases, the diffraction pattern indicated extremely weak additional reflections in the front-reflection region that could be indexed (although with some ambiguity because of their weak.diffuse intensity) as Nb205. It was, therefore, assumed that the majority of the oxygen reported by chemical analysis was not in solution with the NbC although the nitrogen and tantalum were, since there was no indication of NbN or Ta in the X-ray diagrams. The lattice constants reported are not corrected for the decrease due to tantalum in solution (approximately 0.0003A per percent Ta) or the increase due to nitrogen in solution (approximately equal to a corresponding amount of carbon, assuming the carbon radius to be 0.76Å and the nitrogen radius to be 0.71Å).  $^{448}$ 

<sup>488</sup> Kempter, C. and E. K. Storms, J. Chem. Phys. 33, 1873 (1960).

TABLE LXXVI

NEC LATTICE CONSTANT AND CHEMICAL ANALYSIS SUMMARY

	ther	gen	int	6	1	ı	6	8	-
	sis of C	Nitrogen	Percent	0.29	!	!	0.29	0.43	< 0.01
I	Avco Analysis of Impurities	Oxygen	Percent	0.12	;	;	0.26	0, 21	0.25
SIS SUMMAR	Ta Content by Chem. Avco Analysis of Other Anal.	Shieldalloy	Percent	1.80	2.0	! !	1.82	1.95	0.14
TOWN T	Ta Conte	Avco	Percent	2.12	!	!	2.32	1.84	0.16
THE CITE OF THE PROPERTY OF TH	C/Nb by Chem. Anal.	Shieldalloy		0.96	0.93	!	0.97	96 .0	0.96
	C/Nb by	Avco		96 .0	0.88	0.94	0.97	0.96	0.94
	C/Nb	From Kempter and Storms' 488 Data		0.95	0.92	0.95	0.95	0.945	0.93
			×Υ	4.4687	4.4670	4.4688	4.4685	4.4684	4.467 <sub>5</sub>
		Specimen Lattice Code Constant		946A	952C	C-2453	946B	931C	134B

### B. SPECIFIC HEAT DETERMINATIONS

# 1. Introduction

Two experimental techniques were adopted for specific heat determinations. The two were used because of the broad temperature coverage required and the inherent limitations of each system.

The Bunsen type of ice calorimeter <sup>489</sup> shown in figure 6 was chosen for "low" temperature determinations (room temperature to 1900°C). The maximum temperature of operation for this apparatus is determined by the radiant heat transfer from the associated furnace to the calorimeter and by other losses that occur with the transfer of the sample from the furnace to the calorimeter. The photograph in figure 7 shows a cutaway view of internal details of the calorimeter chamber.

A modified pulse technique was adopted for the high-temperature determinations of specific heat. The technique used is similar to that of Rasor and McClelland. The practical limits of temperature coverage of this "high" temperature apparatus shown in figure 8 are approximately  $1800^{\circ}$  to  $3900^{\circ}$ K.

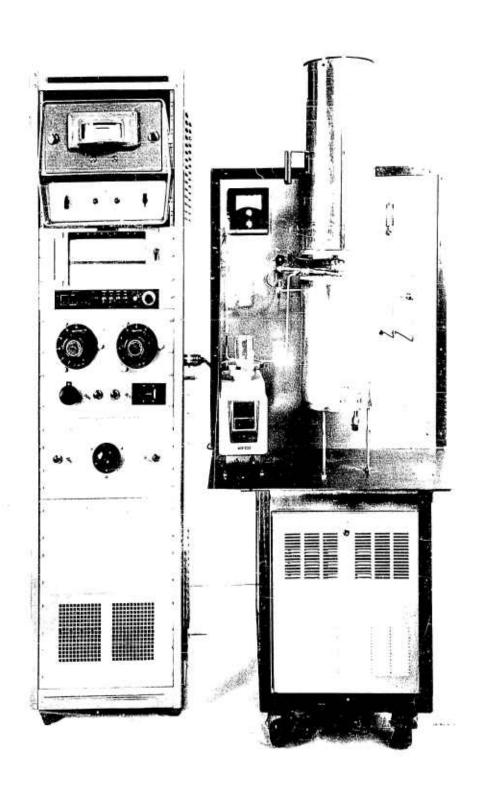
Considerable care was exercised to ensure the accuracy of temperature measurements throughout the specific heat measurements. Secondary calibration standards were continuously maintained in the laboratory, and frequent calibration checks were made of the instruments. The calibration standards used were a gold melting-point apparatus, NBS-certified tungsten strip lamps, NBS-certified freezing point metals, an NBS-certified platinum-resistance thermometer, and platinum - platinum 10 percent rhodium thermocouples with the associated NBS-certified Müller bridge and Werner potentiometer.

An extended range, DK-2, ratio-recording spectrophotometer was used to determine the transmissivity characteristics of any associated glass or quartz windows used during the experimental determinations.

# 2. The Bunsen Ice Calorimeter

The Bunsen ice calorimeter is extensively used to make specific heat determinations in a number of laboratories. A few innovations were introduced into the one used for this work. The designs of the furnace and calorimeter components are shown schematically in figures 9 and 10.

<sup>489</sup> Deem, H. W. and C. F. Lucks, An Improved All Metal Bunsen Type Ice Calorimeter, ISA Conference Paper, PPT-4-58-1 (September 1958).

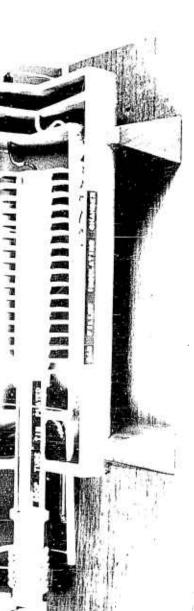


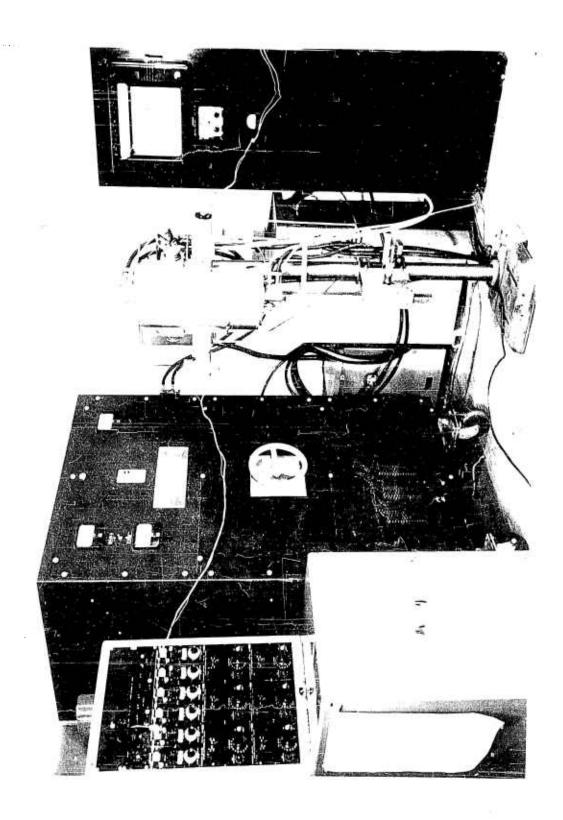
. . . .

# ICE CALORIMETER ASSEMBLY

SAMPLE, PERTON SENEGUAL STRANGES OF STREET MEE TOWN GALORITETES CONFIDEN THE PARTY COST IN SOUTH

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A-END PLATE (LAVA)
B-RELEASE WASHER(SS304)
C-ALIGNMENT HUB (AL203)
D-SUSPENSION WIRE (KANTHAL "A")
E-RESISTANCE WINDING-END (KANTHAL "A")
F-STABILIZING BLOCK-(INCONEL) WITH SIX THERMOCOUPLES
G-SAMPLE HOLDER (SS-304) WITH CENTRAL THERMOCOUPLE
H-RESISTANCE WINDING-CENTER (KANTHAL "A")
I-RESISTANCE WINDING-END (KANTHAL "A")

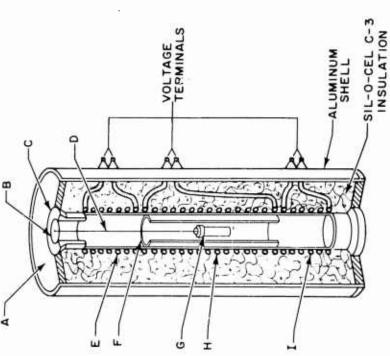


Figure 9 ICE CALORIMETER FURNACE

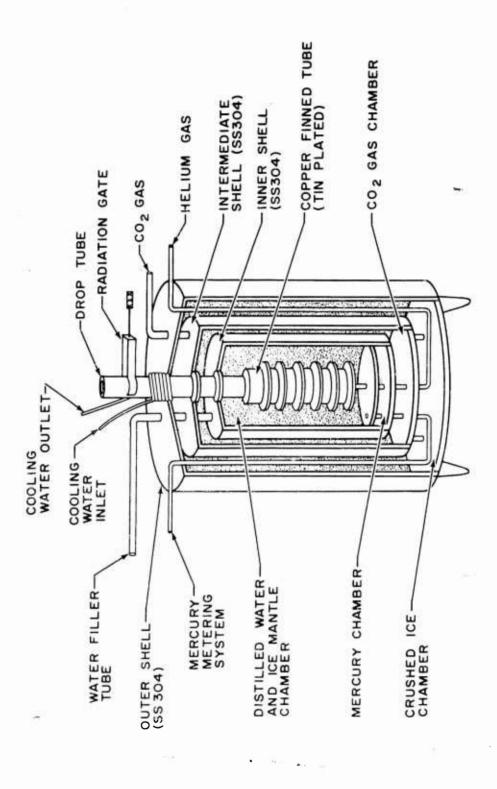


Figure 10 BUNSEN ICE CALORIMETER

The furnace was multiply wound with separate controls associated with each winding. The end windings allowed for the usual end losses and permitted a long hot zone in the vicinity of specimen heating.

A stabilizing slug, (F) in figure 9, was also used along the central furnace area to improve the temperature gradient characteristics. There were seven thermocouples of the platinum - platinum 10 percent rhodium variety located in the vicinity of the furnace center to provide continuous monitoring of the sample area temperature. The distribution of thermocouples consisted of two at the furnace center, located in opposite positions at 0 and 180 degrees; two located 2 inches above the center at 90 and 270 degrees; two located 2 inches below the center at 45 and 225 degrees; and one which traversed the center of the furnace and was inserted in a hole in the sample container (G).

The sample, placed in the sample container in a helium atmosphere, was held in position by a suspension wire (D) and the release washer (B). The release washer was held by an electromagnetic coil until the drop temperature was reached and stabilized.

Considerable care had to be used in the construction of the calorimeter drop tube because of the tendency for failures to occur at joints between dissimilar metals. The finned tube assembly had to be made from a solid copper rod to eliminate the need for welded joints at the bottom plug. A graded weld was found to be necessary to attach the copper, finned tube to the stainless steel at the top of the drop tube.

Located at the top of the drop tube was a silvered radiation gate which was opened prior to, and closed immediately following, a drop to prevent radiant heat transfer. A cooling coil was also incorporated with the drop tube to reduce the heat conduction from the furnace to the calorimeter.

In operation, the inner container to which the drop tube is welded was filled with gas-free water through the water-filler tube. After filling of the entire inner chamber with water, mercury was admitted through the mercury-metering system until it filled the mercury chamber and rose approximately three-fourths of an inch in the water chamber. The latter operation displaced water which flowed out through the water-filler tube. The water-filler tube was then sealed off by means of a suitable valve. The system then expelled mercury when ice was formed from cooling of the water in the inner container.

At first, ice mantles were formed on the finned tube by lowering a container of dry ice into the drop tube and oscillating it over the tube length until a sufficient thickness of ice was formed. Later, it was found to be more convenient to form the mantle by injecting into the lower drop tube area a flow of air which had been pre-cooled by passing through a copper

coil immersed in liquid air. This reduced the time required for mantle formation from two days to approximately two hours.

The amount of mercury displaced during melting (or additional freezing) of the previously formed ice mantle after a sample drop gave a measure of the enthalpy change.

CO<sub>2</sub> gas in the intermediate container shown in figure 10 reduced heat leakage to the inner container because of the gas' low thermal conductivity. The entire inner calorimeter assembly was kept at a temperature of approximately 273°K during operation by crushed ice between the outer and intermediate shells. The mercury-metering tube and the helium gas tube were passed through the crushed-ice bath to pre-cool the fluids. The helium gas was passed up the drop tube since its presence assisted in the heat transfer from the sample container to the copper finned tube. A negligible amount of heat was carried away by the helium.

A number of checkout tests were run on the Bunsen ice calorimeter apparatus. One important test was conducted on the heat-leak rate and its effect on the life of the ice mantle. Heat-leak values, as evaluated from short time observations, are plotted in figure 11. The average value of the heat-leak rate from the short-time observations (taken as representative for normal operating conditions) was determined to be 2.06 cal/hr or 18.84 grams of mercury per day using a calibration factor of 62.560 cal/g.

From the results in figure 12, it appears that a heat-leak value of 5.77 cal/hr or 52.8 grams of mercury per day is applicable in the case of long - term tests (not normally used). The higher leak rate for the long-term tests was ascribed to the depletion of ice during over-night interruptions of the experiments.

The lower value was chosen as the characteristic heat-leak rate under actual test conditions where ice depletion will not occur. The latter value is sufficiently low to indicate a negligible effect upon specific heat measurements in the apparatus regardless of furnace alignment or temperature. The further precaution was taken of adopting the standard procedure of moving the furnace away from the drop tube after a sample drop (corresponding to the case of no furnace alignment in figure 11). Further tests planned for the future included some at higher furnace temperatures.

Another test revealed that the average temperature reading of the six thermocouples in the sample region of the furnace could not be used as the drop temperature. It was therefore decided to incorporate a permanent thermocouple in such a way as to read the temperature in a small well in the capsule for this measurement.

A brief study was made of the properties of the drop-capsule material. The results are summarized in Table LXXVII.

The calorimeter was calibrated with synthetic sapphire as a standard which had been established by the measurements of Ginnings and Furukawa. <sup>28</sup> As a result of 12 determinations at approximately  $450^{\circ}$ K, the calibration factor was found to be  $62.560 \pm 0.675$  cal/g of mercury or  $261.707 \pm 2.824$  international joules/g of mercury. The factor is lower by 3.20 percent than

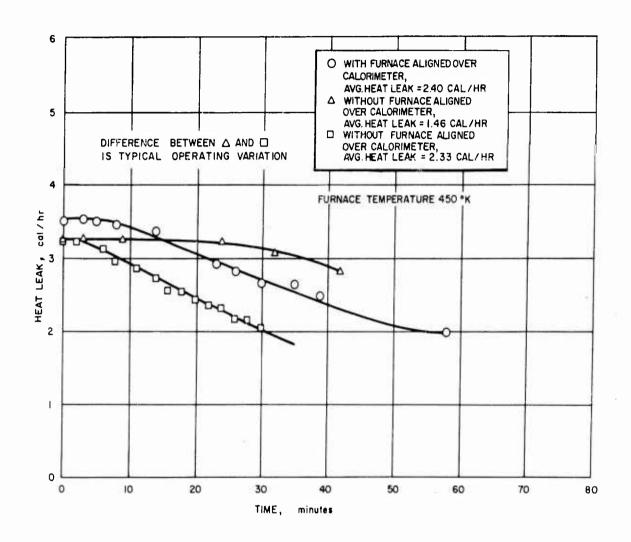


Figure 11 HEAT-LEAK CHARACTERISTICS OF AVCO BUNSEN ICE CALORIMETER

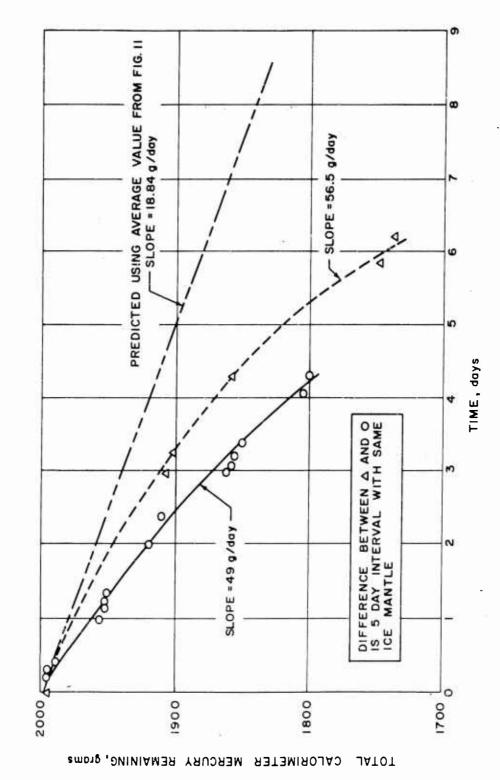


Figure 12 BUNSEN ICE CALORIMETER ICE MANTLE LIFE AS INFLUENCED BY HEAT LEAK AT NORMAL AMBIENT TEMPERATURE OF 294°K

TABLE LXXVII

SPECIFIC HEAT OF BUNSEN ICE CALORIMETER SAMPLE CAPSULE\*

OVER A LIMITED TEMPERATURE RANGE

Temperature	Change in Enthalpy**	Specific Heat						
°K	cal/g	cal/ <sup>o</sup> K g						
325	4.843	0.094						
324	5.160	0.101						
403	14. 21 3	0.109						
400	14. 676	0.116						
399 .	13.570	0.108						
398	13.124	0.105						
396	14. 656	0119						
405	14. 276	0.108						
401	13. 326	0.104						
Average values								
324.5	5.001	0.097						
400.3	13.977	0.110						

<sup>\*</sup>Capsule was of type 304 stainless steel with a 0.030-inch thick aluminum sealing washer. Capsule weight was 19.764 grams included herein.

<sup>\*\*</sup>Using a calibration factor of 62.560 cal/g of displaced mercury.

the value of Ginnings and Corrucini  $^{30}$  of 270.  $37 \pm 0.06$  international joules/g of mercury. Electrical calibration will be used to determine whether this uncertainty is inherent in the use of synthetic sapphire as a calibration standard.

### 3. High-Temperature Pulse Method of Specific Heat Determination

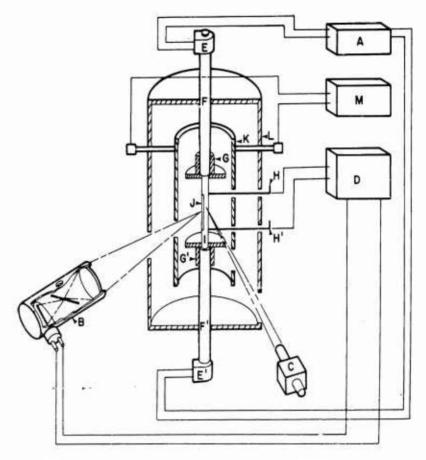
The pulse-method apparatus used for high-temperature specific heat measurements is illustrated schematically in figure 13. This apparatus was used at temperatures above 1900°K because radiative and convective losses make it very difficult to use the drop method at such high temperatures.

The furnace used in the pulse-method apparatus was of the graphite-resistance type with a flowing helium atmosphere. The original working chamber, 4 inches in diameter by 8 inches in length, was capable of operation at temperatures up to  $3000^{\circ}$ K when used as designed. As adapted for specific heat determinations however, the maximum operating temperature was found to be  $2600^{\circ}$ K.

Since the inside of the furnace chamber is essentially a blackbody enclosure, emissivity corrections were not needed for optical pyrometer temperature determinations on enclosed samples.

The operating procedure was first to heat the sample with the furnace heater (K) to the desired temperature. Power for the heaters was supplied by a 20 kilowatt a-c source (M), capable of raising the furnace temperature to nearly 2500°K in a period of about 30 minutes. After sufficient time for the ambient temperature to stabilize, a high current from the d-c power supply (A) was pulsed through the sample (I). Contact with the sample was provided by the water-cooled electrodes (E, E') and the tungsten electrodes (F, F'). The graphite shields (G, G'), located on the tungsten electrodes, served to reduce end-radiation losses and acted as an alignment guide for the sample.

The d-c through the specimen caused a constant power to be dissipated uniformly throughout the sample volume. If no significant amount of heat were lost or measurements were made before such losses became sizable, the temperature of any sample region increased linearly with time. The specific heat at constant pressure,  $C_p^{\circ}$ , could then be computed from the current, I, through the specimen, the potential drop, E, across a uniformly heated region of mass, m, and the rate of temperature increase as a function of time, dT/dt. The relationship between these quantities and  $C_p^{\circ}$  is given by equation (253),



- DC POWER SUPPLY RECORDING OPTICAL PYROMETER В
- MICRO-OPTICAL PYROMETER
- SIX CHANNEL RECORDER-DYNAGRAPH D
- E-E' DC ELECTRODES-COPPER
- F-F' ELECTRODE EXTENSION-TUNGSTEN
- G-G' RADIATION SHIELDS-GRAPHITE
- H-H' POTENTIAL PROBES-TUNGSTEN
  - SPECIMEN
- SPECIMEN SLOT
- FURNACE HEATER-GRAPHITE
- RADIATION SHIELD-GRAPHITE
  - AC POWER SUPPLY

Figure 13 HIGH-TEMPERATURE SPECIFIC HEAT APPARATUS

$$C_{p}^{\circ} = \frac{EI}{Jm (dT/dt)} , \qquad (253)$$

where J is the mechanical equivalent of heat.

The specimens, 1/2 inch in diameter and 4 inches in length, were slotted over a 2-inch center portion. The slots which were 1/16-inch wide and 1/4-inch deep extended the measurement time from less than 0.1 to 0.2 sec. This is due to the fact that the rate of rise of the specimen surface temperature was influenced sooner than the rate of rise of the center temperature by radiation losses to the heater element after a heat pulse.

The ambient temperature in the furnace was determined with a pyro-optical pyrometer, C, calibrated against NBS-calibrated tungsten-strip lamps, and corrected for the error introduced by an interposed quartz window. Periodical cross checks of the strip lamps were made with a gold melting-point apparatus. Typical pyrometer and quartz-window corrections are plotted in figure 14. Results of 20 pyrometer and lamp cross checks are summarized in Table LXXVIII. It can be seen that very little variation occurred in the calibration factor during the period of the project (1 year).

An optical pyrometer similar to that described by Rasor and McClelland was used to record the temperature as a function of time on a Dynagraph recorder. The pyrometer used in this work employed a type 925 phototube with an S-1 spectral response. It was capable of response times of less than 0.01 sec. Calibration of this recording optical pyrometer, B in figure 13, was accomplished by comparison of a reading from a corrected, separate, micro-optical pyrometer with the phototube output recorded on a channel in the Offner Electronics Dynagraph recorder.

The determination of the rate of change of temperature as a function of time was done by means of equation (254),

$$\frac{de}{dt} \cdot \frac{ds}{de} \cdot \frac{dT}{ds} = \frac{dT}{dt}$$
 (254)

where

e = applied voltage

t = time

s = number of scale divisions

T = temperature.

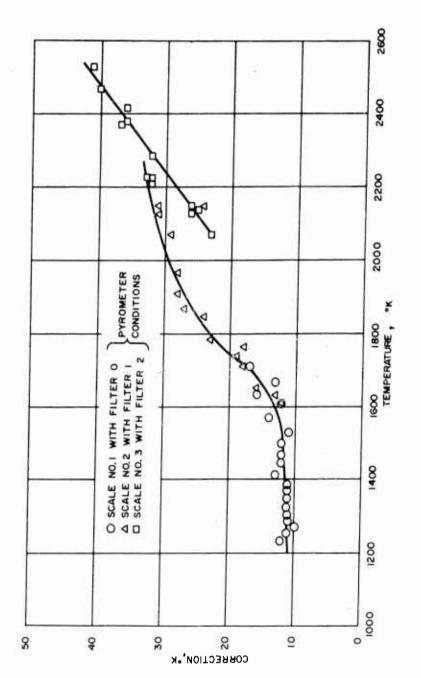


Figure 14 OPTICAL PYROMETER CORRECTION WITH ONE-EIGHTH INCH QUARTZ WINDOW

TABLE LXXVIII

PYRO-OPTICAL PYROMETER AND GOLD MELTING-POINT\* (1336°K)

CROSS-CHECK DATA

Run	Corrected Pyrometer Reading	Thermocouple** Reading	Differenc
No.	°K	°K	°К
,	1225		
1	1337		
2	1335	1333	-2
3	1336		
4	1 3 3 5	1335	0
5	1 3 3 4	1333	-1
6	1336	1335	-1
7	1 3 3 2	1 3 3 0	-2
8	1 327	1333	+6
9	1 3 3 0	1334	+4
10	1328	1332	+4
11	1337		
12	1335	1333	-2
13	1336		
14	1 3 3 5	1335	.0
15	1 3 3 4	1333	-1
16	1336	1335	-1
17	1332	1330	-2
18	1327	1333	+6
19%	1330	1334	+4
20	1328	1332	+4

<sup>\*</sup> High-purity gold strip 1/6-inch wide x 0.005-inch thick.

<sup>\*\*</sup> Platinum-platinum 10 percent rhodium, reference grade.

The first term on the left-hand side of equation (254) was obtained directly from the Dynagraph chart. The second term is a calibration term which was obtained by applying a known potential from a K-3 type potentiometer directly to the Dynagraph. The third term is the optical pyrometer calibration obtained as described above.

The potential drop, E, needed for equation (253) was obtained from the spring-loaded tungsten potential probes (H, H'). The current was determined from the potential drop across a high capacity shunt (2000 amperes maximum). Each of the needed quantities was recorded on a separate channel simultaneously.

The Dynagraph was well-suited for these measurements since it provided zero suppression in each channel, and only the deflections caused by the current pulse were recorded. Its reponse time of less than 1/120 sec and its chart speed of 25 cm/sec were also advantageous. Typical curves from Dynagraph records are illustrated in figure 15.

The specific heat values obtained by the techniques described were estimated to be accurate to within ± 5 percent.

### 4. Discussion of Results of High-Temperature Determinations

High-temperature specific heat determinations were completed with the pulse technique apparatus on four carbides, four borides, and one nitride. Average results at 2000°, 2300°, and 2500°K are summarized in Table LXXIX for purposes of discussion. These data were treated in the same way as those in Table II (section III-C5) of this report.

Most of the values are very large compared to the classical high-temperature limit of lattice harmonic vibration contributions (3R), but this is not unexpected. A few of the values are surprisingly high and still increasing with the temperature. These extremely large values are from samples of low purity (TiC and TiB<sub>2</sub>). Because there is not enough past experience with data on these compounds at such high temperatures, it would be desirable to make a more detailed theoretical analysis, but that is not possible without the use of several other types of unavailable data in very complete form (refer to section III-C of this report for the applicable theoretical background).

For the reasons just-mentioned, it is important to subject high-temperature heat capacity data of this type to the test of comparison with the results of other workers. In the discussions that follow, the advantages of doing this will be evident. A number of positive checks support the general validity of the measurements made on this project. In the cases where there is not the required agreement, further work is required to find out the reasons which very likely will vary from one case to another.

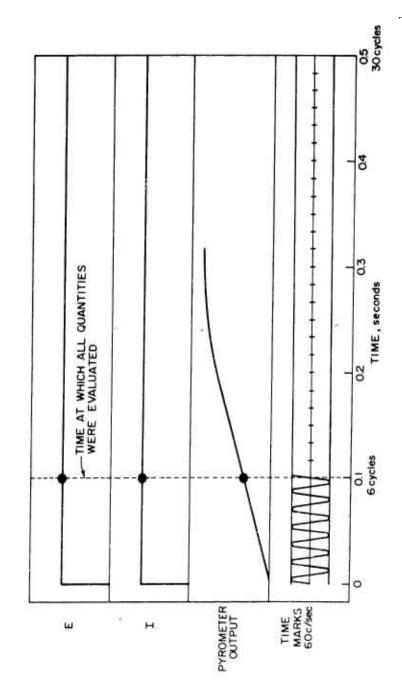


Figure 15 TYPICAL CURVES FROM DYNAGRAPH RECORDS

TABLE LXXIX

SUMMARY OF HIGH-TEMPERATURE SPECIFIC HEAT DATA AT THREE TEMPERATURES

Compound	No. of Atoms/gfw	Molecular Weight	Specific He 2000 <sup>o</sup> K	Specific Heat in cal/ <sup>o</sup> K avg g atom 2000 <sup>o</sup> K 2500 <sup>o</sup> K	vg g atom 2500 <sup>0</sup> K
Carbides					
Niobium Carbide (NbC)	73	104.921	11.54	11.11	11.54
Tantalum Carbide (TaC)	2	192.961	6.75	9.17	9. 26
Zirconium Carbide (ZrC)		103, 231	10.38	10.38	10.38
Titanium Carbide (TiC)	2	59.911	14.68	16.87	18.27
Borides					
Zirconium Diboride (ZrB2)	٤	112.86	12.79	13.81	13.92
Tungsten Boride (WB)	7	194. 68	10.61	11.10	11.78
Titanium Diboride (TiB2)	3	69.54	11.75	14.81	16.74
Nitrides					
Titanium Nitride (TiN)	2	61.908	69.9	7.18	7.58
Graphite	1	12.011	5.89	5.89	6.02

One particularly important aspect of the work has been the verification of the purity of all test samples. This was done in pre-test analyses in nearly all cases. It resulted in the discontinuation of studies on the molybdenum boride sample because it was found to consist of four phases, Mo<sub>2</sub>B, MoB, MoC, and Mo. A few post-test analyses were carried out to investigate any chemical or phase changes that might occur during the specific heat determinations.

#### a. Carbon

Carbon is a common element which has many uses in high-temperature technology in the form of graphite because of its extremely high melting point (in fact, it sublimes at one atmosphere without melting). Yet, its thermodynamic properties at high temperatures are still not known with any degree of assurance. Outstanding deficiencies in its available thermodynamic data are its equilibrium vapor species, the heats of vaporization of its vapor species, spectroscopic data for the vapor species other than  $C_2$ , and the specific heat of the solid at high temperatures. It was stated in section IV-A4a of this report that thermodynamic functions of graphite up to 6000°C could not be provided until better specific heat data became available. A review of the available data is therefore in order.

The available specific heat data for carbon are plotted in figure 16 for comparison purposes. Some of the additional points obtained on this project are given in Table LXXX and plotted in the figure also. The agreement between sets of data from different sources <sup>27</sup>, <sup>29</sup>, <sup>173</sup> is not very good except for that between the points from this project and the curve of Rasor and McClelland. <sup>27</sup> The sharp rise above 3000°C needs confirmation. Extrapolation to the sublimation point is obviously impossible.

#### b. Niobium Carbide (NbC)

The X-ray diffraction pattern of the niobium carbide specimen used in the specific heat determinations was that of NbC plus a weak pattern of Nb<sub>2</sub>O<sub>5</sub>. The results of the chemical analyses were as follows:

Element	Percent
.Vb	86.66
Total C	10.81
Free C (continued	<0.01 on p.1-354)

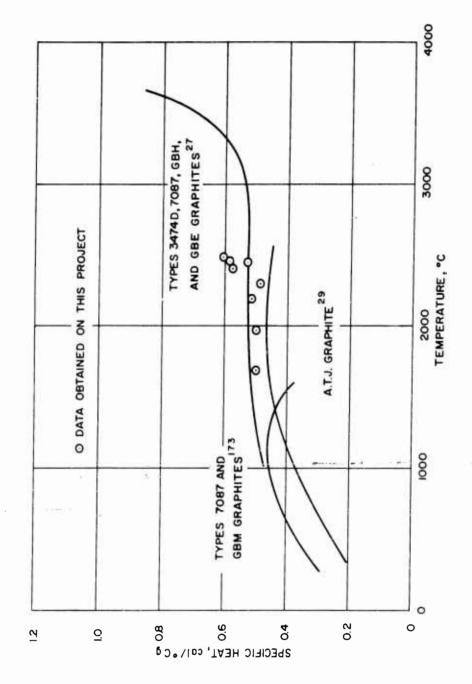


Figure 16 THE SPECIFIC HEAT OF CARBON VERSUS TEMPERATURE

TABLE LXXX
GRAPHITE HEAT CAPACITY

T,°K	cal/ K g	cal/ K g atom
1993	0.493	5. 92
2188	0.526	6. 32
2298	0.480	5.77
2429	0.570	6.85
2452	0.524	6. 29
2461	0.588	7.06
2471	0.601	7. 22
2483	0.448	5.38

(continued from p.1-351)

Element	Percent
Ta	1.82
Fe	0.06
Mg	0.0003
N	0.47, 0.46
0	0.22

Al, V, Ti, Zr, Ni, Mn, Hf, and Cr were not detected.

Since an unreported transition was discovered at ~2440°K and heat capacity values were high in the first series of specific heat measurements on NbC, the work was repeated with another sample to avoid any possibility of an accidentally wrong or impure sample. The temperature region in the vicinity of the transition point was extensively studied; several runs were made in both directions of increasing and decreasing temperature. Another purpose of repeated re-cycling of test runs was to detect any drift in specific heat with time due to reduction of the sample by the carbon vapor in the furnace.

The results are summarized in Table LXXXI and figures 17 and 18.

The transition was found to be completely reversible. A transition temperature of 2437°K was chosen. The nature of this transition remains to be clarified. The available information about the phase diagram of the Nb-C system <sup>241</sup>, <sup>490</sup> provides no clues as to its nature since a broad homogeneity range exists at the stoichiometric composition. Other investigators <sup>29</sup> have not reported evidence for its existence, but the density of points in their work in the region of the transition temperature was not sufficient for this purpose.

The only available data from two sources are compared in figure 19. It is evident from this comparison that more experimental work will be required on the heat capacity of NbC.

#### c. Tantalum Carbide (TaC)

X-ray analysis of the tantalum carbide test specimen showed it to be a single phase of TaC. The results of the chemical analyses were as follows:

<sup>490</sup> Storms, E. K. and N. M. Krikorian, J. Phys. Chem. 64, 1471 (1960).

TABLE LXXXI

NIOBIUM CARBIDE (Nbc) HEAT CAPACITY (APPROXIMATELY 97.5 PERCENT PURITY)

Run	Temp		C <sup>o</sup> p	Run	Temp		Cp
No.	*K	cal/*K g	cal/°K avg g atom	No.	*K	cal/ K g	cal/"K avg g atom
1	1763	0.151	7.92	3	2237	0.214	11.23
1	1817	0.163	8.55	5	2237	0.224	11.75
1	1.840	0.178	9.34	2	2263	0.236	12.38
1	1868	0.221	11.60	5	2265	0.210	11.02
4	1952	0.210	11.02	7	2265	0.269	14. 11
1	1961	0.208	10.91	3	2278	0.209	10.97
3	1970	0.230	12.07	2	2286	0 . 259	13.59
1	1971	0.225	11.81	4	2293	0.241	12.64
1	1983	0.225	11.81	2	2298	0.245	12.85
1	2051	0.220	11.54	5	2301	0.200	10.49
4	2053	0.237	12.43	3	2308	0.199	10.44
1	2068	0.234	12.28	2	2339	0.236	12.38
1	2077	0.232	12.17	5	2342	0.233	12.23
5	2091	0.202	10.60	2	2345	0.208	10.91
1	2095	0.234	12.28	3	2346	. 0. 204	10.70
3	2115	0.236	12.38	4	2351	0.199	10.44
ì	2141	0.219	11.49	6	2360	0.238	12.49
= 1	2146	0.231	12.12	6	2367	0.236	12.38
5	2154	0.210	11.02	3	2376	0.188	9.86
4	2154	0.216	11.33	5	2376	0 . 220	11.54
1	2158	0 . 241	12.64	5	2409	0.230	12.07
2	2193	0.203	10.65	4	2414	0.222	11.65
2	2199	0 - 245	. 12.85	2	2419	0 . 248	13.01
2.	2206	0.270	14.17	3	2421	0.266	13.96

TABLE LXXXI (Concl'd)

Run	Temp		C <sub>o</sub>
No.	*к	cal/°K g	cal/°K avg g atom
7	2421	0.273	14. 32
2	2425	0.259	13.59
5	2440	0.290	15. 22
3	2451	0.258	13.54
5	2453	0. 268	14.06
7	2457	0.286	15.01
6	2464	0.240	12.59
3	2471	0.206	10.81
4	2475	0 . 228	11.96
2	2475	0.206	10.81
2	2477	0.209	10.97
2	2488	0.223	11.70
2	2494	0.233	12.23
2	2506	0.236	12.38
3	2507	0.221	11.60
2	2515	0.213	11.18
6	2518	0.235	12.33
3	2529	0.224	11.75

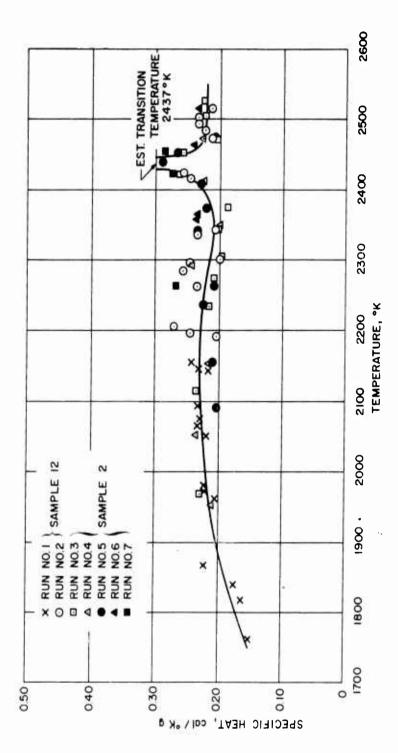


Figure 17 SPECIFIC HEAT OF NIOBIUM CARBIDE VERSUS TEMPERATURE

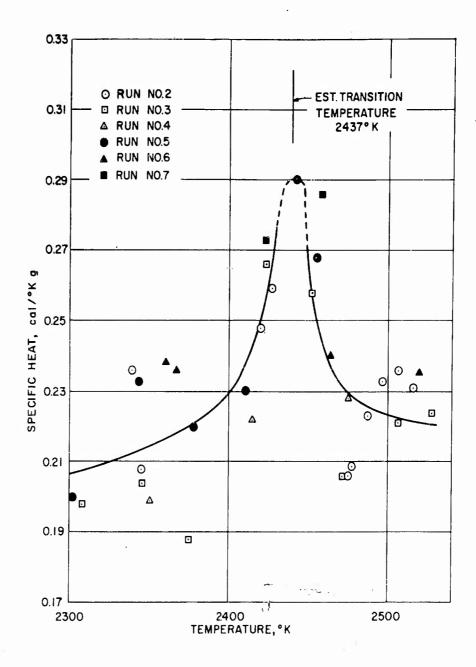


Figure 18 DETAILS OF REVERSIBLE TRANSITION IN NIOBIUM CARBIDE

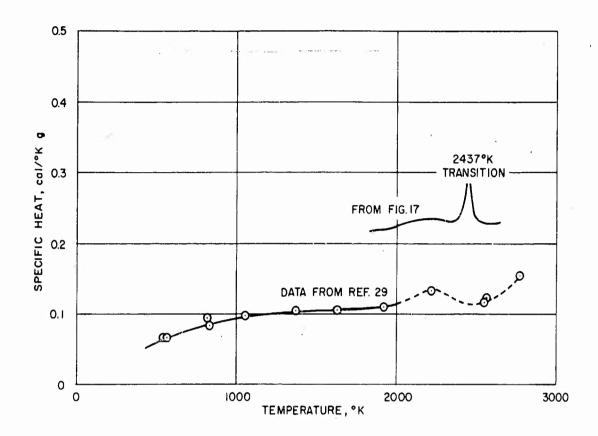


Figure 19 COMPARISON OF NIOBIUM CARBIDE SPECIFIC HEATS

Element	Percent
Total C	6.27 Avg.
Free C	0.04
0	0.18 Avg.
Ta	90.48
Ti	0.90
Fe	0.20
Mn	0.07
Hf	0.22
Nb	1.62
Zr	0.17
Cu	<0.01
Ct	<0.01 .
Ni	<0.01
N	0.09

The results of the high-temperature specific heat measurements are summarized in Table LXXXII and figure 20. A comparison of data from all sources is made in figure 21. The Southern Research Institute data<sup>29</sup> appear to have the best overall temperature dependence, but their general level appears to be slightly low in comparison with that of the other two sets of data.

Better agreement between the TaC specific heat data from various sources <sup>29</sup>, <sup>491</sup> would be desirable for the preparation of thermodynamic tables. Further measurements were being made on a second specimen at the time of report writing to help resolve these discrepancies.

<sup>491&</sup>lt;sub>Margrave</sub>, J.L. Private Communication (21 March 1961).

TABLE LXXXII

TANTALUM CARBIDE (Tac) HEAT CAPACITY (APPROXIMATELY 96.7 PERCENT PURITY)

Temp		Cp	Temp		C <sub>p</sub>
°K	cal/°K g	cal/°K avg g atom	*K	cal/*K g	cal/ "K avg g atom
1763	0.0691	5.98	2321	0.0922	7.97
1780	0.0786	6.80	2349	0.0888	7.68
1789	0.0800	6.92	2360	0.0908	7 . 85
1804	0.0855	7.39	2379	0.0892	7.71
1939	0.0693	5.99	2396	0.0935	8.09
1997	0.0945	8.17	2401	0.0966	8.35
2023	0.0710	6.14	2406	0.0845	7.31
2052	0.0822	7.11	2408	0.1027	8.88
2058	0.0793	6.86	2426	0.0831	7.19
2068	0.0857	7.41	2433	0.0917	7.93
2076	0.0832	7.20	2448	0.0837	7.24
2078	0.0953	8. 24	2448	0.1086	9 . 39
2115	0.0768	6.64	2455	0.1080	9.34
2125	0.1011	8.74	2460	0.0858	7.42
2132	0.0791	6.84	2460	0.0972	8.41
2188	0.1054	9.12	2465	0.1065	9. 21
2234	0.0833	7.20	2472	0.0728	6.30
2258	0.0824	7.13	2474	0.1090	9.43
2291	0-0905	7.83	2474	0.0958	8. 29
2297_	0.1065	9 - 21	2507	0.0878	7.59
2309	0.1070	9.25	2544	0.0782 .	6.76
2316	0.0946	8.18			

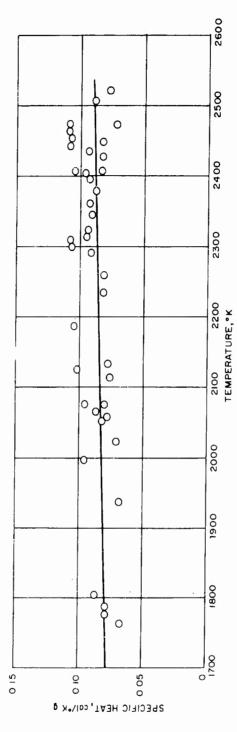


Figure 20 SPECIFIC HEAT OF TANTALUM CARBIDE VERSUS TEMPERATURE

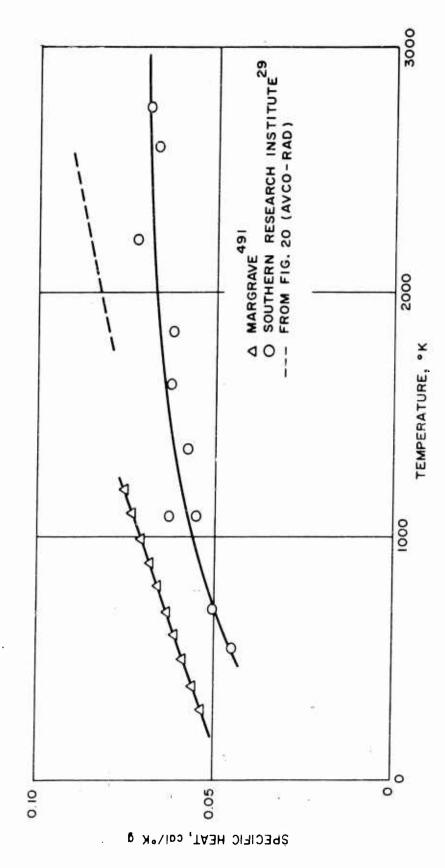


Figure 21 COMPARISON OF TANTALUM CARBIDE SPECIFIC HEATS

### d. Titanium Diboride (TiB2)

The X-ray diffraction diagram of the titanium diboride specimen was composed of a TiB<sub>2</sub> pattern and weak additional lines that were not identified. The following results of the chemical analyses showed that the specimen was only about 92 percent pure:

Element	Percent
o	0.77
С	1.24
В	26.61
Total Ti	64.90
Cu	0.005
A1	<0.1
Mo	
Zr	0.51
Nb	0.09
Hf	<0.1
Fe	0.17
Cr	
v	
Mg	<0.001
Ni	

Specific heat measurements were continued on the impure TiB<sub>2</sub> specimen since it was felt that corrections could be made later for the impurities and that the results would provide information on the effect of impurities on C<sub>p</sub><sup>o</sup> values at high temperatures. The results are summarized in Table LXXXIII and figure 22.

TABLE LXXXIII

TITANIUM DIBORIDE (TiB<sub>2</sub>) HEAT CAPACITY (Approximately 92 percent purity)

	C <sub>p</sub> °
cal/ <sup>o</sup> K g	cal/ <sup>O</sup> K avg g atom
0.384	8.28
0.423	9.13
0.388	8. 39
0.366	7.90
0.542	11.78
0.527	11.45
0.559	12. 15
0.546	11.85
0.541	11.73
0.588	12.75
0.581	12.59
0.611	13.26
0.604	13.10
0.607	13.17
0.675	14.65
0.647	15.00
0.680	15.76
0.680	15.76
	0. 384 0. 423 0. 388 0. 366 0. 542 0. 527 0. 559 0. 546 0. 541 0. 588 0. 581 0. 611 0. 604 0. 607 0. 675 0. 647 0. 680

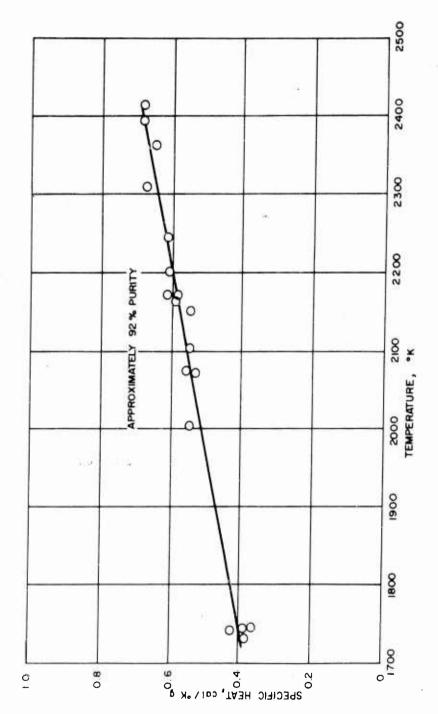


Figure 22 SPECIFIC HEAT OF TITANIUM DIBORIDE VERSUS TEMPERATURE

A comparison of these results with those of Margrave 491 (purity unspecified) is shown in figure 23. The specific heat of the impure specimen appears to be exceedingly high. Nothing else was found in the measurements to account for these high results. The surprisingly large apparent effect of the impurities in this specimen should be further investigated.

## e. Titanium Carbide (TiC)

X-ray diffraction analysis of the titanium carbide specimen showed it to consist of a single phase of TiC. The following results of chemical analyses showed its purity to be approximately 95 percent:

	аррголинатог, 75 р	
Element	Percent	
Cu	0.004	
A1	<0.1	
Mn		
Zr	0.56	
Nb	0.09	
Hf	<0.1	
Fe	0.12	
Cr		
v		
Мg	<0.001	
Ni		
Total Ti	77.41	
Free Ti	0.5	
Total C	17.78	
Free C	0.43	

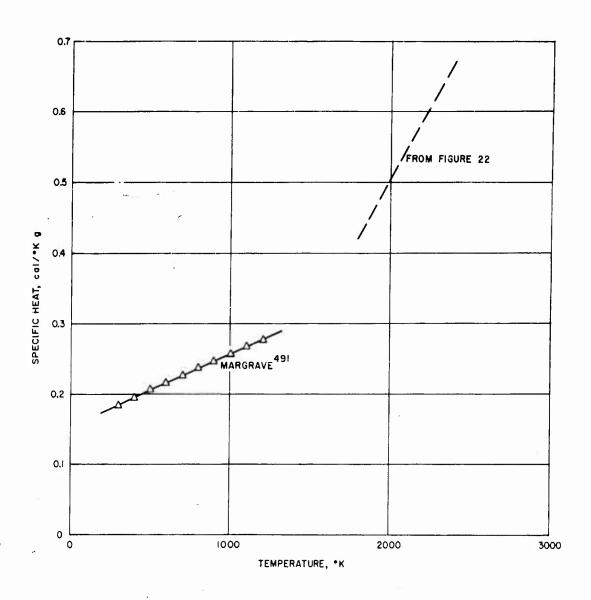


Figure 23 COMPARISON OF TITANIUM DIBORIDE SPECIFIC HEATS

The results of the specific heat measurements are summarized in Table LXXXIV and figure 24. Figure 25 shows a comparison of available specific heat data on TiC. 56, 464 The agreement between different sets of data is very poor. Impurities here again appear to have a large effect on both the level and slope of the specific heat versus temperature line obtained on this project.

#### f. Titanium Nitride (TiN)

The specific heat determinations on TIN were made in connection with another project wherein analytical data were not obtained. The results are reported here because of their importance to this project.

The results are summarized in Table LXXXV and figure 26. The data from various sources are compared in figure 27. The agreement between the sets of data is better in this case than in the others already considered. The purity of the TiN specimen used on this project was therefore probably satisfactory.

#### g. Tungsten Boride (WB)

X-ray diffraction analysis of the tungsten boride specimen revealed the existence of a single phase of WB. The following results of the chemical analyses showed that the sample purity was approximately 98.9 percent:

Element	Percent
W	93.7
В	5.16
С	0.09
o	0.16
N	0.01
Impurities	~0.88

The results of the specific heat determinations are summarized in Table LXXXVI and figure 28. The values in units of cal/°K avg g atom seem reasonable for the temperature range covered.

TABLE LXXXIV

TITANIUM CARBIDE (Tic) HEAT CAPACITY

Temperature	C <sub>p</sub> °		
°ĸ	cal/ <sup>o</sup> K g	cal/ <sup>o</sup> K avg g atom	
2023	0.467	13.99	
2113	0.535	16.03	
2186	0.520	15. 58	
2279	0.564	16.90	
2353	0.589	17.64	
2449	0.604	18.09	
2506	0.602	18.03	
2412	0.476	13.99	
2252	0.510	15. 28	
2121	0.559	16.75	

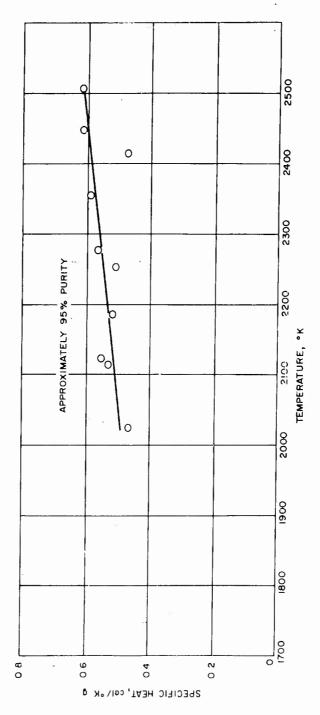


Figure 24 SPECIFIC HEAT OF TITANIUM CARBIDE VERSUS TEMPERATURE

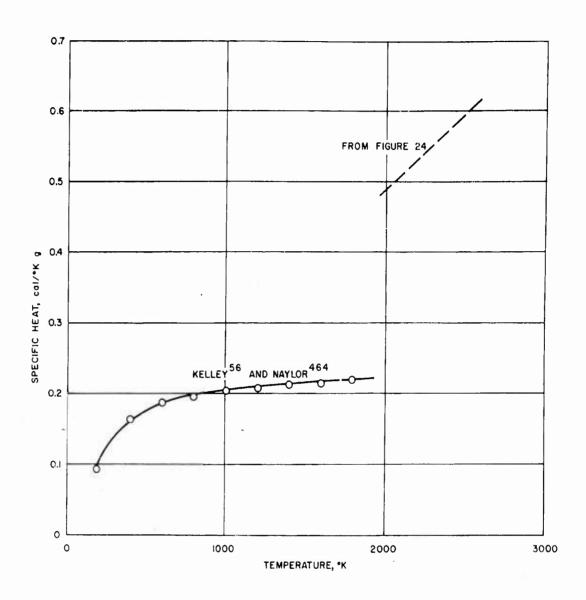


Figure 25 COMPARISON OF TITANIUM CARBIDE SPECIFIC HEATS

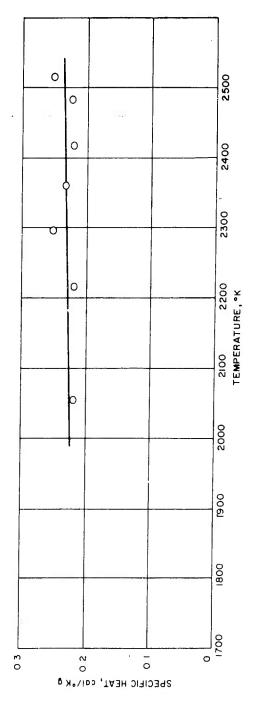


Figure 26 SPECIFIC HEAT OF TITANIUM NITRIDE VERSUS TEMPERATURE

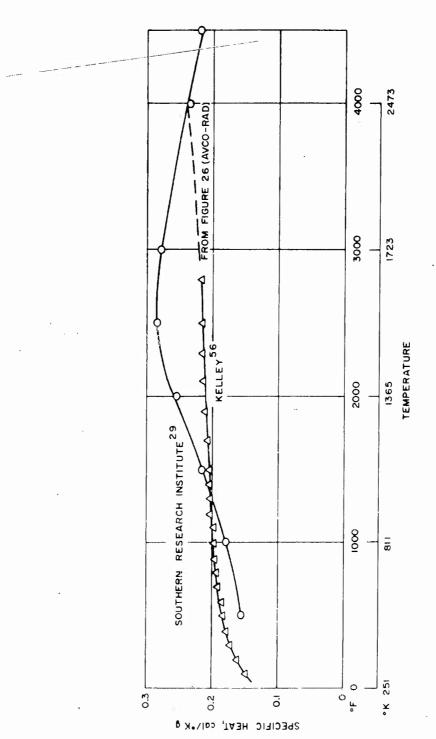


Figure 27 COMPARISON OF TITANIUM NITRIDE SPECIFIC HEATS

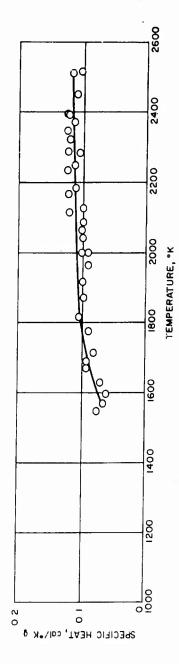


Figure 28 SPECIFIC HEAT OF TUNGSTEN BORIDE VERSUS TEMPERATURE

TABLE LXXXV

TITANIUM NITRIDE (Tin) HEAT CAPACITY

- Ĺ -

Temperature	Сŷ		
, o <sup>K</sup>	cal/ <sup>o</sup> K g	cal/ <sup>o</sup> K avg g atom	
2052	0.219	6.78	
2217	0.220	6.81	
2298	0.253	7.83	
2360	0.234	7.24	
2418	0.221	6.84	
2482	0.223	6.90	
2512	0.253	7.83	

TABLE LXXXVI

TUNGSTEN BORIDE (WB) HEAT CAPACITY
(APPROXIMATELY 98.9 PERCENT PURITY)

Temp.	C°		Temp.	С°	
°K	cal/°K g	cal/°K avg g atom	°К	cal/°K g	cal/°K avg g atom
1556	0.074	7.20	2118	0.121	11.78
1574	0.069	6.72	21 29	0.101	9.83
1597	0.065	6.33	2169	0.123	11.97
1630	0.076	7 · 40	2192	0.114	11.10
1674	0.091	8.86	2232	0.122	11.88
1688	0.091	8.86	2247	0.117	11.39
1718	0.085	8. 27	2281	0.110	10.71
1775	0.091	8.86	2286	0.125	12.17
1819	0.108	10.51	2321	0.118	11.49
1868	0.102	9.93	2345	0.129	12.56
1920	0.101	9.83	2379	0.118	11.49
1961	0.094	9.15	2393	0.123	11.97
2000	0.107	10.42	2399	0.125	12.17
2000	0.100	9.73	2458	0.116	11.29
2057	0.104	10.12	2518	0.109	10.61
2074	0.107	10.42	2518	0.120	11.68
2086	0.102	9.93			
	9				

# h. Zirconium Diboride (ZrB2)

The X-ray diffraction diagram of the zirconium diboride specimen contained a pattern of hexagonal ZrB<sub>2</sub> plus a weak pattern of ZrC. The following results of the chemical analyses indicated a purity of approximately 95.8 percent:

Element	Percent
Zr	78.94
В	16.86
o	1.36
Total C	0.37
Hf	<0.25
Fe	0.18
Ti	0.14
Mg	<0.01
Cu	<0.05
Mn	<0.01
v	<0.2
Nb	. <0.01
Ni	<0.5
Cr	<0.1
Λ1	<0.3
N	0.14

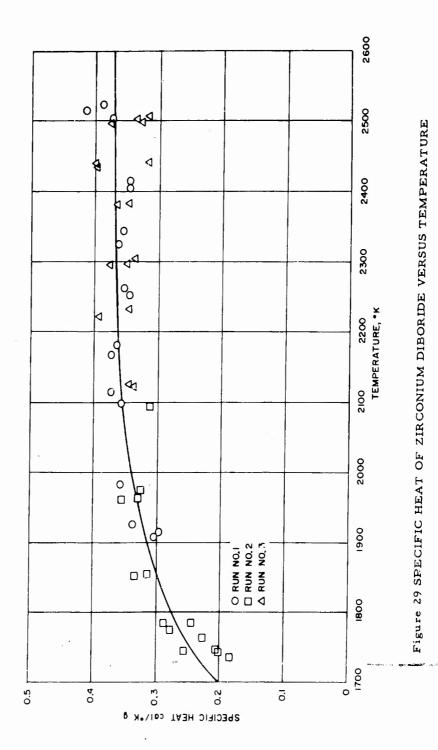
Results of the specific heat determinations are summarized in Table LXXXVII and figure 29.

Repeated runs on the same specimen of ZrB<sub>2</sub> revealed no drift in specific heat versus time. This was taken as evidence that the effect of reactions with the carbon vapor in the furnace was negligible.

TABLE LXXXVI

ZIRCONIUM DIBORIDE (Z:B2) HEAT CAPACITY
(APPROXIMATELY 95.8 PERCENT PURITY)

Run	Temp.		Cp	Run	Temp.		Cp
No.	°ĸ	cal/ <sup>0</sup> K g	cal/ K avg g atom	No.	°к	cal/ <sup>O</sup> K g	cal/ K avg g atom
2	1739	0.183	6.88	1	2169	0.372	14.00
2	1742	0.200	7.52	1	2183	0.367	13, 81
2	1745	0.255	9.59	3	2224	0.392	14.75
2	1749	0.205	7.71	3	2232 -	0.347	13.05
2D	1765	0.228	8.58	1	2253	0.345	12.98
2D	1776	0.279	10.50	1	2265	0.352	13.24
2D	1786	0.288	10.84	3	2298	0.375	14.11
2D	1786	0.242	9, 10	3	2298	0.349	13.13
2	1852	0.333	12.53	3	2306	0.337	12.68
2	1856	0.315	11.85	ì	2 3 2 7	0.361	1 3. 58
1	1909	0.304	11.44	1	2345	0.357	13.43
1	1914	0.298	11.21	3	2382	0.365	13.73
1	1929	0.339	12.75	3	2384	0.346	13.02
2	1961	0.355	13.36	1	2408	0.346	13.02
2	1966	0.330	12,42	1	2414	0.346	13.02
2	1974	0.326	12.26	3	2437	0.389	14.63
1	1983	0.359	13.51	3	2440	0.389	14.63
2	2097	0.311	11.70	3	2443	0.314	11.81
1	2100	0.358	1 3. 47	3	2498	0.376	14.15
1	2115	0.372	14.00	3	2500	0.326	12. 26
3	2121	0.339	12.75	3	2504	0.332	12, 49
3	2127	0.344	12.94	3	2507	0.315	11.85
				1	2507	0.371	13.96
				1	2518	0.415	15. 61
				1	2521	0.389	14.63



1-380

# i. Zirconium Carbide (ZrC)

The X-ray diffraction diagram of the ZrC specimen contained a pattern of ZrC plus a weak pattern of ZrB<sub>2</sub>. The results of the following chemical analyses revealed the sample purity to be approximately 94.7 percent:

Element	Percent
Zı	84. 23
0	1.21
Total C	10.46
Hf	0.78
Fe	0.19
Ti	0.14
Мд	<0.01
Cu	0.15
Mn	0.02
v	0.07
Nb	<0.3
Ni Ni	<0.2
Cr	
<b>A</b> 1	0.12
Free C	0.25
N	1.03

Specific heat determinations were repeated several times in this case also in an attempt to detect any effect of the carbon vapor. No effect can be detected in the data which are summarized in Table LXXXVIII and figure 30. Specific heat data from various sources are compared in figure 31. Sample impurities (~4.3%) are probably again the cause of the high values in the figure 30 data.

TABLE LXXXVIII

# ZIRCONIUM CARBIDE (Zrc ) HEAT CAPACITY (APPROXIMATEI Y 94.7 PERCENT PURITY)

Run	Temp.		С°р	Run	Temp.	C <sub>p</sub> °	
No.	•к	cal/*K g	cal/*K avg g atom	No.	*к	cal/*K g	cal/*K avg g atom
3	1639	0.204	10.53	2	2132	0.196	10.12
3	1648	0.171	8.83	3	2138	0.213	10.99
3	1675	0 - 225,	11.61	1	2146	0.205	10.58
3	1696	0.187	9.65	3	2147	0.186	9.60
3	1721	0.200	10.32	3	2164	0.223	11.51
3	1799	0.193	9.96	4	2166	0.215	11.10
3	1814	0.195	10.07	3	2169	0.234	12.08
3	1897	0.221	11.41	4	2172	0.210	10.84
3	1915	0.196	10.12	. 3	2175	0.247	12.75
1	1955	0.206	10.63	1	2189	0.231	11.92
3	2017	0.182	9.39	1	2198	0.225	11.61
1	20 23	0.204	10.53	2	2206	0.208	10.74
1	2057	0.204	10.53	4	2232	0 - 211	10.89
4	2071	0.208	10.74	4	2238	0.217	11.20
3	2080	0.202	10.43	1	2243	0.211	10.89
4	2080	0 208	10.74	2	2249	0.189	9.76
2	2085	0208	10.74	2	2252	0.201	10.38
3	2094	0.189	9.76	4	2286	0.203	10.48
4	2094	0 - 213	10.99	1	2298	0.213	10.99
2	2100	0.221	11.41	4	2306	0.200	10.32
4	2107	0 232	. 11.98	2	2310	0.186	9.60
4	2113	0.224	11.56	4	2364	0.167	8.62
1	2113	0.224	11, 56	1	2364	0.191	9.86
2	2118	0 210	10.84	4	2367	0.182	9.39

TABLE LXXXVIII (Concl'd)

1       2403       0.178       9.19         4       2411       0.176       9.08         4       2420       0.181       9.34         4       2471       0.180       9.29         4       2474       0.199       10.27         4       2483       0.187       9.65         4       2486       0.181       9.34	Run	Temp.		C <sub>p</sub> °
4     2411     0.176     9.08       4     2420     0.181     9.34       4     2471     0.180     9.29       4     2474     0.199     10.27       4     2483     0.187     9.65       4     2486     0.181     9.34	No.	•к	cal/°K g	cal/°K avg g atom
4     2420     0.181     9.34       4     2471     0.180     9.29       4     2474     0.199     10.27       4     2483     0.187     9.65       4     2486     0.181     9.34	1	2403	0.178	9.19
4     2471     0.180     9.29       4     2474     0.199     10.27       4     2483     0.187     9.65       4     2486     0.181     9.34	4	2411	0.176	9.08
4     2474     0.199     10.27       4     2483     0.187     9.65       4     2486     0.181     9.34	4	2420	0.181	9.34
4 2483 0.187 9.65 4 2486 0.181 9.34	4	2471	0.180	9. 29
4 2486 0.181 9.34	4	2474	0.199	10.27
	4	2483	0.187	9.65
4 2402 0 106 10 12	4	2486	0.181	9.34
4 2492 0.190 10.12	4	2492	0.196	10.12
4 2495 0.191 9.86	4	2495	0.191	9.86
4 2499 0.196 10.12	4	1	0.196	10.12

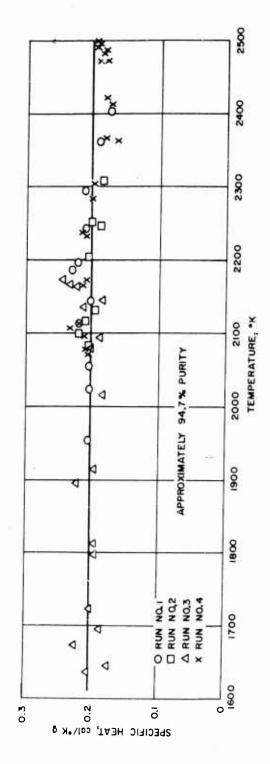


Figure 30 SPECIFIC HEAT OF ZIRCONIUM CARBIDE VERSUS TEMPERATURE

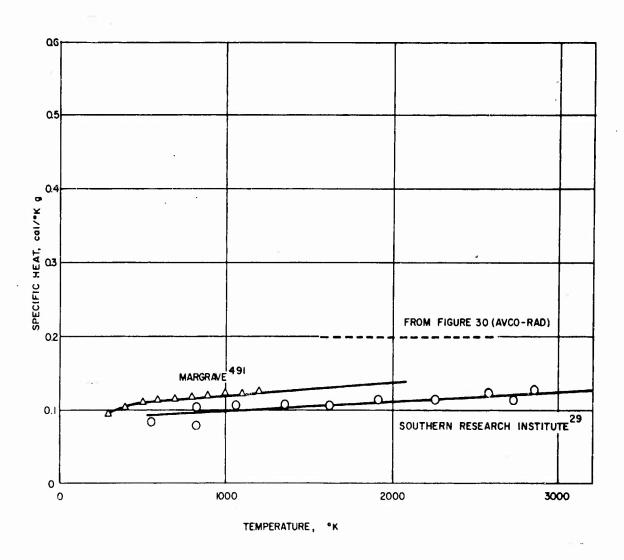


Figure 31 COMPARISON OF ZIRCONIUM CARBIDE SPECIFIC HEATS

#### C. SPECTROSCOPIC STUDIES

#### 1. Introduction

Two important experimental techniques for the study of the vapors of refractory materials are as follows: (a) the vapor effusion technique with mass spectrometric identification of vapor species, and (b) the recording of the optical absorption or emission spectra of the vapors. These two techniques complement each other in that each provides needed data which the other cannot give.

The effusion-mass spectrometer technique, which has provided most of the published data, provides species identification and vapor pressures as a function of temperature of the various species in equilibrium with the condensed phase. From these quantitative data, one can calculate a number of thermodynamic properties, but a complete thermodynamic analysis requires the use of molecular parameters provided by optical spectroscopy.

Experiments utilizing optical spectroscopy can also be made to give quantitative data on the overall vapor-condensed phase equilibria, but usually not as easily and unambiguously as the effusion-mass spectrometer method. The great value of the optical spectroscopic technique is that it can give information on the intrinsic properties of the vapor species themselves. For example, the optical spectra yield molecular vibration frequencies which are needed for statistical mechanical calculations of free-energy functions, entropies, and enthalpies. Optical spectra also yield molecular configurations, force constants, bond strengths, and bond lengths, which are necessary for a basic understanding of chemical bonding and chemical reactions at high temperature. The latter parameters of similar compounds are often used to estimate vibration frequencies, moments of inertia, etc., for statistical mechanical calculations on species whose spectra have not been studied.

Part of the program of experimental studies in Phase III of this project was concerned with the determination of the molecular quantities just discussed for the vapor species in equilibrium with the solid phases of the refractory compounds included in the scope of the contract.

## 2. Experimental Technique

Absorption spectroscopy has been utilized in these studies of refractory compound vapors in preference to emission spectroscopy because it presents fewer basic experimental difficulties. The emission spectrum of a high-temperature vapor can be observed if the radiation emitted by the gaseous molecules can be distinguished from that scattered and emitted by hot particles condensed from the vapor. If condensation is successfully minimized or avoided, the use of a sensitive detection system will permit the emission

spectrum to be observed over a short optical path. Unfortunately, it is experimentally difficult to avoid condensation in systems at very high temperature, and other measures must be taken to circumvent the problem. When an absorption spectrum is recorded, the problems presented by emitting and scattering condensate particles can be greatly reduced by modulation of the light from the source before passing it through the vapors. A tuned detection system can then discriminate the transmitted light from the light which originates in the hot zone. This does, however, require a relatively long optical path.

The present absorption work was performed with light paths of up to 200 feet through the hot vapors. Such long paths were achieved by the use of the White multiple reflection technique. The absorption spectrum could be observed conveniently when the vapor pressure above the refractory sample was only a few microns. Being able to work at low vapor pressure presented a number of advantages, among which were the following:

- a. Small quantities of material could be used and the sample was not lost rapidly.
- b. It was not necessary to have inert gas present. Hence, convection currents were eliminated, and particle condensation was greatly reduced.
- c. Reactions between the hot container and the material under study were usually not serious when the vapor pressure of the material was low
- d. Since convection currents were eliminated, it was not necessary to confine the vapors to a uniformly heated tube, and the refractory material could be evaporated from a hot filament, thus keeping power input and heat removal requirements down to a minimum.

A schematic diagram of the experimental apparatus is given in figure 32. Figure 33 is a photograph of the experimental apparatus (not including the power supply), and figure 34 shows some details of the interior of the reaction chamber. The entire heating, cooling, and optical assembly was mounted on an aluminum channel which slid out of the vacuum tank as shown in figure 34.

The heating element from which the material was evaporated consisted of a tungsten ribbon 0.004 inch thick, 1-1/2 inches wide, and 24 inches long. This ribbon was heated by the current from a bank of batteries and could reach temperatures above 3000°K. One end of the tungsten ribbon was connected directly to the electrically grounded channel. The other end went to

<sup>492</sup> White, J. N., J. Optical Soc. Am. 32, 285 (1942).

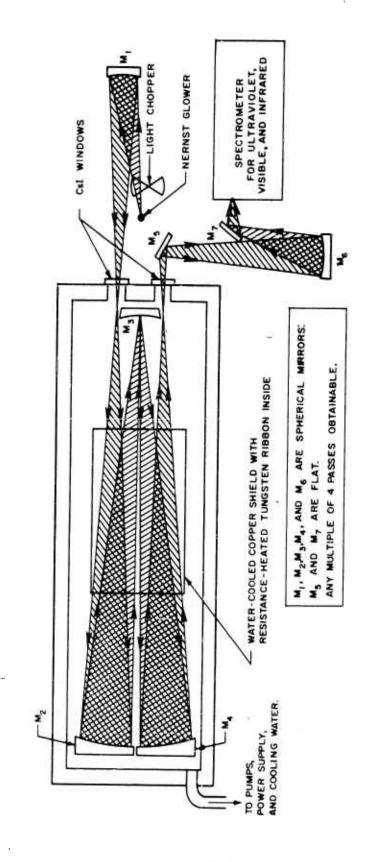
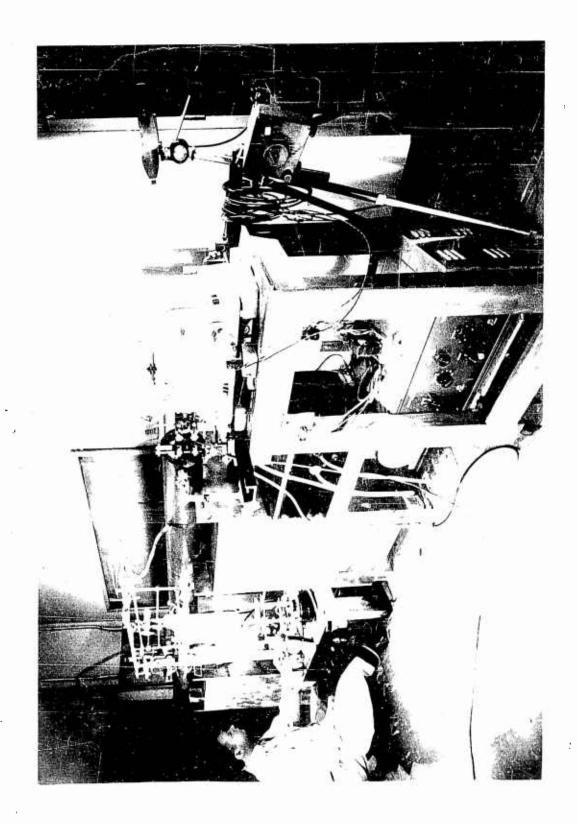
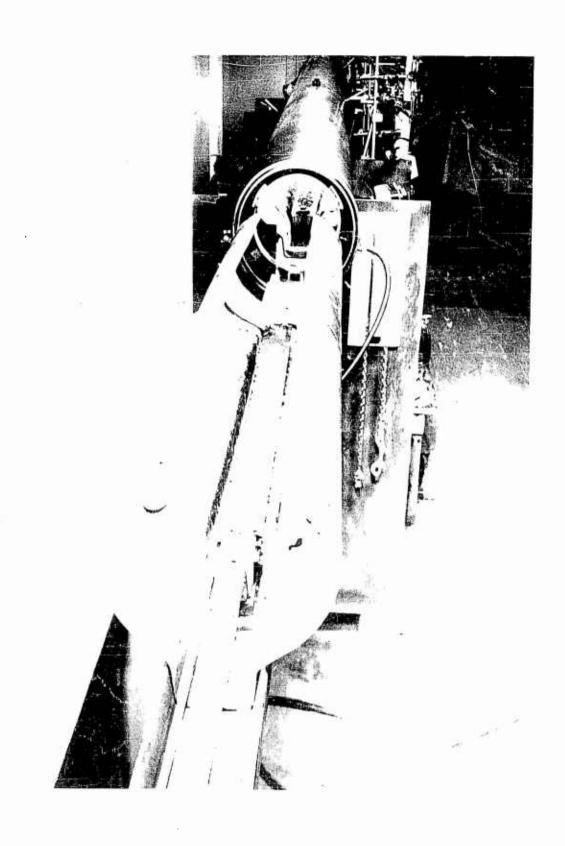


Figure 32 SCHEMATIC OF APPARATUS WITH FOLDED LIGHT PATH



::: ::: ::: :::



the plus side of the batteries through a flexible cable which was springloaded to prevent the tungsten ribbon from going slack when it expanded on heating.

The heat radiated by the hot filament was removed from the interior of the vacuum tank by means of a water-cooled copper shield (shown in Fig. 34) which surrounded the sample. The heating element was sufficiently remote from the mirrors so that the latter did not heat up excessively or become coated with the condensed refractory vapor.

The vacuum chamber consisted of a steel pipe 8 inches in diameter and 11 feet long. The ends of the pipe were closed with Lucite discs in which were mounted KBr or CsI windows. It was evacuated by means of mechanical pumps to about 2 microns of pressure.

The spherical mirrors were aluminum-coated and had a 10-foot radius of curvature.

In operation, light from the Nernst glower source was projected into the White mirror system as a 4X-enlarged image; and, after being passed the desired number of times through the vapors, it was focused as a much-reduced image into the Perkin-Elmer monochromator. The number of light passes through the vacuum chamber depended on the angle between the mirrors paired at one end of the cell. When a total light path of 1000 feet was used (200 feet over the filament), the transmitted light was still detectable over the spectral region accessible with sodium chloride optics. The 13-cycle light modulation took place prior to traversal through the vapor. The tuned detection system responded only to light which had been passed through the vapors and not to unmodulated light emitted or scattered by hot particles or gases in the tank. By the use of various prisms and detectors, the spectral region from 0.2 and 40 microns could be covered.

A typical experiment was performed as follows:

- 1) The powdered refractory was sprinkled on the tungsten ribbon.
- 2) The carriage was pushed into the vacuum tank, water and power connections were made, and the optical system was adjusted for the desired number of traversals, which might be 100 or less.
- 3) The tank was evacuated to a pressure of 1 or 2 microns.
- 4) The desired current, usually between 200 and 500 amperes, heated the filament and slowly vaporized the refractory powder.

- 5) The absorption spectrum of the vapors was recorded while they were diffusing to and depositing on the water-cooled shield.
- 6) The filament temperature was read by sighting with an optical pyrometer through the Lucite disc at one end of the vacuum chamber.

### 3. Experimental Results

#### a. Silicon Carbide

Silicon, evaporated from a carbon filament, and silicon carbide, evaporated from a tungsten filament, both yielded the absorption spectrum shown in figure 35. The light path through the heated vapors was approximately 150 feet long.

According to Drowart et al the vapors in equilibrium with silicon carbide at 2200°K include approximately  $5 \times 10^{-6}$  atmosphere each of SiC<sub>2</sub> and Si<sub>2</sub>C .  $^{493}$  They are the most predominant species in the vapor, except for silicon atoms.

In the optical spectrum, there appeared to be one strong broad band centered at about 1080 cm<sup>-1</sup> and two weaker bands centered at about 850 cm<sup>-1</sup> and 600 cm<sup>-1</sup>, respectively. The breadth of the bands was considerably greater than one is accustomed to seeing in absorption spectra at ordinary temperatures. This breadth may be attributed both to the spreading of the rotational structure due to the high temperature and to the superposition of "hot" bands on the fundamental band. It appears to be impossible to locate the band origin exactly. Therefore, the best that can be done is to choose the center of the band and to assign to it the corresponding vibrational frequency. 493

Kleman has observed blue-green electronic emission bands, which he ascribed to  $\mathrm{SiC}_2$ , and from an analysis of the spectrum, predicted infrared bands at 1742 and 591 cm<sup>-1</sup>, but not at 1080 cm<sup>-1</sup>. <sup>494</sup> It, therefore, seemed likely that the emitter of the 1080 cm<sup>-1</sup> band was  $\mathrm{Si}_2\mathrm{C}$ . Drowart assumed  $\mathrm{Si}_2\mathrm{C}$  to be a linear asymmetric molecule, by analogy with  $\mathrm{SiC}_2$ , and estimated its vibration frequencies to be  $\omega_1$  = 799 cm<sup>-1</sup>,  $\omega_2$  = 265 cm<sup>-1</sup>, and  $\omega_3$  = 446 cm<sup>-1</sup>. It appeared more likely, however, that the structure of the  $\mathrm{SiC}_2$  molecule was linear symmetric (Si-C-Si) because the magnitude of the vibrational force constants shows definitely that the Si-C bond is stronger than that of Si-Si (for Si-C, k = 3.1 x 105 dynes per cm, and for Si-Si, k = 2.1 x 105 dynes per cm). <sup>493</sup>

<sup>493</sup>Drowart, J., G. DeMaria, and M. G. Inghram, J. Chem. Phys. 29, 1015 (1958).

<sup>494</sup>Kleman, B., Astrophys. J. 123, 162 (1956).

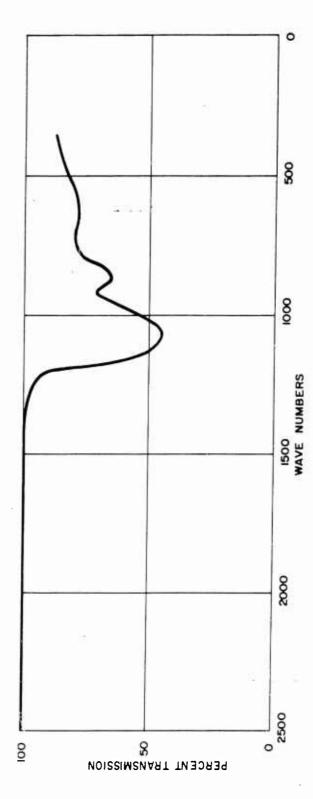


Figure 35 INFRARED ABSORPTION SPECTRUM OF VAPORS FROM A SILICON-CARBON SYSTEM HEATED TO 2200° K

The assumption that the structure is Si-C-Si permits the calculation of the force constants from the observed infrared spectrum. 400 Only the  $\omega_3$  band is expected to occur in the region from 2 to 15 microns.  $\omega_1$  is not infrared active because of symmetry considerations; and  $\omega_2$ , the bending mode, will occur at longer wavelengths. The 1080 cm<sup>-1</sup> band must therefore be associated with  $\omega_3$ , and the corresponding force constant is  $k = 3.4 \times 10^5$  dynes per cm. This value of k corresponds to the bond strength of the Si-C bonds in  $SiC_2$ , where k = 2.9 $x 10^5$  dynes per cm, and to that in SiC, where  $k = 3.1 \times 10^5$  dynes per cm.  $\omega_1$ , associated with the symmetric stretching vibration, was calculated from k to be 447 cm<sup>-1</sup>. If the bending force constant,  $k_{\delta}$ , is similar to that measured for  $CO_2$  and  $CS_2$ , or approximately 0.65 x  $10^{-11}$ dyne-cm/rad, the doubly degenerate vibrational mode,  $\omega_2$ , will occur at about 435 cm<sup>-1</sup>. No particular band is evident at that frequency in figure 35. If the band exists, it must be very weak and is probably overlapped by the broad 591 cm<sup>-1</sup>  $\omega_1$  band of SiC<sub>2</sub> which is perhaps discernible in the spectrum.

The somewhat narrower band which shows in the spectrum at 850 cm<sup>-1</sup> may possibly be due to an impurity; it does not seem likely that it would be due to any species containing only silicon and carbon. Pure silicon was vaporized, and its spectrum was recorded to see whether this band might possibly be due to Si<sub>3</sub>. This was found not to be the case. The silicon vapor showed no absorption bands in the region from 2 to 15 microns even at high partial pressure.

#### b. Molybdenua Trioxide

As stated in section IV-B5, there were no spectroscopic data reported for the gaseous species of molybdenum oxides. The properties of these oxides made them good candidates for study by the techniques described in section V-C2 above, and the investigation was undertaken.

The infrared absorption spectrum of the vapors from  $M_0O_3$  is shown in figure 36. It consists of one strong band centered at about 810 cm<sup>-1</sup>.  $M_0O_3$  was reported 427, 417 to vaporize principally as the trimer,  $M_0O_3$ . A likely structure for this trimer appears to be a puckered, 6-membered ring of alternating molybdenum and oxygen atoms with the other 6 oxygen atoms doubly bonded to the molybdenum atoms, 3 above the ring and 3 below.

The vibrational pattern of such a large molecule is undoubtedly extremely complicated, but it can be expected to have as a predominant feature the stretching of the 6 Mo = 0 bonds. Hence, it seems reasonable to attribute the one strong band observed to the stretching vibration between oxygen and the rest of the molecule. This permits the calculation

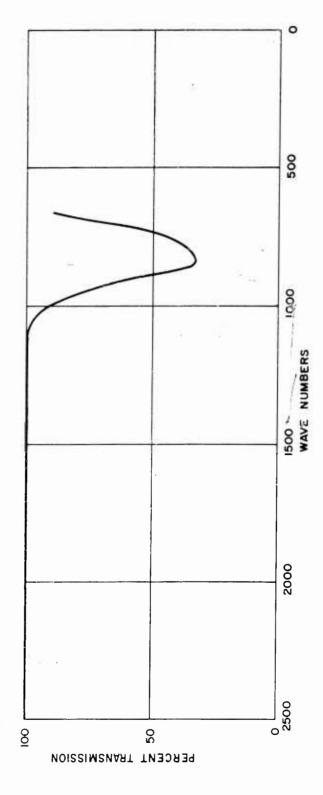


Figure 36 INFRARED ABSORPTION SPECTRUM OF VAPORS FROM MOLYBDENUM TRIOXIDE HEATED TO 1040\*K

of the stretching force constant, k, from equation (255), where  $\mu$  is the reduced mass, and  $\nu$  the frequency.

$$\nu = \frac{1}{2\pi} \sqrt{\frac{k}{\mu}} \quad . \tag{255}$$

The value thus obtained is  $k = 6.0 \times 10^5$  dynes/cm.

This value of k can then be used to calculate vibrational frequencies for the molecules  $\text{MoO}_2$  and  $\text{MoO}_3$  if the reasonable assumption is made that the Mo = O bonds in  $\text{MoO}_2$ ,  $\text{MoO}_3$ , and  $\text{Mo}_3\text{O}_9$  are similar. This calculation yields the values  $\omega_1 = 794 \text{ cm}^{-1}$  and  $\omega_3 = 915 \text{ cm}^{-1}$ , for a linear  $\text{MoO}_2$  molecule. The estimated value of the k used in the calculation of section IV-B5b of this report would yield  $\omega_1 = 778 \text{ cm}^{-1}$  and  $\omega_3 = 898 \text{ cm}^{-1}$  for a linear  $\text{MoO}_2$ . The experimental observations thus tend to confirm the estimates used in the calculations. To revise the calculations to correct for the slight discrepancy between the estimated and experimentally measured values does not seem justified at present since the uncertainties would still remain in the value of  $\omega_2$ , and they would affect the thermodynamic functions to a greater extent than the uncertainties in  $\omega_1$  and  $\omega_3$ .

Further spectroscopic study of the gaseous molecules  ${\rm CrO_3}$ ,  ${\rm MoO_3}$ , and  ${\rm WO_3}$  over the full spectral range out to 250 cm<sup>-1</sup> will undoubtedly provide a better insight into the molecular properties, and reduce the uncertainties involved in estimating the molecular configurations and ribrational frequencies of these species.

#### c. Tungsten Trioxide

Tungsten trioxide, like molybdenum trioxide, was reported to vaporize chiefly as the trimer,  $^{417}$  which probably has the same structure as the latter, consisting of a 6-membered ring of alternating tungsten and oxygen atoms plus 6 other oxygen atoms doubly bonded to the tungstens. Its one strong infrared absorption band, which is shown in figure 37, could therefore also be assigned to the stretching vibration between oxygen and the rest of the molecule just as in the case of molybdenum trioxide. In fact, the MoO3 and WO3 molecules are analogous in most respects; and for the reasons outlined in the preceding paragraph, calculations based on the W3O9 spectrum will not be made until further experiments have been conducted.

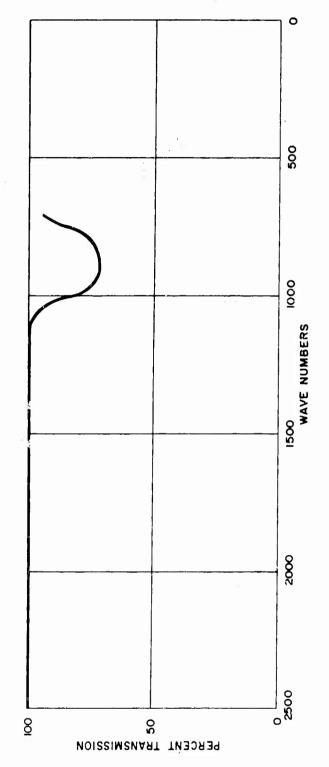


Figure 37 INFRARED ABSORPTION SPECTRUM OF VAPORS FEOM TUNGSTEN TRIOXIDE HEATED TO 1640\* K

#### d. Boron Oxides

# 1) $B_2O_3$

The infrared absorption spectrum of the vapors from  $B_2O_3$  is shown in figure 38. The path length through the gas for this experiment was approximately 200 feet. Analytical reagent-grade boric anhydride powder was sprinkled on the tung sten ribbon and vaporized at the temperatures given in the figure. From the appearance of the ribbon, there seemed to be no appreciable amount of reaction between the  $B_2O_3$  and the tungsten.

In an article on gaseous  $B_2O_3$  and  $B_2O_2$ , White et al  $^{495}$  have published an infrared emission spectrum of  $B_2O_3$ , and from it, have calculated force constants, vibrational frequencies, and thermodynamic functions. The three bands they observed in emission are marked in dotted lines at the bottom of figure 38. The band at 2050 cm<sup>-1</sup> was the strongest in emission, the one at 1300 cm<sup>-1</sup> was less strong, and the one at 740 cm<sup>-1</sup> was the weakest. As figure 38 shows, the relative intensities in absorption are much different from this. Actually, the 2050 cm<sup>-1</sup> band, White's strongest, does not appear at all in the absorption spectrum, except at the highest temperatures. The effect of the Planck function on the emission intensity would account for only a small part of this intensity discrepancy.

Dows and Porter  $^{496}$  also studied the infrared emission of  $_{203}$  and observed a band in the vicinity of 2000 cm<sup>-1</sup>. This was the only band they observed. The present results are, therefore, in disagreement with those of two previous groups of investigators on the presence of a strong  $_{203}$  band near 2000 cm<sup>-1</sup>. The absorption spectrum of solid  $_{203}$  does not show a band in the vicinity of 2000 cm<sup>-1</sup>; however, it is similar to (but not identical with) the spectrum presented herein for the vapor. The solid shows bands near  $_{3400}$  cm<sup>-1</sup> (0-H?),  $_{1470}$  cm<sup>-1</sup>, and  $_{750}$  cm<sup>-1</sup>. The spectrum of the solid was recorded from Baker-purified boric anhydride dispersed in a KBr pellet.

An investigation of the vapor of  $B_2O_3$  by the matrix isolation technique has also been reported. 497 The spectrum in this case differs from both of those described above.

<sup>495</sup> White, D., D. E. Mann, P. N. Walsh, and Λ. Sommer, J. Chem. Phys. 32, 481 (1960).

<sup>496</sup> Dows, D. A. and R. F. Porter, J. Am. Chem. Soc. 78, 5165 (1956).

Union Carbide Corp., Research in Physical and Chemical Principles Affecting High Temperature Materials for Rocket Nozzles, Semiannual Progress Report to ARPA, Union Carbide Research Inst., Tuxedo, N. Y. and Parma Research Center, Cleveland (31 December 1960).

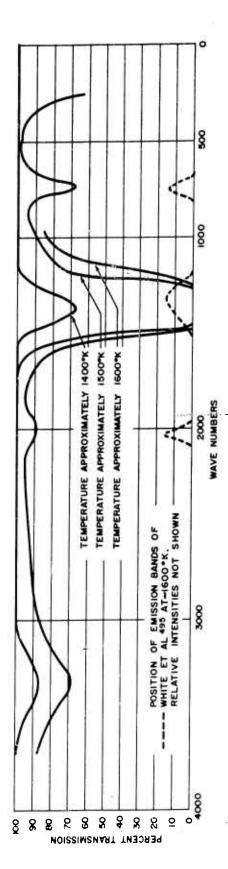


Figure 38 INFRARED ABSORPTION SPECTRUM OF VAPORS FROM BORIC ANHYDRIDE AT TEMPERATURES BETWEEN 1400\* AND 1600\* K

Because agreement between investigators on the spectrum of  $B_2O_3$  was not achieved, it did not seem justified to make vibrational assignment until the discrepancies had been resolved. If the 1350 cm<sup>-1</sup> and the 720 cm<sup>-1</sup> bands in the absorption spectrum in figure 37 come from the same molecule as the 1300 and 740 cm<sup>-1</sup> emission bands of White et al, <sup>495</sup> then the 2040 cm<sup>-1</sup> emission band of White et al<sup>495</sup> must have come from some other boroncontaining species.

This may also have been the case in the work of Dows and Porter.  $^{496}$  The investigation of  $B_2O_3$  is being continued at present. Conclusions from the spectrum of  $B_2O_3$  should be held in abeyance until the above discrepancies are removed.

### 2) $B_2O_2$

 $B_2O_2$  was prepared both by reaction of MgO with boron and by reaction of  $B_2O_3$  with boron. In each case, a material was produced which gave the infrared absorption spectrum shown by the solid curve in figure 39. The powdered  $B_2O_3$ -boron and MgO-boron mixtures were reacted on the tungsten ribbon at a ribbon temperature of approximately  $1400^{\circ}$ K. The light path through the vapor was approximately 200 feet.

Boron which was isotopically enriched to 90 percent B10 was also reacted with MgO and the spectrum of the product recorded. This spectrum is shown by the dotted curve in figure 39. The isotopically enriched elemental boron must have been purer than the naturally occurring isotopic mixture because the 940 cm<sup>-1</sup> and 1180 cm-1 bands are weaker in the B10 spectrum. The weakening of these bands plus the fact that they were not isotopically shifted would identify them as impurity bands. The 2550 cm<sup>-1</sup> band was also not shifted. The 3500 cm<sup>-1</sup> and 500 cm<sup>-1</sup> bands were not investigated for isotopic shift. The 3500 cm<sup>-1</sup> band was most likely due to hydrated species of some kind. Only the 1410 cm<sup>-1</sup> was isotopically shifted, the shift being between 30 and 50 wave numbers. The latter band was therefore the only one that could be attributed definitely to  $B_2O_2$ . If  $B_2O_2$  were a linear, symmetric molecule like its isoelectronic analog,  $C_2N_2$ , it should have only one fundamental band in this part of the infrared spectrum.

White et al  $^{495}$  attributed an emission band at 1890 cm $^{-1}$  to  $_{202}$ , and from it, calculated thermodynamic functions. However, no absorption was observed at that wavelength in the present work.

The infrared active  $\omega_3$  vibration of linear symmetric  $B_2$   $O_2$  should experience an isotopic shift of +42 cm<sup>-1</sup> in going from  $B^{11}$  to  $B^{10}$ .

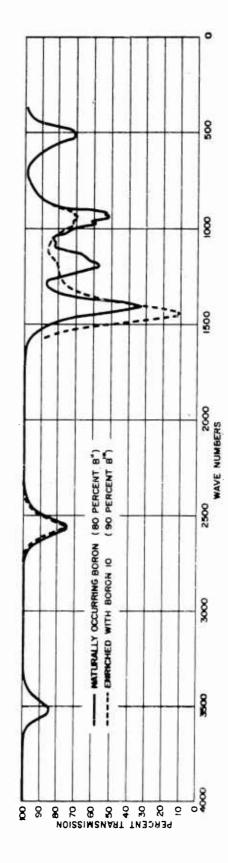


Figure 39 INFRARED ABSORPTION SPECTRUM OF B<sub>2</sub>O<sub>2</sub> VAPORS FORMED AT 1400°K

The observed shift of +30 to +50 cm<sup>-1</sup> thus tends to confirm the chemically plausible assumptions that  $B_2O_2$  is the actual species produced in these reactions and is a linear, symmetric molecule.

The effect of an unknown amount of condensate-particle contamination is an ever-present problem in this type of work. The present apparatus was used in an attempt to minimize the problem, but it remained to be proved that this goal had been achieved. Several experiments were planned at the end of the report period to settle this question. For example, in the case of the  $\rm B_2O_3$  spectrum, it is possible that the 2040 cm $^{-1}$  emission band of White et al $^{495}$  comes from  $\rm B_2O_3$  monomer and the 1300 cm $^{-1}$  and 740 cm $^{-1}$  bands come from ploymers or condensate particles.

## VI. RECOMMENDATIONS

This report naturally does not bring down the final curtain on the subject of the thermodynamics of highly refractory compounds. A number of important theoretical problems remain to be solved, complete and accurate basic data are still not available for a majority of the species of interest, and many refinements remain to be made in the methods and procedures in current use for estimating missing property data.

The specific heat of condensed phases at high temperatures is a subject worthy of further attention both from the theoretical and experimental standpoints. The theory of vibrational contributions to the specific heat of solids is sufficiently well-advanced, but this suffices only at low temperatures as defined in this project. Some progress has been made in elucidating anharmonicity corrections, <sup>24</sup>, <sup>498</sup>, <sup>499</sup> but much more needs to be done in applying the theory to specific crystal systems. It appears from what few data are available that other important contributions arise at high temperatures, and that theoretical expressions for their temperature dependence are unavailable.

This lack of theoretical background is felt most in extrapolations of  $C_p^o$  data to temperatures beyond those of the available data. Such extrapolations should be carried out separately on the various contributions to  $C_p^o$  from an understanding of how each contribution depends upon the temperature. Such practices as assuming  $C_p^o$  to be constant or extrapolating empirical equations for its total value introduce large uncertainties which are difficult to estimate since changes in curvature may occur in  $C_p^o$  versus T at high temperatures (see Fig. 2).

The situation with respect to liquids is the least satisfactory; no attempts have been made to base estimates of  $C_p^o$  values for liquids on sound theories.

The difficulties of measuring specific heats of condensed phases at high temperatures are very great, and data from various sources most often do not agree. Resorting to experimentation, therefore, does not necessarily result in a reduction in the uncertainties associated with high-temperature thermodynamics. A high degree of confidence in high-temperature thermodynamic property values will come after convincing theoretical interpretations are found for reproducible measurements of  $C_p^\circ$  versus temperature.

Samples of interesting high-refractory compounds with a high degree of purity are not readily available, and it is very likely that many of the property determinations in the past have been on samples of doubtful purity unless this has been specifically determined. It would appear that some more work in refining

<sup>498</sup> Ludwig, W., J. Phys. Chem. Solids 4, 283 (1958).

Maradudin, A. A., P. A. Flinn, and R.A. Colderwell-Horsfall, Anharmonic Contributions to Vibrational Thermodynamic Properties of Solids, II. The High Temperature Limit, Sci. Paper 029-G000-P 7 for AFOSR, Westinghouse Research Labs., Pittsburgh (13 February 1961).

<sup>500</sup> Powel, R. Critique on the Analytical Representation of Specific Heat Data, WADC TN 57-308, AD 142 059 (Novembe. 1957).

preparative methods is desirable, so that basic property measurements can be made on pure rather than technical grade samples.

Related to the latter problem is the fact that many interesting refractory compounds can be nonstoichiometric in composition. In fact, theoretical considerations indicate that all compounds can be included in the nonstoichiometric category. <sup>501</sup> Their composition can change whenever some vaporization is allowed to occur at high temperature before it becomes congruent during preparation, study, or end use. Recent studies <sup>501</sup>, <sup>502</sup> have shown that this behavior is related to the existence of lattice defects. Nonstoichiometry is an important high-temperature thermodynamic phenomenon which should receive increased attention both from the basic and applied standpoints.

The two types of data most often missing in connection with refractory compounds and their vapor species are heats of formation and spectroscopic constants. Methods for estimating heats of formation have not been developed, and more experimental measurements are needed to fill the gaps in existing data. Although the estimation of spectroscopic constants is often done, eventual confirmation of the values is desirable. In the case of complex polymeric vapor species such as those of the Mo-O and W-O systems, some information about the molecular structure must be available before any estimation of the spectroscopic constants can be attempted. Optical spectroscopic methods appear to be the most neglected of those that can be used in the study of refractory compound vapors.

<sup>501</sup> Anderson, J. S., Significance of Non-stoichiometry on Metal Compounds, In: The Physical Chemistry of Metallic Solutions and Intermetallic Compounds, vol. II, Chemical Publ. Co., N.Y. (1960), p. 234.

<sup>&</sup>lt;sup>502</sup>Rees, A. L. G., Chemistry of the Defect Solid State, Wiley, N.Y. (1954), 136 p.

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